

## Article

# An Experimental Study on the Transportation Characteristics of Perfluoro(2-methyl-3-pentanone) in a Straight Pipe

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**Abstract:** Gaseous fire suppressants are usually stored in a vessel via pressurization, and then discharged out through pipelines. The flow behaviors of the agents in pipes greatly affect its dispersion in space, as well as the fire extinguishing results. Here, an experimental study was carried out on the transportation characteristics of perfluoro(2-methyl-3-pentanone) ( $C_6F_{12}O$ ) in a horizontal straight pipe with the temperature and pressure recorded synchronously. At a filling pressure of 1800 kPa and a filling density of  $517 \text{ kg}\cdot\text{m}^{-3}$ , the agent release was completed in 2.0 s with the pipeline pressure peak of 1145 kPa and the pipeline temperature nadir of  $-10.6^\circ\text{C}$ . In comparison to that of bromotrifluoromethane ( $CF_3Br$ ) under the same conditions, the temperature and pressure curves of  $C_6F_{12}O$  exhibited similar varying trajectories but a much smaller amplitude, which could be ascribed to their different thermophysical properties. When keeping the other conditions unchanged, raising the filling pressure  $C_6F_{12}O$  reduces the discharge duration and the pipeline temperatures. Increasing the filling density extends the discharge duration, but shows little influence on the pipeline temperatures. The results were expected to provide useful information for the model validation and engineering design of a  $C_6F_{12}O$  fire-suppressing system with a predictable performance.

**Keywords:**  $C_6F_{12}O$ ; fire suppressant; transportation; pipe; pressure; temperature



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## 1. Introduction

Great efforts have been devoted to looking for ideal halon replacers since the use of  $CF_3Br$  was banned, by the Montreal Protocol and its subsequent revisions, for its effect on the ozone layers. Perfluoro(2-methyl-3-pentanone), denoted as  $C_6F_{12}O$ , has become one of the most promising halon replacers with satisfactory environmental friendliness, as well as fire extinguishing efficiency and toxicity [1]. Since being proposed by 3 M as a new kind of clean fire suppressant, numerous studies have been conducted on  $C_6F_{12}O$ , including studies on its physicochemical properties [2,3], fire extinguishing capacity [4,5], material compatibility [6,7], thermal decomposition products [8], etc. These studies provide valuable directions on the model computation and practical applications of  $C_6F_{12}O$  in the context of real fire suppression. In 2003,  $C_6F_{12}O$  was recognized as an available halon alternative and substitute in the significant new alternatives policy (SNAP) program of the United States Environment Protection Agency (EPA) [9]. It was also listed in the fire extinguishing system design standards of ISO 14520 and NFPA 2001 [10,11]. Currently,  $C_6F_{12}O$  is widely used in the areas of electrical and electronic cabinets, ships, libraries, etc.

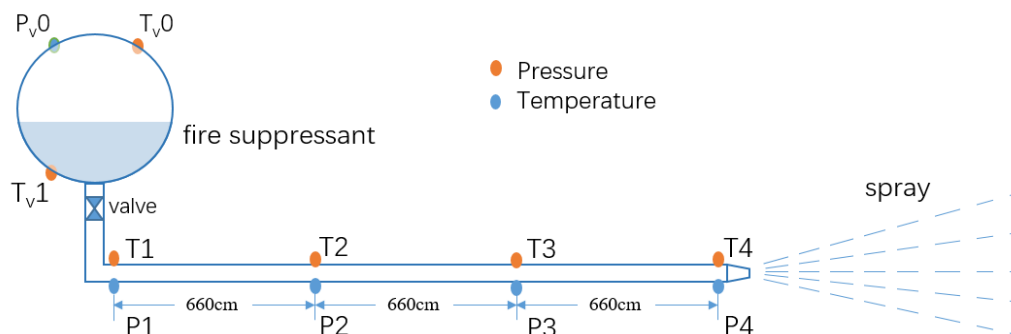
Similar to many other gaseous fire suppressants of halons and hydrofluorocarbons (HFCs),  $C_6F_{12}O$  is usually stored in a vessel via pressurization. Once the valve was actuated, the pressurized agent was ejected into the piping manifold and then distributed into space. The transportation characteristics of the fire suppressant in the pipes showed a great influence on its atomization and its distribution in space, as well as in its fire extinguishing results [12]. Therefore, understanding the state of  $C_6F_{12}O$  in pipes is indispensable for creating an effective fire suppression system design.

Although extensive research has been carried out on  $C_6F_{12}O$ , as mentioned above, seldom have the transportation behaviors of  $C_6F_{12}O$  in pipes been seen. Recently, Fan reported the flow characteristics of  $C_6F_{12}O$  in a complex pipeline with multi-branches [13]. By comparing the experimental data with hydraulic calculations, it was deduced that  $C_6F_{12}O$  only conformed to single-phase flows in the initial upstream section of the pipeline, but presented with a two-phase flow state in the following main pipe and downstream section of the pipeline. In comparison to that of bromotrifluoromethane ( $CF_3Br$ ), which has been tested within detailed studies under various conditions [14–17], investigations on  $C_6F_{12}O$  have been scarce up till now. More accurate experiments are still necessary for a better understanding of the flow behaviors of  $C_6F_{12}O$  in pipes.

In this work, the discharge process of  $C_6F_{12}O$  in a horizontal straight pipe was, in a full scale, experimentally studied. The pressures and temperatures in the vessel and pipes were recorded with a high sampling rate. Meanwhile,  $CF_3Br$  was tested as a counterpart for comparison since it has always served as the baseline for screening halon replacer candidates. The effects of source pressure and the filling density on the flow parameters of  $C_6F_{12}O$  were explored by a series of contrast trials. The transportation characteristics of  $C_6F_{12}O$  in the pipe were summarized based on experimental observations and its thermophysical properties.

## 2. Materials and Methods

Figure 1 schematically illustrates a typical experimental setup of the agent discharge system. A spherical vessel with the volume of 3.89 L was connected with a horizontal straight pipe through a solenoid valve. The pipe was 2.0 m long with an inner diameter of 14 mm. A convergent nozzle with an inner diameter of 12 mm was also equipped at the end of the pipe.



**Figure 1.** Schematic illustration of the experimental setup.

The pressure (P) and temperature (T) data in the vessel and the pipe were synchronously traced by thermocouples and pressure sensors with a sampling frequency of 4096 Hz. As shown in Figure 1, two thermocouples were installed on the top ( $T_{v0}$ ) and the bottom of the vessel ( $T_{v1}$ ), respectively. The other four thermocouples were anchored equidistantly on the pipe with a spacing of 0.66 m (T1–T4). There were five pressure sensors installed on the system. One located the upper part of the vessel ( $P_{v1}$ ) and four other ones positioned on the pipe (P1–P4). At each measuring point of the pipe, the thermocouple and the pressure sensor were arranged face to face. The measuring errors of temperature, pressure and agent mass were estimated as 1.0%, 0.5% and 1.0%, respectively. The errors were mainly caused by the instruments and the discharge system. In addition to these, the error of agent mass also originated from the loss in the filling process. The pressure sensors, thermocouples and the electronic scale were all calibrated before measurements were taken.

$C_6F_{12}O$  and  $CF_3Br$  with a purity above 99.5% were chosen as the fire suppressants. As is the case in a typical experiment, the vessel was first pumped in order for it to become a vacuum. Then, it was filled with a certain amount of liquid  $C_6F_{12}O$ , then pressurized

by nitrogen until reaching the desired pressure. After that, the P–T recording system was started. Once the fast-opening solenoid valve was actuated, the agent in the vessel was forced out into the straight pipe and discharged from the nozzle into an unconfined space. The test of  $\text{CF}_3\text{Br}$  was conducted in the same discharge system under similar conditions. Table 1 lists the tests with different filling pressures and filling densities. The filling pressure is the source pressure in the vessel that was achieved by nitrogen pressurization. The filling density was defined as the mass agent of the liquid divided by the vessel volume. All the tests were conducted at a room temperature of about 20 °C.

**Table 1.** The discharge tests of the  $\text{C}_6\text{F}_{12}\text{O}$  and  $\text{CF}_3\text{Br}$  used.

Test Sequence	Agent	Agent Mass (kg)	Filling Density ( $\text{kg}\cdot\text{m}^{-3}$ )	Filling Pressure (kPa)
1	$\text{C}_6\text{F}_{12}\text{O}$	2.01	517	1822
2	$\text{CF}_3\text{Br}$	2.02	519	1846
3	$\text{C}_6\text{F}_{12}\text{O}$	2.12	545	1910
4	$\text{C}_6\text{F}_{12}\text{O}$	2.08	535	2540
5	$\text{C}_6\text{F}_{12}\text{O}$	2.14	550	3230
6	$\text{C}_6\text{F}_{12}\text{O}$	1.02	262	1799
7	$\text{C}_6\text{F}_{12}\text{O}$	2.05	527	1812
8	$\text{C}_6\text{F}_{12}\text{O}$	3.02	776	1813

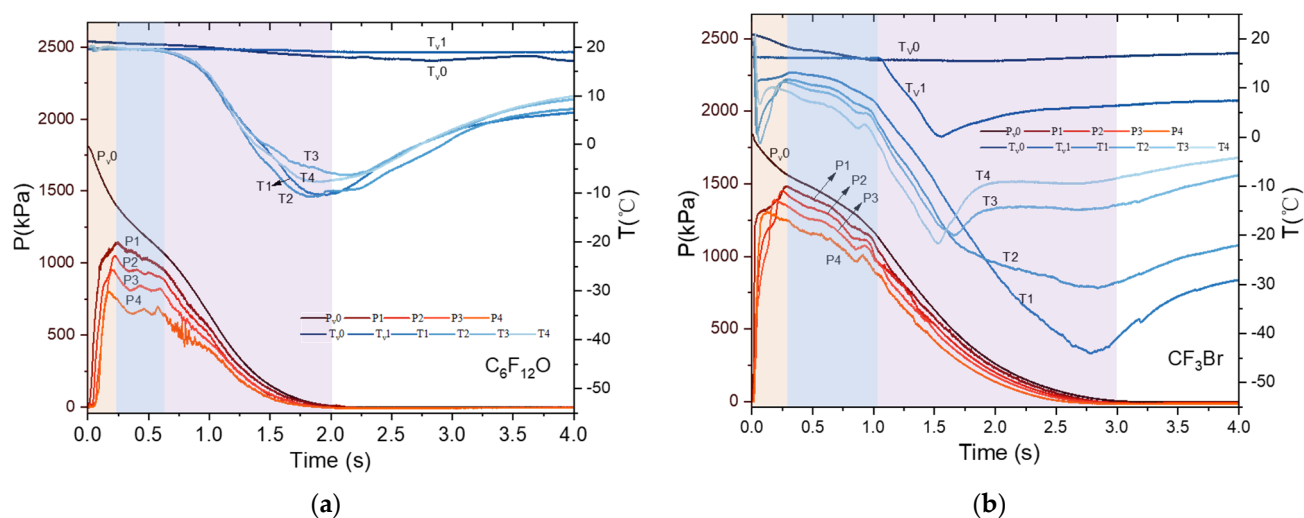
### 3. Results and Discussion

#### 3.1. Pressures and Temperatures in the Discharge System

Figure 2a shows, in test 1 of  $\text{C}_6\text{F}_{12}\text{O}$ , all of the pressure and temperature profiles as a function of time. The plots of the vessel pressure ( $P_v0$ ) and the pipeline pressure ( $P1$ – $P4$ ) are located in the lower part of the pattern. Upon the beginning of the agent spray,  $P_v0$  dropped continuously from 1822 kPa to atmospheric pressure. The time length of such a process was defined as the discharging duration ( $t_d$ ). From the trace of  $P_v0$  versus time, the  $t_d$  of test 1 was determined as 2.0 s. Different to the uninterrupted dropping of  $P_v0$ , the pipeline pressure plots ( $P1$ – $P4$ ) exhibited an asymmetric hump shape, which could be roughly divided into three stages of “rapid increase, gentle decrease and continuous decrease”. Taking  $P1$  as an example, in the first stage of 0–0.23 s (marked in yellow),  $P1$  increased rapidly from zero to a peak pressure of 1145 kPa, at a high rising rate of  $4978 \text{ kPa}\cdot\text{s}^{-1}$ . Then, it declined gently with fluctuations at an average rate of  $488 \text{ kPa}\cdot\text{s}^{-1}$  in the time range of 0.23–0.63 s (marked in blue). In the final stage of 0.63–2.0 s (marked in pink),  $P1$  decreased continuously from 950 kPa to zero at an average decreasing rate of about  $693 \text{ kPa}\cdot\text{s}^{-1}$ . The peak pressure decreased farther down the pipe from  $P1$  (1145 kPa) to  $P4$  (803 kPa) with the gap between the neighboring points of 100–150 kPa. Meanwhile, the time by which the four measuring points reached the peak pressure increased upstream from  $P4$  (0.18 s) to  $P1$  (0.23 s), with an interval of about 15–20 ms.

The temperature curves of test 1 are located in the upper part of Figure 2a. The two T plots of the vessel that are at the top decreased very slowly, with a total reduction of about 3.3 °C for the upper gas ( $T_v0$ ) and only 0.5 °C for the liquid below ( $T_v1$ ). The piping temperature plots ( $T1$ – $T4$ ) were kept nearly flat in the period of 0–0.63 s. In the following stage, they declined quickly to levels below zero, showing a total reduction of about 26–30 °C. The nadir point of  $T1$  was as low as  $-10.6$  °C.

Figure 2b presents the P–T profiles from the trial of  $\text{CF}_3\text{Br}$  (test 2), which followed trajectories that are similar to those of  $\text{C}_6\text{F}_{12}\text{O}$ , albeit with distinct details. From the monotonically declining curve of  $P_v0$ , the  $t_d$  of  $\text{CF}_3\text{Br}$  was determined as 3.0 s, which is much longer than that of  $\text{C}_6\text{F}_{12}\text{O}$ . Likewise, the piping pressure plots were hump shaped with a quick rise and a slow drop. The peak pressures of  $P1$ – $P4$  were in the range of 1300–1570 kPa, which were about 400–500 kPa higher than those of  $\text{C}_6\text{F}_{12}\text{O}$ . However, the spacing of the peak values of  $P1$ – $P4$  (60 kPa) was only half of that of  $\text{C}_6\text{F}_{12}\text{O}$ .



**Figure 2.** Pressure and temperature profiles versus time in the tests: (a) C<sub>6</sub>F<sub>12</sub>O and (b) CF<sub>3</sub>Br.

In the vessel of CF<sub>3</sub>Br, T<sub>v,0</sub> dropped by 5 °C in the range of 0–1.0 s. Then, it was kept nearly flat until the end of the agent's release. Meanwhile, T<sub>v,1</sub> remained constant within the initial stage and then decreased rapidly to zero (1.0–1.5 s) at a rate of about 32 °C·s<sup>−1</sup>. There were two big drops in the piping temperature traces (T<sub>1</sub>–T<sub>4</sub>). The first occurred at the beginning of discharge with a drop of 9–21 °C, and the second was in the latter part of discharge with a reduction of 25–40 °C. At the end of the agent's release, all the temperature points in the pipe fell below −20 °C. T<sub>1</sub> even reached the lowest point of −44 °C, which is significantly lower than that of C<sub>6</sub>F<sub>12</sub>O.

### 3.2. Transportation Characteristics of C<sub>6</sub>F<sub>12</sub>O in the System

The nonlinear changes in Figure 2 imply complex flow behaviors with respect to the suppressants during the rapid release process. As shown above, the P–T profiles of C<sub>6</sub>F<sub>12</sub>O exhibited a varying trend that was similar to CF<sub>3</sub>Br but with a much lower amplitude, which could be ascribed to their different thermophysical properties. Table 2 listed some of the typical parameters of the two agents, revealing their remarkable differences regarding vapor pressure and boiling points. At a room temperature and atmospheric pressure, the C<sub>6</sub>F<sub>12</sub>O was a liquid, while the CF<sub>3</sub>Br was a gas. When stored in the vessel and fed through a pipe, the agents experienced phase changes between gas and liquid with the pressure changing. Based on the P–T data acquired, the transportation properties of C<sub>6</sub>F<sub>12</sub>O in the system were analyzed comparatively with CF<sub>3</sub>Br as a reference.

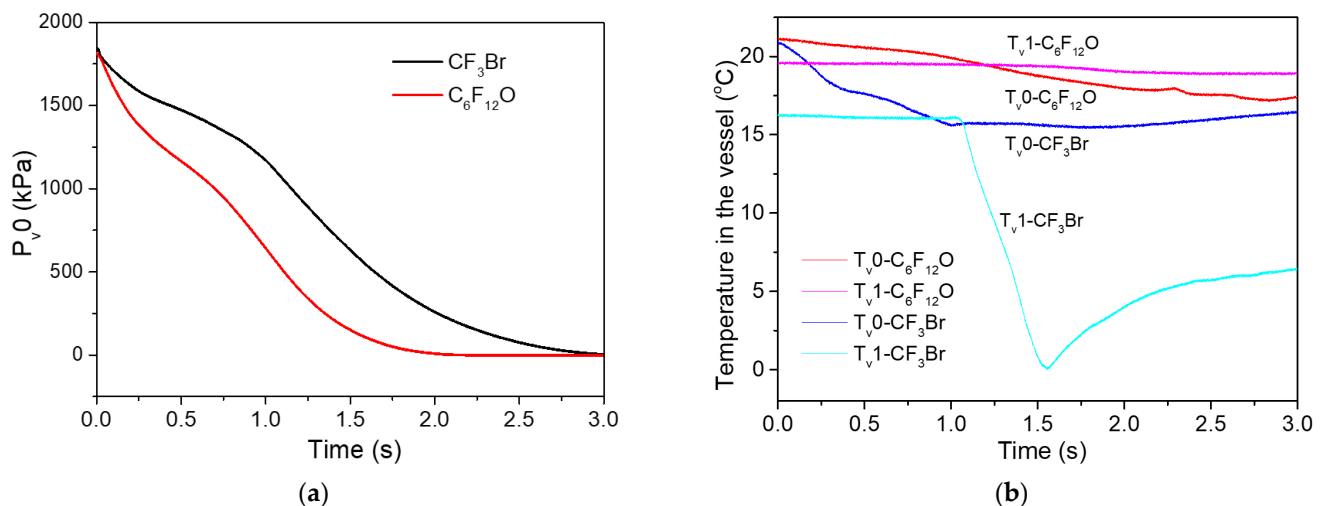
**Table 2.** The typical parameters of C<sub>6</sub>F<sub>12</sub>O and CF<sub>3</sub>Br [2,18].

Agent	Molecular Weight	Boiling Point (°C)	Vapor Pressure (kPa)	Liquid Density (kg·m <sup>−3</sup> , 22 °C)
C <sub>6</sub> F <sub>12</sub> O	316	49.2	40	1.60
CF <sub>3</sub> Br	149	−57.8	1620	1.57

#### 3.2.1. Variations in the Vessel

Both C<sub>6</sub>F<sub>12</sub>O and CF<sub>3</sub>Br were stored as liquids in a vessel under a nitrogen pressurization of about 1800 kPa. The liquid located at the lower part of the vessel with nitrogen dissolved, while the ullage was a mixture of nitrogen and agent vapor. As the system was depressurized, a dissolution of nitrogen and vaporization of liquefied agent occurred, which counteracted the pressure decline in the vessel and extended the discharge duration. As is confirmed by Figure 3a, both P<sub>v,0</sub> plots were characteristics of the pressure offset in the middle stage with reduced dropping rates. For the C<sub>6</sub>F<sub>12</sub>O with a lower vapor pressure and higher boiling point, the pressure compensating effect was relatively weak since there

was little vaporization and what gas there was mainly came from the process of nitrogen separating from the liquid. As to the  $\text{CF}_3\text{Br}$  with a much higher vapor pressure and lower boiling point, the effect of pressure offset was stronger from the combined contributions of nitrogen dissolution and agent vaporization. Therefore, the  $P_{v0}$  of  $\text{CF}_3\text{Br}$  decreased at a slower rate than that of  $\text{C}_6\text{F}_{12}\text{O}$ .



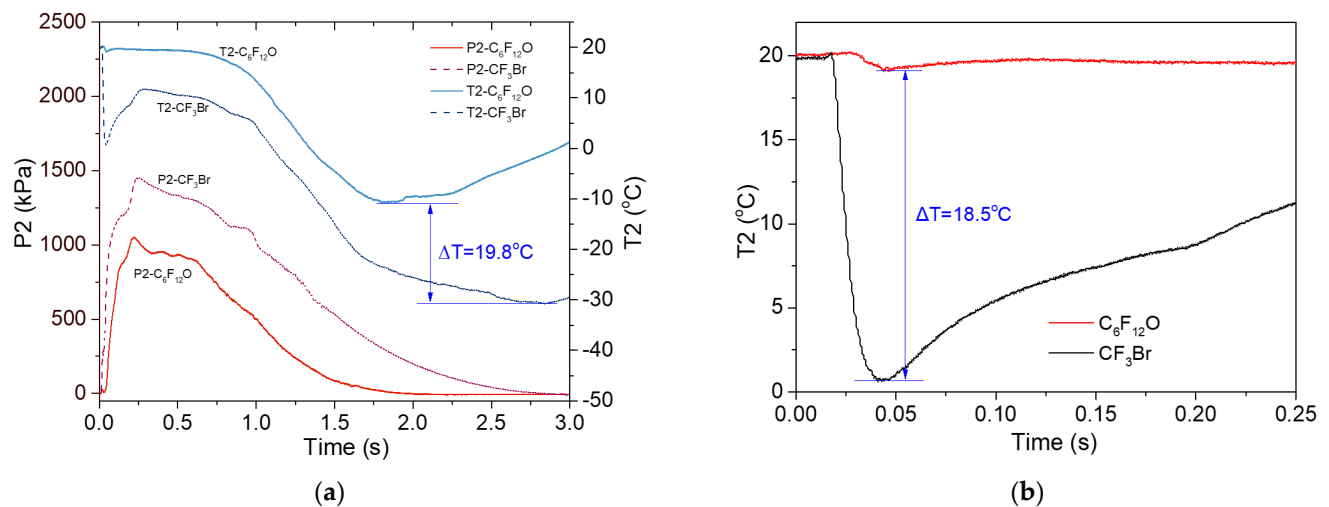
**Figure 3.** Comparison of the P–T profiles in the vessel of the two tests: (a)  $P_{v0}$ ; (b)  $T_{v0}$  and  $T_{v1}$ .

Figure 3b shows the variation of temperatures in the vessel during release process of  $\text{CF}_3\text{Br}$ . The  $T_{v0}$  first decreased by 5 °C in the initial 1.0 s, and this was due to gas expansion and liquid vaporization. Then, it reached a plateau, indicating a new single-phase gas status in the vessel. The vessel filled with “liquid, vapor and nitrogen” transformed into one filled with the gaseous mixture of “nitrogen and vapor”. Much different to that of  $\text{CF}_3\text{Br}$ , the  $T_{v0}$  of  $\text{C}_6\text{F}_{12}\text{O}$  decreased steadily and slowly along with only gas expansions and with little phase change.

The  $T_{v1}$  of  $\text{CF}_3\text{Br}$  initially did not change much since it was submersed in the liquid [19]. As the liquid in the vessel ran out, it experienced a vaporization of the liquid and an expansion of the remaining gas in the vessel, which showed a big temperature reduction of about 15 °C. The  $T_{v1}$  of  $\text{C}_6\text{F}_{12}\text{O}$  remained constant in the first stage, similar to that of  $\text{CF}_3\text{Br}$  for comparable reasons. In the latter part with gas discharge, only a small temperature drop of 0.3 °C was displayed. When considering its low vapor pressure and high boiling point, there were little phase changes taking place in the vessel of  $\text{C}_6\text{F}_{12}\text{O}$ . Therefore, the reduction in  $T_{v1}$  was minimal during the whole process.

### 3.2.2. Variations in the Pipe

Initially, the pipe was full of air when at an atmospheric pressure. Once the valve was opened, the ullage pressure in the vessel drove the liquid  $\text{C}_6\text{F}_{12}\text{O}$  out from the vessel into the pipe. Before the agent entered the pipe, the pressure wave propagated forward, which made the pressure sensors in the pipe first detect a pressure increase [20]. When the pressure wave arrived at the nozzle, it was restricted by the convergent nozzle and a pressure bounce back was triggered [21]. Thus the air in the pipe was compressed by the pressures from the two ends, which led to a temperature rise. As seen in Figure 4, with T2 and P2 serving as examples, in this very initial stage of only about 30 ms, both the temperature and the pressure in the pipe increased.



**Figure 4.** Comparison of the P–T profiles of the two tests: (a) P2 and T2; (b) T2.

After this short period, the pressurized liquid C<sub>6</sub>F<sub>12</sub>O flowed into the pipe. For the pressure difference, the liquid agent entering the pipe would evaporate immediately, together with the escape of the dissolved nitrogen. Such a process further improved the pressure in the pipe, but led to a temperature decrease due to the endothermic process of vaporization. With more fluid flowing into the pipe, both P2 and T2 went up again. When the fluid filled the pipe, P2 attained the peak value. In this very short stage with the pipeline pressure increasing, the agent in the pipe existed mainly in a gaseous state.

With the discharge ongoing, the C<sub>6</sub>F<sub>12</sub>O that flowed into the pipe entered a steady state under the co-effects of the driving force of nitrogen and the friction resistance from the pipe wall. The T2 curve remained stable and the P2 decreased gently. During this middle stage, the fluid in the pipe existed mainly as a liquid, as well as a small amount of nitrogen and C<sub>6</sub>F<sub>12</sub>O vapor, which is typical of a gas-liquid two-phase flow. As the pressure dropped, the mass ratio of gas to liquid in the pipe increased. With the liquid C<sub>6</sub>F<sub>12</sub>O gradually being consumed, the release process enters the final period with the agent in the pipe being in the form of nitrogen and C<sub>6</sub>F<sub>12</sub>O vapor. The expansion of gas brought about a big temperature decrease. At the end of the discharge, the pressure and temperature curves simultaneously went downward to the nadirs.

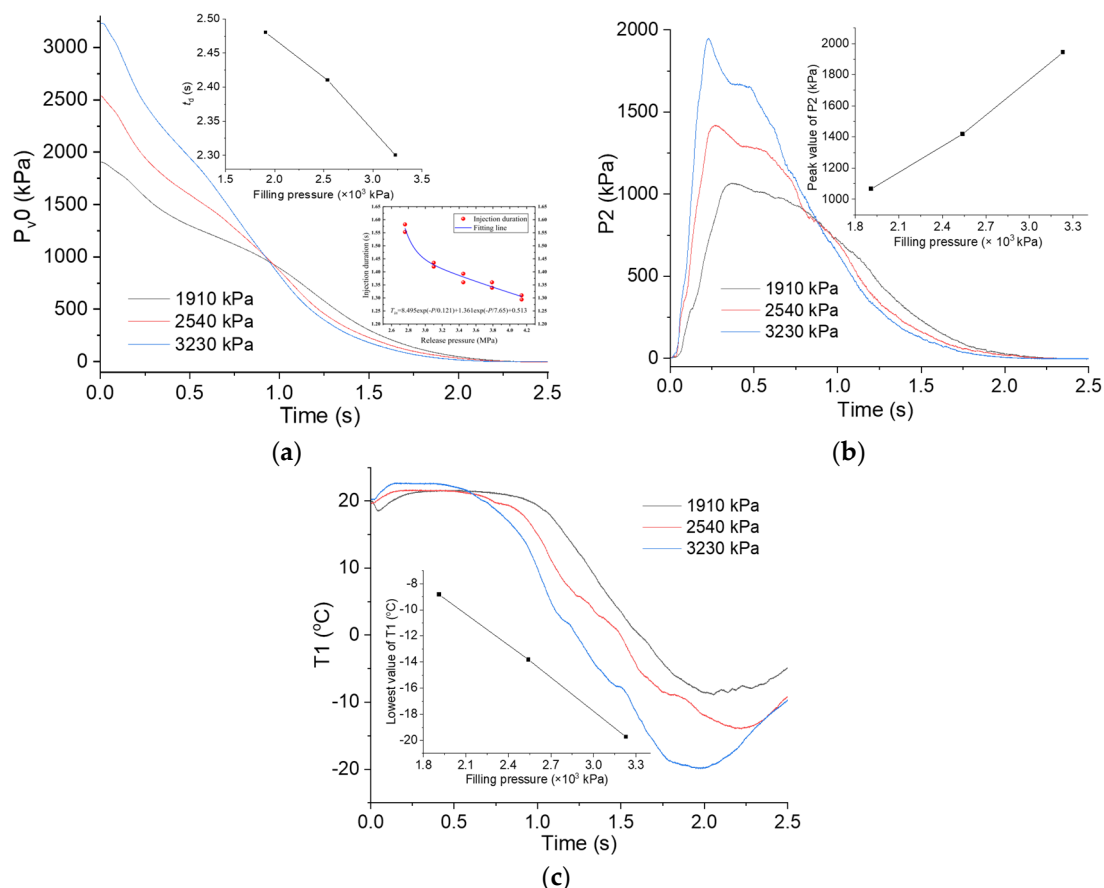
The P2 and T2 profiles of CF<sub>3</sub>Br are also presented in Figure 4a for the purpose of comparison. The comparable trajectory implies similar phase changes as were described above. However, there are also some remarkable differences. During the whole release process, the P2 of CF<sub>3</sub>Br remained above that of C<sub>6</sub>F<sub>12</sub>O, and the T2 of CF<sub>3</sub>Br stayed below that of C<sub>6</sub>F<sub>12</sub>O. Moreover, the T2 of CF<sub>3</sub>Br exhibited two much bigger temperature drops. Under the experimental conditions, the CF<sub>3</sub>Br vapor was liquefied during the nitrogen pressurization, which contained superheat [20]. When the CF<sub>3</sub>Br liquid entered the pipe, intense flashing vaporization occurred, resulting in the first temperature reduction. As is shown in Figure 4b, the nadir temperature of CF<sub>3</sub>Br was 18.5 °C lower than that of C<sub>6</sub>F<sub>12</sub>O. In the following stage with an evolving gas-liquid two-phase flow, the CF<sub>3</sub>Br in the pipe displayed a higher pressure and lower temperature than that of C<sub>6</sub>F<sub>12</sub>O. When it came to the final stage with a gas expansion, the second big temperature drop appeared, with the gap between the two T2 nadirs of 19.8 °C.

In the test of CF<sub>3</sub>Br, it was also observed that P1 had the highest peak pressure, and that P4 hit the peak pressure first out of all the four piping pressures that were similar to C<sub>6</sub>F<sub>12</sub>O. Considering fluid behaviors in the pipe, such phenomena may be attributed to the restriction of the convergent nozzle. It was known that the strength of pressure wave waned along the pipe. As the nearest point to the valve, P1 sensed the highest peak pressure for the least pressure loss. On the other hand, as the nearest point to the nozzle,

P4 first showed the peak value because the bounce back of the pressure wave reached P4 prior to the other three measuring points.

### 3.3. Effect of the Filling Pressure on the Flow Behaviors of $C_6F_{12}O$

Figure 5a displays the  $P_v0$  plots from the three tests at the filling pressures of 1910, 2540 and 3230 kPa, whilst keeping the mass of the  $C_6F_{12}O$  similar, respectively. With the filling pressure increasing, the  $P_v0$  declined at a faster rate. As is seen in the pattern inset in the upper part of Figure 5a, the  $t_d$  approximately decreased linearly with the source pressure rising. This was different to the result of  $CF_3Br$  that was reported by Jia (which was inset in the lower part of Figure 5a), where the injection duration first decreased sharply and then decreased steadily when the release pressure reached a certain value [17]. In their tests of  $CF_3Br$ , flashing vaporization contributed the most to the pressure compensation in the vessel, which led to the elongation of  $t_d$ . The proportion of such contribution was relatively high at low filling pressures, but dropped at higher filling pressures. However, in the current experiments of  $C_6F_{12}O$ , the pressure compensation was much smaller, and the source pressure dominated the discharge duration. Further, more tests at varied filling pressures were needed to validate the result.



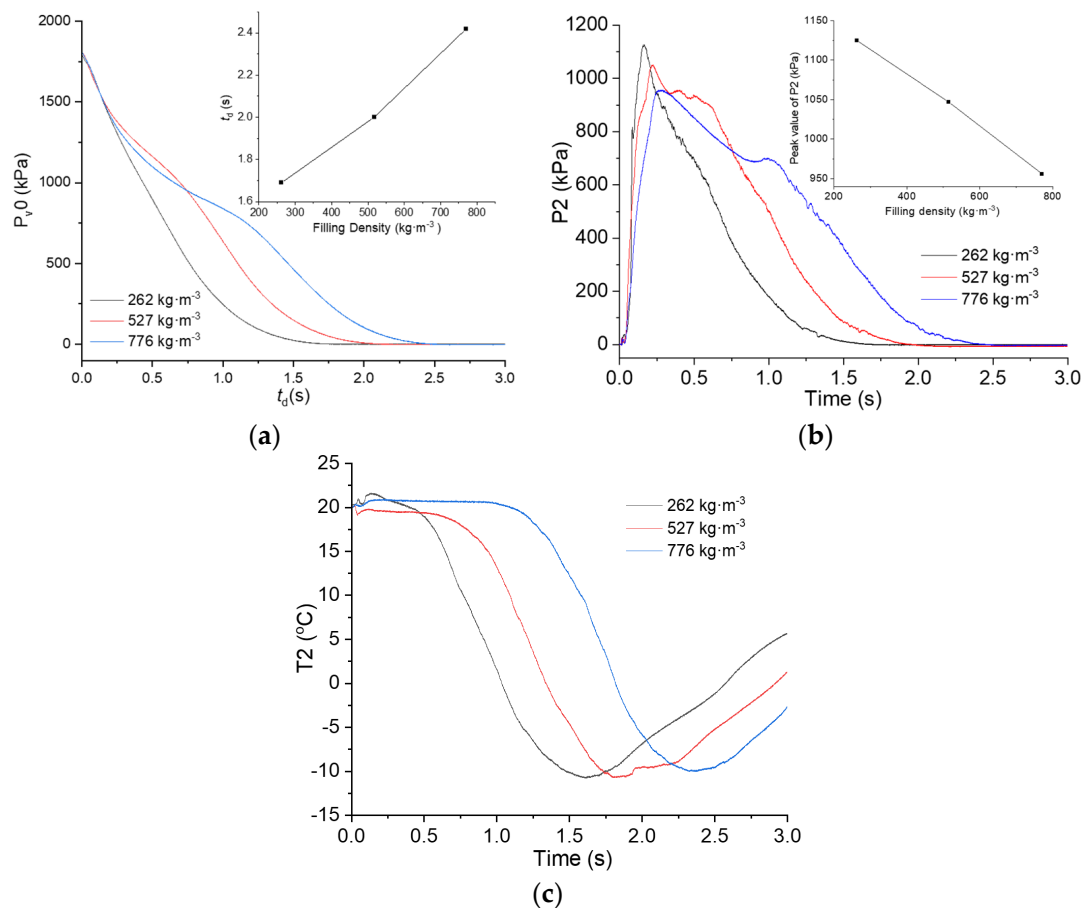
**Figure 5.** P–T profiles of the  $C_6F_{12}O$  tests at different filling pressures: (a)  $P_v0$ , the pattern inset in the upper part showed  $t_d$  at different filling pressures, pattern inset in the lower part was due to the  $CF_3Br$  from ref. [17]; (b)  $P_2$ , the pattern inset showed the peak values of  $P_2$  at different filling densities; (c)  $T_1$ , the pattern inset showed the  $T_1$  nadir at different filling pressures.

Figure 5b,c presents the P–T variations in the pipe of  $C_6F_{12}O$  at the three filling pressures. In Figure 5b, with  $P_2$  as an example, the peak values of  $P_2$  increased with the filling pressure rising, while the piping temperature decreased with the source pressure increasing. As shown in Figure 5c, at the  $P_v0$  of 1910, 2540 and 3230 kPa,  $T_1$  showed the lowest values of  $-8.8$ ,  $-13.8$  and  $-19.7$   $^{\circ}C$ , respectively. Similarly, a nearly linear

relationship was exhibited in the patterns inset in Figure 5b,c. For the current system, the rapid release could be regarded as an adiabatic expansion process. The source pressure in the vessel was the driving force for the agent transportation. With the agent flowing, the pressure energy would transform into dynamic energy and heat energy. Higher filling pressures not only accelerated the fluid flow and shortened the discharge time, but also led to a lower temperature in the pipe.

### 3.4. Effect of the Filling Density on the Flow Behaviors of $C_6F_{12}O$

Figure 6a shows the changes that were tracked in  $P_{v0}$  in the  $C_6F_{12}O$  tests at different filling densities. With the agent mass increasing, the  $t_d$  correspondingly increased (as is seen in the pattern inset in Figure 6a). Meanwhile, the peak pressure of the pipe went down. As shown in Figure 6b, with P2 as an example, the peak value decreased from 1170 kPa to 956 kPa when the filling density increased from 262 to 776  $kg \cdot m^{-3}$ , which also displayed a nearly linear varying trend (as is seen in the pattern inset in Figure 6b). Figure 6c gave the temperature traces of T2 in the three tests. With the filling density rising, the time that the plot began decreasing was postponed, but the decreasing rate and the nadir value remained unchanged. The lowest point was around  $-10^\circ C$  for all the three T2 plots.



**Figure 6.** P–T profiles of the  $C_6F_{12}O$  tests at different filling pressures: (a)  $P_{v0}$ , the pattern inset showed the  $t_d$  of the tests at different filling densities; (b) P2, the pattern inset showed the peak values of P2 at different filling densities; (c) T2.

## 4. Conclusions

In this work, the transportation characteristics of  $C_6F_{12}O$  in a straight pipe during a rapid release process were studied by tracking the temperature and pressure variations simultaneously. The effects of the filling pressure and the filling density on the flow

behaviors of  $C_6F_{12}O$  were examined through a series of tests. Based on the experimental data, the main conclusions were drawn as follows:

- Under the driving of pressurized nitrogen, the  $C_6F_{12}O$  was sprayed out of the pipe very rapidly. In the process of just a few seconds, the agent in the pipe experienced complex changes within the three stages of “gas, gas-liquid mixture and gas”. The intermediate stage exhibited characteristics of gas-liquid two-phase flow, which is where the fluid was dominated by liquid  $C_6F_{12}O$  together with a small amount of vapor and nitrogen;
- Upon the release of  $C_6F_{12}O$ , the pressure in the vessel went steadily downward until it reached zero, while the vessel temperature just showed a minor drop of several degrees Celsius. The pipeline pressure plots exhibited an asymmetric hump shape, which contained three stages of “rapid increase, gentle decrease and continuous decrease”. In the first two stages, the piping temperature remained stable. However, a big drop of about 30 °C in the piping temperature occurred in the third stage of gas discharge;
- In comparison to that of the  $CF_3Br$  released under similar conditions, the temperature and pressure curves of  $C_6F_{12}O$  exhibited similar trajectories, but with much lower varying amplitudes. Moreover, such differences can be mainly ascribed to their different vapor pressures and boiling points;
- With other conditions being the same, raising the filling pressure in the vessel of the  $C_6F_{12}O$  reduced the discharge duration and the pipeline temperatures. Increasing the filling density extended the discharge duration, but showed little influence on the pipeline temperatures.

The experimental data were expected to validate the computer code predictions of  $C_6F_{12}O$  in pipeline transportations, which will be useful for the design of a  $C_6F_{12}O$  fire suppressing system in the areas of aircraft, shops, libraries, etc.

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