



Article Isolation and Purification of Single Gold Nanoclusters by Alternate Pumping Chromatography

Malvina Supper ¹, Virginia Birner ¹, Lukas Gromotka ², Wolfgang Peukert ², and Malte Kaspereit ^{1,*}

- ¹ Institute for Separation Science & Engineering, Friedrich-Alexander-Universität Erlangen-Nürnberg, Egerlandstr. 3, 91058 Erlangen, Germany
- ² Institute of Particle Technology, Friedrich-Alexander-Universität Erlangen-Nürnberg, Cauerstr. 4, 91058 Erlangen, Germany
- * Correspondence: malte.kaspereit@fau.de

Abstract: Alternate pumping chromatography is applied to obtain atomically precise glutathionestabilized gold nanoclusters in high purity from synthesized mixtures. On the basis of anion exchange chromatography, the feasibility of isolating a single cluster, $Au_{10}GSH_{10}$, as well as two different clusters simultaneously ($Au_{25}GSH_{18}$ and $Au_{29}GSH_{20}$) is demonstrated. In addition, $Au_{18}GSH_{14}$, which is present only in trace amounts, is successfully enriched. A simple design procedure is proposed that allows using columns with different retention behavior. Successful experiments with large injection amounts confirm the potential of the concept for preparative-scale productions of high-quality nanoparticulate products.

Keywords: nanoparticles; nanoclusters; chromatography; recycling; alternate pumping

1. Introduction

The quality of nanoparticulate products depends on their particle size distribution (PSD). The narrower a product's PSD, the higher its value, since the more defined its properties, such as light absorption and emission, color brilliance and catalytic and physiological activity. While many laboratory-scale syntheses can deliver narrow PSDs, scaling up to industrial conditions generally leads to less favourable, broader PSDs, which limits the product quality. Achieving well-defined properties then requires a subsequent classification. Yet, for nanoparticles (NPs) with their sizes between 1 and 100 nm, suitable industrial-scale separation technologies are still missing.

Such classification is challenging due to the very small property differences between the NPs within a PSD as well as by their tendency to agglomerate. For such types of problem, chromatography appears promising, since it exhibits unprecedented resolution power, has scalability from the milligram to multi-ton scale and has high flexibility given by the multitude of exploitable retention mechanisms [1]. At the analytical scale, chromatography is already applied for size-selective separations of nanomaterials. In many cases, size exclusion chromatography (SEC) is used, for example, for separations of CdS and ZnS-NPs [2], AuNPs [3–6] and ZnS quantum dots [7].

Fischer [8] also performed semi-preparative SEC of CdS colloids using a column with 32 mm ID. More details on SEC for NPs are given in [9,10]. Due to its limited separation power, SEC appears suitable for the classification of broader or multimodal systems as in [6] and for the removal of impurities. Aiming at high resolution of narrow PSDs requires exploiting the higher separation efficiency of interaction-based chromatography. For example, reversed-phase HPLC was applied for identifying small cationic metal clusters [11] and monitoring the PSDs of Au/Pt-NPs [12,13]. Furthermore, separations of Au nanoclusters (AuNCs), which are in the scope of this work, were accomplished by interaction-based retention mechanisms, ranging from conventional and non-aqueous reversed-phase [14,15] over ion-pairing [16–18] and hydrophilic interactions [19,20] to anion exchange [20].



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Copyright: © 2023 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). Apart from the achievements at analytical-scale, a systematic development of preparative chromatography for the classification of nanoparticulate products is missing. This is hampered by several challenges. Syntheses mixtures are often complex, containing various species of different sizes together with impurities. Furthermore, despite the efficiency of modern columns, separation among individual nanoclusters or providing nanoparticles with narrow size fractions remains very challenging. In conjunction with the large injection amounts required in preparative chromatography, this limits the achievable resolution.

Several process concepts exist that provide enhanced performance in preparative applications; for overviews, see [21–23]. These include gradients, multi-column schemes, such as the simulated moving bed concept [24,25], as well as recycling processes. The latter are particularly interesting for the problem at hand. They enhance resolution by recycling the chromatogram, or parts thereof, several times over the same column. The simplest mode, closed-loop recycling (CLR) [26–30], utilizes a single column and a recycle pump.

The backmixing by the latter, however, limits the achievable separation. This is resolved by alternate pumping (AP) [31–33], also known as twin-column recycling, which does not need a recycle pump. In AP, the unresolved portion of the chromatogram is transferred from one column directly into a second one. Afterward, the column order is reversed, and this is repeated as often as needed. The rather simple concept greatly increases efficiency. It was used successfully for challenging separations of macromolecules [32], isomers [33], enantiomers [34], drug impurities [35] and natural products [36].

The most striking examples are the baseline resolution of enantiomers and isotopes with selectivities as low as 1.01 [37]. The concept has been extended further by also incorporating gradient steps [38–40]. To our knowledge, the only application of AP to NPs was presented by Al-Somali et al. [41], who separated thiol-stabilized AuNPs by SEC. While baseline separation was not possible for the studied case (see below), the authors found that CLR and specifically AP increased the resolution strongly enough to detect a multimodal PSD.

Conventional NPs have a continuous PSD, which makes baseline separations impossible. In contrast, nanoclusters (NCs) are discrete, atomically precise structures consisting of a few up to few hundred atoms. NCs, and specifically gold nanoclusters (AuNCs) as studied here, are a particularly attractive field of application. In contrast to AuNPs, they have discrete electronic energy levels, giving them exceptional physico-chemical properties [42]. Importantly, these properties strongly depend on the size of the cluster. Differently sized AuNCs have been studied extensively for applications in optics, catalysis, sensing and analysis, biotechnology and medicine.

Current applications include, among many others, the sensing of molecular interactions [43], nanoprobes for neurotransmitters [44] and catalysts for the electrochemical reduction of CO_2 [45]. An overview on the field is given in [46]. However, conventional synthesis protocols deliver mixtures of various cluster sizes along with impurities. For the optimization of product properties, it is of great interest to devise methods capable of isolating single clusters from such mixtures.

The scope of this work is to experimentally investigate the applicability of alternate pumping as a high-resolution scheme for the separation of discrete NCs. For this, we exploit the significantly higher—in comparison to SEC—separation power of interaction-based chromatography. As an example problem, we apply anion-exchange chromatography to separate small glutathione-stabilized AuNCs that contain between 10 and 29 gold atoms. To our knowledge, neither the use of alternate pumping for nanoparticulate products on the basis of interaction chromatography nor its application to isolate atomically precise nanoclusters has been investigated.

The paper is organized as follows. After a short discussion of the principle of AP and its practical implementation, different experimental case studies are presented. In a first step, the simultaneous isolation of two larger AuNCs is studied, followed by the purification of a single, smaller cluster. Thereafter, the isolation of an intermediately-sized cluster, that is present only in trace amounts, is investigated. Finally, the applicability of the

concept under preparative conditions is evaluated by experiments with strongly increased injection amounts.

2. Experimental

2.1. Materials

For synthesis of the AuNCs, sodium tetrachloroaurate(III) dihydrate (NaAuCl₄, purity 99%), reduced glutathione (GSH, \geq 98%) and ammonium acetate (NH₄Ac, \geq 99%) were purchased from Sigma-Aldrich. Methanol (HPLC gradient grade), BisTris buffer (\geq 99%) and sodium borohydride (NaBH₄, \geq 97%) were from Carl Roth. Ammonium acetate (analysis grade) used for chromatography was purchased from Merck.

2.2. Synthesis

The samples separated in this work were synthesized along the procedures described in [19,20]. For this, 12.5 mL solution of 5 mM sodium tetrachloroaurate (NaAuCl₄) and 20 mM GSH were prepared in methanol, stirred for 30 min at room temperature, then cooled to 0 °C and stirred for another 30 min. Subsequently, under vigorous stirring, 3.13 mL of aqueous 150 mM sodium borohydride (NaBH₄), also cooled to 0 °C, were added as reducing agent. After 3 h reaction time, the produced Au nanoclusters were centrifuged off, washed three times with methanol and dried under ambient conditions.

2.3. Chromatography

The chromatographic experiments were performed using an Ultimate3000 HPLC system (Dionex, Germany) equipped with a quaternary gradient pump (model LPG-3400A), an autosampler (WPS-3000SL), a thermostatted column compartment (TCC-3000) and a diode array detector (DAD-3000). Column switching in the AP experiments was realized using two electrically driven analytical-scale six-port/three-channel switching valves (Knauer, Germany). Due to pressure drop constraints of the detector placed between the columns, for liquid connections PEEK tubing with a relatively large bore of 0.25 mM was used.

Chromatographic conditions were adapted from [20]. Two anion chromatography columns PRP-X100, 4.6×250 mm, particle size 10 μ m, pore size 100 Å, ion exchange capacity 0.019 mequiv/g (PS-DVB functionalized with triethyl ammonium; Hamilton, USA) were used in the experiments. An aqueous eluent buffered with 20 mM BisTris and a varying content of ammonium acetate (500 to 1000 mM) was applied. The latter serves as a modifying salt to adjust the elution strength. The pH of the mobile phase was not adjusted but resulted as 7.5.

Eluents were prepared with ultrapure water from an Aquinity2 unit (MembraPure, Germany). The flow rate was either 0.4 or 0.7 mL/min. All experiments were conducted at 25 °C. For improved reproducibility, the column was regenerated between the experiments by flushing for 10 min with 1000 mM NH_4Ac , followed by 40 min re-equilibration with the eluent at the same flow rate as in the experiments. Sample suspensions were prepared in the eluent to the required concentration.

3. Principle and Basic Design of Alternate Pumping

Recycling concepts are a type of straightforward approach to enhance the resolution of a chromatographic separation. The most frequently used one is closed-loop recycling (CLR) [26–29]. In CLR, an only partially resolved chromatogram is recycled as often as needed over the same column until sufficient resolution is achieved. Ideally, this corresponds to interconnecting several columns in series, by which the column length and efficiency are increased without increasing the pressure drop. In technical plants, however, the required recycle pump causes strong band broadening, which sacrifices the beneficial effect to a large extent. Thus, CLR is limited when it comes to high-resolution separation.

Alternate pumping (AP) is a two-column approach that circumvents the dispersion problem, since it does not require a recycle pump. In AP, the unresolved portion of a

chromatogram leaving one column is transferred directly into a second (usually identical) column. After the transfer, the column order is reversed. This 'recycling' is repeated as often as necessary. The peak resolution increases with the square root of cycles [47], which facilitates a remarkable resolution power as shown in [37]. It is worth mentioning that AP differs in several aspects from CLR. In CLR, the complete column content is recycled, which essentially fixes the cycle time.

More flexibility can be achieved by so-called peak shaving, by which sufficiently pure product fractions are removed in each cycle [30]. However, by the CLR principle impurities are 'trapped' within the system and may spread over the elution profiles. Targeted removal of such impurities would require additional fractionations and is very difficult for impurities closely eluting to the target peak. In contrast, the use of two columns in AP offers more degrees of freedom. Removal ('shaving') of impurities occurs inherently in each cycle, minimizing the spreading of their bands.

As will be shown in a later example, impurity removal can be enhanced further by asymmetric switching operations such that, during operation, specific peaks are either retained within the process or removed. Finally, the implementation of additional peak shaving as well as gradient steps are rather straightforward [40]. The price to be paid for the enhanced efficiency and flexibility of AP is the higher solvent consumption. While CLR does not require additional solvent, in AP, fresh solvent is introduced permanently.

AP processes can be realized by different setups, usually based on one or two conventional multiport switching valves. Here, we apply the scheme in Figure 1 with two columns (A, B), a detector (D) and two six-port/three-channel switching valves (V1, V2). The two switching positions of the valves (*I*, *II*) facilitate four different arrangements of columns and detector as listed in the allocation table in Figure 1. Such a setup is particularly suited when only a single detector is available, since the latter can be placed at any column outlet at the desired times. Using two detectors, both column outlets can be monitored permanently.

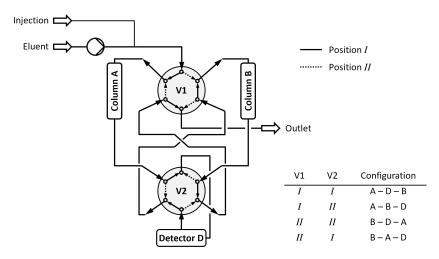


Figure 1. Schematic setup for alternate pumping chromatography as used in this work. Two switching valves (V1 and V2) are used to adjust the desired order of the columns (A and B) and the detector (D). The table lists the configurations that result from the different valve positions (indicated as "*I*" and "*II*" and by solid and dashed lines, respectively).

Figure 2 illustrates the course of the concentration profiles in an AP process that isolates a target compound (*c*) from a mixture with five components (a–e). At the start, the column order is A–B, and the injection is applied to A. The outlet profile of A (Figure 2, top row) after the first cycle is only partially resolved. In the second cycle, column B (second row) delivers a somewhat improved resolution. During the first two cycles, significant proportions of the early and late eluting components (gray peaks) already leave the system through the outlet (bottom row).

In consecutive cycles, the resolution enhances further, and increasing amounts of now also close-eluting impurities are removed. In the final cycle, the component *c* leaves column A in essentially pure form. Note that the third row of Figure 2 shows the elution profiles as they would pass a detector permanently located between the columns. This corresponds to switching only between the configurations A–D–B and B–D–A in Figure 1, and this is the procedure applied experimentally in Section 4.

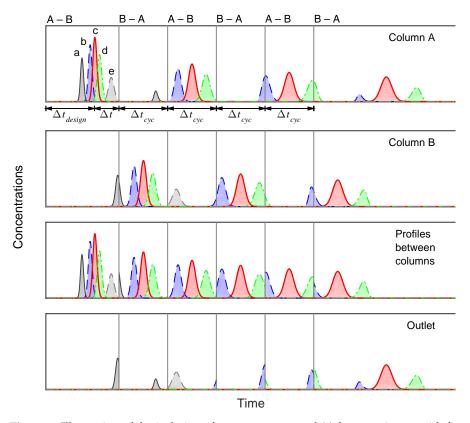


Figure 2. Illustration of the isolation of a target compound (*c*) from a mixture with five components (a–e) within six AP cycles. Top row—outlet of column A, second row—outlet of column B, third row—profiles between both columns, and bottom—process outlet. Vertical lines mark the end of each cycle.

When inspecting Figure 2, one notices that, while the resolution increases with every cycle, the peak broadening and dilution also increase. This is expected and has to be considered in the design. For a large number of cycles, the width of the target peak will eventually exceed the cycle duration. Then, its trailing and/or leading parts will leave the process through the outlet, thus, causing a decrease in yield or requiring additional measures.

The main task in designing an AP process is to find appropriate switching times or durations for the individual cycles. This is straightforward for scenarios as in Figure 2, where a specific target component should be isolated from its neighboring peaks. Two design tasks have to be met here. The first is to keep a desired portion of the chromatogram that elutes at a specific time Δt_{design} within the 'elution window' of each cycle. This is clearly achieved when choosing the duration of all cycles as $\Delta t_{cyc} = \Delta t_{design}$.

In most cases, Δt_{design} will be the retention time of the target peak; for the example in Figure 2, this is component *c* (marked in red). The second task is to decide about the relative position of the recycled portion in the elution windows. Usually, a centered position will be desired. In such cases, the end of the first cycle must be delayed by a time difference Δt

equal to half of the cycle duration. In summary, for the switching times, $t_s^{(i)}$ (*i* denotes the cycle number) holds

$$t_s^{(1)} = \Delta t_{design} + \Delta t , \qquad (1a)$$

$$t_s^{(i)} = t_s^{(i-1)} + \Delta t_{cyc}$$
, for $i = (2 \dots n_{cyc-1})$, (1b)

where n_{cyc} is the total number of cycles. The last cycle, $i = n_{cyc}$, is typically chosen longer to achieve complete elution. With the mentioned conditions for recycling and centering on a target peak, $\Delta t_{cyc} = \Delta t_{design}$ and $\Delta t = \Delta t_{design}/2$, one obtains from Equations (1a) and (1b) all switching times simply as

$$t_s^{(i)} = \left(i + \frac{1}{2}\right) \Delta t_{design} \quad \text{for } i = \left(2 \dots n_{cyc-1}\right).$$
⁽²⁾

It should be noted that, beyond such simple scenarios, the switching times can be adjusted in a more flexible manner to meet specific design goals. Corresponding examples are given in Section 4. Further design considerations are given in [37,47].

4. Results

4.1. Chromatographic Separation Problem

As an example, Figure 3 (left) shows the isocratic separation of a synthesized sample at conditions typical also for the later alternate pumping experiments. The earlier peaks correspond to discrete gold nanoclusters (AuNCs) of different sizes (see below), while the unresolved large peak after about 14 min contains strongly retained synthesis impurities, including various larger clusters. The latter peak shows a strong tailing such that the baseline is reached only after about 25 min, which indicates the presence of some strongly retained impurities. The mixture potentially contains small amounts of even stronger retained components, which may be responsible for the small retention time drifts observed in repetitive injections. Reproducibility was improved greatly after including the washing/equilibration step described in Section 2.3.

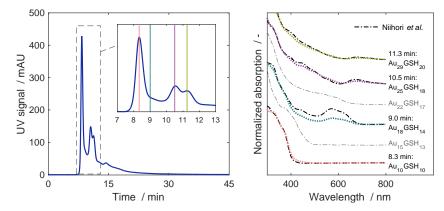


Figure 3. Example chromatogram and identification of selected AuNCs. (**left**) Chromatogram for the injection of 80 μ L sample with 1 g/L, eluent with 725 mM NH₄Ac and 20 mM BisTris, flow rate 0.4 mL/min, and 25 °C—column A. (**right**) Comparison of normalized UV-VIS spectra from [18] to spectra measured at the four different times marked in the inset on the left.

As demonstrated in [18–20], chromatographic peaks of individual AuNCs can be identified unambiguously based on their distinct UV-VIS spectra. Even in the case of the incompletely separated chromatogram in Figure 3 (left), we can identify four different clusters. We denote the individual species by Au_xGSH_y , where *x* indicates the number of gold atoms of a cluster, and *y* is the number of attached glutathione (GSH) ligands. The comparison of the measured spectra to those reported by Niihori et al. [18] in Figure 3

(right) reveals that the spectra at the four marked times closely correspond to (ordered by their elution times) $Au_{10}GSH_{10}$, $Au_{18}GSH_{14}$, $Au_{25}GSH_{18}$ and $Au_{29}GSH_{20}$.

In addition, experiments with shallow gradients as in [20] (an example is given in Figure S1 in the Supporting Information, SI), as well as some of our AP experiments, reveal that the first peak also contains a small amount of Au₁₅GSH₁₃. A corresponding example along with the identification of all the mentioned cluster sizes is given in Figure S2 in the SI. Furthermore, electrospray ionization–mass spectrometry (ESI/MS) of cluster samples synthesized under the same conditions confirmed the presence of the mentioned clusters and, additionally, trace amounts of Au₁₁GSH₁₁ and Au₁₂GSH₁₁, which cannot be resolved chromatographically [19,20]. In the following, we denote the individual peaks only by the number of Au atoms of their main component (e.g., 'Au₁₀' denotes the corresponding peak, even if it contains small amounts of other species).

The above results indicate that the elution behavior is strongly affected or fully controlled by the ion exchange mechanism, since the elution order is along the number of charged GSH ligands. Consequently, resolution under iscratic conditions can be enhanced by lowering the salt concentration. An example is given in Figure 4. It can be seen that lowering the salt concentration from 725 mM, as used in Figure 3 (left) to 665 mM, allows for a better resolution. Separation is enhanced in particular among the smaller clusters and between those and the larger clusters.

For example, the separation factor, α (the calculation is explained in the next section) between Au₁₀ and Au₂₅ increases by 35% (from 1.7 to 2.6) by decreasing the NH₄Ac level to 665 mM. In contrast, despite their stronger retention, the separation between Au₂₅ and Au₂₉ is improved by only 9% (α increases from 1.14 to 1.29). Further improvement of the separation is possible with shallow salt gradients; an example is given in Figure S1 in the SI. For a detailed study of the role of salt concentration and gradient development, we refer to [20].

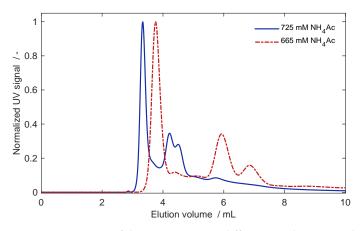


Figure 4. Separation of the AuNCs at two different conditions. For better comparison, the UV signals were normalized to their maxima and, since different flow rates were used and plotted against the elution volume. Blue, solid line—725 mM NH₄Ac and flow rate 0.4 mL/min (same chromatogram as in Figure 3 (left). Red, dash-dotted line—665 mM NH₄Ac and flow rate 0.7 mL/min. All other conditions were as in Figure 3.

4.2. Separation by Alternate Pumping

The scope of this work is to demonstrate the applicability and potential of alternate pumping for resolving challenging separation problems that occur when synthesizing nanoparticulate materials. Therefore, rather than aiming at optimizing separation conditions for conventional isocratic or gradient chromatography, we intentionally chose conditions that led to only partial separations as in Figure 3 (left). The shown chromatogram is typical for this type of application and serves as a reference example. It reveals that isolating one or more specific clusters from a synthesis solution requires accomplishing two separation tasks simultaneously. The first is to resolve closely eluting components,

while the second is the removal of early and late eluting impurities that are present in the complete elution profile.

In a first step, the elution behavior of the two columns (A, B) is compared in Figure 5 under the same conditions as in Figure 3. Inspection of Figure 5 reveals that the elution order is identical and that the resolution is similar for both columns. However, the retention times for column B are significantly lower. This may be due to the different lab histories of the columns or due to batch-to-batch differences in their manufacturing. A clearer picture is obtained on the basis of thermodynamic parameters. From the void times of the columns, t_0 , as taken from the injection peak distortions and after subtracting the system's void time, we find the total porosities for column A and B as 0.5 and 0.48, respectively.

This difference is too small to explain the observed discrepancies. Table 1 compares the capacity factors, k'_i , for the three significant peaks of Au₁₀, Au₂₅ and Au₂₉ in Figure 5, calculated from their retention times as $k'_i = (t_{R,i} - t_0)/t_0$. Based on this, the capacities of column B are between 6% and 10% lower than for column A. However, the separation factors $\alpha = k'_j/k'_i$ between two consecutive peaks *i* and *j* also given in Table 1, differ by less than 3%. This similarity simplifies the coupling of these different columns in AP experiments.

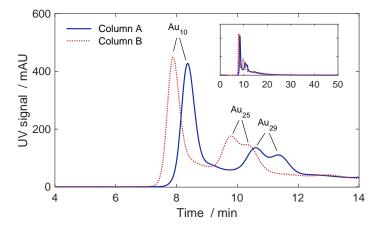


Figure 5. Comparison of chromatograms for the two columns A and B under the same conditions as in Figure 3 (left).

Peak	Column A			Column B			Difference/%	
	t_R	k'	α	t_R	k'	α	$\Delta k'$	Δα
Au ₁₀ Au ₂₅ Au ₂₉	8.37 10.60 11.33	0.613 1.042 1.183	1.701 1.135	7.88 9.78 10.28	0.579 0.960 0.1060	1.657 1.104	5.5 7.9 10.4	2.6 2.7

Table 1. Retention characteristics of the two columns for the chromatograms in Figure 5.

4.2.1. Isolation of Two Larger Clusters

As a first example, we apply alternate pumping to isolate the two largest identifiable clusters, Au₂₅ and Au₂₉, together from the rest of the mixture. This corresponds to purifying and further resolving the double peaks visible in Figure 5 at around 11 min (column A) and 10 min (column B).

Since the differences of the retention times between the two columns are too large to be ignored, designing suitable switching times requires adapting the procedure in Section 3. The simplest way would be to use an average value of the retention times for Δt_{design} in Equation (2), i.e., $\Delta t_{design} = \frac{1}{2} \left(t_R^{(A)} + t_R^{(B)} \right)$. While, in many cases, this will be sufficient, it will cause a certain 'swing' of the positions of target peaks from cycle to cycle.

This may lead to a loss of product, particularly if the retention times differ strongly and many cycles are performed. Such a situation can be circumvented by using different values for Δt_{cyc} in each cycle. Specifically, after the first cycle, one simply alternates the cycle duration in odd and even cycles between $t_R^{(A)}$ and $t_R^{(B)}$.

When adopting this strategy for the isolation of the two species Au₂₅ and Au₂₉, the cycle durations should correspond to the *mean* retention times of both peaks (or, alternatively, to the elution time of the valley between the two peaks) determined for each of the two columns separately, i.e., $\bar{t}_R^{(A)} = 1/2 \left(t_{R,Au25}^{(A)} + t_{R,Au29}^{(A)} \right)$ and $\bar{t}_R^{(B)} = 1/2 \left(t_{R,Au25}^{(B)} + t_{R,Au29}^{(B)} \right)$. From Table 1, these mean times are found as $\bar{t}_R^{(A)} = 10.97$ min and $\bar{t}_R^{(B)} = 10.03$ min. In the first cycle, injection is performed onto column A. Thus, according to Equation (2), the switching after cycle 1 is at $t_s^{(1)} = 1.5 \cdot \bar{t}_R^{(A)} = 16.45$ min. In cycle 2, the target species migrate through column B. Thus, $t_s^{(2)} = t_s^{(1)} + \bar{t}_R^{(B)} = 26.48$ min. In cycle 3, $t_s^{(3)} = t_s^{(2)} + \bar{t}_R^{(A)} = 37.45$ min and so forth.

Figure 6 shows the results of corresponding AP runs with six cycles. As in all our experiments, switching of the two valves was performed such that the process configuration altered between A–D–B and B–D–A only (*cf.* Figure 1). That is, the UV-VIS detector always monitors the outlet of the relevant column (analogous to the third row of Figure 2). It can be seen in Figure 6 that the two target peaks of Au₂₅ and Au₂₉ elute—as desired—in the center of all elution windows. The unwanted Au₁₀ is completely removed after the first two cycles.

In subsequent steps, the distance between the target peaks and remaining earlier impurities increases progressively, and by cycle 4, the latter are essentially removed. In parallel, during each cycle, the resolution between Au_{25} and Au_{29} increases. Although this was not the main goal of the experiment, in the last cycle, they are almost fully separated. Considering the selectivity, α , between Au_{29} and Au_{25} is about 1.1 only (see Table 1), this indicates the efficiciency of AP. Note that, in the last cycle, the baseline also drops to zero, which shows that all later eluting impurities are removed.

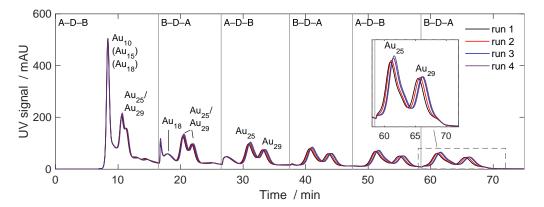


Figure 6. Alternate pumping experiments for the simultaneous isolation and purification of the two clusters Au_{25}/Au_{29} . Injection of 80 µL sample at 1 g/L. Four consecutive runs with six cycles each were performed at identical conditions. Each experiment was preceded by a regeneration step. For further experimental conditions, see Figure 3.

Some further observations from Figure 6 deserve mentioning. In cycles 2 and 3, one notices a small temporary peak of Au_{18} (and presumably of Au_{22}), which was not resolved in the first cycle. This also underlines the significant separation power of AP. Further, the inset of Figure 6 reveals a slight shoulder at the Au_{25} peak, whose origin could not be clarified from the spectra. The shoulder gradually evolved during the previous cycles, which indicates that it may be a component chemically similar to Au_{25} .

The reproducibility of the four consecutive experiments shown in Figure 6 is considered good, in particular when considering that these are recycle experiments with long

run times. Nonetheless, one observes a slight drift of the Au₂₅ and Au₂₉ peaks. Since the column was regenerated between all runs and the areas of these peaks are increasing slightly, we attribute this to a marginal shift in the relative composition of the sample. Additional experiments indicated that this may occur within the first few hours for freshly prepared samples as used here, potentially due to slow redispersion kinetics of the larger clusters. The effect is, however, very small.

Finally, with increasing number of cycles, the band broadening of the target peaks in Figure 6 increases, and their height decreases. While this is to be expected, it limits the achievable separation. Determining the column efficiency over several cycles by the half-height methods gives a number of theoretical stages of approximately 1.100 per column for the target peaks. This is not very high for analytical columns; however, it should be noted that these numbers include the repetitive extra-column dispersion in the valves, tubes and the detector. Higher efficiencies are certainly possible for the given system by, for example, optimizing the salt concentration, pH, temperature and particle size of the stationary phase and by minimizing the system dispersion.

4.2.2. Isolation of a Single Cluster

Below, we consider the typical design goal of isolating a single species out of the mixture. For this, we aim at isolating Au_{10} , which corresponds to the first peak in the chromatograms in Figure 5.

The design is performed analogously to the previous example, with the difference that the cycle durations and switching times are now determined from the retention times of Au₁₀ on the two columns, $t_{R,Au10}^{(A)}$ and $t_{R,Au10}^{(B)}$ (for values, see Table 1). Accordingly, we set $t_s^{(1)} = 1.5 \cdot t_{R,Au10}^{(A)} = 12.55$ min, $t_s^{(2)} = t_s^{(1)} + t_{R,Au10}^{(B)} = 20.43$ min, $t_s^{(3)} = t_s^{(2)} + t_{R,Au10}^{(A)} = 28.8$ min, etc.

Figure 7 shows a corresponding AP experiment with six cycles. As desired, the target peak of Au_{10} is maintained as centered in all cycles. The late eluting impurities and Au_{29} are removed. Au_{18} , which elutes very close to Au_{10} , is removed only partially; however, the two are resolved well. However, the main peak in the last cycle shows two peak shoulders. According to the spectra measured, these belong to Au_{15} and Au_{25} (see Figure S2I in Supplementary Materials). Au_{15} is present in trace amounts and elutes too close to Au_{10} to allow for separation. In contrast, the shoulder formed by Au_{25} appears contradictory, since this is retained strongly enough to be separated from Au_{10} already in the first cycle.

Gritti [40] mentions that peaks of strongly retained species can appear in late cycles of AP. He termed this appositely as 'peak echo'. This can occur if strongly retained species elute only after several cycles. It is, however, not the reason for the peaks of Au₂₅ observed here in cycles 2, 4, 5 and 6. As seen in Figure 7, Au₂₅ enters into column B during cycle 1 and starts eluting from that column at 20 min., before the end of cycle 2. A proportion of Au₂₅ is thereby sent to column A. Considering the retention time of Au₂₅ (see Table 1), this part will elute from column A at about (20 + 10.6 = 30.6) min, which is during the next cycle (cycle 4; configuration B–D–A).

Thus, it leaves the process unnoticed. The Au₂₅ peak after column B in cycle 4 (at 31 min) has a different origin. Cycle 3 starts while Au₂₅ is being transferred from column B to column A. The switching in this particular moment relocates most of the system's peripheral volume (the detector and some tubing) from the outlet of column B to its inlet. Thereby, the contained Au₂₅ is recycled into the same column. The positions of the Au₂₅ peak in the later cycles 4 through 6 are then consistent with the retention times of this carry-over of Au₂₅. While in cycle 5, Au₂₅ is hidden under the peak of Au₁₀, and it elutes late enough in the last cycle to form the observed shoulder.

Problems with strongly retained components can be resolved, for example, by integrating gradient-based cycles into the process to shave off early and late impurities [40,48]. However, in our case, a simple adjustment of the switching strategy is sufficient to resolve the observed problem. For this, the first cycle is shortened such that it ends right after the transfer of the target peak onto the next column. By this, the stronger retained species, including Au_{25} , are kept in column A, from where they leave the process in cycle 2.

Figure 8 shows a corresponding experiment. In comparison to Figure 7, the first cycle was shortened to 10.0 min, while the other switching times were kept identical. As can be seen in Figure 8, this prevents the transfer of Au_{25} . The resulting longer cycle 2 leads to re-centering the target peak of Au_{10} ; simultaneously, it provides more time for eluting the strongly retained impurities from column A. Overall, a better purification of Au_{10} is achieved, and Au_{25} is eliminated from the target peak.

Separation between Au_{10} and Au_{15} is, as expected, not achieved. The two small peaks marked by the asterisk (*) are assumed to have their origin in the switching of dead volumes during the transfer of impurities. This is similar to the previous example; however, the two peaks originate here from the switch after the first cycle. The difference of their positions in cycles 3 and 4 fits the retention time of Au_{25} . However, concentrations are too low to attribute them to any component. In fact, only in the first cycle, could Au_{25} be identified based on its spectrum, underlining a successful purification.

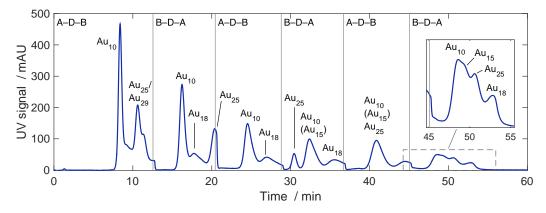


Figure 7. Alternate pumping experiment with six cycles for the isolation of Au_{10} . The main peak in the final cycle contains not only the very closely eluting Au_{15} but also the stronger retained Au_{25} . The appearance of Au_{25} there as well as at 31 and 42 min is an 'echo' of its carry-over during the switch from cycle 2 to cycle 3 (see text). For chromatographic conditions, see Figure 3. For the identification of individual clusters, see Figure S2 in the SI.

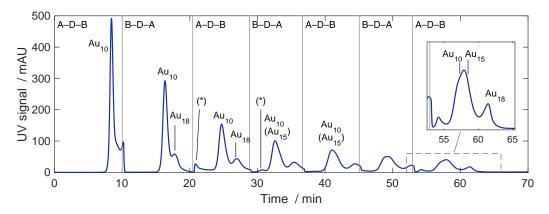


Figure 8. Alternate pumping experiment with seven cycles for the isolation of Au_{10} . In comparison to Figure 7, the design was adjusted by a shorter first cycle, which facilitated an essentially complete removal of Au_{25} . All other switching times were identical to those in Figure 7. The peak marked by (*) may represent a trace amount of Au_{25} but could not be identified due to its low concentration. For chromatographic conditions, see Figure 3.

The examples above demonstrate that single Au nanoclusters can be obtained by alternate pumping from complex matrices. This is somewhat easier for the larger clusters Au₂₅ and Au₂₉ than for Au₁₀, where the achievable purity is limited due to trace amounts of the closely eluting Au₁₅. From a practical perspective, care must be taken in the experimental design, since, during switching, certain amounts of undesired components may be recycled present in the system's peripherial volume. Such detrimental effects can be limited by adapting the switching strategy.

4.2.3. Isolation of Trace Compounds

A relevant application of alternate pumping is to isolate trace components from mixtures. As an example, we aimed here at isolating Au_{18} , which is present in the mixture in a small amount only.

Since Au_{18} is not resolved as an identifiable peak in conventional isocratic runs (see Figure 3), the process was designed such that two consecutive AP experiments were performed. For a first run, the retention time was approximated from the position in Figure 3 where the spectrum was allocated to Au_{18} . Although this did not lead to sufficient centering of the Au_{18} peak, the resolution was sufficient over several cycles (similar as in Figures 7 and 8) to deduce its retention times on the individual columns, thereby, allowing us to adjust the switching times.

The result is shown in Figure 9. As in the previous example, a short first cycle followed by a longer second one were applied, by which the late eluting impurities, including Au₂₅ and Au₂₉, were mostly already cleaved off in the first cycle. However, a small amount of Au₂₅ remained in the system as the only detectable impurity. No complete separation between Au₁₈ and Au₂₅ was achieved in the last cycle, despite that the separation factor between the two is, with $\alpha \approx 1.3$, not particularly low.

The challenge in this case is clearly that Au_{25} is present in much larger amounts than Au_{18} . Furthermore, in the last cycles, the band of Au_{18} hits the boundaries of the elution windows leading to a loss of this compound that further decreases its peak height. From this, it becomes clear that performing a large number of cycles requires choosing switching times extremely accurately. When considering typical experimental inaccuracies, column ageing, etc., at some point, this could be realized only using an online controller.

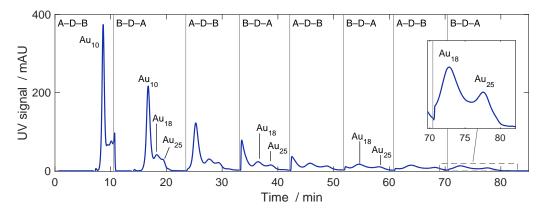


Figure 9. Alternate pumping experiment with eight cycles for the isolation of the trace component Au_{18} . As for the example in Figure 8, the switching strategy was adapted to remove late eluting impurities by a short first cycle followed by a longer second cycle. The cycle durations were 10.5, 12.975, 9.65, 9.0, 9.65, 9.0 and 9.65 min. For chromatographic conditions, see Figure 3.

Given the difficulty of the problem, the separation achieved in Figure 9 is still impressive. However, it is clear that, under the given conditions, the feasibility limit is more or less reached. A better resolution will require higher column efficiency in terms of stage numbers and/or higher separation factors. This may be achieved by, for example, changing the operating conditions or improved process concepts—for example, a pre-fractionation by gradient chromatography as proposed in [40].

4.2.4. Separation of Larger Amounts

A particularly attractive application of alternate pumping would be to quantitatively isolate the AuNCs. To investigate the applicability of the process under preparative conditions, we performed AP experiments for significantly larger injection concentrations.

In a first step, we repeated the experiments for the simultaneous separation of Au₂₅ and Au₂₉ in Figure 6 using injection concentrations of 1, 5 and 20 g/L. The use of freshly prepared solvent caused slightly reduced retention times; in comparison to the data in Section 4.2.1, $\bar{t}_R^{(A)} = 10.50$ min and $\bar{t}_R^{(B)} = 9.57$ min instead of 10.97 and 10.03 min, respectively. The switching times were adjusted accordingly. The results in Figure 10 show the expected scaling of the signals (note that, for the highest injection concentration, the detector reaches its maximum value in the first cycles). The figure reveals that, for all injected concentrations, the achieved separation is very good.

Moreover, the normalized signals for the last cycle (see inset) show that, even for the highest injection concentration, the peak symmetry and extent of separation are affected only slightly. However, the retention times are shifted to lower values with increasing concentrations, indicating slightly nonlinear, 'favorable' sorption equilibria. In the last cycle of the experiment with 20 g/L, the peak of Au_{25} touches the left boundary of the elution window. Thus, if larger amounts should be separated, preventing the loss of product will require a corresponding design method accounting for nonlinear conditions. Finally, fractions were taken around the two peak maxima of the last cycle and analyzed by gradient runs.

The signals were too low for the quantitative evaluation or identification of spectra. However, the results indicate that the peak of Au_{25} was essentially free of Au_{29} but contained trace amounts of two species assumed to be Au_{18} and Au_{22} . The peak of Au_{29} contained trace amounts of the same species but also a remainder of Au_{25} . Thus, while the separation is considered very good, complete separation of all clusters cannot be claimed.

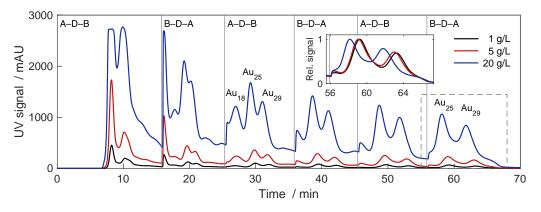


Figure 10. Alternate pumping experiments for the simultaneous isolation of Au_{25} and Au_{29} for increasing injection concentrations of 1, 5 and 20 g/L. The inset shows the normalized signals for the last cycle. Cycle durations: 15.75 min for the first cycle, followed by 9.57 min for configuration B–D–A and 10.5 min for configuration A–D–B. Other conditions analogous to Figure 6.

Figure 11 shows a corresponding study for the isolation of the single cluster of Au_{10} . Except for the higher injection concentrations, the conditions were analogous to those in Figure 8. Again, the switching times were adjusted to consider the shifted retention times. While, in the previous example, slight differences of peak shapes and retention times were observed, they are here almost unaffected (see inset). Only the tail of the peak for 20 g/L indicates the presence of a larger amount of impurities.

The constant retention time of Au_{10} indicates that the sorption is still in the linear range and that the separation of even larger amounts should be possible at these conditions. Finally, it should be noted that the adapted design method used in Section 4.2.2 (see Figure 8) also provided here a complete removal of Au_{25} . This was confirmed also by

gradient analysis of a fraction of the last peak, which indicated the presence of small amounts of presumably Au₁₅ and Au₁₈ only.

The above results underline that alternate pumping is an attractive technology for producing nanoparticulate materials in unprecedented purity even from complex synthesis mixtures. The high resolution efficiency, in particular in conjunction with the high capacity of ion exchange columns and the use of water as a green solvent, make this a very promising approach with respect to future scale-up and industrial productions of nanoparticles with high quality.

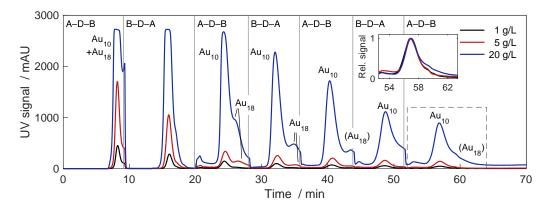


Figure 11. Alternate pumping experiments for the isolation of Au_{10} for injection concentrations of 1, 5 and 20 g/L. The inset shows the normalized signals for the last cycle. Cycle durations: 9.1 min for cycle 1, 10.77 min for cycle 2, followed by 8.1 min for configuration A–D–B and 7.72 min for configuration B–D–A. Other conditions analogous to Figure 8.

5. Summary and Conclusions

For the first time, alternate pumping was applied successfully for the simultaneous isolation and purification of nanoparticulate materials from synthesized mixtures using interaction-based chromatography. As an example problem, atomically precise glutathione-stabilized Au nanoclusters were separated by anion exchange chromatography. A simple design procedure suggested that is also applicable when using columns with different retention behaviors.

The feasibility of the approach was demonstrated in several experimental studies. In the first step, two nanoclusters of different sizes, namely Au_{25} and Au_{29} , were isolated simultaneously from the mixture with good reproducibility. The purification of the investigated single Au_{10} cluster was found to be more difficult. Separation from the closely eluting Au_{15} was not possible under the chosen conditions. The occurrence of the more strongly retained cluster Au_{25} in the product peak could be eliminated by a modified design procedure. In a third example, Au_{18} , a trace compound in the mixture, was purified successfully. Complete separation from Au_{25} was, however, not achieved. Under the chosen conditions, band broadening in particular limits the process performance.

Finally, the applicability for preparative separations was evaluated by performing alternate pumping experiments with injection concentrations up to 20 g/L. Again, the simultaneous isolation of Au_{25} and Au_{29} and the purification of Au_{10} were considered. Even for the highest injection amounts, remarkable separation was achieved. The retention behavior remained largely linear in the whole range of conditions, allowing not only for simple design but also indicating that larger amounts may be separated. The development of corresponding preparative-scale applications would benefit from design methods that account for nonlinear sorption equilibria as well as from suitable process analytical techniques based on, for example, on-line mass spectrometry.

The obtained results underline that alternate pumping chromatography, specifically on the basis of interaction-based chromatography, has great potential for achieving highly precise separations of nanoparticulate products at a preparative scale. **Supplementary Materials:** The following supporting information can be downloaded at: https://www.mdpi.com/article/10.3390/separations10030214/s1.

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