



Article Multilayer Graphene Oxide Supported ZIF-8 for Efficient Removal of Copper Ions

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Highlights:

- A multilayer graphene based adsorbent was prepared by a simple method;
- Adsorbents have high adsorption capacity and a high specific surface area;
- The multilayer structure of graphene layer provides a framework for ZIF, adding more adsorption sites.

Abstract: To address the performance deterioration of ZIF-8 for the adsorption of copper ions caused by powder volume pressure and particle aggregation, we employed multilayer graphene oxide (MGO) as a support to prepare composite adsorbents (MGO@ZIF-8) by using the in situ growth of ZIF-8 on MGO. Due to a good interfacial compatibility and affinity between ZIF-8 and graphene nanosheets, the MGO@ZIF-8 was successfully prepared. The optimal Cu²⁺ adsorption conditions of MGO@ZIF-8 were obtained through single factor experiments and orthogonal experiments. Surprisingly, the Cu²⁺ adsorption capacity was significantly improved by the integration of MGO and ZIF-8, and the maximum Cu²⁺ adsorption capacity of MGO@ZIF-8 reached 431.63 mg/g under the optimal adsorption conditions. Furthermore, the kinetic fitting and isotherm curve fitting confirmed that the adsorption law of Cu²⁺ by MGO@ZIF-8 was the pseudo-second-order kinetic model and the Langmuir isotherm model, which indicated that the process of Cu²⁺ adsorption was monolayer chemisorption. This work provides a new approach for designing and constructing ZIF-8 composites, and also offers an efficient means for the removal of heavy metals.

Keywords: multilayer graphene oxide; ZIF-8; in situ growth; heavy metal adsorption; adsorption kinetics

1. Introduction

In recent years, the development of modern industry has led to the increasingly serious pollution of heavy metal ions (such as chromium, lead, and copper), which has caused serious harm to human health and social development [1,2]. Some studies have noted that when the intake of copper exceeds standard levels, it will generate a burden to human organs, causing metabolic disorders and liver cirrhosis [3,4]. Therefore, how to effectively reduce and eliminate copper ion (Cu^{2+}) pollution has become an important social and economic issue [5,6].

Currently, chemical deposition, ion exchange, adsorption and membrane separation have been used to dislodge Cu^{2+} from wastewater [7,8]. Among them, adsorption has been regarded as one of the most efficient strategies, since it has advantages of high-removal efficiency, ease of operation, and practical, low-budget and low environmental impact [9,10]. In particular, the elimination of Cu^{2+} adsorption process can provide additional technical and economic benefits. Therefore, it is necessary to study the application of novel adsorbents



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Copyright: © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). to consolidate their industrial application [11–13]. In this direction, it has been reported that two-dimensional (2D) nanomaterials show potential as promising adsorbents for heavy metal removal [14–16]. For instance, 2D graphene oxide (GO) with large surface area includes reactive functional groups (carboxyl, hydroxyl, and carbonyl groups) and exhibits high affinity with metal ions [17]. However, the adsorption capacity of GO is mainly restricted to the number of surface functional groups, thus there is a high need to improve the Cu²⁺adsorption of MGO sheets [18,19].

In addition, metal-organic frameworks (MOFs) have been widely used as a hazardous remediation agent in heavy metal precipitation and adsorption because of their distinct porosity, adsorption capacity, high specific surface areas, tunable porous structure, and modifiability [20]. However, the analysis and discussion of the interaction between adsorbent and adsorbed material, as well as the adsorption mechanism, are still insufficient [21–23]. It should be noted that the structure of the adsorbent (e.g., molecular particle size, functional groups, molecular polarity and solubility) has an effect on adsorption performance [24,25]. Due to their crystalline character, MOFs accumulate in powder form. Investigations into MOFs have shown that their ability to remove Cu^{2+} is largely dependent on the duality of their particles [26–29]. However, MOF powders tend to accumulate, which greatly limits the exposure of adsorption sites and leads to a decrease in adsorption capacity. Inspired by this, the conjugation of MOFs with suitable substrates is considered as a feasible approach to meet the needs of the application [30-32]. Herein, we propose a facile strategy for the in situ growth of ZIF-8 between laminated graphene channels to form ZIF-8/graphene composites, whereby the MGO interlayer supports and disperses the attachment of ZIF-8 particles, and is well retained. The results show that the porous property of graphene provides channels for water transport, and that MGO@ZIF-8 can be used to adsorb Cu²⁺ efficiently. This work offers a new adsorbent for the removal of heavy metals and can broaden its application for use in environmental treatment.

2. Experimental

2.1. Materials

MGO was purchased from Carbon Feng Technology of Suzhou, methyl alcohol was bought from Tianjin Yongda Chemical Reagent Co., Ltd. (Tianjin, China), 2-Methylimidazole (2-Melm) was obtained from Tokyo Kasei Kogyo Co. of Japan, and sodium dodecylbenzene sulfonate (DBS) was gained from J&K Technology Co. of China in Xiamen city. Polyvinyl pyrrolidone (PVP) was purchased from Tianjin Feng Chuan Chemical Reagent Technology Co., Ltd. (Tianjin, China). All materials employed in this study were of analytical grade without further purification. Ultra-pure water was used in the experiments. A magnetic constant temperature stirrer, MYP19-2 type, was obtained from Shanghai Meiyingpu Instrument Manufacturing Co., Ltd. (Shanghai, China).

2.2. Synthesis of MGO@ZIF-8

As shown in Figure 1, DBS was ultrasonically dissolved in 120 mL methyl alcohol, and 60 mg of MGO was added after dissolution to prepare the MGO suspension. Then, 4 mg of PVP was poured into the suspension, and after subjecting to ultrasound for 1 h, the supernatant was removed and centrifuged for 10 min. After that, the precipitation obtained was redispersed into methyl alcohol, and 5.622 g of 2-Melm was added into the dispersion solution until it was completely dissolved.. Subsequently, the dispersion was placed on a magnetic stirrer at moderate speed, and methyl alcohol of zinc nitrate (2.572 g) was slowly added at 298 K and stirred for 1 h. Finally, the precipitation was collected by centrifugation, and the activated MGO@ZIF-8 was prepared after vacuum drying.



Figure 1. The preparation process of MGO@ZIF-8.

2.3. Assessment of MGO@ZIF-8 for Cu²⁺ Adsorbing Capacity

In the process of undertaking the adsorption experiment, the effects of different pH, adsorption time, adsorption temperature and the amount of adsorbent were investigated for MGO@ZIF-8, and the adsorption of Cu²⁺ was observed. An appropriate amount of copper sulfate was dissolved in deionized water to prepare a certain concentration of copper ion solution, and we then adjusted the effect of different pH (1–7) on the adsorption amount with hydrochloric acid and sodium hydroxide at 35 °C. The effect of different adsorption times (0–110 min) on the adsorption capacity was investigated every 10 min at pH = 6 at 35 °C. The effect of different temperatures (25–50 °C) on the adsorption capacity was investigated at pH = 6. The effect of different adsorbent dosages (1–8 mg) on the adsorption capacity was investigated at pH = 6 and 35 °C. The corresponding adsorption capacity was obtained according to adsorption capacity shown in Formula (1) [33–35].

$$q_t = \frac{(c_0 - c_t)}{M} V \tag{1}$$

where $c_0 \text{ (mg/L)}$ is the solution initial concentration; $q_t \text{ (mg/g)}$ is adsorption quantity; $c_t \text{ (mg/L)}$ is the residual concentration of the target substance at time T; M (mg) is the mass of adsorbent; and V (L) is the volume of the solution.

2.4. Standard Curve of Cu^{2+}

 Cu^{2+} solutions with different concentration gradients were prepared, and the concentration of copper ions was detected according to a flame atomic absorption instrument. The standard curve of Cu^{2+} was drawn by software, as shown in Figure 2.



Figure 2. Standard curve of Cu²⁺.

2.5. Adsorption Kinetics

In the study, the dynamics were fitted Lagergren quasi-first-order kinetics equation and quasi-second-order kinetics equation [36–38], as shown below.

Lagergren quasi-first order kinetic equation:

$$\ln(Q_e - Q_t) = \ln Q_e - K_1 t \tag{2}$$

Lagergren quasi-second-order kinetics equation:

$$\frac{t}{Q_{\rm t}} = \frac{1}{Q_{\rm e}^2 K_2} + \frac{t}{Q_{\rm e}}$$
(3)

wherein Q_e (mg/g) is the adsorption capacity at equilibrium; Q_t (mg/g) expresses the adsorption capacity at any moment; K_1 (min⁻¹) represents the constant of Lagergren first-order kinetics; and K_2 (g/(min·mg)) denotes the constant of the Lagergren second-order kinetics.

2.6. Adsorption Isotherms

The adsorption isotherms were employed based on the Freundlich adsorption isotherm model and Langmuir adsorption isotherm model [39–41]. The Langmuir adsorption isotherm is shown as:

$$\frac{C_{\rm e}}{q_e} = \frac{1}{q_{max}k_L} + \frac{C_e}{q_{max}} \tag{4}$$

In Equation (4), $q_e (mg/g)$ is named as amount of metal ions adsorbed by adsorbent per unit weight; $q_{max} (mg/g)$ represents complete single-layer coverage of the corresponding maximum adsorption capacity; $C_e (mg/L)$ denotes the equilibrium concentration of metal ions; and K_L (L/mg) means a constant for the free energy of adsorption. The slope and intercept of C_e/q_e versus c_e is able to derive the values of q_{max} and k_L , respectively.

The Freundlich adsorption isotherm is shown as:

$$_{e} = k_{F}C_{e}^{1/n} \tag{5}$$

In Equation (5), q_e (mg/g) indicates the equilibrium adsorption capacity, and K_F and *n* express the respective Freundlich constants for adsorption capacity and adsorption intensity. The adsorption process is favorable if 1/n is smaller than unity. The slope and intercept of log q_e versus log C_e can calculate the values of K_F and *n*, respectively.

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3. Results and Discussion

3.1. Characterization of Adsorbents

3.1.1. SEM and AFM Analysis

The SEM and AFM images of the samples are displayed in Figure 3. As shown in Figure 3a, the MGO was a superposition of multi-layered structures. ZIF-8 grew uniformly between the graphene layers with a crystal size distribution between 50 and 150 nm (Figure 3b). Graphene provided a supporting framework for ZIF-8 [42,43], preventing the reduction in the specific surface area caused by the volume pressure of the ZIF-8 powder. This porous structure can increase the active sites for metal ion adsorption and improve adsorption performance. It can be seen from Figure 3b that ZIF-8 was uniformly distributed on the hierarchical surface of the MGO, and the fully exposed surface could provide more attachment sites for copper ions, which effectively improves the adsorption performance of the composites [44,45].



Figure 3. SEM images of the samples: (a) MGO, and (b) MGO@ZIF-8; and AFM images of the samples: (c) MGO@ZIF-8, and (d) MGO@ZIF-8.

3.1.2. XRD Diffraction and FT-IR Spectroscopy

In order to verify the phases and components of the samples, they were characterized by XRD (Figure 4a). As can clearly be seen, the XRD patterns of ZIF-8 showed that strong diffraction peaks at 7.13°, 10.19°, 7.05° and 17.84°, corresponded to (001), (002), (112) and (222) crystal planes of ZIF-8, suggesting that the pure ZIF-8 was prepared successfully. Moreover, a diffraction peak in MGO located at 20 value of 26.21°, which corresponded well to the (111) crystal plane of MGO, and importantly, no other diffraction peaks of other crystal phases were observed [46]. Amazingly, the characteristic peaks of MGO and ZIF-8 simultaneously appeared in the acquired XRD patterns of MGO@ZIF-8, suggesting that the desirable MGO@ZIF-8 composite was successfully prepared without forming any other new crystals.



Figure 4. (a) XRD patterns of the samples; (b) FT-IR spectra analysis.

The chemical groups of the three samples were further examined according to FT-IR spectroscopy, as shown in Figure 4b. Therein, no peaks appeared at the MGO, however, obvious characteristic peaks at (a) 3431 cm⁻¹, (b) 2927 cm⁻¹ and (g) 421 cm⁻¹ due to N-H stretching, C-H bending vibrations and Zn-N stretching were observed in ZIF-8, respectively. Different from the spectra of the MGO and ZIF-8, the bonding interaction diagram shows that ZIF-8 in MGO@ZIF-8 appeared a "blue shift" phenomenon at the position of (d) 1586 cm⁻¹, and moved to (c) 1649 cm⁻¹, due to the change of the dipole moment of the C=C and C=N groups after MGO and ZIF-8 were recombined [47].

3.1.3. Specific Surface Area and BET Analysis

Nitrogen adsorption–desorption analysis was used to observe the porous structures of MGO@ZIF-8 based on the Brunauer–Emmett–Teller (BET) method. According to the definition given by the International Society for Theoretical and Applied Chemistry (IUPAC), the nitrogen isotherm of MGO@ZIF-8 belongs to a type IV isotherm (obvious increasing uptake at high P/P₀), which indicates that the adsorption of MGO@ZIF-8 was as monolayers, as shown in Figure 5, and the BET specific surface area of MGO@ZIF-8 calculated from nitrogen isotherm was found to be 249.7 m²/g. In addition, as shown in Figure 6, the central aperture of MGO@ZIF-8 was about 3 nm, and the pore diameter was present at 2–15 nm, confirming that the composite material was mesoporous and had a large specific surface area [48,49]. Therefore, it was also verified that the adsorption performance of MGO@ZIF-8 could be improved by the composite of ZIF-8 and MGO.



Figure 5. Isotherms of MGO@ZIF-8.



Figure 6. Aperture distribution curve of MGO@ZIF-8.

3.1.4. XPS Analysis

X-ray photoelectron spectroscopy (XPS) spectra was conducted to further probe the differences in the chemical composition of the composite surface after surface modification,

and the interactions between the MGO@ZIF-8 and Cu²⁺. The wide scanning XPS spectra of MGO@ZIF-8 before and after Cu²⁺ adsorption are exhibited in Figure 7a,e, respectively. Compared with the pristine MGO@ZIF-8, it can clearly be seen that the Cu $2p_{3/2}$ peak presented in the composite of Cu-MGO@ZIF-8, confirming that MGO@ZIF-8 was able to adsorb Cu²⁺. Additionally, the energy spectrum of Zn 2p with absorption peaks at 1045.08 eV and 1022.08 eV fully indicated the existence of Zn $2p_{1/2}$ and Zn $2p_{3/2}$ (Figure 7b), suggesting that MGO@ZIF-8 was successfully synthesized [50]. The difference of 23 eV between the two peaks effectively confirmed that the valence state of Zn in MGO@ZIF-8 was 2s, which was consistent with reports in the known relevant literature. Figure 7c displayed the C1s energy spectrum of MGO@ZIF-8 material at 285.57 eV and 284.85 eV, corresponding to C-N and C=N in dimethylimidazole and organic ligands in ZIF-8 material, respectively. The energy spectrum of O 1s was present in MGO@ZIF-8 (Figure 7d), simultaneously O=C-O at 532.78 eV and Zn-O at 529.86 eV appeared in MGO@ZIF-8, which also indicated that ZIF-8 successfully combined into the layers of MGO. In particular, the energy spectrum of Cu 2p, which was Cu $2p_{1/2}$ and Cu $2p_{3/2}$ at 168 eV and 368 eV, respectively, could be explained by the composite material having an adsorption effect on Cu^{2+} , and the adsorption process was chemical adsorption.



Figure 7. XPS analysis of: (**a**) survey scan of MGO@ZIF-8, (**b**) Zn 2p, (**c**) C 1s, (**d**) O1s,(**e**) survey scan of Cu-MGO@ZIF-8, and (**f**) Cu 2p.

3.2. Adsorption Mechanism

3.2.1. pH Effect on Cu²⁺ Adsorption by MGO@ZIF-8

As is known to all, the pH value of a solution is an important determinant that affects the adsorption of metal ions by adsorbents, as it not only affects the kinds of metals in the solution, but also has a great influence on the surface properties of the adsorbent. Although it has been proved that most MGO adsorbents have good adsorption capacity for Cu^{2+} , they depend on pH value, which is not conducive to practical application [51]. In this study, the pH effect on the MGO@ZIF-8 adsorption capacities for Cu^{2+} was researched at pH from 1 to 7 and the results are displayed in Figure 8. Evidently, MGO@ZIF-8 showed different Cu^{2+} adsorption capacity with the change in pH, indicating that wide adaptability was dependent on pH. It can clearly be seen that the Cu2+ adsorption capacity increased with pH increasing from 1 to 6, as the increase of pH in the solution resulted in attenuating the electrical repulsion force, which increased the adsorb possibility of metal ions on the surface of MGO@ZIF-8. When pH = 6, MGO@ZIF-8 delivered the highest adsorption capacity with a Cu^{2+} adsorption mass of 450 mg/g. However, when the pH increased to 7, the Cu²⁺ adsorption capacity of MGO@ZIF-8 decreased, which was mainly caused by the protonation of functional groups in the composite, leading to a positive charge on the material surface, and a competitive combination of hydrogen ions and copper ions occurred in the solution.



Figure 8. Effect of pH on Cu²⁺ adsorption.

3.2.2. Temperature Effect on Cu²⁺ Adsorption by MGO@ZIF-8

For the sake of examining the influence of the temperature effect on Cu^{2+} adsorption, different reaction temperatures were used to study the concentration of Cu^{2+} solution with an adsorption time of 2 h. The study found that the temperature of Cu^{2+} solution for MGO@ZIF-8 adsorption capacity engendered a positive effect, as shown in Figure 9. Under the extension of 25 °C to 35 °C with the same initial concentration of the Cu^{2+} solution, it was obvious that q_e increased when the temperature was raised. Therefore, the adsorption reaction was conjectured to be endothermic. Raised temperatures expedited the thermal motion of Cu^{2+} , creating an increased physical adsorption rate of Cu^{2+} on the MGO@ZIF-8 surface. However, the elevated temperature increased energy that was relied upon within the adsorption process; stable chemical bonds formed between MGO@ZIF-8 and Cu^{2+} , working to enhance the q_e . However, the adsorption rate slowed down with the increase in temperature, because the adsorption of the adsorbent material for the solution system was close to equilibrium when the adsorption capacity reached 430 mg/g [52].



Figure 9. Effect of temperature adsorption.

3.2.3. Effect of Adsorbent Amount on Cu²⁺ Adsorption of MGO@ZIF-8

The influence of the dosage of adsorbent on adsorption is one of the important indices to evaluate the properties of adsorbent materials. Consequently, it is of great significance to explore the optimal feeding ratio of materials to maximize their utilization rate. Figure 10 shows the comparison of Cu^{2+} adsorption effects of ZIF-8, MGO and MGO@ZIF-8 at different dosages. Obviously, among the three samples, MGO showed the worst adsorption effect on Cu^{2+} , while the adsorption effect of ZIF-8 was better than the composite MGO@ZIF-8 when the amount of material was 1.0–2.0 mg, which may have been due to the better dispersion of the appropriate amount of ZIF-8 in the adsorption system [53]. However, the adsorption of Cu^{2+} by MGO@ZIF-8 was superior to pure ZIF-8 when MGO@ZIF-8 and ZIF-8 were at the same amount, which was due to the synergistic effect between MGO and ZIF-8. In addition, ZIF-8 did not show agglomeration under the influence of MGO, providing more adsorption sites.



Figure 10. Effect of amount of adsorbent on adsorption.

3.2.4. Time-Dependent Adsorption Behavior

The adsorption kinetic of MGO@ZIF-8 to adsorb Cu^{2+} at about 25 °C was also investigated. As shown in Figure 11, the adsorption of the MGO@ZIF-8 for Cu^{2+} showed different time-dependent behaviors, and the equilibrium for Cu^{2+} was attained within 2 h. Initially, it was clear that the growth rate of the adsorption capacity of MGO@ZIF-8 at 0–70 min increased significantly fast. After 70 min, the adsorption rates of MGO@ZIF-8 decreased to a certain extent, approaching the adsorption equilibrium, verifying that the combination of MGO and ZIF-8 could improve the adsorption effect of ZIF-8 [54].



Figure 11. Time-dependent adsorption behavior of MGO@ZIF-8.

3.2.5. Analysis of Orthogonal Experiment Results

In order to explore the optimum condition for MGO@ZIF-8 to adsorb copper ions, the pH, adsorption temperature, quantity of adsorbent and adsorption time were selected to design research, based on the four factors and three levels of an orthogonal experiment. The selection of horizontal conditions for each factor are displayed in Table 1, and the experimental results were intuitively calculated and analyzed, as shown in Table 2. The adsorption amounts were analyzed, and the results are shown in Table 2. The adsorption of copper ions by MGO@ZIF-8 was optimal when the pH value was 6, the adsorption time was 70 min, the adsorption temperature was 35 °C, and the adsorbent was 5 mg. As displayed in Table 3, the Cu²⁺ adsorption capacity with the reported materials were compared, and the results showed that the Cu²⁺ adsorption capacity of MGO@ZIF-8 prepared in this work was higher than the materials described in previous literature.

Table 1. Selection of experimental factor level conditions	Table 1.	e 1. Selection of e	experimental	factor	level	conditions.
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Level	рН	Time (min)	Temperature (°C)	Amount of Adsorbent (mg)	Results (mg/g)
1	5	50	30	4	
2	6	60	35	5	Q
3	7	70	40	6	

Tab	le 2.	The	experimental	result	s are	intuitive	ly ca	lcula	ated	and	anal	lyzed	•
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	Influence Factor									
Number	рН	Time (min)	Temperature (°C)	Amount of Adsorbent (mg)	(mg/g)					
1	5	50	30	4	390.05					
2	5	70	35	5	437.21					
3	5	70	40	6	410.37					
4	6	50	35	4	420.45					
5	6	60	40	5	400.52					
6	6	70	30	6	440.83					
7	7	50	40	5	403.16					
8	7	60	30	6	384.91					
9	7	70	35	2	397.42					
K_1	412.333	404.333	404.667	395.677						
K_2	420.000	407.000	418.000	426.667						
$\overline{K_3}$	394.667	415.667	404.333	404.667						
Ř	25.333	11.334	13.667	31.000						

Sorbent	Adsorption Capacity	рН	Temperature (°C)	Reference
CD-CA/PDA	73.46	6	25	[10]
Magnetite Nanoparticles	6.28	7	30	[12]
Fe ₃ O ₄ @zeolite NaA	86.54	4	25.15	[6]
Tyr-Mt	28.31	5	15	[11]
Modified latex sponge	125.8	5.85	40	[38]
PVA/GO	44.7	5.8	50	[47]
GO/PEI/CMC	302.04	5.0-5.5	25	[55]
MGO@ZIF-8	431.63	6	35	This work

Table 3. Comparison of Cu²⁺ adsorption capacity of MGO@ZIF-8 with similar and other previously used adsorbents.

3.2.6. Adsorption Kinetics

The quasi-first-order and quasi-second-order fitting results of the time curve for Cu²⁺ adsorption effect of MGO@ZIF-8 are shown in Figure 12, and copper ion adsorption kinetic parameters of MGO@ZIF-8 were obtained according to the fitting results. As shown in Table 4, the actual maximum adsorption equilibrium quantity was 431.63 mg/g, and the theoretical adsorption quantity was 489.82 mg/g, based on the quasi-first-order kinetic fitting, which was quite different from the actual result. However, during the quasi-secondorder kinetic fitting of the adsorption time curve, the theoretical maximum adsorption capacity was 432.50 mg, which was consistent with the experimental result, and the quasisecond-order fitting coefficient R^2 was 0.997 > 0.983, as shown in Figure 13 and Table 4, thus, the quasi-second-order fitting result was good, because the MGO@ZIF-8 had the expected Cu^{2+} adsorption capacity [56]. Based on the fitting results, the adsorption process of MGO@ZIF-8 was in better agreement with the quasi-second-order kinetics, and the adsorption rate was positively correlated with the quadratic power of the maximum adsorption capacity under appropriate adsorption conditions. These results indicated that the Cu²⁺ adsorption behavior of the MGO@ZIF-8 adsorbent well-fitted the pseudo-secondorder equation, in which the adsorption process was controlled by the chemical adsorption mechanism.



Figure 12. Pseudo-first-order and pseudo-second-order nonlinear fitting of dynamics.

Table 4. Copper ion adsorption kinetic parameters of MGO@ZIF-8.

	Pseudo-First-Order			Pseudo-Second-Order			
Copper Ion	$Q_{\rm e}$ (mg/g)	K_1 (min $^{-1}$)	$Q_{\rm e}$ (mg/g)	R^2	K_2 (g/(mg·min))	$Q_{\rm e}$ (mg/g)	R^2
Cu	431.63	0.05	489.82	0.983	0.0014	432.50	0.997



Figure 13. Pseudo-first-order (a), and pseudo-second-order (b), linear fitting of dynamics.

3.2.7. Adsorption Isotherm

More importantly, in order to estimate the Cu²⁺ adsorption capacity of MGO@ZIF-8 on the basis of Cu²⁺ concentration and the parameters, the adsorption isotherm was performed. Figure 14 and Table 5 list the parameters and fitting condition for the Langmuir and Freundlich models, in which it can be seen that the Cu²⁺ adsorption capacity of MGO@ZIF-8 significantly increased before the initial Cu²⁺ concentration increased to 70 mg/L, then was close to the stable values, as shown in Figure 14a,c. Table 5 shows that although both models were suited to fit the Cu²⁺ adsorption isotherm by MGO@ZIF-8, the Langmuir model delivered a higher correlation coefficient of R² (0.999), which confirmed that the adsorption process was controlled by chemical interactions and took place on the homogeneous surface of the MGO@ZIF-8. In addition, the theoretical maximum Cu²⁺ adsorption capacity of 458.2 mg/g was obtained according to the Langmuir model.



Figure 14. (**a**) Langmuir nonlinear fitting; (**b**) linear fitting for MGO@ZIF-8 adsorption of copper ions; (**c**) Freundlich nonlinear fitting; and (**d**) linear fitting for copper ion adsorption.

	Langmuir			Freundlich		
T/K	Qe	К _L	R ²	<i>K_F</i> 0.27318	1/n	R ²
308	458.20	0.016	0.999		0.653	0.963

Table 5. Adsorption isothermal model parameters of MGO@ZIF-8 for Cu²⁺.

4. Conclusions

In conclusion, ZIF-8 was loaded into the interlayer of MGO by a simple in situ growth, to prepare MGO@ZIF-8. The maximum adsorption capacity of MGO@ZIF-8 achieved 431.63 mg/g when pH was 6, the temperature was 35 °C, and the adsorption time was 70 min. The excellent adsorption was attributed to the layered structure of graphene that provided ZIF-8 with uniformly distributed growth sites. The adsorption law of Cu²⁺ on MGO@ZIF-8 complied with the pseudo-second-order kinetic model and the Langmuir model, which confirmed that the process was monolayer chemisorption and a spontaneous endothermic process. The simple preparation process effect helped obtain MGO@ZIF-8 with high adsorption, which has potential application prospects in the field of heavy metal treatment.

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References

- 1. Ansone-Bertina, L.; Ozols, V.; Arbidans, L.; Dobkevica, L.; Sarsuns, K.; Vanags, E.; Klavins, M. Metal–Organic Frameworks (MOFs) Containing Adsorbents for Carbon Capture. *Energies* 2022, *15*, 3473. [CrossRef]
- Atasoy, A.D.; Bilgic, B. Adsorption of Copper and Zinc Ions from Aqueous Solutions Using Montmorillonite and Bauxite as Low-Cost Adsorbents. *Mine. Water Environ.* 2017, 37, 205–210. [CrossRef]
- Casolla, B.; Kuchcinski, G.; Bodenant, M.; Leys, D.; Labreuche, J.; Cordonnier, C.; Hénonet, H. Prédicteurs de pronostic fonctionnel à 1 an chez les survivants d'un infarctus étendu de l'artère cérébrale moyenne traité par hemicraniectomie décompressive. *Rev. Neurol.* 2021, 176, S80. [CrossRef]
- 4. Bo, S.; Ren, W.; Lei, C.; Xie, Y.; Cai, Y.; Wang, S.; Gao, J.; Ni, Q.; Yao, J. Flexible and porous cellulose aerogels/zeolitic imidazolate framework (ZIF-8) hybrids for adsorption removal of Cr(IV) from water. *J. Solid State Chem.* **2018**, 262, 135–141. [CrossRef]
- Bui, T.T.; Nguyen, D.C.; Hua, S.H.; Chun, H.; Kim, Y.S. Sonochemical Preparation of a Magnet-Responsive Fe₃O₄@ZIF-8 Adsorbent for Efficient Cu²⁺ Removal. *Nanomaterials* 2022, *12*, 753. [CrossRef]
- 6. Cao, J.; Wang, P.; Shen, J.; Sun, Q. Core-shell Fe₃O₄@zeolite NaA as an Adsorbent for Cu²⁺. *Materials* **2020**, *13*, 5047. [CrossRef]
- 7. Bhagat, S.K.; Pyrgaki, K.; Salih, S.Q.; Tiyasha, T.; Beyaztas, U.; Shahid, S.; Yaseen, Z.M. Prediction of copper ions adsorption by attapulgite adsorbent using tuned-artificial intelligence model. *Chemosphere* **2021**, *276*, 130162. [CrossRef]
- 8. Çelekli, A.; Bozkuş, B.; Bozkurt, H. Development of a new adsorbent from pumpkin husk by KOH-modification to remove copper ions. *Environ. Sci. Pollut. Res.* 2018, 26, 11514–11523. [CrossRef]
- 9. Chen, D.; Liu, X.; Nie, H. Crumpled graphene balls as rapid and efficient adsorbents for removal of copper ions. *J. Colloid Interface Sci.* 2018, 530, 46–51. [CrossRef]
- Chen, H.; Zhou, Y.; Wang, J.; Lu, J.; Zhou, Y. Polydopamine modified cyclodextrin polymer as efficient adsorbent for removing cationic dyes and Cu²⁺. J. Hazard. Mater. 2019, 389, 121897. [CrossRef]
- 11. Chu, Y.; Zhu, S.; Wang, F.; Lei, W.; Xia, M.; Liao, C. Tyrosine-Immobilized Montmorillonite: An Efficient Adsorbent for Removal of Pb²⁺ and Cu²⁺ from Aqueous Solution. *J. Chem. Eng. Data* **2019**, *64*, 3535–3546. [CrossRef]
- Jorge, E.Y.C.; Sánchez, R.M.; Chacón, J.J.; Diaz-Castañon, S.; Piñar, F.C. Magnetite nanoparticles as adsorbent material for Cu²⁺ ions from aqueous solution. *Part. Sci. Technol.* 2017, *36*, 778–784. [CrossRef]

- Dou, W.; Liu, J.; Li, M. Competitive adsorption of Cu²⁺ in Cu²⁺, Co²⁺ and Ni²⁺ mixed multi-metal solution onto graphene oxide (GO)-based hybrid membranes. *J. Mol. Liq.* 2020, 322, 114516. [CrossRef]
- Du, T.; Wang, J.; Zhang, T.; Zhang, L.; Yang, C.; Yue, T.; Sun, J.; Li, T.; Zhou, M.; Wang, J. An Integrating Platform of Ratiometric Fluorescent Adsorbent for Unconventional Real-Time Removing and Monitoring of Copper Ions. ACS Appl. Mater. Interfaces 2020, 12, 13189–13199. [CrossRef] [PubMed]
- 15. Fronczak, M.; Demby, K.; Strachowski, P.; Strawski, M.; Bystrzejewski, M. Graphitic Carbon Nitride Doped with the s-Block Metals: Adsorbent for the Removal of Methyl Blue and Copper (II) Ions. *Langmuir* **2018**, *34*, 7272–7283. [CrossRef] [PubMed]
- Silva Filho, E.C.; Santos Júnior, L.S.; Santos, M.R.M.C.; Fonseca, M.G.; Sousa, K.S.; Santana, S.A.A.; Airoldi, C. Thermochemistry of interaction between cellulose modified with 2-aminomethyl pyridine and divalent cations. *J. Therm. Anal. Calorim.* 2013, 114, 423–429. [CrossRef]
- 17. Furukawa, S.; Reboul, J.; Diring, S.; Sumida, K.; Kitagawa, S. Structuring of metal-organic frameworks at the mesoscopic/macroscopic scale. *Chem. Soc. Rev.* **2014**, *43*, 5700–5734. [CrossRef]
- Georgiou, E.; Mihajlović, M.; Petrović, J.; Anastopoulos, I.; Dosche, C.; Pashalidis, I. Single-stage production of miscanthus hydrochar at low severity conditions and application as adsorbent of copper and ammonium ions. *Bioresour. Technol.* 2021, 337, 125458. [CrossRef]
- Hosseinzadeh, H.; Pashaei, S.; Hosseinzadeh, S.; Khodaparast, Z.; Ramin, S.; Saadat, Y. Preparation of novel multi-walled carbon nanotubes nanocomposite adsorbent via RAFT technique for the adsorption of toxic copper ions. *Sci. Total Environ.* 2018, 640–641, 303–314. [CrossRef]
- 20. Huang, Y.; Peng, J.; Huang, X. Allylthiourea functionalized magnetic adsorbent for the extraction of cadmium, copper and lead ions prior to their determination by atomic absorption spectrometry. *Mikrochim. Acta* **2019**, *186*, 51. [CrossRef]
- 21. Hussain, M.S.; Musharraf, S.G.; Bhanger, M.I.; Malik, M.I. Salicylaldehyde derivative of nano-chitosan as an efficient adsorbent for lead(II), copper(II), and cadmium(II) ions. *Int. J. Biol. Macromol.* **2020**, *147*, 643–652. [CrossRef] [PubMed]
- Joshi, J.; Kanchan, D.; Joshi, M.; Jethva, H.; Parikh, K. Dielectric relaxation, complex impedance and modulus spectroscopic studies of mix phase rod like cobalt sulfide nanoparticles. *Mater. Res. Bull.* 2017, 93, 63–73. [CrossRef]
- Kalbarczyk, M.; Szcześ, A.; Sternik, D. The preparation of calcium phosphate adsorbent from natural calcium resource and its application for copper ion removal. *Environ. Sci. Pollut. Res.* 2020, 28, 1725–1733. [CrossRef] [PubMed]
- 24. Klimmek, S.; Stan, H.-J.; Wilke, A.; Bunke, G.; Buchholz, R. Comparative Analysis of the Biosorption of Cadmium, Lead, Nickel, and Zinc by Algae. *Environ. Sci. Technol.* 2001, *35*, 4283–4288. [CrossRef] [PubMed]
- Kołodyńska, D.; Majdańska, M.; Budnyak, T.M. Lanthanum and copper ions recovery from nickel-metal hydride cells leaching solutions by the oxide adsorbent Pyrolox[®]. J. Environ. Chem. Eng. 2019, 7, 103003. [CrossRef]
- Lin, Y.; Hong, Y.; Song, Q.; Zhang, Z.; Gao, J.; Tao, T. Highly efficient removal of copper ions from water using poly(acrylic acid)-grafted chitosan adsorbent. *Colloid Polym. Sci.* 2017, 295, 627–635. [CrossRef]
- Liu, C.; Bai, R.; Hong, L. Diethylenetriamine-grafted poly(glycidyl methacrylate) adsorbent for effective copper ion adsorption. J. Colloid Interf. Sci. 2006, 303, 99–108. [CrossRef]
- Liu, C.; Bai, R.; Ly, Q.S. Selective removal of copper and lead ions by diethylenetriamine-functionalized adsorbent: Behaviors and mechanisms. *Water Res.* 2008, 42, 1511–1522. [CrossRef]
- 29. Liu, C.; Liang, X.; Liu, J.; Yuan, W. Desorption of copper ions from the polyamine-functionalized adsorbents: Behaviors and mechanisms. *Adsorpt. Sci. Technol.* **2016**, *34*, 455–468. [CrossRef]
- 30. Niuniavaite, D.; Baltakys, K.; Dambrauskas, T.; Eisinas, A. Cu²⁺, Co²⁺ and Cr3+ adsorption by synthetic dibasic calcium silicate hydrates and their thermal stability in a 25–1000 °C temperature range. *J. Therm. Anal.* **2019**, *138*, 2241–2249. [CrossRef]
- 31. Mariyam, S.; Zuhara, S.; Al-Ansari, T.; Mackey, H.; McKay, G. Novel high capacity model for copper binary ion exchange on e-waste derived adsorbent resin. *Adsorption* **2022**, *28*, 185–196. [CrossRef]
- 32. Marjub, M.M.; Rahman, N.; Dafader, N.C.; Tuhen, F.S.; Sultana, S.; Ahmed, F.T. Acrylic acid-chitosan blend hydrogel: A novel polymer adsorbent for adsorption of lead (II) and copper (II) ions from wastewater. J. Polym. Eng. 2019, 39, 883–891. [CrossRef]
- 33. Mone, M.; Lambropoulou, D.A.; Bikiaris, D.N.; Kyzas, G. Chitosan Grafted with Biobased 5-Hydroxymethyl-Furfural as Adsorbent for Copper and Cadmium Ions Removal. *Polymers* **2020**, *12*, 1173. [CrossRef]
- Mongioví, C.; Lacalamita, D.; Morin-Crini, N.; Gabrion, X.; Placet, V.; Ribeiro, A.R.L.; Ivanovska, A.; Kostić, M.; Bradu, C.; Staelens, J.-N.; et al. Use of chènevotte, a valuable co-product of industrial hemp fiber, as adsorbent for copper ions: Kinetic studies and modeling. *Arab. J. Chem.* 2022, 15, 103742. [CrossRef]
- 35. Niu, Y.; Ying, D.; Li, K.; Wang, Y.; Jia, J. Fast removal of copper ions from aqueous solution using an eco-friendly fibrous adsor-bent. *Chemosphere* **2016**, *161*, 501–509. [CrossRef]
- Othman, N.A.F.; Selambakkannu, S.; Abdullah, T.A.T.; Hoshina, H.; Sattayaporn, S.; Seko, N. Selectivity of Copper by Amine-Based Ion Recognition Polymer Adsorbent with Different Aliphatic Amines. *Polymers* 2019, 11, 1994. [CrossRef]
- Prasad, J.; Singh, A.K.; Haldar, K.K.; Tomar, M.; Gupta, V.; Singh, K. CoFe2O4 nanoparticles decorated MoS2-reduced graphene oxide nanocomposite for improved microwave absorption and shielding performance. RSC Adv. 2019, 9, 21881–21892. [CrossRef]
- Qiu, L.; Phule, A.D.; Wen, S.; Zhang, X.; Chen, Q.; Zhang, Z.X. Multifunctional Adsorbent: Oleophobic Latex Sponge for Removing Dyes and Cu²⁺ from Sewage Waste. *Macromol. Mater. Eng.* 2021, 306, 2100096. [CrossRef]

- Quintero-Álvarez, F.G.; Rojas-Mayorga, C.K.; Mendoza-Castillo, D.I.; Aguayo-Villarreal, I.A.; Bonilla-Petriciolet, A.; Hamad, H. Physicochemical modeling of the adsorption of pharmaceuticals on MIL-100-Fe and MIL-101-Fe MOFs. *Adsorpt. Sci. Technol.* 2022, 2022, 4482263. [CrossRef]
- Razak, M.R.; Yusof, N.A.; Aris, A.Z.; Nasir, H.M.; Haron, M.J.; Ibrahim, N.A.; Johari, I.S.; Kamaruzaman, S. Phosphoric acid modified kenaf fiber (K-PA) as green adsorbent for the removal of copper (II) ions towards industrial waste water effluents. *React. Funct. Polym.* 2020, 147, 104466. [CrossRef]
- 41. Shahzad, A.; Jang, J.; Lim, S.-R.; Lee, D.S. Unique selectivity and rapid uptake of molybdenum-disulfide-functionalized MXene nanocomposite for mercury adsorption. *Environ. Res.* **2019**, *182*, 109005. [CrossRef] [PubMed]
- Shan, S.; Sun, X.-F.; Xie, Y.; Li, W.; Ji, T. High-Performance Hydrogel Adsorbent Based on Cellulose, Hemicellulose, and Lignin for Copper (II) Ion Removal. *Polymers* 2021, 13, 3063. [CrossRef] [PubMed]
- Sheng, P.X.; Ting, Y.-P.; Chen, J.P.; Hong, L. Sorption of lead, copper, cadmium, zinc, and nickel by marine algal biomass: Characterization of biosorptive capacity and investigation of mechanisms. *J. Colloid Interface Sci.* 2004, 275, 131–141. [CrossRef] [PubMed]
- 44. Song, Y.; Kong, A.; Ji, Y.; He, B.; Wang, H.; Li, J. Adsorption for copper(II) ion with chitosan-SP/PET composite adsorbent enhanced by electric field. *Adsorpt. Sci. Technol.* **2019**, *37*, 274–287. [CrossRef]
- Sun, H.; Xia, N.; Liu, Z.; Kong, F.; Wang, S. Removal of copper and cadmium ions from alkaline solutions using chitosan-tannin functional paper materials as adsorbent. *Chemosphere* 2019, 236, 124370. [CrossRef] [PubMed]
- Yermiyahu, Z.; Lapides, I.; Yariv, S. Thermo-XRD analysis of the adsorption of Congo-red by montmorillonite saturated with different cations. J. Therm. Anal. 2002, 69, 317–332. [CrossRef]
- 47. Tan, P.; Wen, J.; Hu, Y.; Tan, X. Adsorption of Cu²⁺ and Cd²⁺ from aqueous solution by novel electrospun poly (vinyl alcohol)/graphene oxide nanofibers. *RSC Adv.* **2016**, *6*, 79641–79650. [CrossRef]
- Tang, Y.-B.; Yin, L.-C.; Yang, Y.; Bo, X.-H.; Cao, Y.-L.; Wang, H.; Zhang, W.; Bello, I.; Lee, S.-T.; Cheng, H.-M.; et al. Tunable Band Gaps and p-Type Transport Properties of Boron-Doped Graphenes by Controllable Ion Doping Using Reactive Microwave Plasma. ACS Nano 2012, 6, 1970–1978. [CrossRef]
- 49. Wang, H.; Fang, S.; Zuo, M.; Li, Z.; Yu, X.; Tang, X.; Sun, Y.; Yang, S.; Zeng, X.; Lin, L. Removal of copper ions by cellulose nanocrystal-based hydrogel and reduced adsorbents for its catalytic properties. *Cellulose* **2022**, *29*, 4525–4537. [CrossRef]
- Sunding, M.; Hadidi, K.; Diplas, S.; Løvvik, O.; Norby, T.; Gunnæs, A. XPS characterisation of in situ treated lanthanum oxide and hydroxide using tailored charge referencing and peak fitting procedures. *J. Electron. Spectrosc. Relat. Phenom.* 2011, 184, 399–409. [CrossRef]
- Yaras, A.; Arslanoğlu, H. Valorization of Paper Mill Sludge as Adsorbent in Adsorption Process of Copper (II) Ion from Synthetic Solution: Kinetic, Isotherm and Thermodynamic Studies. *Arab. J. Sci. Eng.* 2017, 43, 2393–2402. [CrossRef]
- 52. Zeatoun, L.; Yousef, S. The use of activated and non-activated tar sands as adsorbents for copper ion removal. *Adsorpt. Sci. Technol.* **2004**, *22*, 223–235. [CrossRef]
- Zhan, M.; Jia, H.; Fan, J.; Yu, H.; Amador, E.; Chen, W. Two D-π-A Schiff-Base-Functionalized Silica Gel Adsorbents for Preconcentration of Copper Ions in Foods and Water for Detection. *Anal. Chem.* 2019, *91*, 6103–6110. [CrossRef] [PubMed]
- 54. Zhang, X.-F.; Wang, Z.; Song, L.; Yao, J. In situ growth of ZIF-8 within wood channels for water pollutants removal. *Sep. Purif. Technol.* **2021**, *266*, 118527. [CrossRef]
- Liu, H.; Guo, J.; Zhou, Y.; Qian, J. Preparation and Adsorption Performance of Efficient Adsorbent for Heavy Metal Copper(II) Using Graphene-Oxide-Based Composites. *ChemistrySelect* 2020, *5*, 11354–11360. [CrossRef]
- 56. Zhu, H.; Yang, X.; Cranston, E.D.; Zhu, S. Flexible and Porous Nanocellulose Aerogels with High Loadings of Metal-Organic-Framework Particles for Separations Applications. *Adv. Mater.* **2016**, *28*, 7652–7657. [CrossRef]