

Supplementary material

Conversion of argan nutshells into novel porous carbons in the scope of circular economy: adsorption performance of emerging contaminants

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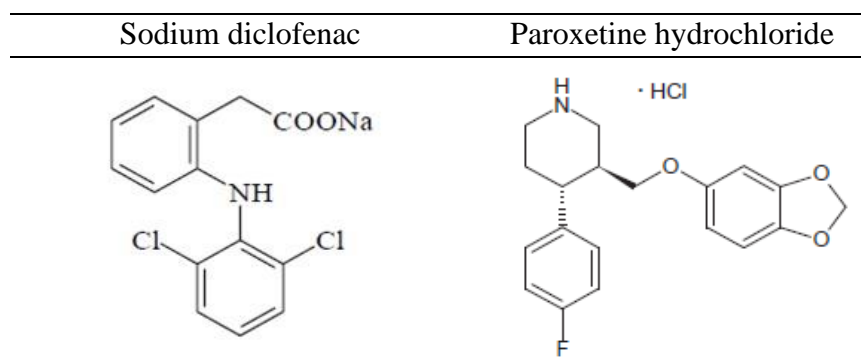


Figure S1. Molecular structures of the pharmaceutical compounds used in the present study.

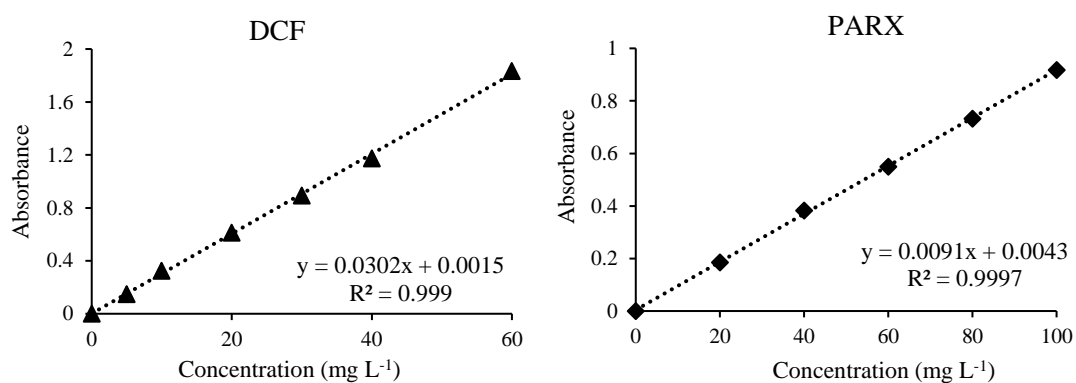


Figure S2. Calibration curves of DCF and PARX determined by UV-Vis spectrophotometry.

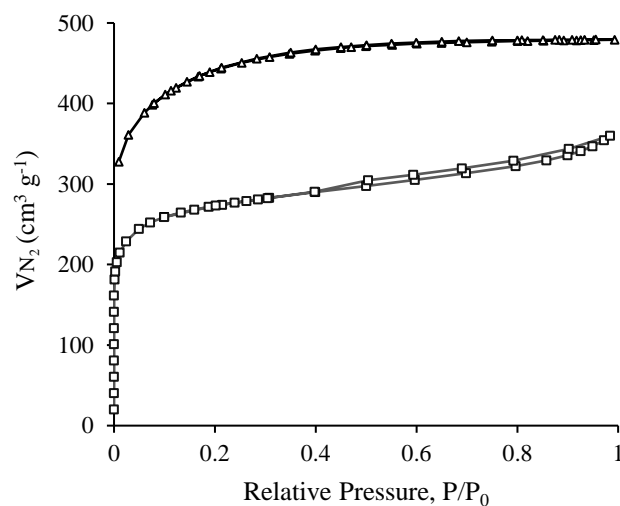


Figure S3. N₂ adsorption-desorption isotherms of ACK and CC carbon samples.

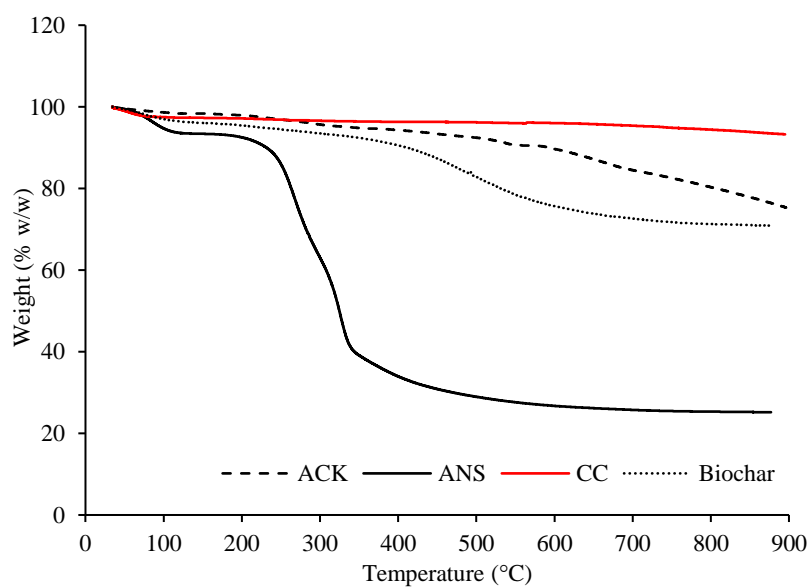


Figure S4. TGA curves of ANS biomass, biochar, ACK, and CC under argon atmosphere.

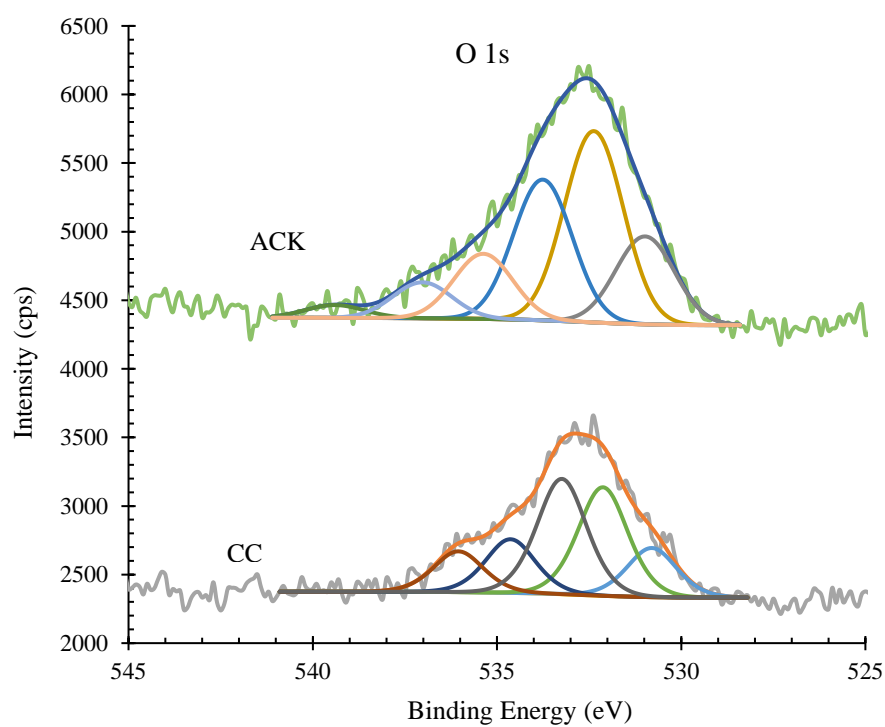
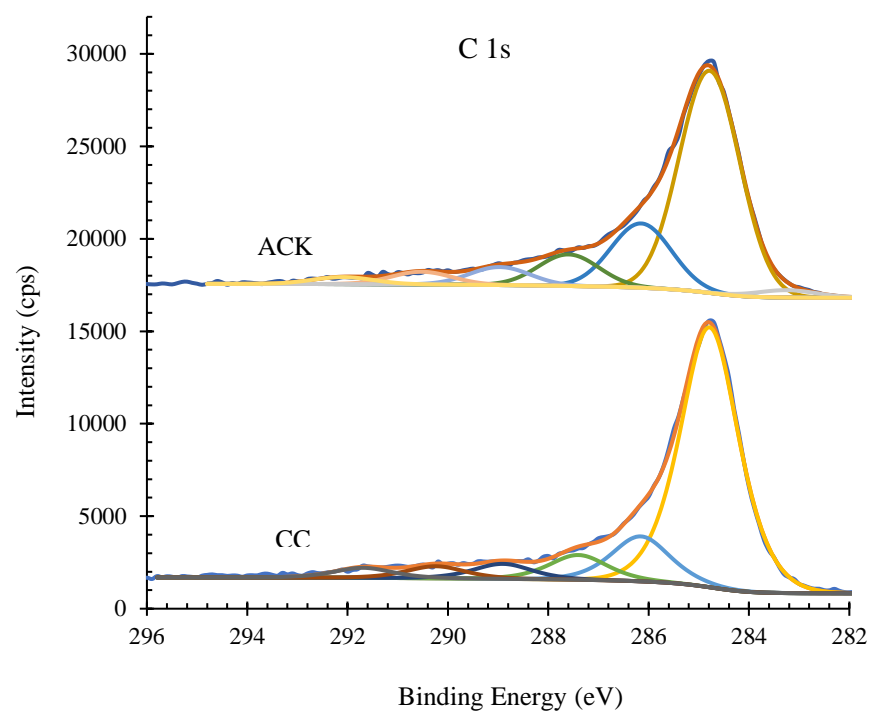


Figure S5. XPS peak fitted profiles of C 1s and O 1s regions of ACK and CC carbons.

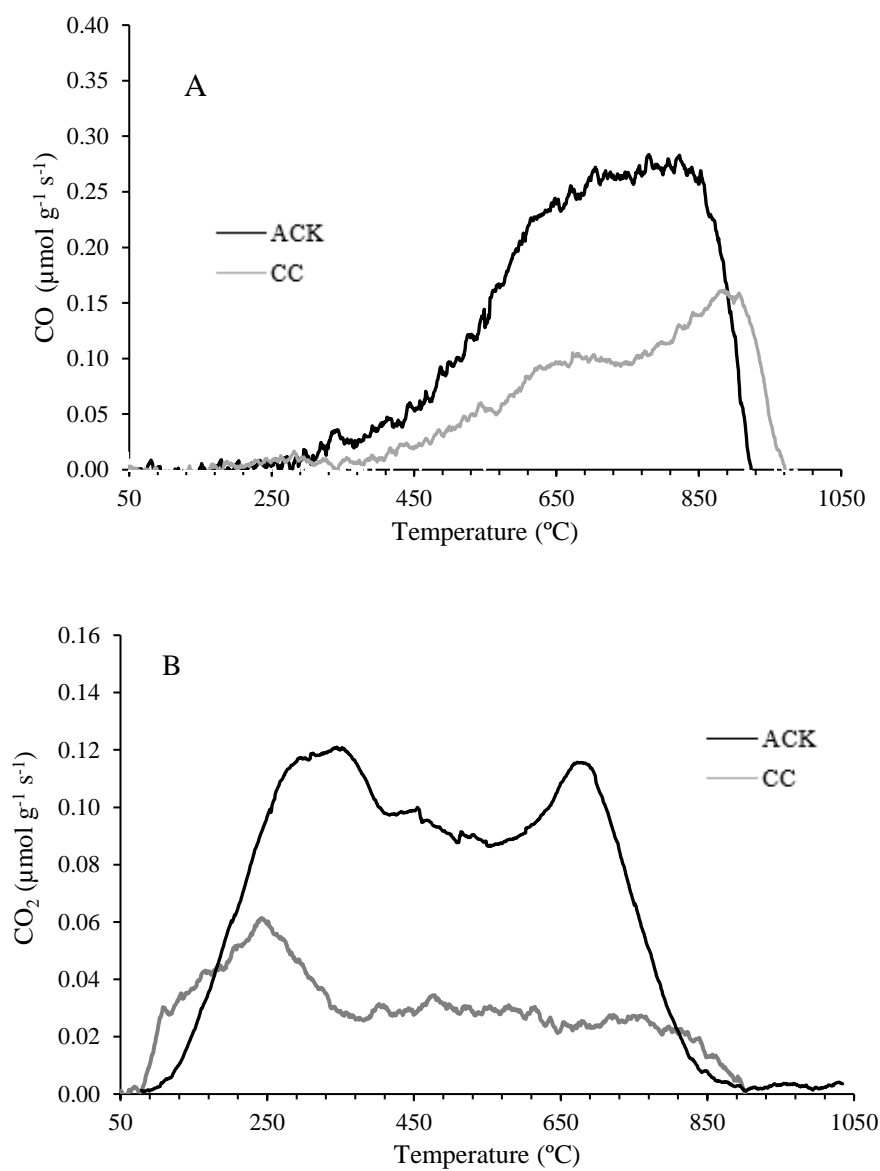


Figure S6. TPD spectra of the carbons: A) CO and B) CO₂ evolution.

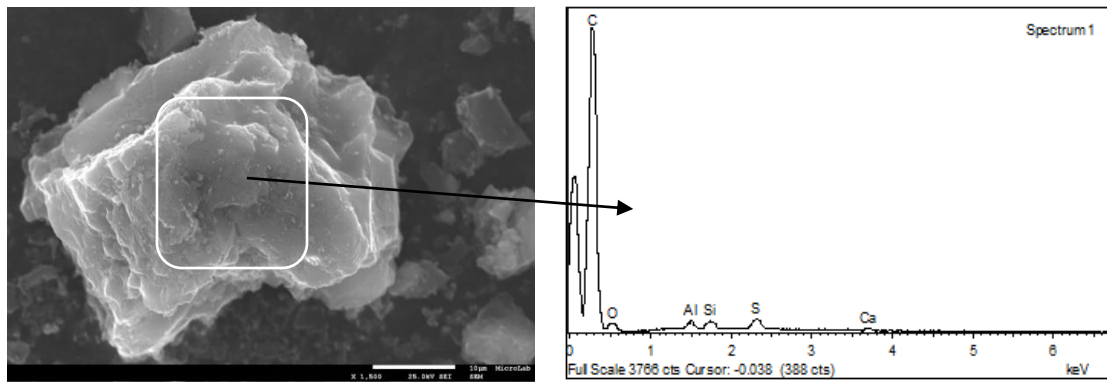


Figure S7. SEM image of CC sample with magnification 1500× and the corresponding EDS spectrum [29].

Table S1. Equations of the kinetic models and isotherm models used in the present work.

<i>Kinetic models</i>	Equation
Pseudo 1 st order (PFO)	$q_t = q_e \times (1 - e^{-k_1 \times t})$ $k_1 \text{ (min}^{-1}\text{), pseudo-1}^{\text{st}} \text{ order rate constant}$
Pseudo 2 nd order (PSO)	$q_t = \frac{q_e^2 \times k_2 \times t}{1 + (k_2 \times q_e \times t)}$ $k_2 \text{ (g mg}^{-1} \text{ min}^{-1}\text{), pseudo-2}^{\text{nd}} \text{ order rate constant}$
<i>Adsorption isotherms models</i>	Equation
Langmuir	$q_e = \frac{q_m \times K_L \times C_e}{1 + K_L \times C_e}$ $q_m \text{ (mg g}^{-1}\text{), monolayer adsorption capacity; } K_L \text{ (L mg}^{-1}\text{), Langmuir constant}$

Freundlich	$q_e = K_F C_e^{1/n}$ <p> K_F (mg g⁻¹)/(mg L⁻¹)ⁿ, Freundlich isotherm constant; n (dimensionless), adsorption intensity </p>
Sips	$q_e = \frac{q_{ms} K_s (C_e)^{n_s}}{1 + K_s (C_e)^{n_s}}$ <p> q_{ms} (mg g⁻¹), maximum adsorption capacity; K_s (L mg⁻¹), Sips equilibrium constant; n_s (dimensionless), heterogeneity of the binding surface. </p>

q_e - amount of adsorbate uptake per mass of adsorbent at equilibrium; q_t - amount of adsorbate uptake per mass of adsorbent at time t ; C_e - amount of solute in the aqueous phase at equilibrium (mg L⁻¹)