



Article Numerical Investigation of MWCNT and SWCNT Fluid Flow along with the Activation Energy Effects over Quartic Auto Catalytic Endothermic and Exothermic Chemical Reactions

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Abstract: A mathematical model is created to analyze the impact of Thompson and Troian slip boundaries over a contracting/expanding surface sustaining nanofluid-containing carbon nanotubes along a stagnation point flow. Both multi-wall (MWCNTs) and single-wall (SWCNTs) carbon nanotubes are taken into consideration, with water serving as the base liquid. The flow is obtained due to the stretching or contracting of the surface. The thermal radiation, activation energy, buoyancy impacts, and chemical processes called quartic autocatalysis are additionally added to the original mathematical model. The MATLAB-constructed bvp4c function involving the three-stage Lobatto IIIa formula for the numerical results of dimensionless velocity, concentration, and temperature profiles are used. By contrasting it against a published paper in this limited instance, it is determined whether the suggested mathematical model is legitimate. In this sense, a remarkable consensus is achieved. Graphical representations are used to depict the behavior of many non-dimensional flow variables, such as the slip velocity parameter, the inertia coefficient, the porosity parameter, and the solid volume fraction. Surface drag force computations are reported to examine the effects at the permeable stretching surface. It has been shown that increasing the slip velocity factor increases the fluid streaming velocity while decreasing the surface drag force. If the endothermic/exothermic coefficient increases, the local thermal transfer efficiency falls. For nanofluids, the changing viscosity factor increases axial velocity while decreasing temperature distribution. Additionally, the solid volumetric fraction improves the temperature distributions by lowering the concentration profile and speed.

Keywords: stagnation point; magnetohydrodynamics; endothermic and exothermic reaction; heat generation/absorption; activation energy; carbon nano tubes

MSC: 76W05; 76D05; 7604

1. Introduction

When industries and scientists were seeking out greater and better thermal characteristics in fluids used on a regular basis for diverse tasks, Mesuda et al. [1] suggested the introduction of nano-sized particles in ordinary fluids in 1993. Later, the term nanofluid was officially defined by Choi and Eastman [2], and these fluids became a prime focus of researchers. Nanoparticles are typically 1–100 nm in size, but this might vary significantly depending on their sizes and shapes. Water, ethylene glycol, and oil are commonly used base fluids. A nanofluid is a combination of nanosized materials and a base liquid. These nanoparticles are suspended in a base fluid that is colloidal in nature and has weaker



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Copyright: © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). thermal conductivity. The major goal of nanosized particles is intended to improve the thermal conductivity of fluids, as well as increase heat transmission. Because of their structure, nanosized particles have unique physical and chemical features and contribute to the development of thermophysical systems. Nanofluids have a wide range of applications, such as in nano-drug delivery, pharmaceutical operations, heating/cooling appliances, fuel cells, and microelectronics. Nanofluids are utilized as coolants in the thermal exchange systems of automobiles and nuclear reactors. However, they are also useful due to their regulated optical features.

Carbon nanotubes are cylinder-type shapes that are formed by rolling or folding a graphite sheet. They have unique mechanical, thermophysical, and chemical properties. Because of their cylindrical form, huge surface area, and small size, carbon nanotubes offer advantages over other macro/nanoparticles. Carbon nanotubes are categorized as SWCNTs or MWCNTs based on their number of graphene layers. The effects of the nanofluid in the physiological examination of cilia were highlighted by Sadaf and Nadeem [3]. Sivasankaran et al. [4] investigated the heat production of nanofluids in the cavity. Ahmed et al. [5] investigated the flow of multi-walled and single-walled carbon nanotubes (MWCNT and SWCNT) across a circular stretchable semi-infinite zone containing water as the base fluid. Hosseinzadeh et al. [6] concentrated on the MWCNTs and SWC-NTs combined in ethylene glycol flowing between the two rotating discs with extensible qualities in it; the effects of MHD and thermal radiations were considered, and findings revealed that the fluid system's instability and the volume fraction of the nanosized particles decreases as the radiation increases. Ramzan et al. [7] investigated a physical system of gyrotactic microorganisms and CNTs submerged in water that was flowing on the top of a vertical cone immersed in a permeable medium by using the bvp4c MATLAB software and discovered that increasing the suction parameter reduces the nanofluid stream velocity. They also considered chemical reactions, thermal radiation, and species stratification. Khan et al. [8] examined the flow at the stagnation point of carbon nanotubes moving across an extended surface in the applied magnetic field, as well as thermal radiation, homogeneous and heterogeneous reactions, and heat absorption/generation. By applying the shooting method, numerical consequences revealed that MWCNTs had a greater induced magnetic field than SWCNTs. Ramazan et al. [9] studied CNTs and gyrotactic microorganisms in a fluid moving through a vertical cone enclosed by porous media. Joule heating, thermal radiation, MHD, and the homogeneous and heterogeneous reactions were all thought to be important inside the fluid system. According to the results obtained by using bvp4c MATLAB software, the flow of the fluid decreases with increasing magnetic force. Khan et al. [10] used the homotopy analysis method (HAM) to study a radiant bioconvective MHD nanofluid flow across an elongated oscillating plane and discovered that the temperature of the nanofluid increases as the buoyancy ratio increases. Sergii et al. [11] presented an analytical theory for the electrostatic interactions between two spherical dielectric particles with arbitrary charge distributions expanded in multipolar terms submerged in a polarizable ionic solvent and with arbitrary radii and dielectric constants. Yu [12] presented a new formalism regarding reciprocity and arbitrarily accommodated many dielectric spheres of different dielectric constants and sizes while being rigorous at the Debye–Hückel level. Some further prominent articles highlighting the use of nanofluid are as follows: refs. [13–17]. A chemical reaction is the interaction of two or more chemicals, which leads to the composition of one or more new chemical substances. A chemical reaction is the breaking of old bonds in order to form a new bond chemically. This is also known as the chemical change caused by the interaction of two or more chemical substances. The temperature of the system rises or decreases when energy is transferred to or from the environment during a chemical process. Exothermic reactions are chemical processes for which energy is discharged into the atmosphere (i.e., outside of the system). Energy is typically conveyed as heat energy, which causes the atmosphere to heat up. The burning process is an illustrative example of an exothermic reaction. Endothermic reactions are chemical reactions that extract energy from their environment. Normally, the energy is shifted as heat, raising the temperature of the reaction mixture. Chemically reactive models, such as biological systems and combustion, are represented by homogeneous/heterogeneous reactions. The surfaces of the catalysts experience heterogeneous reactions, but the fluid itself experiences homogenous reactions. In practice, homogeneous and heterogeneous reactions can be observed in a number of different fields, including air pollution, food processing, ignition, and biological processes. The species of chemical reactions together with the activation energy phenomenon plays a major role in various engineering fields. Mass transport and chemical processes can be seen in the consumption as well as production of reactant species. Regarding the existence of thermal dissipation, Maleque [18] was interested in the study of the impact of endothermic/exothermic chemical processes having Arrhenius activation energy on magnetohydrodynamic-free convective and the mass transfer flow. Recently, Bejawada et al. [19] investigated a magnetohydrodynamic Casson fluid flow with chemical reaction properties along with a porous Forchheimer medium over a non-linear sheet. Suleman et al. [20] used the shooting technique to show how the concentration of nanoparticles in a silver-water nanofluid mixture decayed due to upsurging homogeneous and heterogeneous reactions influenced by viscous dissipation, MHD, thermal radiation that was not linear, and Joule heating moving through a nonlinear extending cylinder. Imtiaz et al. [21] explored the streaming of the two-dimensional magnetohydrodynamic viscous fluid flow passing over a stretched sheet. The solution was approximated with the use of a quasi-linearization method and the implicit finite difference approach, taking into account the significant impact of homogeneous and heterogeneous reactions, thermal radiation, and Joule heating. The study discovered that viscous fluids had lower fluid speed and concentration than viscoelastic fluids, and both homogeneous and heterogeneous reactions have a negative effect on fluid viscosity. Suleman et al. [22] used the shooting approach to analyze silver-water nanofluids with MHD, nonlinear heat radiation, and homogeneous and heterogeneous reactions through a nonlinear extended cylinder. Despite a greater radiation impact, the results showed better thermal conditions. Doh et al. [23] further investigated homogeneous and heterogeneous reactions with silver water nanofluids on a revolving permeable disc with changing disc thickness.

During fluid flow research, it is frequently thought that small-scale slips can happen at a fluid-solid interface as a result of uncertainty at the intense stress levels in methodologies such as polymer extraction. Fluid motion at a geometry surface is affected by such fluid slip impacts. Khan et al. [24] investigated the viscous hydromagnetic fluid flow across the permeable rotatable disk with non-linear thermal radiation and partial slip by considering the shooting method. The findings revealed a clear decline in surface friction as slip estimation increased. Using the Crank-Nicolson approach, Hamid et al. [25] investigated the natural convection of the Prandtl fluid, which was flowing at a point of stagnation across an infinite elongated plate. The geometry of the model is presented on the Figure 1. When studying slip at the sheet surface and MHD, it was discovered that when a slip impact was combined with a low magnetic field, the velocity increased dramatically. Reddy et al. [26] investigated magnetohydrodynamic Eyring-Powell fluid flow regarding nonlinear radiation, solutal slippage, temperature, velocity, and chemical processes using a Range-Kutta 4th order scheme. Kiyasatfar [27] investigated the convective slip flow of a non-Newtonian fluid among parallel plates with circular microchannels using the power-law model. The results show that for both geometries, lowered fluid stream speed and increased heat exchange rates and molecule stability occurred in rising slip situations.

According to the aforementioned studies, fewer expeditions are explored for the study of the Thompson and Troian slip forms. In the existence of suction/injection, for nanofluids based on the Yamada and Ota model consisting of two nanoparticles, i.e., single and multiwall carbon nanotubes suspended in a base fluid (water), the flow velocity, temperature, and concentration of nanofluid in the presence of the Cattaneo–Christov heat flux model are taken into account. Stagnation point flow is taken over the infinitely expanding sheet. Chemical reactions, nonlinear heat generation, and activation energy are the main key points that are focused on the current problem. The modeled equations are solved by the bvp4c technique. Graphs are drawn for the different parameters to better understand their impact on velocity and temperature.



Figure 1. Geometry of the model [25].

2. Mathematical Model

Here, we consider the two-dimensional Newtonian nanofluid flowing over the sheet which is linearly stretched along the *x*-axis. A stagnation point flow is considered along with a magnetic field which is applied normally to the flow. Heat generation, chemical reaction, activation energy, and convection are also prominent impacts that are taken into account. Importantly Thompson and Troian slip mechanisms are employed on the surface. Single and multi-wall carbon nanotubes are taken as nanoparticles which are mixed in water. The fluid flow is compressible, and the Boussinesq approximation is valid for the case of the present problem. Free convection behavior is taken due to buoyancy forces. The momentum equation comprises the buoyancy phenomenon, stagnation point, and free convection phenomenon. Heat transfer is determined in a more precise manner with the utilization of the Cattaneo–Christov heat flux expression instead of classical Fourier law expression in the energy equation. Sometimes, extra energy is required to proceed with a chemical reaction due to the slow collision of fluid molecules. This is why an activation energy expression is utilized in energy as well as concentration equations. The governing modeled PDEs are derived from the law of conservation of mass, Newton's second law of motion, the second law of thermodynamics, and Fick's second law of diffusion. After accounting for the boundary layer estimation, the system can be represented as follows [6-8,18].

$$\frac{\partial v}{\partial y} + \frac{\partial u}{\partial x} = 0, \tag{1}$$

$$v\frac{\partial u}{\partial y} + u\frac{\partial u}{\partial x} = v_{nf}\frac{\partial^2 u}{\partial y^2} + U_{\infty}\frac{dU_{\infty}}{dx} + g\frac{(1-\phi)\beta_f\rho_f + \phi\beta_s\rho_s}{\rho_{nf}}(T-T_{\infty}) - \frac{\sigma_{nf}B^2(x)}{\rho_{nf}}(u-U_{\infty}),\tag{2}$$

$$v \frac{\partial T}{\partial y} + u \frac{\partial T}{\partial x} + \tau \begin{cases} u \frac{\partial u}{\partial x} \frac{\partial T}{\partial x} + v \frac{\partial v}{\partial y} \frac{\partial T}{\partial y} + u^2 \frac{\partial^2 T}{\partial x^2} + v^2 \frac{\partial^2 T}{\partial y^2} \\ + 2uv \frac{\partial^2 T}{\partial x \partial y} + v \frac{\partial u}{\partial y} \frac{\partial T}{\partial x} + u \frac{\partial v}{\partial x} \frac{\partial T}{\partial y} \end{cases} = \alpha_{nf} \frac{\partial^2 T}{\partial y^2} \\ + \frac{Q_0}{(\rho c_p)_{nf}} (T - T_\infty) + \beta K_r^2 \left(\frac{T}{T_\infty}\right)^n exp \left[-\frac{E_a}{KT}\right] (C - C_\infty),$$

$$(3)$$

$$v\frac{\partial C}{\partial y} + u\frac{\partial C}{\partial x} = D_m \frac{\partial^2 C}{\partial y^2} - K_r^2 \left(\frac{T}{T_\infty}\right)^m exp\left[-\frac{E_a}{KT}\right](C - C_\infty),\tag{4}$$

where *T* represents the fluid temperature, *C* represents the concentration, and (v, u) reresents the velocity components in the (y, x). The parameter D_m stands for the mass diffusion coefficient, K_r which is the rate of limiting factor for the chemical process, $(\beta = \pm 1)$ is the endothermic/exothermic factor, and $\left(\frac{T}{T_{\infty}}\right)^n exp\left[-\frac{E_a}{KT}\right]$ represents the Arrhenius expression, where *n* represents a unit-less rate constant (-1 < n < 1). The thermophysical characteristics of the nanofluid are presented in Table 1. The corresponding boundary conditions are as follows:

$$u|_{y=0} = u_t + u_w(x) = mx + \gamma^* (1 - \xi^* \frac{\partial u}{\partial y})^{-1/2} \frac{\partial u}{\partial y}, \ v|_{y=0} = 0, \ C|_{y=\infty} \to C_{\infty}, \ C|_{y=0} = C_w,$$

$$u|_{y=\infty} \to U_{\infty}(x), \ T|_{y=\infty} \to T_{\infty}, \ T = T_w(x) = (T_0 x + T_{\infty})|_{y=0},$$
(5)

Physical Attributes	Base Fluid (H_2O)	MWCNT	SWCNT
$C_p(J/kgK)$	4179	796	425
$\rho(kg/m^3)$	997	1600	2600
K(W/mK)	0.613	3000	6600
$\sigma(\Omega m)^{-1}$	$5.5 imes10^{-6}$	10^{7}	10 ⁶

Table 1. Thermophysical characteristics of nanofluid and base.

The thermophysical properties are represented as defined from the Yamada and Ota model:

$$\mu_{nf} = \frac{\mu_f}{(1-\phi)^{2.5}}, \quad \alpha_{nf} = \frac{\kappa_{nf}}{\rho_{nf}(C_p)_{nf}}, \quad \nu_{nf} = \frac{\mu_{nf}}{\rho_{nf}},$$

$$\rho_{nf} = (1-\phi)\rho_f + \phi\rho_{CNT}, \quad \frac{k_{nf}}{k_f} = \frac{2\phi\frac{k_{CNT}}{k_{CNT}-k_f}\ln\frac{k_{CNT}+k_f}{2k_f} + (1-\phi)}{2\phi\frac{k_f}{k_{CNT}-k_f}\ln\frac{k_{CNT}+k_f}{2k_f} + (1-\phi)}, \quad (6)$$

$$\frac{\sigma_{nf}}{\sigma_f} = 1 + \frac{3\left(\frac{\sigma_s}{\sigma_f} - 1\right)\phi}{\left(\frac{\sigma_s}{\sigma_f} + 2\right) - \left(\frac{\sigma_s}{\sigma_f} - 1\right)\phi}.$$

Introducing dimensionless variables, we obtain:

$$\eta = y_{\sqrt{\frac{c}{\nu_f}}}, \ v = -\sqrt{\nu_f c} f(\eta), \ u = U_{\infty} f'(\eta), \ \theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}, \ \phi(\eta) = \frac{C - C_{\infty}}{C_w - C_{\infty}}$$
(7)

After simplification, we convert the system of PDEs into the following ODEs:

$$\frac{1}{(1-\phi+\phi\frac{\rho_{CNT}}{\rho_{f}})(1-\phi)^{2.5}}f'''+f''f-f'^{2}+1+\frac{\phi\frac{\rho_{CNT}\beta_{CNT}}{\rho_{f}\beta_{f}}-\phi+1}{(1-\phi+\phi\frac{\rho_{CNT}}{\rho_{f}})}\lambda\theta+\frac{\left(1+\frac{3\left(\frac{\sigma_{s}}{\sigma_{f}}-1\right)\phi}{\left(\frac{\sigma_{s}}{\sigma_{f}}+2\right)-\left(\frac{\sigma_{s}}{\sigma_{f}}-1\right)\phi}\right)M}{(1-\phi+\phi\frac{\rho_{CNT}}{\rho_{f}})}(1-f')=0, \quad (8)$$

$$\frac{k_{nf}}{k_f}\theta'' + Pr\left(1 - \phi + \phi \frac{(\rho C_p)_{CNT}}{(\rho C_p)_f}\right) \left[(f\theta' + D_c\theta - f'\theta) - \gamma(f^2\theta'' + ff'\theta') + \beta\sigma\lambda_1(1 + \gamma_T\theta)^n exp\left[-\frac{E}{1 + \gamma_T\theta}\right]\phi\right] = 0,$$
(9)

$$\phi_c'' + S_c f \phi_c' - \sigma S_c (1 + \gamma_T \theta)^m exp \left[\frac{-E}{1 + \gamma_T \theta} \right] \phi_c = 0.$$
⁽¹⁰⁾

The transformed boundary conditions of (5) are:

$$f(0) = 0, f'(0) = \epsilon + \gamma_1 [1 - \xi f''(0)]^{-1/2} f''(0), \ \phi_c(0) = 1, \ \theta(0) = 1, f'(\eta) = 1, \ \theta(\eta) = 0, \ \phi_c(\eta) = 0 \ at \ \eta \to \infty.$$
(11)

The different non-dimensional parameters seen in Equations (8)–(11) are explained as:

$$M = \frac{\sigma_{nf}B^{2}(x)}{c\rho_{f}}, Pr = \frac{v_{f}}{\alpha_{f}}, D_{c} = \frac{Q_{0}}{c(\rho c_{p})_{f}}, \gamma = \tau c,$$

$$\gamma_{T} = \frac{T_{w} - T_{\infty}}{T_{\infty}}, \epsilon = \frac{m}{c}, \xi = c\sqrt{\frac{c}{v_{f}}}b^{*}, E = \frac{E_{a}}{KT_{\infty}},$$

$$\sigma = \frac{K_{r}^{2}}{c}, S_{c} = \frac{v_{f}}{D_{A}}, \lambda_{1} = \beta \frac{C_{w} - C_{\infty}}{T_{w} - T_{\infty}}, \gamma_{1} = a\sqrt{\frac{c}{v_{f}}}.$$
(12)

The skin friction coefficient C_f and local Nusselt number Nu_x are explained as:

$$C_f = \frac{\tau_w}{\rho_f U^2}, \ \tau_w = (\frac{\partial u}{\partial y} \mu_{nf})_{y=0},$$
(13)

$$Nu_x = \frac{xq_w}{k_f(T_w - T_0)}, \quad q_w = (-\frac{\partial T}{\partial y}k_{nf})_{y=0}, \tag{14}$$

The dimensionless form of the surface drag and the heat transfer rate is given below:

$$R_e^{1/2}C_f = \left(\frac{1}{(1-\phi)^{2.5}}\right)f''(0), \ R_e^{-1/2}Nu_x = \left(-\frac{k_{nf}}{k_f}\right)\theta'(0) \ and \ R_e = \frac{cx^2}{v_f}.$$
 (15)

3. Numerical Solution

With the help of the bvp4c technique, which is a built-in function in MATLAB, the mathematical Equations (8)–(10) subject to condition (11) are solved numerically after setting $\eta = \eta_{max}$, where η_{max} is different for different combinations of the physical parameters. Alternatively, the $[0, \infty)$ domain is restricted to $[0, \eta_{max}]$. For the purpose of the solution, we first convert the system of equations into first-order ODEs. The following variables are used for the purposes of conversion.

$$y_7 = \phi', y_6 = \phi, y_5 = \theta', y_4 = \theta, y_3 = f'', y_2 = f', y_1 = f.$$
 (16)

Hence, the system of equations are transformed as:

$$y_{2} = y_{1}^{\prime}, \qquad 0 = y_{1}(0) \\ y_{3} = y_{2}^{\prime}, \qquad \varepsilon + \gamma_{1}[1 - \xi y_{3}(0)]^{-1/2}y_{3}(0) = y_{2}(0) \\ (1 - \phi)^{2.5}(1 - \phi + \phi \frac{\rho_{CNT}}{\rho_{f}})[y_{2}^{2} - y_{1}y_{3} - 1 - \\ \frac{\phi \frac{\rho_{CNT}\rho_{CNT}}{\rho_{f}\rho_{f}} + 1 - \phi}{(1 - \phi + \phi \frac{\rho_{CNT}}{\rho_{f}})}\lambda y_{4} - \frac{\left(1 + \frac{3\left(\frac{\sigma_{5}}{c_{f}} - 1\right)\phi}{\left(1 - \phi + \phi \frac{\rho_{CNT}}{\rho_{f}}\right)}\right)M}{(1 - \phi + \phi \frac{\rho_{CNT}}{\rho_{f}})}(1 - y_{2})] = y_{3}^{\prime}, \qquad 1 = y_{2}(\eta) \\ y_{5} = y_{4}^{\prime}, \qquad 1 = y_{4}(0), \\ \frac{-k_{f}}{k_{nf}}\left(\frac{Pr(1 - \phi + \phi \frac{(\rho_{C}C_{p})_{CNT}}{(\rho - \varphi)_{f}})}{(1 - \phi + \phi \frac{(\rho_{C}C_{p})_{CNT}}{(\rho - \varphi)_{f}})}\right)[y_{1}y_{5} + D_{c}y_{4} - y_{2}y_{4} \\ - \gamma y_{1}y_{2}y_{5} + \beta\sigma\lambda_{1}(1 + \gamma_{T}y_{4})^{n}exp\left[\frac{-E}{1 + \gamma_{T}y_{4}}\right]y_{6}] = y_{5}^{\prime}, \qquad 0 = y_{4}(\eta) \\ y(7) = y_{6}^{\prime}, \qquad 1 = y_{6}(0) \end{cases}$$

$$(17)$$

Every numerical solution is obtained by putting $\epsilon = 10^{-5}$, where ϵ is defined as the tolerance.

4. Step-by-Step Graphical Detail of the Problem

4.1. Problem Formulation

The governing modeled PDEs are highly nonlinear in nature and derived from the law of conservation, Newton's second law of motion, the second law of thermodynamics, and Fick's second law of diffusion. Yamada and Ota's nanofluid has been employed in the case of SWCNT and MWCNT in order to check the behavior of nanoparticles on fluid flow. The momentum of fluid flow is scrutinized with the inclusion of MHD, stagnation point, and buoyancy effects. A heat transfer analysis has been carried out with the inclusion of heat generation, Cattaneo–Christov and activation energy effects, whereas mass transfer analysis is studied with the utilization of the activation energy phenomenon.

4.2. Modeling

The governing modeled PDEs are highly nonlinear in nature and embedded with various physical effects. The PDEs are renovated into ODEs with the utilization of similarity transformations in order to dimensionalize the PDEs. It is easy to understand the behavior of fluid in the case of dimensionless parameters such as the Prandtl number *Pr*, Schmidt number *Sc*, Nusselt number *Nu*, etc.

4.3. Numerical Process

The dimensionless system of equations can be handled numerically with the utilization of the Lobatto IIIA scheme incorporated with the MATLAB built-in bvp4c scheme. During this procedure, the nonlinear modeled PDEs with the inclusion of various effects in momentum, energy, and concentration equations are transformed into ODEs with the help of similarity variables. In the second step, these dimensionless ODEs are stepped down into first-order ODEs for the Lobatto IIIA scheme. The tolerance level for the case of the present problem was 10^{-6} , with an interval of computation of [0,4] instead of $[0,\infty]$. All the numerical results have been obtained by considering $\eta = 4$. The detailed procedure of the proposed numerical scheme is presented in the table mentioned below.

4.4. Numerical Results

The behavior of the obtained numerical outcomes was scrutinized in terms of its impact on velocity, temperature, and concentration fields. The physical quantities of interest, such as heat transfer, Nusselt number, and Sherwood number, were computed as a result of magnification in various dimensionless numbers obtained during the numerical simulation of the problem. The impact of the dimensionless parameters on the velocity, temperature, and concentration fields is portrayed in terms of figures and tables.

4.5. Analysis

The accuracy and convergence of the proposed numerical scheme have been checked with the comparison of obtained numerical results with the existing literature. In order to obtain the convergence criterion, the tolerance level for the case of the present problem was 10^{-6} , and the domain for the case of the numerical solution was taken to be $\eta = 4$ instead of $\eta = \infty$. The convergence criterion was achieved if the value of the obtained outcome was less than the tolerance level.

5. Results and Discussions

After employing the bvp4c model, we obtained the required results in the form of graphs and tables that highlight the impact of various parameters on the velocity, temperature, concentration, skin friction, and Nusselt number. The values of the dimensionless parameters used in this study are in the range of $0.1 \le K \le 1$; for the magnetic number, the range is $0.1 \le M \le 2$, while the range for the shear rate is $0.1 \le \xi \le 0.8$. The volume fraction of nanoparticles is in the range of $0.01 \le \phi \le 0.06$, the Schmidt number is in the range of $0.5 \le S_c \le 1.5$, the Prandtl number has a value in $3 \le Pr \le 9$, the velocity ratio parameter is in the range of $0.1 \le \epsilon \le 0.5$, the velocity slip lies in $0.1 \le \gamma_1 \le 0.5$, the chemical reaction effect is in the range of $0.1 \le \beta \le 0.5$, the activation energy lies in $0.1 \le E \le 1$, the power law index is in the range of $0.1 \le m \le 0.5$, and the fitted rate constant is in the range of $0.1 \le n \le 0.5$.

Figures 2 and 3 show the impact of the solid volume fraction of CNTs on the thermal situation and axial velocity. For higher ϕ , the fluid stream speed decreases, while temperature increases because of the direct relationship between the concentration of nanoparticles and their thermal conductivity. Higher values of the parameter ϕ have a favorable influence on a system having higher thermal conductivity, resulting in an improved temperature profile. Figure 4 shows the influence of a velocity ratio parameter ϵ on the fluid speed. The velocity profile improves as a result of the direct impact of ϵ based on the stream flow rate. Figure 5 shows the effect of a slip velocity parameter γ_1 on $f'(\eta)$, indicating the positive influence of γ_1 on the stream velocity of the fluid. As the slip effects on a wall become more significant, there is a small amount of friction and hence small resistance to fluid motion. Figure 6 shows an increasing behavior in the velocity field against increasing magnetic parameters. Usually, the magnetic field acts as an opposing agent and resists the fluid motion due to the presence of external Lorentz forces, but here, due to the employed slip mechanism, the behavior reverses, and an inclination in fluid velocity is observed.



Figure 2. Problem formulation of the proposed model.



Figure 3. Modelling of the proposed modeled PDEs and their conversion into ODEs.





Figure 4. Conversion of PDEs into first-order ODEs and Lobatto111a scheme.



Figure 5. Impact of obtained numerical results on velocity, temperature and concentration fields.



Figure 6. Analysis of obtained results.

Figure 7 shows the thermal behavior caused by heat generation through D_c . The heat transfer surrounded by the adjoining fluid layers and surface improves as D_c increases. Higher parameters ultimately generate more heat internally, which causes an increase in the temperature of the nanofluid. Figure 8 shows the effect of the Prandtl number P_r on the temperature profile. The temperature is found to be decreased for expanding P_r . The Prandtl number is the quotient of momentum to thermal diffusivity, and it is used to measure the heat transfer within the solid surface and moving liquid. As the Prandtl number rises, the thermal diffusivity becomes weaker as the fluid temperature decreases. The thermal relaxation parameter γ has an effect on temperature distribution, as shown in Figure 9. For greater values of γ , the temperature, as well as the thickness of the boundary layer, is found to decrease. Figure 10 depicts the effect of the shear rate ξ on a velocity. A high shear rate indicates a lower viscosity, which increases the fluid velocity. Because of the inverse relationship between the mass diffusivity and Schmidt number (S_c), Figure 11 shows an increasing trend in the nanoparticle concentration for increasing values of S_c .

As seen in Figure 12, the value of β , which represents the strength of the chemical reaction, increases as the concentration field $\phi_c(\eta)$ decreases. The chemical reaction reduces the movement of the mass of the fluid. Physically, this is accurate since a chemical reaction is called an exothermic reaction when energy is released into the environment, and an endothermic reaction is when energy is taken from the environment. Figure 13 shows how the concentration profile improves as the activation energy parameter increases. The species *B*, which contains nanoparticles embedded in it, is amplified by the chemical reaction factor (λ_1) . Therefore, the manufacturing of nanoparticles increases. This explains why the system $\phi_c(\eta)$ is increased, as shown in Figure 14. The concentration profile decreases as the rate constant increases, as shown in Figure 15. This is owing to the fact that as σ increases, so does the destructive intensity of chemical reactions. As can be seen in Figure 16, the concentration profile declines as *m* is magnified.

Figures 17–19 show the velocity and thermal behavior caused by exothermic/ endothermic parameters through β . Exothermic reactions are when energy is released due to the interference of two chemical species, while in endothermic reactions, energy is absorbed. If the ratio of energy absorption versus energy release is the same, then the state of this chemical reaction is called isothermic because, in it, the overall energy is balanced. Heat transfer surrounded by the adjoining fluid layers and surface improves as β increases, leading to a velocity profile $f'(\eta)$ that rises. The effect of a velocity ratio parameter ϵ on the skin friction coefficient $C_f R_e^{1/2}$ is seen in Figure 20. A decreasing behavior in skin friction when increasing the values of ϵ increases and the free stream velocity overpowers the extending velocity, generating an enlarged motion about the stagnation point, lowering the drag force on a surface and causing $C_f R_e^{1/2}$ to drop.

The effect of the thermal relaxing time γ and velocity ratio parameter ϵ on the Nusselt number $\theta'(0)$ is shown in Figure 21. $\theta'(0)$ becomes higher for escalating γ . With increasing γ , the time it would take to transport heat between neighboring particles increases, resulting

in a decrement in heat transfer characteristics. On the other hand, an opposing relationship is noted for ϵ , which improves the rate of heat transfer characteristics by increasing the fluid speed. The idea behind the plotting of the Figures 22–26 is inspired from the following references [13,15,16].



Figure 7. Influence of ϕ on temperature pattern.



Figure 8. Influence of ϕ on velocity behavior.



Figure 9. Influence of *c* on velocity profile.



Figure 10. Impact of γ_1 on $f'(\eta)$.



Figure 11. Consequences of *M* on velocity pattern.



Figure 12. Consequences of D_c on temperature pattern.



Figure 13. Consequences of *Pr* on temperature behavior.



Figure 14. Consequences of γ on temperature pattern.



Figure 15. Consequences of ξ on velocity profile.



Figure 16. Consequences of S_c on concentration pattern.



Figure 17. Consequences of β on concentration behavior.



Figure 18. Consequences of *E* on concentration behavior.



Figure 19. Consequences of λ_1 on concentration behavior.



Figure 20. Consequences of σ on concentration behavior.



Figure 21. Consequences of *m* on concentration behavior.



Figure 22. Consequences of β on velocity portfolio.



Figure 23. Consequences of β on temperature portfolio.



Figure 24. Consequences of β on temperature portfolio.



Figure 25. Consequences of λ on skin friction.



Figure 26. Consequences of γ on temperature gradient.

The findings from bvp4c MATLAB software and the earlier work of Ramzan et al. [7] for increasing ϕ values exhibit great consistency, as shown in Table 2. From comparison analysis, it is quite clear that the obtained results are quite reliable.

Table 2. The work of Ramzan et al. [7]'s limited case is compared with statistical data on surface drag force as well as local Nusselt number versus Prandtl number.

	Ramzan et a	al. [7] <i>f''</i> (0)	Ramzan et a	l. [7] $-\theta'(0)$	Present $f''(0)$	Results	Present $-\theta'(0)$	Results
φ	SWCNT	MWCNT	SWCNT	MWCNT	SWCNT	MWCNT	SWCNT	MWCNT
0.01	0.338910	0.337270	1.105710	1.079040	0.338995	0.337276	1.105710	1.079043
0.1	0.408120	0.390070	4.806290	4.277160	0.408107	0.390084	4.806290	4.277160
0.2	0.504530	0.464660	12.30352	10.56796	0.504522	0.464669	12.30358	10.56796

Table 3 displays a comparison of numerically achieved outcomes with Othman et al. [28] and Wang [29] for diverse values of ϵ by keeping other parameters $M = \lambda = \gamma_1 = \xi = 0$. From the comparison analysis, it is quite evident the proposed numerical is quite trustworthy, and the obtained outcomes are quite accurate.

$R_e^{1/2}C_f$					
	Parameters	C	Comparison Analysis		
φ	ϵ	Othman et al. [28]	Wang [29]	Current	
0	2	-1.887306668	-1.88731	-1.88795	
0	1	0	0	0	
0	0.5	0.71329495	0.7133	0.7136	
0	0	1.232587647	1.232588	1.232600	
0	-0.5	1.495669739	1.49567	1.49590	
0	-1	1.328816861	1.32882	1.32900	

Table 3. Comparison of current numerical outcomes with Othman et al. [28] and Wang [29].

The effects of the volume fraction of the nano-size particle ϕ , non-dimensional velocity profile parameter ϵ , slip factor γ_1 , Schmidt number S_c , exothermic/endothermic parameter β , activation energy E, dimensionless chemical reaction rate constant λ_1 and σ , unitless rate constant m and n, as well as λ , are statistically shown in Table 4, which refers to $C_f Re^{1/2}$. The pattern shows increasing drag force corresponding to λ , E, S_c and ϕ , but $C_f Re^{1/2}$ decreases as the influence of m, n, γ_1 , σ , and ϵ increases.

Table 4. Rheological numerics of $-(1 + \beta)f''(0)$ and $-\theta'(0)$.

										$R_{e}^{1/2}$	$^{2}C_{f}$
e	γ1	φ ₂	λ	S _c	β	Ε	т	σ	п	SWCNT	MWCNT
0.1	0.1	0.01	0.1	0.5	0.5	1	0.5	0.1	0.1	1.118505	1.113907
0.3										0.909755	0.906056
0.5										0.678612	0.675895
0.2	0.1									1.178579	1.175287
	0.2									1.037153	1.034589
	0.3									0.924627	0.922584
	0.5	0.01								0.719589	0.718489
		0.03								0.753620	0.750208
		0.05								0.790372	0.784373
		0.01	0.2							0.709207	0.707394
			0.3							0.721306	0.719536
			0.4							0.733302	0.731576
			0.1	0.1						0.796844	0.793677
				0.3						0.908853	0.905215
				0.5						1.015271	1.011183
				0.5	0.1					1.045206	1.044045
					0.5					0.933344	0.921626
					0.5					0.815149	0.805263
					0.9	0.1				0.631555	0.618866
						0.5				0.755968	0.743733
						1				0.875441	0.863706
						1	0.2			0.835110	0.825900
							0.3			0.745517	0.737508
							0.4			0.655203	0.648064
							0.1	0.1		0.559715	0.552366
								0.5		0.465787	0.459695
								0.9		0.364019	0.365172
								0.1	0.2	0.745179	0.737164
									0.3	0.654127	0.647323
									0.4	0.555421	0.5558216

6. Conclusions

The bvp4c MATLAB software was used to examine the buoyant flow of a nanofluid containing carbon nanotubes, including homogeneous and heterogeneous reactions as well

as heat absorption/generation. The fluid is in a stagnation point flow past a porous shrinking/expanding plane, and the Thompson and Torian slip situations have also been taken into consideration at the boundary. Through naturally occurring factors, the fluid streaming speed, thermodynamic conditions, CNT nano-size particle density, heat transfer rates, and surface drag were investigated. The main observations are summarised as follows:

- Larger magnetic parameters, slip parameters, and velocity ratio factors all cause fluid flow to speed up, but the solid volume fraction causes it to slow down.
- As with the measurements of the heat generation and solid volume ratio, the system is observed to gradually cool down.
- When increasing the slip parameters and velocity ratio, fluid tends to flow smoothly, whereas for the solid volume fractions, surface roughness increased.
- The concentration profile decreases for the larger values of activation energy and exothermic/endothermic parameters.
- The process of heat transmission inside the system was influenced in opposing ways by the velocity ratio parameter as well as the thermal expansion parameter.

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Nomenclature

Symbols

и, v	Velocity component along the x and y directions
Q_0	Volumetric rate of a heat source
Pr	Prandtl number
$U_{\infty}(x)$	Free-stream velocity of the fluid
S _c	Schmidt number
C_f	Surface drag force
N _u	Local heat transfer
f'	Dimensionless stream velocity
Ε	Activation energy
D_c	Dimensionless heat generation parameter
m, n	Unitless rate constants
Greek Symbols	
$ ho_{nf}$	Density of nanofluid
ρ_f	Density of fluid
γ^*	Navier slip length density
ϵ	Velocity ratio parameter
μ_{nf}	Dynamic viscosity shear stress
μ_f	Dynamic viscosity shear stress
$ au_w$	Dynamic viscosity shear stress
α_{nf}	Thermal diffusivity of nanofluid
2	•

τ	Ratio of specific heats
ξ^*	Reciprocal of some critical shear rate
ξ	Critical shear rate
$(\rho C_p)_{nf}$	Heat capacity of nanofluid
β_f, β_s	Coefficient of thermal expansion
$(\rho C_p)_f$	Heat capacity of fluid
γ_1	Non-dimensional slip velocity parameter
σ_{nf}	Electric conductivity of fluid
σ_f	Electric conductivity of fluid
σ_f	Electric conductivity of nanofluid
$\hat{\beta}_{CNT}$	Coefficient of thermal expansion of carbon nanotubes
ϕ	Nanofluid volume fraction
γ	Dimensionless thermal relaxation time
β	Exothermic/endothermic parameter
σ, λ_1	Dimensionless chemical reaction rate
k_{nf}	Thermal conductivity of nanofluid
k _f	Thermal conductivity of fluid
v_{nf}	Kinematic viscosity of nanofluid
k _{CNT}	Thermal conductivity of carbon nanotubes
ρ_{CNT}	Density of carbon nanotubes
$(\rho C_p)_{CNT}$	Heat capacity of carbon nanotubes
$B^2(x)$	Magnetic field strength

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