



Analysis of Unsteady Flow and Heat Transfer of Nanofluid Using Blasius–Rayleigh–Stokes Variable

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Received: 11 February 2019; Accepted: 16 March 2019; Published: 25 March 2019



MDF

Abstract: This article investigates the unsteady flow and heat transfer analyses of a viscous-based nanofluid over a moving surface emerging from a moving slot. This new form of boundary layer flow resembles with the boundary layer flow over a stretching/shrinking surface depending on the motion of the moving slot. The governing partial differential equations are transformed to correct similar form using the Blasius–Rayleigh–Stokes variable. The transformed equations are solved numerically. Existence of dual solutions is observed for a certain range of moving slot parameter. The range of dual solution is strongly influenced by Brownian and thermophoretic diffusion of nanoparticles.

Keywords: unsteady flow and heat transfer; nanofluid; Blasius–Rayleigh–Stokes variable; dual solutions; numerical solution; correlation expressions

1. Introduction

The mechanism of drag and heat loss reduction [1] has been the focus of intensive analysis due to its application in the prevention of loss of mechanical energy. Drag and heat loss reduction may create energy savings, processing time reduction, enhancement in thermal rating, and make equipment more durable. Several well-known methods have been proposed by researchers to reduce the drag and heat loss in physical systems out of them utilization of stretching/shrinking surfaces [2] and enhancing the thermal conductivity of the involved fluid are famous [3].

Nanofluids, an achievement of researchers and scientists of the developing world of nanotechnology, exploit the thermal conductivity of solids to enhance the thermal conductivity of a fluid by adding nano-sized solid particles. Materials commonly used for nanoparticles include oxides such as alumina, silica, titania and copper oxide, and metals such as copper and gold. Carbon nanotubes and diamond nanoparticles have also been used to realize nanofluids. Nanoparticles vary from 1 to 100 nm in diameter. Thermal conductivity can be increased up to two times by adding small amount of nanoparticles. Popular base fluids include water and organic fluids such as ethanol and ethylene glycol. The volumetric fraction of the nanoparticles is usually below 5%.

A wide range of nanofluids exist in nature, like blood, which is a complex biological compound, made up of different nanoparticles that perform various functions at molecular level. A number of natural processes occurring in atmosphere and biosphere have wide variety of composition of different fluids and nanoparticles. Manufacturing and industrial waste materials are also composed of nanoscale particles and fluids. Various self-assembly processes for nanostructures generate from the addition of nanoparticles in base fluid. Considering the wide-ranging uses of nanofluid in industry and science, and the model of nanofluid presented by Buongiorno [4], many experimentalists and researchers have showed great interest in the study of nanofluids in the last few years [5–12].

Keeping the fact in view that the unsteady flows are more generalized, and the applications of nanofluids and stretching surfaces in drag and heat loss reduction, this article analyzes the unsteady flow of nanofluid over a moving surface. The study of flow over a linearly stretching sheet was initiated by Crane [13]. He derived the analytical solution of two-dimensional momentum equations. This notable work of Crane [13] has been studied by many researchers in many directions. Some recent works on the topic of stretching/shrinking surfaces are References [14–18] and the references given therein.

In 1997, Todd [19] introduced a new family of unsteady boundary layer flow over a moving surface emerging from a moving slot. He proposed a new set of transformations containing the Blasius–Rayleigh–Stoke variable to write the governing unsteady partial differential equations in similar form. Fang et al. [20] conducted the heat-transfer analysis for this boundary layer flow. In this article, we carry out the numerical analysis of unsteady flow of nanofluid past a movable surface emerging from a moving slot by converting the governing coupled unsteady partial differential equations into similar form using the transformation involving the Blasius–Rayleigh–Stoke variable. The results are presented graphically and the effects of nanoparticles on skin friction, Nusselt number and Sherwood number are discussed in detail. Dual solutions are observed for a specific range of moving slot parameter and are found to be altered due to the presence of nanoparticles. Furthermore, the numerical data is used to write the correlation expressions for certain important flow quantities by performing linear regression. Correlation expressions enable the readers to obtain the values of numerical results for different values of involved parameters from analytical expressions.

2. Mathematical Formulation

Consider the unsteady two-dimensional flow and heat transfer of an incompressible viscous-based nanofluid over a heated moving semi-infinite plate. The surface is emerging out along the *x*-axis from a moving slot (see Figure 1 for geometry of the problem). At time t = 0, the fluid is at rest. The governing boundary layer [21] equations are given as:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0 \tag{1}$$

$$\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} = v \frac{\partial^2 U}{\partial Y^2},$$
(2)

$$\frac{\partial T}{\partial t} + U \frac{\partial T}{\partial X} + V \frac{\partial T}{\partial Y} = \sigma \frac{\partial^2 T}{\partial Y^2} + \varepsilon \left(D_B \frac{\partial T}{\partial Y} \frac{\partial C}{\partial Y} + \frac{D_T}{T_{\infty}} \left(\frac{\partial T}{\partial Y} \right)^2 \right), \tag{3}$$

$$\frac{\partial C}{\partial t} + U \frac{\partial C}{\partial X} + V \frac{\partial C}{\partial Y} = D_B \frac{\partial^2 C}{\partial Y^2} + \frac{D_T}{T_{\infty}} \frac{\partial^2 T}{\partial Y^2},$$
(4)

where *U* and *V* are the velocity components in *X* and *Y* directions. *T* is the fluid temperature, *C* is the nanoparticles volume fraction, *v* is the kinematic viscosity, σ is the thermal diffusivity of the fluid, ε is the ratio of heat capacities of the nanoparticles $(\rho c)_p$ and base fluid $(\rho c)_f$, D_B and D_T are the Brownian and thermophoretic diffusion coefficients respectively. For water nanofluids at room temperature with nanoparticles of 1–100 nm diameters, the Brownian diffusion coefficient ranges from 4×10^{-10} to 4×10^{-12} m²/s. For alumina/water and copper/water $(\rho c)_p$ is 3.1 and 3.4 MJ/m³ respectively. The thermophoretic diffusion is equal to 6×10^{-5} for aluminum/water nanofluid and 6×10^{-6} for copper/water nanofluid.



Figure 1. Systematic diagram of the problem. δ , δ_c , δ_T represent the thicknesses of momentum, thermal and nanoparticles concentration boundary layers respectively.

The corresponding boundary conditions are:

$$U(X, Y, t) = 0, V(X, Y, t) = 0, T(X, Y, t) = 0, C(X, Y, t) = 0 \text{ at } t = 0,$$

$$U(X, Y, t) = U_W, V(X, Y, t) = 0, T(X, Y, t) = T_W, C(X, Y, t) = C_W \text{ at } Y = 0,$$

$$U(X, Y, t) \to 0, T(X, Y, t) \to T_{\infty}, C(X, Y, t) \to C_{\infty} \text{ as } Y \to \infty.$$
(5)

Since the unsteady flow is a generalized case of steady flow, Todd [19] generalized the Blasius and Rayleigh–Stokes variables to get similar equations for the boundary layer flow of viscous fluid over a moving surface, termed as the Blasius–Rayleigh–Stokes variable:

$$\eta = Y / \sqrt{\cos(\alpha)\nu t + \sin(\alpha)(\nu X / U_W)}.$$
(6)

This variable depicts that the slot at Y = 0 is moving with a constant speed $-U_w \cot \alpha$. To obtain similarity solutions for the system of Equations (1)–(5), we introduce the following similarity variables

$$\psi(x, y, t) = U_W \sqrt{\cos(\alpha)\nu t + \sin(\alpha)(\nu x/U_W)} f(\eta),$$

$$\theta(\eta) = \frac{T - T_{\infty}}{T_W - T_{\infty}}, \quad \phi(\eta) = \frac{C - C_{\infty}}{C_W - C_{\infty}},$$
(7)

in the governing equations to get the following ordinary differential equations:

$$f''' + \frac{1}{2}(\cos \alpha)\eta f'' + \frac{1}{2}(\sin \alpha)ff'' = 0,$$
(8)

$$\theta'' + \frac{\Pr}{2}((\cos\alpha)\eta + (\sin\alpha)f)\theta' + N_b\theta'\phi' + N_t{\theta'}^2 = 0,$$
(9)

$$\phi'' + \frac{Le}{2}((\cos\alpha)\eta + (\sin\alpha)f)\phi' + (\frac{N_t}{N_b})\theta'' = 0,$$
(10)

subject to boundary conditions:

$$f(\eta) = 0, \ f'(\eta) = 1, \ \theta(\eta) = 1, \ \phi(\eta) = 1 \text{ at } \eta = 0,$$

$$f'(\eta) \to 0, \ \theta(\eta) \to 0, \ \phi(\eta) \to 0 \text{ as } \eta \to \infty,$$
(11)

where prime represents the differentiation with respect to variable η . Pr is Prandtl number, N_t is thermophoresis diffusion parameter, N_b is Brownian diffusion parameter and *Le* is Lewis number given by the following expressions:

$$\Pr = \frac{\nu}{\sigma}, \ N_b = \frac{\varepsilon D_B(C_W - C_\infty)}{\sigma}, \ N_t = \frac{\varepsilon D_T(T_W - T_\infty)}{T_W \sigma}, \ Le = \frac{\nu}{D_B}.$$
 (12)

The range of the parameters of interest, namely thermophoresis diffusion parameter and Brownian diffusion parameter is given as: $N_b \in (0.0, 0.5)$ and $N_t \in [0.0, 0.5)$.

3. Results and Discussions

In this special case of unsteady flow, the slot is moving with constant speed $-U_w \cot(\alpha)$. For $\alpha = \pi/2$, the surface velocity is zero as in the case of Sakiadis flow [22]. For $0 < \alpha < \pi/2$, the slot is moving with the constant speed $U_w \cot(\alpha)$ in the opposite direction of stretching surface and the situation is termed as leading-edge accretion. For $\alpha \in (\alpha_L, 0) \cup (\pi/2, \alpha_U)$, the direction of slot motion is same as stretching sheet and the situation is termed as leading-edge ablation. As $\alpha \to 0$, the speed of slot approaches infinity in opposite direction to the stretching surface, which correspond to the Rayleigh starting-plate problem. The analytical solution for this case has been obtained using the perturbation method (see Appendix A). Since the exact analytical solution of the system (8)–(11) is not available for general α , we adopt the numerical method for the solution. In Table 1, the comparison of numerical results of skin friction with results of Fang [20] is tabulated. In Table 2, the comparison of the analytical result for $\alpha = 0$ is given with the numerical solution. Tables 1 and 2 establish the reliability of our results.

α(°)	$-f^{''}(0)$ (Fang [17])	Present Study
90°	0.443748	0.443872
60°	0.576684	0.576685
	0.613527	0.613526
0°	0.564190	0.564189
-30°	0.416304	0.416303
-48° (upper solution)	0.239052	0.239055
-48° (lower solution)	0.00150569	0.00149961

Table 1. Comparison of Fang [20] and Present study for values of different moving slot parameters.

Table 2.	Comparison	of analytical and	l numerical solut	ions for Nusselt a	nd Sherwood numbe	er for $\alpha = 0$.
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Parameters Values	$-oldsymbol{ heta}'(0)$ (Analytical)	$-oldsymbol{ heta}'(0)$ (Numerical)	$-oldsymbol{\phi}'(0)$ (Analytical)	$- oldsymbol{\phi}'(0)$ (Numerical)
$Pr = 1, Le = 0.5, N_b = 0.01, N_t = 0.01$	0.5541896	0.5603877	0.0884477	0.0718526
$Pr = 1, Le = 0.5, N_b = 0.05, N_t = 0.0$	0.5541896	0.5532004	0.39894228	0.39894228
$Pr = 1, Le = 1.0, N_b = 0.05, N_t = 0.0$	0.55418958	0.5502023	0.56418958	0.56418958
$Pr = 1, Le = 2.0, N_b = 0.02, N_t = 0.01$	0.55418958	0.5551755	0.67603707	0.68467843

The numerical solution domain of α , ($\alpha_L < \alpha < \alpha_U$), for the skin friction and Nusselt number mentioned by Fang [20] also hold for Sherwood number. In this study, we focus on the effects of nanoparticles on the heat transfer and behavior of nanoparticles concentration for the surface accretion and ablation.

Figure 2 demonstrates numerical solutions of velocity profile for various values of slot moving constant α ranging between $-\pi/4 < \alpha < \alpha_U$. In Figure 3 the dual solution for the velocity profile is plotted for $\alpha = -48^\circ$. The thickness of boundary layer is much greater for lower solution branch as compared to upper solution branch.



Figure 2. Velocity profiles for varying slot moving parameter α .



Figure 3. Profiles of velocity for different branches at $\alpha = -48^{\circ}$.

Figure 4 represents the dual solution for a fixed value of moving slot parameter $\alpha = -48^{\circ}$, with two distinct values of Prandtl number. For the above-mentioned values of parameters, both solutions show maximum temperature gradient which can be viewed in the region away from the wall. The change of heat transfer at the wall is less for lower solution as compared to the upper solution. The thermal layer thickness is greater for lower solution as compare to upper solution branch.



Figure 4. Temperature and its flux profiles for several branches at $\alpha = -48^{\circ}$ for varying *Pr* with $N_b = 0.01$ and $N_t = 0.001$.

Figures 5 and 6 illustrate the numerical solution domain of reduced Nusselt number as a function of α for different values of Brownian and thermophoretic diffusion parameters, N_b and N_t respectively. For Nusselt number, the correlation expression in the form of N_b and N_t has also been written by applying the linear regression on the set of 2401 numerical values. The values of coefficients and constant of the correlation expression in the form

$$-\theta'(0) = C + C_B N_b + C_T N_t$$

for $N_b \in (0.01, 0.5)$ and $N_t \in (0.0, 0.5)$ is given in Table 3 with maximum percentage error for different Prandtl number and moving slot parameter.



Figure 5. Effects of slot moving parameter α on reduced Nusselt number for varying N_b with Pr = Le = 1.0 and $N_t = 0.1$.



Figure 6. Effects of slot moving parameter α on reduced Nusselt number for varying N_t with Pr = Le = 1.0 and $N_b = 0.1$.

Table 3. Correlation expression for reduced Nusselt number and maximum percentage error defined for varying Prandtl number and moving slot parameter considering values of Brownian and thermophoresis diffusion parameters in the interval (0.01, 0.5).

Pr	Le	α	С	C_B	C_T	Max. % Error	Solution Curve
0.5	1.5	30	0413	-0.226	-0.132	2.60%	-
1.0	1.0	30	0.605	-0.261	-0.168	1.760%	-
1.0	1.0	0.0	0.601	-0.253	-0.161	2.650%	-
2.0	1.5	30	0.877	-0.305	-0.21	0.986%	-
1.0	1.0	-49	0.235	-0.101	-0.075	2.430%	Upper Solution
1.0	1.0	-49	0.004	-0.002	-0.002	7.970%	Lower Solution

It is observed that the Nusselt number decreases with an increase in parameters N_b and N_t , since higher temperatures correspond to higher Brownian and thermophoretic diffusion which resultantly reduces the surface heat flux. The same observation can be made from the correlation expressions since the coefficients of N_b and N_t are negative for all value of Pr and α . Furthermore, it is seen that dual solutions exist for a certain interval of slot moving parameter α and that interval can be viewed in Figures 5 and 6. The important observation is that the range of α reduces dramatically with an increase of N_t and the duality of solution vanishes for $N_t = 0.05$. For this reason, the correlation expression for $\alpha = -49^\circ$ is derived for $N_t \in (0.0, 0.01)$. The variation of N_b has no effect on the duality of the solution.

For a fixed value of moving slot parameter $\alpha = -49^{\circ}$, Figures 7 and 8 show the dual solution for the variation of N_b and N_t . The thickness of concentration boundary layer is greater for the smaller solution branch. As the value of N_b increases, the concentration boundary layers become thinner for upper as well as for lower solution domains. The concentration thickness of boundary layer is less for the lower solution branch. As the value of N_t increases, the concentration boundary layers become thicker for upper and lower solution domains. In Figures 9–11, the effects of Lewis number, thermophoretic diffusion and Brownian diffusion on the nanoparticles concentration flux at the surface are plotted. The Sherwood number is plotted against the moving slot parameter α . Dual solution for Sherwood number is observed in the interval (-53° , -49.5°). Figure depicts that Sherwood number is growing function of α in the interval (-49.5° , 30°), and decreasing function in the interval (30° , α_U). As Le increases, i.e., the dominancy of viscous diffusion increases over the Brownian diffusion, the mass flux at the surface increases. Similar effects of Brownian diffusion and opposite effects of thermophoretic diffusion on Sherwood number are observed. In dual solution range, the effects of thermophoretic and Brownian diffusions on Sherwood number are found negligible.



Figure 7. Dual solutions of nanoparticles concentration profile for $\alpha = -49^{\circ}$ and varying N_b , with Pr = Le = 1.0, $N_t = 0.001$.



Figure 8. Dual solutions of nanoparticles concentration profile for $\alpha = -49^{\circ}$ and varying N_t , with Pr = Le = 1.0, $N_b = 0.05$.



Figure 9. Effects of slot moving parameter α on reduced Sherwood number for varying *Le* with Pr = 1.0, $N_b = 0.05$, $N_t = 0.001$.



Figure 10. Effects of slot moving parameter α on reduced Sherwood number for varying N_b with Pr = Le = 1.0, $N_t = 0.001$.



Figure 11. Effects of slot moving parameter α on reduced Sherwood number for varying N_t with Pr = Le = 1.0, $N_b = 0.05$.

4. Conclusions

In this work, the unsteady flow and heat transfer of a viscous-based nanofluid over a moving surface emerging from a moving slot has been considered. The effects of involved parameters on the temperature and concentration profiles are illustrated graphically. Furthermore, the variation of reduced Nusselt and Sherwood numbers with the involved parameters; namely Lewis number, Brownian motion parameter and thermophoretic diffusion parameter; are presented graphically.

The obtained results are concluded as follows:

- With the increase in the value of Brownian diffusion parameter *N*_b, the temperature enhances while the nanoparticles volume fraction decreases.
- By increasing the thermophoretic diffusion parameter *N*_t, both temperature and nanoparticles concentration are increased.
- Concentration of nanoparticles reduces with the enhancement of Lewis number Le.
- Dual solutions exist for both thermal and concentration boundary layers. The mass flux rate attains the maximum value of slot moving parameter *α*, as the Lewis number is increased.
- Heat flux at the surface $-\theta'(0)$ reduces with the increase of N_b and N_t in the upper solution branch. The reduced Sherwood number $-\phi'(0)$ is enhanced when N_b is increased, whereas it reduces with increasing N_t .

Author Contributions: Conceptualization and Supervision, A.A.; Methodology, S.M.; Writing—Original Draft Preparation, D.L., S.M. and A.A.; Writing—Review and Editing, U.F. and A.A.; Funding Acquisition, D.L. and U.F.

Funding: This research was funded by China Postdoctoral Science foundation (No. 189607).

Acknowledgments: Adeel Ahmad would like to acknowledge the support by the CIIT Research Grant Program of COMSATS University Islamabad, Pakistan (No. 16-68/CRGP/CIIT/ISB/17/71141).

Conflicts of Interest: The authors declare no conflict of interest.

Nomenclatures

U	Velocity component in X direction
V	Velocity component in Y direction
U_w	Plate velocity
ψ	Stream function
Т	Temperature
T_{∞}	Ambient temperature
T_W	Wall temperature
С	Nanoparticles concentration
C_{∞}	Ambient nanoparticles concentration
C_W	Wall nanoparticles concentration
η	Similarity variable
α	Moving slot parameter
D_B	Brownian diffusion coefficient
D_T	Thermophoretic diffusion coefficient
Le	Lewis number
N_b	Brownian diffusion parameter
N_t	Thermophoretic diffusion parameter
Pr	Prandtl number
φ	Nondimensional nanoparticles
	concentration
θ	Nondimensional temperature
ν	Kinematic viscosity
σ	Thermal diffusivity
ε	Ratio of heat capacities of the nanoparticles
$(\rho c)_f$	Heat capacity of fluid
$(\rho c)_p$	Heat capacity of nanoparticles

Appendix A

For $\alpha = 0$, the governing equations reduce to

$$f''' + \frac{1}{2}\eta f'' = 0,$$
 (A1)

$$\theta'' + \frac{\Pr}{2}\eta\theta' + N_b\theta'\phi' + N_t{\theta'}^2 = 0,$$
(A2)

$$\phi'' + \frac{Le}{2}\eta\phi' + \frac{N_t}{N_b}\theta'' = 0.$$
(A3)

We derive the analytical expressions for the skin friction, Nusselt number and Sherwood number subject to the boundary conditions in Equation (A1). The exact solution of Equation (A1) is:

$$f'(\eta) = 1 - erf\left(\frac{1}{2}\eta\right) \tag{A4}$$

It is noted that the magnitude of thermophoretic and Brownian diffusion parameters for nanoparticles is very small [1,9], therefore we consider N_b and N_t of $O(\varepsilon)$, $\varepsilon \to 0$. We expand θ and ϕ in small parameter ε and write

$$\begin{aligned} \theta &= \theta_o + \varepsilon \theta_1 + \dots \\ \phi &= \phi_o + \varepsilon \phi_1 + \dots \end{aligned}$$
 (A5)

By substituting the expressions in Equation (A5) in Equations (A2) and (A3), the leading order boundary value problem is given by

$$\theta_o'' + \frac{\Pr}{2}\eta\theta_o' = 0, \tag{A6}$$

$$\phi_{o}^{''} + \frac{Le}{2}\eta\phi_{o}^{'} + \frac{\tau}{\beta}\theta^{''} = 0, \tag{A7}$$

where β and τ are constants of O(1) such that $N_b = \beta \varepsilon$ and $N_t = \tau \varepsilon$. The solution of above boundary value problem can be written as

$$\theta'_{o}(y) = \frac{\sqrt{\Pr}}{\sqrt{\pi}} e^{-\frac{1}{4} \Pr \eta^{2}},$$

$$\phi'_{o}(y) = -\frac{\tau \Pr\left(\sqrt{\Pr}e^{-\frac{1}{4} \Pr \eta^{2}} - \sqrt{Le} \ e^{-\frac{1}{4} Le \eta^{2}}\right) + \beta(Le - \Pr)\sqrt{Le} \ e^{-\frac{1}{4} Le \eta^{2}}}{\sqrt{\pi}\beta(Le - \Pr)}.$$
(A8)

The first order system can be written as

$$\frac{\partial^2 \theta_1}{\partial y^2} + \frac{1}{2} \Pr \eta \frac{\partial \theta_1}{\partial y} + \beta \frac{\partial \theta_o}{\partial y} \frac{\partial \phi_o}{\partial y} + \tau \left(\frac{\partial \theta_o}{\partial y}\right)^2 = 0$$
(A9)

$$\frac{\partial^2 \phi_1}{\partial y^2} + \frac{1}{2} Le\eta \frac{\partial \phi_1}{\partial y} + \frac{\tau}{\beta} \frac{\partial^2 \theta_1}{\partial y^2} = 0$$
(A10)

with the boundary conditions

$$\begin{aligned} \theta_1 &= 0, \ \phi_1 = 0 \ \text{at} \ \eta = 0 \\ \theta_1 &= 0, \ \phi_1 = 0 \ \text{as} \ \eta \to \infty \end{aligned}$$
 (A11)

For the above boundary value problem, the exact solution is given by

$$\theta_{1}'(\eta) = e^{-\frac{1}{4}\Pr\eta^{2}} \left(1 - \frac{\sqrt{\Pr}}{\sqrt{\pi}} \beta \operatorname{erf}\left(\frac{1}{2}\sqrt{Le}\eta\right) - \frac{\sqrt{\Pr}}{\sqrt{\pi}} \frac{\tau}{Le - \Pr} \left(Le \operatorname{erf}\left(\frac{1}{2}\sqrt{\Pr}\eta\right) - \operatorname{Prerf}\left(\frac{1}{2}\sqrt{Le}\eta\right) \right) \right)$$
(A12)

$$\begin{split} \phi_{1}^{\prime}(\eta) &= \frac{\tau}{\beta\sqrt{\pi}(Le-\Pr)} e^{-\frac{1}{4}Le\eta^{2}} \left(\Pr\sqrt{\pi}e^{-\frac{1}{4}(\Pr-Le)\eta^{2}} + \frac{\tau\PrLe \operatorname{erf}(\frac{1}{2}\sqrt{2\Pr-Le}\eta)}{\sqrt{2\Pr-Le}} - \right. \\ \left. \sqrt{\Pr^{3}} \left(\frac{(Le-\Pr)\beta-\Pr\tau}{Le-\Pr} \right) \left(\operatorname{erf}\left(\frac{1}{2}\sqrt{Le}\eta\right) e^{-\frac{1}{4}(\Pr-Le)\eta^{2}} - \frac{\sqrt{Le}}{\sqrt{\Pr}} \operatorname{erf}\left(\frac{1}{2}\sqrt{\Pr\eta}\right) \right) + \left((Le-\Pr)\beta - \tau\Pr\right) \\ \left. \sqrt{Le} \operatorname{erf}\left(\frac{1}{2}\sqrt{\Pr\eta}\right) - \tau \frac{\sqrt{Le^{3}\Pr^{3}}}{Le-\Pr} \left(\sqrt{Le} \operatorname{erf}\left(\frac{1}{2}\sqrt{\Pr\eta}\right) e^{-\frac{1}{4}(\Pr-Le)\eta^{2}} - \sqrt{\Pr}\operatorname{erfi}\left(\frac{1}{2}\sqrt{Le}\eta\right) \right) \right), \end{split}$$
(A13)

where erf is the error function and erfi is the imaginary error function.

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