

Supplementary Material

Enhancing the Green Synthesis of Glycerol Carbonate: Carboxylation of Glycerol with CO₂ Catalyzed by Metal Nanoparticles Encapsulated in Cerium Metal–Organic Frameworks

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Chemicals

Ammonium Cerium(IV) nitrate ($\geq 99.5\%$), 1, 4-benzenedicarboxylic acid (BDC) (98 %), and sodium borohydride (98 %) were purchased from Sigma Aldrich, Poland. 1, 3, 5-benzenetricarboxylic acid (BTC) ($\geq 98\%$) were supplied by Chemat (Poland). Pyridine (99+ %), chlorotrimethylsilane (98 %) and Glycerol (99 %) were supplied by Thermo Scientific (Germany), polyethylenimine (PEI), $M_w \approx 600$ Da (Sigma Aldrich, Poland), and hydrogen tetrachloroaurate ($\geq 99.9\%$, Sigma Aldrich, Poland). 1, 8-diazabicyclo[5.4.0]undec-7-ene (98 %, Merk, Germany), 1, 1, 1, 3, 3, 3-Hexamethyldisilazane ($\geq 98\%$, ROTH). N-N-Dimethylformamide (99.8 %) and methanol (99.8 %) were supplied by POCH, Poland. Solvents were dried using activated molecular sieves before use and all other chemicals were used as supplied.

Crude GL was obtained from edible commercial rapeseed oil as follows: 250 mL of canola oil was pumped into the reaction using a peristaltic pump. 50 mL of 1M methanol solution of KOH was added using the same pump. The reactor was switched on to start the transesterification and stirred for 30 min. At the end of the transesterification, the resultant mixture was allowed to settle without agitation and two layers were obtained. The bottom layer (crude GL) was collected. It was dried over molecular sieves to ensure complete exclusion of any water content. Estimated quantification based on comparison with moles of GL per mL of $>99\%$ pure commercial GL found the crude GL fraction to be about 48-54% GL after simple drying.

Calculation of conversion, yield, TOF and TON

The calculations were performed using the following equations:

$$\text{Conversion } [\%] = \frac{(n_{GL(start)} - n_{GL(final)})}{n_{GL(start)}} \times 100\% \quad (\text{eq. S1})$$

$$\text{Yield } [\%] = \frac{n_{GLC(final)}}{n_{GL(start)}} \times 100\% \quad (\text{eq. S2})$$

where $n_{GL(start)}$ is starting amount of GL (in mmoles), $n_{GL(final)}$ – mmoles of GL found in post reaction mixture, $n_{GLC(final)}$ – mmoles of GLC found in post reaction mixture, $n_{GL(converted)}$ - mmoles of GL converted.

Taking into account very low conversion (14%, see Table 2, run 6) for the pristine MOF (without Au) observed after 25 h it can be concluded that there is very small (negligible) contribution of catalytic activity of the MOF without embedded Au, and Turnover Number (TON) and Turnover Frequency

(TOF) parameters were exclusively calculated based on moles of Au as an active component, and the amount of GL converted):

$$\mathbf{TON}_{GL} = \frac{n_{GL(\text{converted})}}{n_{Au}} = \frac{n_{GL(\text{start})} - n_{GL(\text{final})}}{n_{Au}} \quad (\text{eq. S3})$$

$$\mathbf{TOF}_{GL} [\text{h}^{-1}] = \frac{\mathbf{TON}_{GL}}{\text{reaction time (in hours)}} \quad (\text{eq. S4})$$

or basing on the produced GLC:

$$\mathbf{TON}_{GLC} = \frac{n_{GLC(\text{final})}}{n_{Au}} \quad (\text{eq. S5})$$

$$\mathbf{TOF}_{GLC} [\text{h}^{-1}] = \frac{\mathbf{TON}_{GLC}}{\text{reaction time (in hours)}} \quad (\text{eq. S6})$$

where n_{Au} is the estimated amount of Au (in mmoles) in 50 mg of the whole catalyst (Au + MOF). Amount of Au in the catalyst was determined using ICP-MS results, and mass of Au was 1.25 mg ($n_{Au} = 0.0064$ mmol).

Using eq. S3 and S4, with $n_{GL(\text{converted})} = 52\% \times 12.5$ mmol = 6.5 mmol and for reaction time 13 hours, **TON_{GL} is 6.5 mmol/0.0064 mmol = 1016, and $TOF_{GL} = 1016/13$ hours = 78 h^{-1} .**

The same calculations with eq. S5 and S6, with $n_{GLC(\text{final})} = 44\% \times 12.5$ mmol = 5.5 mmol gave **$TON_{GLC} = 5.5/0.0064 = 859$, and $TOF_{GLC} = 66$ hr^{-1} .**

Our parameters can be compared with the results described in the literature. For example, Kulal *et al.*¹ used Zn/CeO₂ catalyst (molar fraction $x_{Zn} = 0.105$), and TON and TOF values calculated from the results presented by these authors in Table S5, 0.99 mmol of catalyst caused 90.4% conversion of 10 mmol of GL during 1.8 hour (ie., 9 mmol of GL was converted), therefore, $TON_{GL} = 9\text{mmol}/0.99\text{mmol} \approx 9$, and $TOF = 9/5 = 1.8$ h^{-1} . TON and TOF values based on the results obtained by Liu *et al.*² for 1.72 g of CeO₂ catalyst (10mmol) and with $n_{GLC(\text{final})} = 7.9$ mmol (yield=78.9% after 5 hours) obtained $TON_{GLC} = 7.9\text{mmol}/10\text{mmol} = 0.79$, and $TOF_{GLC} = 0.79/5\text{h} = 0.16$ h^{-1} .

Table S1. ICP-MS results of the Au(H₂)@MOF1 catalyst

Catalyst	mg of Au/20 mg catalyst	mg of Ce /20 mg of catalyst
Fresh catalyst	0.501	10.768
Spent catalyst	0.344	8.805

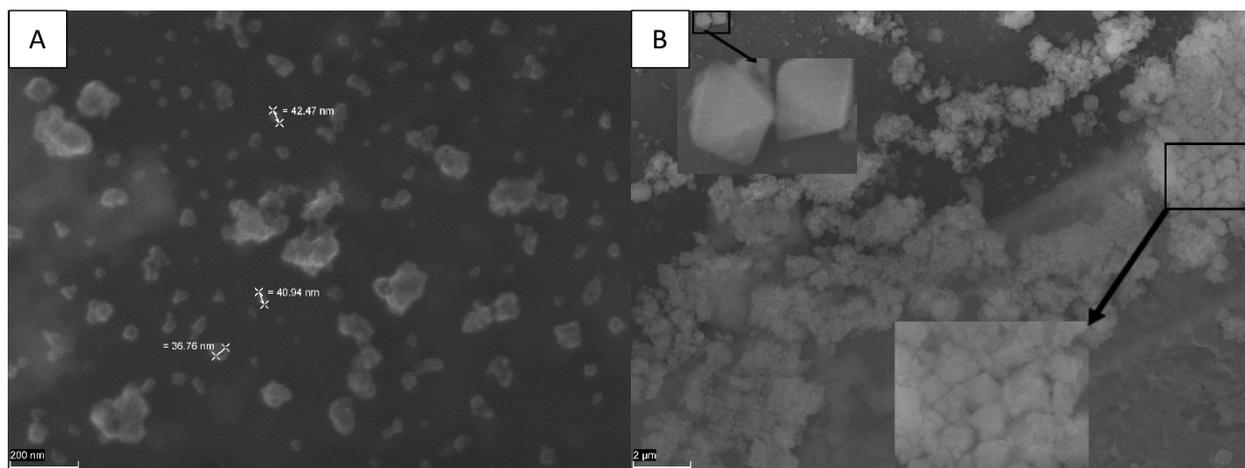


Figure S1. SEM images of the pure MOF showing. A) An area with many small MOF nanoparticles less than 100 nm. B) Large octahedral particles surrounded by aggregates (small particles).

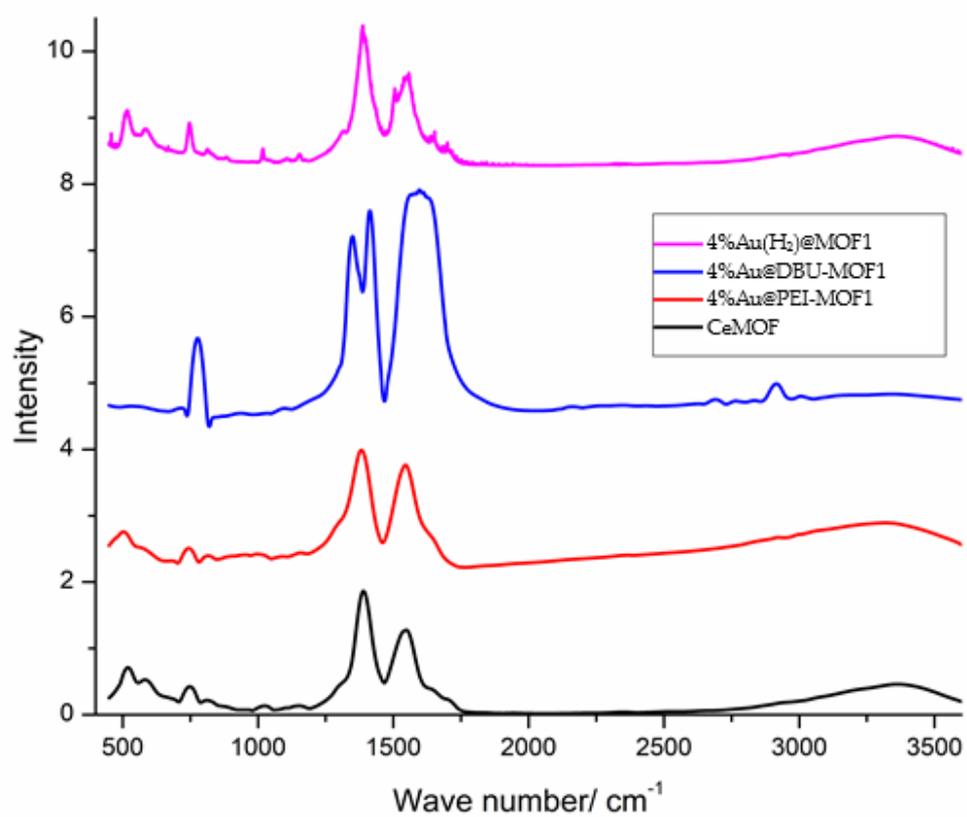


Figure S2. FTIR of the synthesized materials.

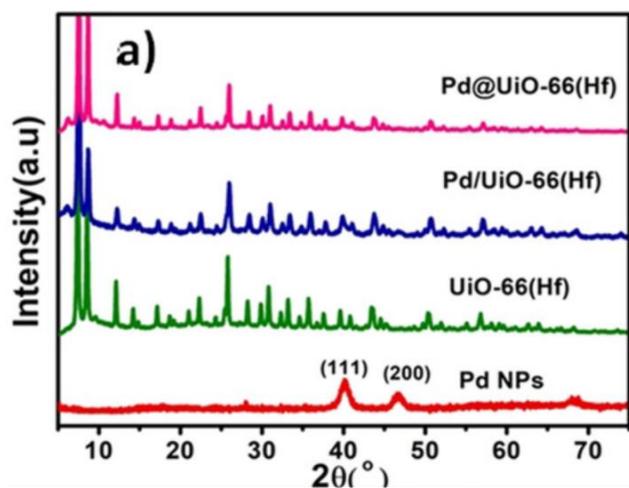


Figure S3A.
Literature XRD for UiO-66 (Hf) and Pd/UiO-66(Hf) Pd@UiO-66(Hf).³
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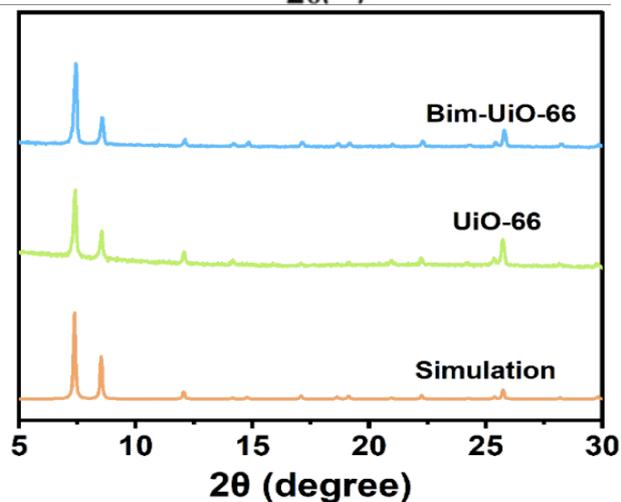


Figure S3B.
Literature XRD for UiO-66 (Zr).⁴
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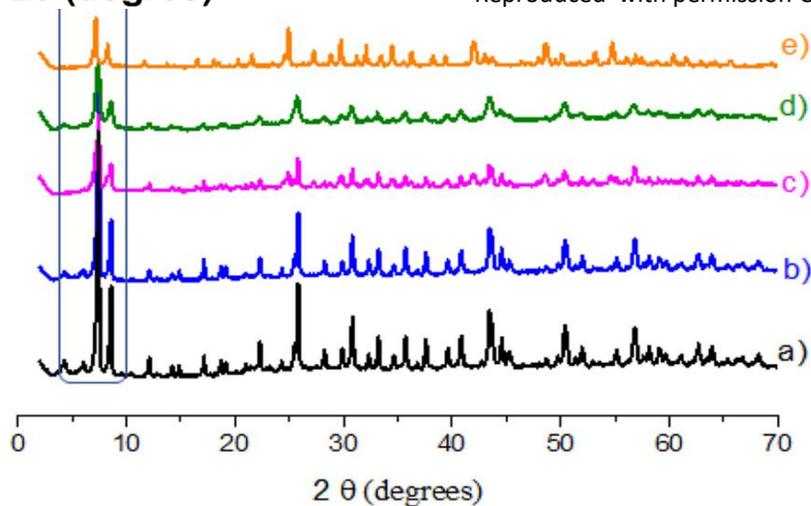


Figure S3C.
PXRD patterns of UiO-66-(Zr)-NH₂ (a), UiO-66(Zr)-NH₂-200@UiO-66(Ce) (b), UiO-66(Zr)-NH₂-25@UiO-66(Ce) (c), UiO-66(Ce)-200@UiO-66(Zr)-NH₂ (d), and UiO-66(Ce) (e). The inset shows a zoom-in view of the low-angle region.⁵Reproduced with permission. Copyrights ACS.

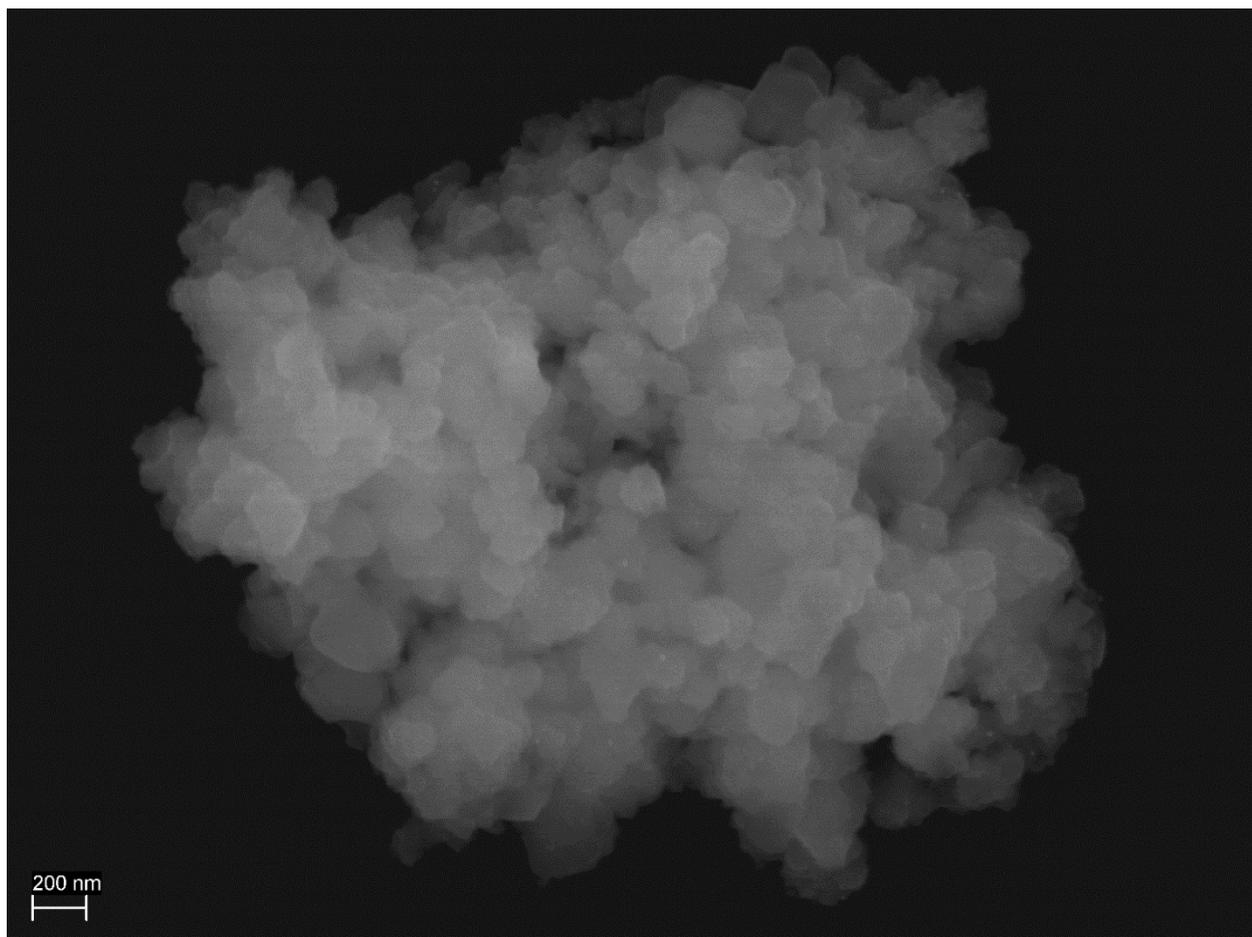


Figure S4. SEM image of 4%Au(H₂)@MOF1.

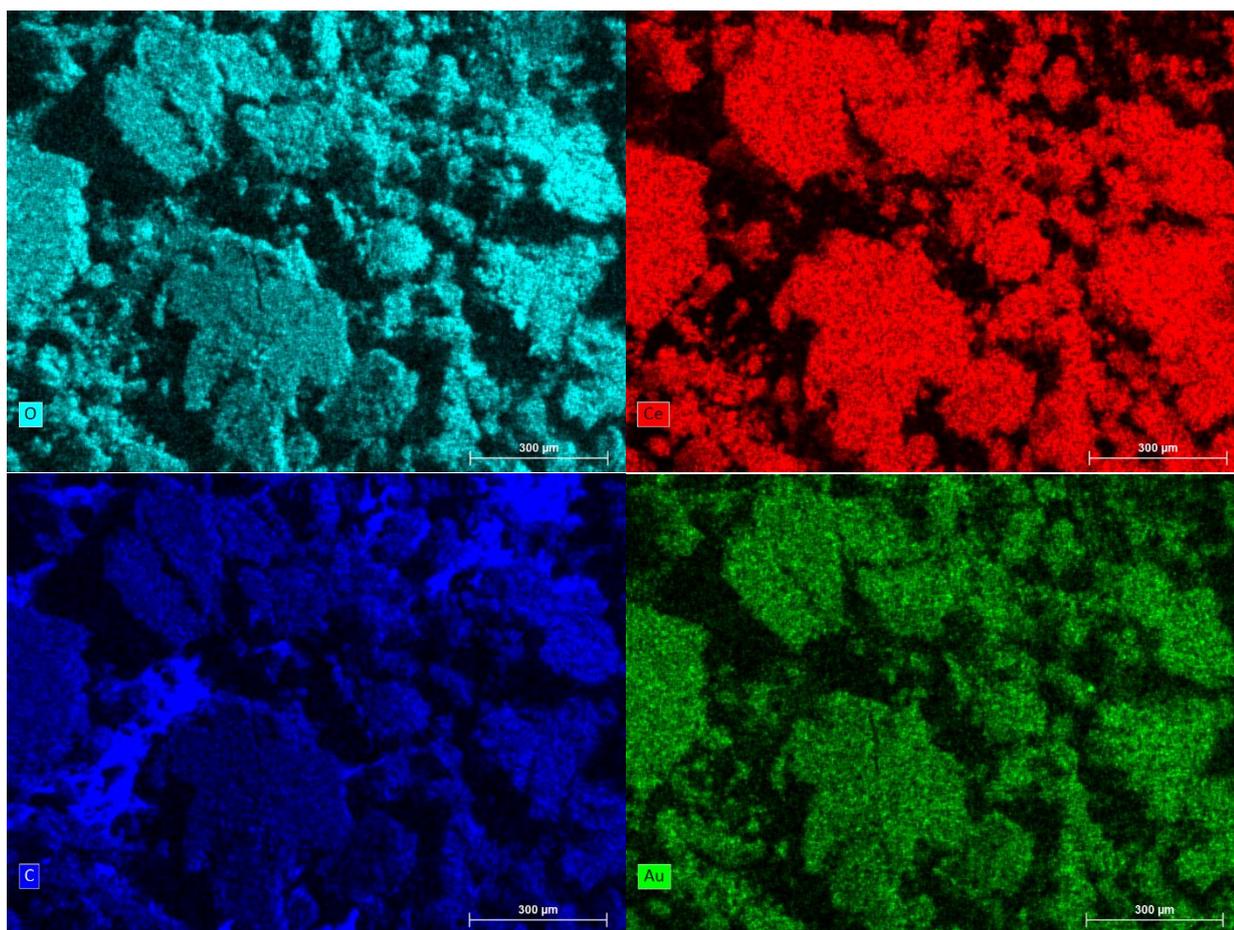


Figure S5. SEM EDS elemental mapping of 4%Au(H₂)@MOF1.

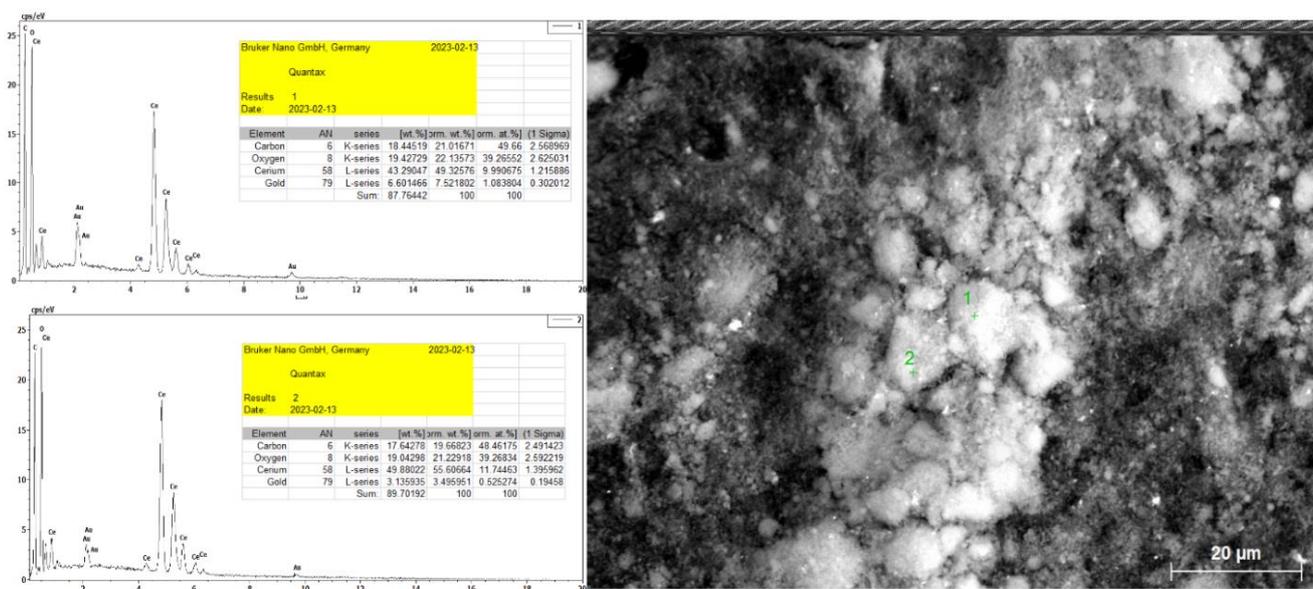


Figure S6. EDS elemental composition for 4%Au(H₂)@MOF1.

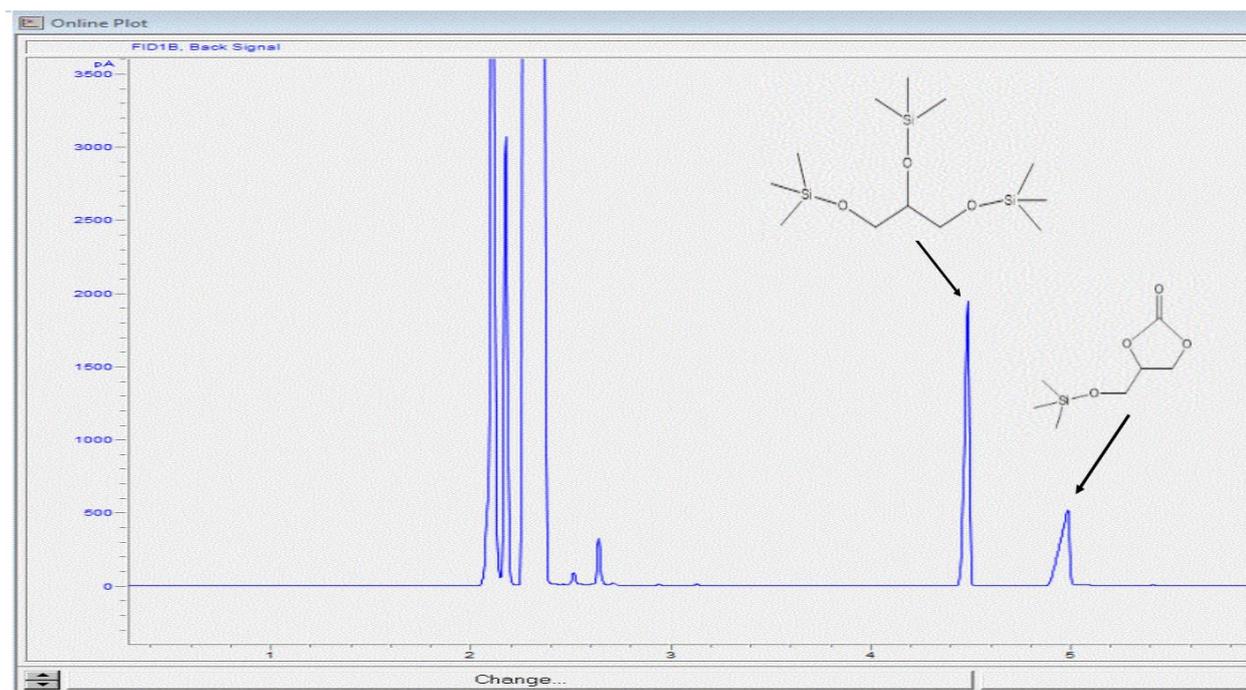


Figure S7. Chromatogram of silylated GL and GC. The peak of the internal standard (cumene) is at about 2.7 min.

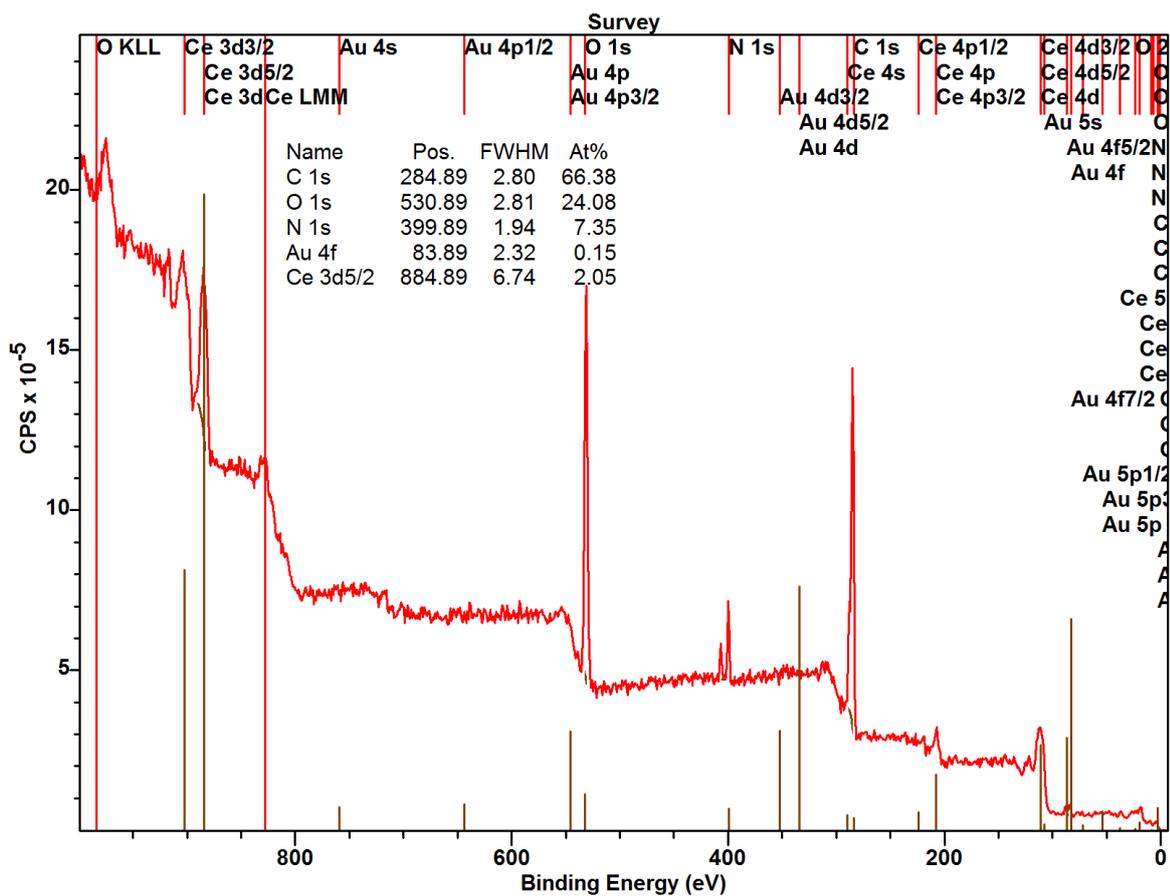


Figure S8. Survey XPS spectra of Au(H₂)@MOF1.

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