

Article



Characterizations of Biomasses for Subsequent Thermochemical Conversion: A Comparative Study of Pine Sawdust and Acacia Tortilis

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Abstract: The bioenergy production potential from biomasses is dependent on their characteristics. This study characterized pine sawdust samples from Zimbabwe and acacia tortilis samples from Botswana using conventional and spectrometry techniques. The ultimate analysis results for pine were 45.76% carbon (C), 5.54% hydrogen (H), 0.039% nitrogen (N), 0% sulphur (S) and 48.66% oxygen (O) and, for acacia, were 41.47% C, 5.15% H, 1.23% N, 0% S and 52.15% O. Due to the low N and S in the biomasses, they promise to provide cleaner energy than fossil-based sources. Proximate analysis results, on a dry basis, for acacia were 3.90% ash, 15.59% fixed carbon and 76.51% volatiles matter and 0.83%, 20% and 79.16%, respectively, for pine. A calorific value of 17.57 MJ/kg was obtained for pine, compared with 17.27 MJ/kg for acacia, suggesting they are good thermochemical feedstocks. Acacia's bulk energy density is five times that of pine, making it excellent for compressed wood applications. Though the ash content in acacia was much higher than in pine, it fell below the fouling and slagging limit of 6%. In pyrolysis, however, high ash contents lead to reduced yields or the quality of bio-oil through catalytic reactions. Fourier transform infrared spectrometry indicated the presence of multiple functional groups, as expected for a biomass and its derivatives.

Keywords: biomass; characterization; lignocellulosic; bioenergy

1. Introduction

1.1. Background and Purpose of the Study

A sustainable biomass-to-bioenergy conversion requires adequate knowledge of both the supply capacity and quality of the biomass [1]. The utilization of a biomass for bio-energy is limited by the biomass' low bulk and energy density, resulting in increased transportation and handling costs per unit energy potential or produced [2]. Most biomasses also have high moisture and mineral contents, along with wide-ranging, nonuniform physical and chemical properties [3]. These physical and chemical properties affect biomass-to-bioenergy conversion processes and the entire value chain, as further described in Table 1. Therefore, it is crucial to assess the quality of a biomass by evaluating these physicochemical properties and their corresponding effects on the thermochemical conversion process and quality of products. Such characterization results would aid the design and development of necessary biomass pretreatment methods that improve its quality, efficiency of the conversion process and quality of products.

The properties of lignocellulosic biomasses widely vary with the diversity of the tree species. Even for the same species from different geographical origins, there can be notable differences that could be caused by the different climatic and soil conditions, as demonstrated by several studies made on pine biomass in various forms [4–8]. For instance, studies of pine biomass from Spain and Canada yielded different results for the ultimate analysis, with those produced in Spain giving a lower threshold carbon (C), hydrogen (H), nitrogen (N), Oxygen (O) and sulphur (S) composition of 48.3%, 5.2%, 0.16%, 46.2% and 0.14%, compared with those grown in Canada yielding 49.0%, 6.4%, 0.14%, 44.45% and 0.01%, respectively [7,8].

The main motivation of this study is to investigate the different types of biomass materials from different geographical locations. Thus, we chose *Acacia tortilis*, a "new" biomass yet to be explored for thermochemical processes, and made a comparison with the widely studied pine. Even so, characterizing the Zimbabwean pine will give specific facts about the feedstock in this particular geographical location, while providing a point of reference for comparison with acacia. Moreover, the pine studied in this research is in the form of sawmill residues, whose properties will also vary with different storage conditions. This further justifies the need to characterize this feedstock from specified locations.

The properties of the two biomasses are useful in predicting the most efficient logistic, pretreatment and biomass-to-bioenergy conversion methods and conditions [9]. Ultimately, the characterization of feedstocks would help explain experimental biomass-to-bioenergy conversion profiles and how product yields and quality relate to biomass properties. This knowledge will be used for subsequent pyrolysis experiments in this study. Regardless, the characterization study was generalized to include the effects of biomass properties on other thermochemical biomass-to-bioenergy conversions, such as combustion, torrefaction and gasification.

1.2. The Significance of Biomass Characterisation for Bioenergy Applications

Biomass physicochemical properties are relevant in many ways at various points of a biomass process flow, especially for upstream activities and midstream conversion stages [10]. Figure 1 shows the process flow steps affected by the physicochemical properties of a biomass.



Figure 1. Relevant physicochemical properties of a biomass at different process flow steps. Reproduced with permission from Cai et al. [9], Review of physicochemical properties and analytical characterization of lignocellulosic biomass; published by Elsevier, 2017.

Álvarez et al. [1] investigated the thermochemical properties of four short-rotation woody coppices to determine their energy production potential, with an emphasis on characterization as a critical requirement for the efficient and sustainable exploitation of biomass resources. Tumuluru et al. [11] and

Mani et al. [12] examined the grinding energy requirements and physical properties of hammer-milled cereals and energy crops. They found that physical properties like the moisture content and initial particle size affected grinding energy requirements, while bulk and tapped density affected the storage requirements, size of the handling systems and conversion efficiency. Several studies have examined the efficacy of particular pretreatment methods such as torrefaction, chemical or biological treatments in enhancing specific desirable fuel or physical properties [11–14]. Biomass characterization has been used to determine the effect of such a pretreatment on physicochemical and thermal properties. In Table 1, we present a summary discussion on the relevance of selected properties to logistic and unit processes of the biomass process flow chart as provided in the literature.

| Physicochemical Property | Relevance/Significance | Literature |
|---|--|------------|
| Density (particle, bulk and tapped) | Useful for design of storage, handling and transportation facilities. Bulk and tapped density also help determine flowability and compressibility of biomass through the <i>Carr</i> and <i>Hausner</i> indices. | [1,9,11] |
| Compressibility | Useful for the design of storage, handling and feeding facilities. Higher compressibility shows that more feedstock can be stored or transported in a fixed volume. | [9,15] |
| Moisture content | A useful parameter in giving drying, storage, feeding and handling specifications. It affects the energy input in the conversion process. Higher moisture implies higher energy requirements. | [9,16] |
| Ash content | Indicates a potential risk of fouling or slagging during combustion or gasification. Higher ash/mineral content indicates a higher risk for fouling and slagging in combustion and gasification, the critical value being 6%. Ash also catalyzes the breakdown of pyrolysis vapors into water, carbon dioxide and other simpler molecules. This reduces yields and the quality of bio-oil. | [13,16,17] |
| Volatile matter | Useful in showing the potential conversion into a desirable gaseous or liquid product. For instance, in pyrolysis, a high VM indicates there can be higher bio-oil recoveries. | [9] |
| Elemental (CHNS-O) ¹ composition | Determines conversion efficiency and product composition. Significant N and S contents indicate a polluting effect. | [13] |
| Functional group composition (as investigated by FTIR) | Useful in predicting the dominant behavior of a substance and its conversion products by analyzing the reactive groups. For instance, the dominance of aliphatic functional groups in a compound can be a good indication of the good fuel properties of liquid derivatives from a feedstock. | [13,17] |
| Fuel/Thermal properties | Indicates the thermochemical conversion efficiency and heating capabilities of fuel (especially in combustion or exothermic phases). | [13,16] |

Table 1. Selected physicochemical properties and their relevance to various process flow steps.

¹ CHNS-O—carbon, hydrogen, nitrogen, sulphur, and oxygen. FTIR: Fourier-transform infrared spectroscopy.

2. Materials and Methods

The physicochemical characterization carried out on the biomasses in this study comprised proximate, ultimate, thermogravimetric and functional group analyses. Compositional analyses were used to determine the fuel potential of the feedstock. The thermal and fuel properties, in terms of heating value, were measured using a bomb calorimeter. Physical properties, namely the particle, bulk and tapped densities, were also determined. The physicochemical, thermal and fuel properties indicate how a feedstock behaves during a thermochemical conversion and the expected energy output from the process. On the other hand, physical properties generally affect the storage and handling logistics.

2.1. Sources of Biomasses Studied

Two lignocellulosic biomass feedstocks from Zimbabwe and Botswana were considered for comparative purposes, given their potential bioenergy benefits to these two nations. Pine sawdust (*Pinus patula spp.*) is a waste product from sawmilling activities in Manicaland Province, situated on the eastern part of Zimbabwe. Sawdust and wood shavings represent the most unutilized waste fractions from the sawmill operations, accumulating at approximately 70,000 tonnes per annum [18]. Heaps of such waste fractions are scattered all over Manicaland Province, marring its aesthetic appeal and posing various ecological threats, including fire, greenhouse gas emissions and wood residue leachate

that has high concentrations of dissolved organic matter [19,20]. The valorization opportunities that have been identified for the sawmill waste include combined heat and power generation from pyrolysis and the gasification/co-gasification of liquid and solid fuels and wood-engineered products [18].

Acacia tortilis is an encroacher species that is debushed from rangelands and urban circles of Botswana. Together with other encroachers, it has significantly reduced the size of quality rangeland available for both domestic and wild animals in Botswana. It costs the local and national government millions of *pulas* annually, since bush control programs have to be carried out to regenerate rangeland grass or improve the aesthetic appeal in villages, towns, cities and highways [21]. However, drought-resistant *Acacia tortilis* quickly rejuvenates after debushing, encouraged by overgrazing. Charis et al. [21] noted that the bush encroachment situation in Botswana was similar to that of Namibia, a country that is successfully valorizing its vast encroacher bush in charcoal, heat and power-generation schemes. They recommended that some of the ideas and other novel schemes, encompassing pyrolysis and gasification of the biomass, be adopted in Botswana.

2.2. Compositional Analysis and Thermal Properties

2.2.1. Thermogravimetric Analyzer

The LECO thermogravimetric analyzer (TGA) 701 (Leco TGA, St Joseph, MI, USA) was used to determine the ash composition, inherent moisture content (MC), fixed carbon (FC) and volatile matter (VM) present in the pine and acacia samples. The TGA was set to comply with the American Society for Testing and Materials (ASTM) E1131-03 and to analyze the MC, ash, VM and FC compositions as described under the ensuing subheadings [22]. The instrument was programmed to perform all these tests at various temperatures. The LECO TGA 701 automatically weighed the samples, giving real-time changes in mass. For the *Acacia tortilis*, the samples were placed in two categories, "with bark" and "debarked", to determine if there would be a significant difference in the TGA profiles and proximate composition for the two groups of acacia biomasses.

Moisture Content

Samples of 1–3 g were put into the automatic sampling containers in the TGA. The exact sample masses were then determined using the automatic balance and, subsequently, ramped the TGA at 10 °C/min to 105 °C to remove all moisture. The drying process was carried out in a dynamic atmosphere of nitrogen gas until a constant "moisture mass" was achieved; then, the TGA automatically engaged the next stage.

Volatiles Content

The TGA was set at 550 °C for volatization, such that, after removing the moisture, the temperature automatically adjusted to the set point within 10 min. Volatization occurred in an inert environment of nitrogen gas until a near-constant mass was achieved.

Ashing

After burning off the volatiles, the lids were removed from the samples, and the biomass samples were reheated to 550 °C in an oxygen-rich environment. The mass that was lost during the ashing process was the fixed carbon, which reacted with oxygen.

2.2.2. Ultimate Analysis

The ultimate analysis was conducted using the Flash 2000 CHNS elemental analyzer (ThermoFisher Scientific, Waltham, MA, USA). The biomass samples were first weighed in the sample containers with the equipment's auto-sampler system, then introduced into the combustion reactor. After combustion in an oxygen-rich environment, the gases given off were carried by a helium flow past a copper-filled layer, through gas chromatography (GC) column where the combustion gases were separated and

detected by a thermal conductivity detector [23]. The oxygen content was calculated from the difference between the cumulative C, H, N and S percentage composition and 100%.

2.2.3. Fourier Transform Infrared Spectroscopy (FTIR) Analysis

The biomass samples were grounded using a hammer-chopper mill fitted with a screen size of 3 mm. The mill product was further ground and sieved to obtain samples of less than 1-mm particle size. An infrared (IR) scan was then conducted for the wavenumber of 4000 to 500 cm⁻¹ for the underflow samples from the sieves using a Vertex70v FTIR spectrometer (Bruker, Ettlingen, Germany) [24].

2.2.4. Calorimetry

The high heating value (HHV) of the biomasses was determined using a bomb calorimeter, Bomb CAL2K-2 (Digital Data Systems, Randburg, South Africa), according to DIN 51,900 T3 standards for the "testing of solid and liquid fuels—determination of gross calorific value". A crucible with a sample of about 1.00-g biomass was placed in the calorimeter. The bomb was then closed and filled with oxygen pressurized to 30 bars. The sample was covered in an adiabatic jacket along with some known quantity of water. It was then ignited electrically, resulting in a rise of the water temperature, enabling automatic evaluation of the HHV of the sample. The calorimeter was calibrated using benzoic acid.

Table 2 summarizes the standard analyses conducted on the biomass and instruments that were used.

Table 2. Standard compositional and thermal analyses and the instruments used. HHV: high heating value and TGA: thermogravimetric analyzer.

| Test Conducted | Standards Used/Reference | Instrument | Manufacturer |
|--------------------|--------------------------|------------------------------------|--|
| Proximate analysis | ASTM E1131-03 | LECO TGA 701 | LECO, St Joseph, MI, USA |
| Ultimate (CHNS-O) | [23] | Flash 2000 CHNS elemental analyzer | ThermoFisher Scientific, Waltham, MA, USA |
| Vertex70v FTIR | [24] | Vertex70v FTIR spectrometer | Bruker, Ettlingen, Germany |
| HHV | DIN 51,900 T3 | Bomb CAL2K-2 | Digital Data Systems, Randburg, South Africa |

2.3. Physical Properties

The MC, in particular, was measured "as received" and also after solar drying for at least three weeks. All the compositional and calorimetric characterizations were only done for dried biomasses in the condition they would be when introduced into the thermochemical conversion system. This criterion would also make the two cases comparable; otherwise, a significant difference in moisture contents would lead to a bias in many properties of the biomasses.

2.3.1. Particle Density

Since a pycnometer was not available, we measured the particle density using relatively large biomass particles whose dimensions could be measured according to the method used by Lam et al. [15]. For pine sawdust, particles with a rectangular geometry were chosen, while cylindrical twigs were more suitable in the *Acacia tortilis* case. In both cases, the particles where further filed on the ends to correctly simulate the relevant geometry. The length, width and height ($L \times W \times H$) of the rectangular sawdust particles were measured, while only the length and diameter (L and D_p) of the *Acacia tortilis* cylindrical particles where determined. Vernier caliper, accurate to the nearest 0.1 mm, was used to measure all the dimensions. The mass of the particles was measured using a scale accurate to the nearest 0.01 g. Particle density (D_p) was determined as:

$$D_p = \frac{M_p}{V_p} \tag{1}$$

where M_p was the mass and V_p the volume of the cylindrical particle. The particle densities of three particles were obtained and used to calculate the mean as the final particle density of the biomasses.

2.3.2. Bulk and Tapped Density

The bulk density for the selected size classes was obtained through sieving. The size ranges (x) that were used are:

- Mixed (as-received basis)—Sawdust comes with a mixed size, while any first grind of *Acacia tortilis* similarly would contain a mixed size range. Since this mixed size is often handled or stored before further pretreatment or conversion, it is useful to determine the bulk and tapped density for this category. A sieve of 10 mm was used for the 1st grind of *Acacia tortilis*.
- Five millimeters < x ≤ 7.1 mm, 3.35 mm < x ≤ 5 mm and 1.70 mm < x ≤ 3.35 mm—The pine sawdust and Acacia tortilis particles were subjected to a sieve classification using 9-mm, 7.1-mm, 5-mm, 3.35-mm and 1.70-mm sieves. The three classes of interest in the subsequent thermochemical conversion were used for the bulk and tapped density determinations.

Feedstock will inevitably be handled in the form it is received before being ground into a final size, depending on the optimum feed particle size stipulated for the conversion equipment and process. For instance, some studies specify a size range of between 1.5–3 mm for fluidized bed pyrolysis or gasification, while larger sizes are acceptable for fixed bed pyrolysis or combustion [25]. In the case where the conversion plant is distant from the storage and pretreatment sites, it would, therefore, be good to know whether to grind the biomass to the size required by the conversion process at the beginning or to handle it in its received state until just before the conversion process.

A digital mass balance was used to weigh a container of known volume (0.280 L), then tared, subsequently. Biomass samples from each size class were then poured into the container from a constant height and leveled off. The actual mass of the biomass on balance was recorded. The bulk density, D_b , was calculated as follows:

$$D_b = \frac{\sum M_p}{V_c} \tag{2}$$

where $\sum M_p$ is the total particle mass, and V_c is the volume of the container. Tapped density D_t was determined by tapping the poured sample 30 times, adding more biomass, then tapping 20 times again. The samples were leveled off, and the mass of the compressed biomass was measured. Tapped density D_t was then calculated as follows:

$$D_t = \frac{\sum M_{tp}}{V_c}.$$
(3)

where $\sum M_{tp}$ is the total mass of the tapped particles. Four sets of experiments were done to obtain a more accurate averaged result, and an error analysis was conducted.

2.3.3. Flowability and Compressibility: The Hausner Ratio and Carr Index

The Hausner ratio and *Carr* index are derived properties calculated from the bulk and tapped densities, indicating the flowability and compressibility of the biomass. The higher the Hausner or *Carr* indices, the more compressible the biomass [11]. The Hausner and *Carr* indices were calculated as follows, using the already defined parameters D_t and D_b :

$$Hausner = \frac{D_t}{D_b} \tag{4}$$

$$Carr = \frac{100(D_t - D_b)}{D_b} \tag{5}$$

3. Results and Analysis

This section catalogues the results obtained from the tests in Section 2. It is mainly divided into two subsections to cover "Compositional and thermal properties" and "Physical properties".

The analyses and discussion of the results were done as they are presented, and then a summary discussion is also supplied in Section 4.

3.1. Compositional and Thermal Properties

3.1.1. Calorimetry, Thermogravimetry, Ultimate and Proximate Analyses

Figure 2 shows a typical TGA profile for a pine sample. The proximate composition was determined from the plateau regions and is shown in Table 2.



Figure 2. Thermogravimetric analyzer (TGA) weight loss curves for pine dust for a sample of 2.80 g.

Figure 2 shows the thermal degradation profile for weight loss against time and temperature rise against time for the sample. As can be seen from the profile, the initial weight loss began after 33 min from the beginning and continued for just over an hour until the 2.80-g sample reduced to 1 g. This long drying duration shows that the pine dust samples had high moisture contents. When the temperature was ramped up to 550 °C, still within the inert environment, another weight-loss profile occurred for 30 min, until the TGA automatically stopped after registering a constant mass. The lids were then taken off to allow free air circulation during the ashing process in an oxygen environment. The exposure to a cool atmosphere explains the sudden drop in temperature from 550 °C to 400 °C. After removing the caps, the temperature was ramped back to 550 °C. The ashing immediately commenced when the temperature had just reached the set point and continued until the sample reached a constant weight; then, the TGA automatically stopped.

Figure 3 shows the TGA weight-loss curves for the debarked acacia and that with bark.

The profiles for the various forms of acacia ("debarked" and "with bark") were mostly the same, with slight variations in the final proximate compositions. Figure 3 shows that there is little loss of weight on the acacia-drying profile duel to the low MC of 3.72% compared to 65.41% for the pine sawdust on an "as-received" basis. No air-drying had yet been done, and the pine dust was coming from humid storage conditions. When the two biomasses' weight-loss profiles were compared, it was noted that the drying step takes slightly less than 30 min for the acacia, while it takes 100 min for the pine. The volatization and ashing steps take 17 and 50 min, respectively. The volatization step is longer for pine dust (30 min), attesting to the higher VC, while the ashing period is almost the same.



Figure 3. TGA weight-loss curves for (a) debarked acacia and (b) acacia with bark.

It was further observed that there were random differences in the proximate composition between debarked samples and those that had bark, with no particular trend. The thinness of the acacia shrub bark layer could make its contribution to the results insignificant. Other authors such as Olatunji et al. [26], however, observed higher ash contents and a lower HHV for samples with bark (from mature trees) compared to the debarked biomass. As a consequence of our findings, only the proximate compositions for the samples with bark were adopted, since it is also quite unlikely that the *Acacia tortilis* will be debarked before conversion or valorization exercises. The calorimetry, thermogravimetry proximate and ultimate analyses results are summarized in Table 3.

Table 3. Results of ultimate and proximate analyses (dry basis) for acacia, compared to the common pine. FC—fixed carbon, VM—volatile matter and MC—moisture content.

| Lignocellulosic | Ultimat | e Analysis (| %)—An Aver | age of 2 | Proximat | te Analysis (% | 6) (Dry Bas | is)—Averages | HHV (MJ/kg) |
|-----------------|---------|--------------|------------|----------|----------|----------------|-------------|---------------------------------------|-------------|
| Biomass | С | Н | Ν | 01 | Ash | FC | VM | MC | |
| ACACIA | 41.47 | 5.15 | 1.23 | 52.15 | 3.90 | 19.59 | 76.51 | 3.72 | 17.267 |
| PINE DUST | 45.76 | 5.54 | 0.039 | 48.66 | 0.83 | 20.00 | 79.16 | 65.41 ² /6.50 ³ | 17.568 |

¹ Oxygen calculated by difference, considering that S = 0. ² Moisture content as received. ³ Moisture content after solar-drying for at least 3 weeks.

Table 3 shows that the HHV for Acacia tortilis is not very different from that of pine dust, though the acacia has a considerably higher ash content and a slightly lower fixed carbon. The higher fixed carbon of the pine dust explains why it would have a higher HHV compared to acacia. The FC of Acacia tortilis corresponds with the low C content in the ultimate analysis (41%), which is also smaller in comparison to the 44% in Acacia Holosericea [17]. The higher VM in the pine dust also indicates it may have a more favorable conversion efficiency, with potential for a higher yield of bio-oil in pyrolysis, for instance. On the other hand, the higher ash content (3.90%) in A. tortilis shows there is a higher mineral content, making it more prone to fouling and slagging compared to the pine; however, the figure is below the critical 6% stipulated for gasification systems [13]. This figure is comparable to Acacia Holosericea with an ash content of 3.91%. It would be interesting to investigate if the mineral content in the acacias would not have a significant impact on the yield and quality of bio-oil obtained through pyrolysis. The pine residues also have more VM (79.16%) than Acacia tortilis (76.51%). However, the latter's VM is higher than other acacia species studied: Acacia holosericea (65.32%), Acacia mangium (65.2%) and Acacia auriculiformis (65.37%). Overall, it does seem that pine dust would be a better feedstock for thermochemical conversions compared to acacia, although this would further depend on the particular conversion and the targeted products.

The ultimate analysis results corroborate with the proximate study, which shows a higher FC content in the pine residues compared to acacia. There was no S detected for both biomass types, though acacia registered a significant N content (1.23%) due to its nitrogen-fixing and retaining capabilities. This N content is considerably higher compared to 0.25% in Acacia Holosericea, and in both acacias, S was not detected. Charis et al. [10] noted that the pine dust from Zimbabwe has relatively lower N and S contents compared to the Canadian (N: 0.14% and S: 0.01%) and Spanish (N: 0.16%–1.6% and S: 0.14%–0.45%), making it a cleaner thermochemical feedstock [5,7]. In general, the low amounts of N and S in the pine dust and acacia imply that the two biomass types have a lower environmental burden compared to fossil fuels. A further comparison of the ultimate, proximate and calorimetric analyses of the sawdust with other pine residues from the literature was made. The HHV for pine sawdust (17.568 MJ/kg) was higher than the value of 15.01 MJ/kg quoted by Braza and Crnkovic [4] but lower than that found by Olatunji et al. [26] of 20.54 MJ/kg. The range is, however, acceptable, and the differences could be due to varying MCs. The pine dust in this study has the lowest C content at 45.76% compared to 48.62% by Braza and Crnkovic [4] and 50.54% by Olatunji et al. [26], as well as the highest O content at 48.66% compared to 43.20% and 41.11% from the two other studies, respectively. Most proximate parameters were found to have values somewhere between those obtained by Braza and Crnkovic [4] and Olatunji et al. [26] except for the MC and fixed carbon, which were the highest for the pine dust in this study. The differences in compositional values for the pine sawdust show how variations can occur due to various storage and environmental factors or as a result of the different soil and climatic conditions in which the trees were nurtured.

3.1.2. FTIR Analysis

Figures 4 and 5 show the peaks obtained from the FTIR scan of the *Acacia tortilis* and pine dust samples, respectively. The functional groups most possibly represented by the peaks were determined by referring to the literature, as shown in Table 4.



Figure 4. Fourier-transform infrared spectroscopy (FTIR) peaks for Acacia tortilis.



Figure 5. FTIR peaks for pine dust.

| Absorption Peak-Acacia | Absorption Peak-Pine | Possible Compounds/Chains Rationale | Type of Vibration Causing the IR Absorption | Literature |
|---------------------------|---------------------------------|---|--|------------|
| 3332.15 | 3337.09 | Phenols, carboxylic acids and alcohols (broader peak) | Hydrogen-bonded OH stretch in cellulose and lignin | [17,27] |
| 2921.86 | 2918.56 | Alkanes or primary amine Alkanes and acids | H-C-H asymmetric and symmetric stretch | [17,27] |
| 2853.83 | | Alkanes or aldehydes | H-C-H asymmetric and symmetric stretch; C-H branch off C=O H-C-H asymmetric and | [17,27] |
| | 2359.45 | Alkanes and acids | symmetric stretch; C-H branch off C=O | [28,29] |
| 2357.78 and 2331.40 | 2342.38 | Carbon dioxide | CO ₂ | [28,29] |
| 1729.82 | 1733.90 | Ketones and aldehydes Carboxylic acid | C=O stretch in hemicellulose | [17,27] |
| 1622.48 | 1616.28 | Alkenes | sp ² C-X double bond | [28,29] |
| 1514.51 | 1507.13 | Secondary Amine confirmed | Ñ-H bend | [28,29] |
| 1454.35 | 1454.35 | Alkanes confirmed | H-C-H bend | [28,29] |
| 1422.69 (actual: 1425) | | Lignin and wood | CH in-plane deformation | [17] |
| | 1419.27 | Alkanes | sp ³ C-H bend | [28,29] |
| 1368.87 and 1317.74 | 1368.93 | | C–H deformation in cellulose and hemicellulose | [17] |
| 1234.77 and 1027.80 | 1261.31, 1229.55 and 1025.60 | Esters or ethers | Alkoxy C-O stretch and C-O stretch in cellulose, hemicellulose or lignin | [28,29] |
| | 897.10 and 721.20 | Aromatic rings and meta di-substituted compounds | sp ² C-H-bending patterns | [28,29] |
| 773.81, 644.00 and 604.05 | 668.16 to 604.56 | Fingerprint regions not easy to unknown compound | interpret for a previously | [17] |

| Iddle 4. Compounds represented by the acadia and blue rink bea | Table 4. C | Compounds re | presented by | / the acacia | and 1 | pine FTIF | R peaks |
|---|------------|--------------|--------------|--------------|-------|-----------|---------|
|---|------------|--------------|--------------|--------------|-------|-----------|---------|

The FTIR image for the pine dust in Figure 5 seems to have more functional groups (16) depicted by the peaks below the 2200-cm⁻¹ wavenumber, compared to 12 groups for the acacia in Figure 4.

Table 4 shows the interpretation of the peaks obtained in the FTIR for the two biomasses. The functional groups at those peaks were identified by comparing with the standards derived from the literature.

Using the FTIR analyses, we identified many functional groups in both biomass samples, attesting to the heterogeneous nature of the biomasses. The FTIR analyses indicated the presence of a wide range of compounds within the cellulose, hemicellulose and lignin structures [30]. Reza et al. [17] explicitly linked the C-H bond stretch in the region 2960–2850 cm⁻¹ to the presence of lignin, hemicellulose and

cellulose in the biomasses. They further associated the area between 2000 and 1650 cm^{-1} to the C-H bonding in cellulose and hemicellulose, while the region 1750-1630 cm⁻¹ was mainly linked with the C=O in hemicellulose. This finding is in tandem with literary works like Ahmed et al. [27] and Naik et al. [7]. The functional groups identified in pine dust are mostly the same as those in Acacia tortilis, though in varying quantities. The peak at wave 2853.83-cm⁻¹ frequency seemed to suggest a more substantial presence of aldehydes or alkanes in the acacia, while the one at 1422.69 cm^{-1} suggested a stronger lignin presence in this hardwood, as expected and compared to the pine softwood. Pine dust also had prominent peaks at 2359.45 cm⁻¹ and 1419.27 cm⁻¹, which suggested a strong presence of alkanes as well. Further analyses would be required to tell the exact comparative alkane compositions. The other peaks at 897.10 cm⁻¹ and 721.20 cm⁻¹ for the pine dust suggested a significant presence of aromatic rings, meta di-substituted compounds. The analyses of pyrolysis products in the latter stages of the bioenergy project using FTIR and other scanning calorimetry methods could help to confirm these results and simulate the possible conversion pathways. The other difference in the FTIR results for the two biomasses was the presence of a broader fingerprint region (six clumped peaks) of unknown functional groups for the pine dust, in the range 604.56–668.16 cm⁻¹. Meanwhile, the Acacia tortilis' lower-end fingerprint region only comprised three unknown peaks at 603.05, 644 and 773.81 cm⁻¹. For both lignocellulosics, the FTIR analyses showed more functional groups than those reported by Reza et al. [17] and Ahmed et al. [27]. The acacia's FTIR results agree with the studies on other acacias published by Reza et al. [17] and Ahmed et al. [27], especially at the peaks depicted by wavenumbers 3332.15 cm^{-1} , 2921.86 cm^{-1} , 2853.83 cm^{-1} , 1729.82 cm^{-1} and 1422.69 cm^{-1} and the corresponding functional groups.

3.2. Physical Properties

The MC has already been covered under the compositional analysis. The results for the other physical properties, mainly the particle, bulk and tapped densities are presented in this section. Using these values, the Hausner and Carr indices, which indicate the compressibility and flowability of the biomasses, were calculated.

3.2.1. Particle Density

The average density from three particles, as calculated by Equation (1) from Section 2.2.1, was 478.8 kg/m³ for pine and 867.3 kg/m³ for the *Acacia tortilis* particles. The average density obtained for the pine dust was close to the 490 kg/m³ stipulated by the *pinus patula* datasheet [31]. Logically, pine residues that have been under various storage conditions and exposed to different weather elements would differ in some physical properties from freshly harvested pine trees. Furthermore, the density of the *Acacia tortilis* (867.3 kg/m³) was almost double that of the pine (478.8 kg/m³), as expected for a hardwood compared to the pine softwood.

3.2.2. Bulk and Tapped Density

Figure 6 shows the mean values obtained from four runs on bulk density and tapped density for both biomasses and the relative standard error associated with the type of biomass. These mean values were then used to calculate the Hausner ratios and Carr's indices for various size ranges.



Figure 6. Bulk and tapped densities for various size classes of pine and acacia samples. Db: bulk densities and Dt: trapped densities.

The bulk and tapped densities of the acacia were at least four times larger than for pine, because they are a function of the number of particles contained in the fixed volume and the mass of each particle, according to Equation (2) in Section 2.2.2. These densities are an essential consideration when the biomass is being transported or stored for subsequent thermochemical conversion. In this case, the energy stored or transported per unit volume would be a lot larger for the *Acacia tortilis* compared to the pine dust. For example, in the size range 3.35 mm < $x \le 5$ mm, one cubic metre of pine dust stored or transported would have equivalent energy of 522.1 MJ compared to 2709.7 MJ for the same size range for acacia. The formula for calculating the bulk energy density (*ED*_b) of the biomass is given by Equation (6):

$$ED_b = D_b \times HHV \tag{6}$$

3.2.3. The Hausner Ratio and Carr index

Figures 7 and 8 show the Hausner ratios and Carr calculated from the mean values of the bulk and tapped densities from Figure 6. The calculations were made according to Equations 4 and 5 provided in Section 2.2.2.

For both samples, the mixed size (as-received basis) had the highest Hausner ratio and Carr's index, indicating higher compressibility. This result is probably because, during tapping, the smaller particles fill in the voids left by the bigger particles. Consequently, it may be desirable to store and transport mixed size fractions (mostly as-received) within a specific range to make optimal use of the space. The acacia biomass also has higher Hausner's ratios and Carr indices than pine, which shows it is a more compressible biomass type.



Figure 7. Hausner ratios for pine and acacia.



Figure 8. Carr indices for pine and acacia.

4. Discussion

The characterization of the two biomass feedstocks makes it possible to predict their behaviors at various steps of the supply chain and add any necessary pretreatments. Table 5 discusses the results obtained from the previous section with regards to their implications on supply-chain (SC) dynamics like transport, handling, storage, conversion and the overall economics, as hinted in Table 1.

| Table 5. | The implications | of the charact | terization res | ults on the | supply-chain | (SC) dynamics, | economics |
|-----------|------------------|----------------|----------------|-------------|--------------|----------------|-----------|
| and the e | environment. | | | | | | |

| Physicochemical Properties | | Comparative Status of the Properties for Acacia and Pine Dust | Potential Effects on SC Dynamics, Economics and Environment |
|--------------------------------|------------------|---|---|
| Elemental composition (CHNS-O) | | Higher N content in <i>A. tortilis</i> compared to pine dust. Both biomasses have no S detected. Higher O/C ratio in <i>A. tortilis</i> (1.25) compared to pine dust (1.06). | Both biomasses have low N and S contents, implying a lower environmental impact compared to fossils [13]. Costs of scrubbing are circumvented. Higher O/C ratio would affect the quality of some products or by-products, such as pyrolysis oil, though marginally compared to the pine dust [32]. |
| | Moisture content | The MC of pine dust (65.41%) on an "as-received" basis is way higher than for acacia (3.72%). Solar-dried pine goes down to 6.50%. | Solar-drying can be used to bring pine dust MC down, but that exposes it to contamination with dust, etc., which affects the quality of conversion products. Other methods of drying would mean extra costs. High MC lowers the HHV of a biomass [33]. |
| Proximate composition | Ash content | Higher ash content in acacia (3.90%) compared to pine dust (0.83%). | The ash in acacia is below the critical fouling and slagging level (6%). It could, however, act as a catalyst in processes like pyrolysis, decreasing the yield and quality of bio-oil [34]. This would, however, need to be confirmed with the actual pyrolysis set-up. |
| Volatile matter | | Higher VM in pine dust (79.16%) compared to acacia (76.51%). | There could be higher yields/recoveries of liquid or gaseous products from conversions like pyrolysis and gasification [9]. It does not, however, indicate the quality of the gas or liquid product. |
| Fixed carbon | | A slightly lower FC in acacia (19.59%) compared to pine dust (20.00%). | The difference is not significant, though it could explain why the acacia has a slightly lower HHV compared to pine dust. |
| HHV | | A slightly lower HHV in acacia (17.267MJ/kg) compared to pine dust (17.568 MJ/kg). | The moderately high HHV means both can be exploited well by thermochemical means, including upgrading their energy value through torrefaction [14]. The latter would bring their energy value closer to that of coal. |
| Densities and | compressibility | The particle, bulk and tapped densities of acacia are about 2–4 times higher than for pine dust. | This fact brings an advantage for acacia in terms of storage and energy density. For the size range 3.35 mm < x \leq 5 mm, acacia has an energy density of 2709.7 MJ/m ³ compared to 522.1 MJ/m ³ for pine dust. More energy values can be recovered for the same volume of stored, transported or fed acacia (Section 3.2.2). Figures 7 and 8 show that the acacia generally has a higher compressibility, and, coupled with the energy density factor, it has a better potential for compressed wood products [18]. |
| Functional groups | | Multiple functional groups for both biomass types. | This result proves there are many compounds in the biomasses, which is also characteristic of some of the conversion products like bio-oil [34]. Consequently, separation and purification to derive chemicals or fuels from the oil becomes a costly and challenging task. |

5. Conclusions and Recommendations

Various literature sources have confirmed the importance of the physicochemical characterizations of biomasses, a primary step in exploring the feasibility of exploiting them for bioenergy. For this particular study, the characterization results concurred with general expectations emanating from the tree classifications. They also compared well with studies of similar biomasses from the literature. The comparative study showed that pine dust has better fuel properties per unit weight than Acacia tortilis due to its higher HHV and fixed carbon, with low ash and oxygen contents. However, since Acacia tortilis' thermochemical properties are not very far from those of pine, and the ash content (3.61%) is about half the critical slagging and fouling value of 6%, it can also be effectively exploited thermochemically [13]. Moreover, the energy density (energy per unit volume) of Acacia tortilis is about four times larger than for the pine dust due to its higher bulk density, giving it an advantage in storage and the actual thermochemical conversions. The considerably higher particle, bulk and tapped densities for Acacia tortilis compared to pine are expected, since the former is a hard wood, while the latter is a soft wood. Such high bulk-energy densities of *Acacia tortilis* also mean that it can be compressed into pellets or briquettes of higher energy values compared to pine dust. Since both biomasses are wastes in their local contexts, and their thermochemical properties are within the recommended ranges, they can be converted by any of the combustion, gasification and pyrolysis routes. They can also be torrefied or carbonized into charcoal to obtain solid fuels of higher heating values. Further experiments can be carried out for the various conversion routes to determine the

optimal conditions and the properties of the products. For storage purposes, it seems more convenient to store the feedstocks as they are received, or after the first grind, while they have a mixed size range that is more compressible than uniform sizes.

There were also some limitations in the study, mainly in the FTIR analysis and particle density measurements. It is ideal to have a library of standards attached to the FTIR spectrometer to identify the functional groups directly; however, the equipment used did not have such a library. Therefore, the literature was used to make inferences, using findings done before by other authors. A pycnometer is recommended for densities of small particles; however, since it was not available, particle dimensions were used as the next most-appropriate method.

Although feedstock characterizations give a broad picture of the expected behavior of a material in subsequent stages, further tests still need to be done to confirm such predictions and derive specific results for the actual logistic and conversion stages.

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Abbreviations and Symbols

| Abbreviation | Explanation |
|-------------------------|---|
| ASTM | American Society for Testing and Materials |
| CHNS-O | Carbon, hydrogen, nitrogen and sulphur; oxygen determined by the difference |
| D_b | Bulk density of particles |
| D_t | Tapped density |
| ED_b | Bulk energy density |
| FC | Fixed carbon |
| FTIR | Fourier-transform infrared spectroscopy |
| GC | Gas chromatography |
| HHV | High heating value |
| L and D_p | Length and diameter of cylindrical acacia particles |
| $(L \times W \times H)$ | Length, width and height dimensions for rectangular pine particles |
| MC | Moisture content |
| $\sum M_p$ | Total particle mass |
| M_p and V_p | Mass and volume of the cylindrical particles |
| $\sum M_{tp}$ | The total mass of tapped particles |
| SC | Supply chain |
| TGA | Thermogravimetric analyzer |
| | |

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