

Article

Electrospark Method in Galvanic Wastewater Treatment for Heavy Metal Removal

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Abstract: The objective of this research is to improve water treatment use of the electric spark method. Studies on the treatment of multicomponent galvanic effluent by the electric spark method using metal loading (Fe, Al) and low-voltage (up to 1000 V) equipment have been carried out. The factors that have the largest influence on the degree of galvanic wastewaters purification are the conditions and parameters of the discharge pulse—an efficiency of approximately 0.8–0.85 has a specific energy, which at moderate concentrations of pollutants can be less than 65 kJ/dm³ (18 kWh/m³)—and the metal loading height. Other variable technological parameters can serve either as scaling tools or as methods for regulating the operation of electrical equipment. The research shows that the degree of purification depends on the specific energy and the height of the metal loading of the reactor, and it weakly depends on the pulse energy and the speed of its input. The concentrations of heavy metals (Zn²⁺, Cr⁶⁺+Cr³⁺, Cu²⁺) in the treated water are significantly lower than their maximal permissible concentrations. The electric spark method allows us to achieve highly efficient results of wastewater treatment from heavy metals.

Keywords: heavy metal analyses; wastewater; electrospark method; water treatment; galvanic processes

1. Introduction

Wastewaters that contain heavy metals present an environmental risk. Anthropogenic sources of biosphere pollution by heavy metals include ferrous and nonferrous metallurgy enterprises (aerosol emissions, industrial discharges), mechanical engineering (galvanic baths, copper plating, nickel plating, chrome plating, cadmium plating), battery recycling plants, road transport, and so on [1–6]. Heavy metals enter into reservoirs with discharges from mining and metallurgical enterprises, as well as chemical and light industry enterprises, where their compounds are used in various technological processes. So, many chromium and nickel salts are used to galvanically coat the surfaces of metal products. Compounds of copper, zinc, cobalt, and titanium are used in the production of dyes, etc. Issues of water quality and status are among the priorities in the environmental policy of European countries [7–11]. Therefore, the question of finding effective wastewater treatment methods containing heavy metals is an urgent issue. There are different physical, chemical, biological,

electrochemical, and galvanocoagulation methods that are used for the treatment of wastewater [12,13]. The most common method of wastewater treatment is a reagent. Its advantages are the relatively high productivity and low energy consumption, and its disadvantages are low efficiency (up to 10% of heavy metal salts remain in solution). The traditionally used biological treatment processes need a large operational area and much time. Chemical coagulation processes are very slow, with a large amount of sludge. The disadvantage of ion exchange techniques is the high cost of purification. Electrocoagulation and electroflotation are promising electrochemical methods. The advantages of the electrocoagulation method are its environmental friendliness, versatility, low operating costs, low energy requirements, minimal chemical additives, and sludge minimization. In particular, it is used for wastewater treatment in the printing, textile, meat processing, oil refining, dairy, and leather industries, in agriculture, and in the service sector: car washes, restaurants, cafes, laundries, etc. Among many methods, coagulation methods for wastewater treatment from heavy metal ions are the most effective and used [14,15]. Reagent coagulation is based on the hydrolysis of polyvalent metal salts (aluminum and iron), which lead to the formation of highly dispersed oxides and hydroxides of these elements, which can actively adsorb impurities of heavy metal ions from wastewater. Significant disadvantages by the reagent purification method are the additional pollution of effluents due to the introduction of cations and anions of reagents, obtaining dehydrated and not recyclable sludge. Coagulants based on iron and aluminum are capable of forming multiply charged multinuclear complexes; therefore, such coagulants have good adsorption characteristics [15,16].

In electrocoagulation methods of galvanic wastewater treatment, adsorption-active hydroxides of iron or aluminum are formed by electro erosion by the electrolytic dissolution of steel or aluminum anodes, respectively. In this case, phenomena such as water electrolysis, particles' polarization, electrophoresis, redox processes, and the interaction of electrolysis products with each other can occur in the electrolyzer [17–20]. Galvanic coagulation consists of passing wastewater through a galvanic coagulator that contains an active anode and cathode mixture, for example, iron and aluminum chips, iron chips, coke [13], etc. Various investigators have been successfully applied the electrocoagulation process (EC) to remove soluble ions of heavy metals from solutions [21,22]. During the electrocoagulation process, the coagulant continuously enters the contaminated water. This method makes it possible to remove contaminants from wastewater, in particular the metals mercury, cobalt, copper [23–25], chromium [26–29], zinc, cadmium, nickel [30–33], arsenic, strontium, cesium [34,35], nitrate, phosphate, sulfide, sulfate, sulfite [36–38], fluoride, boron [39,40], chemical oxygen demand, clay minerals, and organic substances [41–44].

Electro-blasting water treatment is used to intensify coagulation processes, i.e., to accelerate a sediment formation. The essence of this method is to pass through the wastewater short-term electrical pulses with electrodes immersed in the solution. Pulsed electric discharge in a liquid is accompanied by a sharp increase in pressure (up to 100–200 MPa), exposure to strong electromagnetic and acoustic fields, cavitation, which creates a powerful flow of liquid, a sharp rise in temperature, and other effects. The discharge interval is practically a low-temperature plasma, which transmits energy to the treated medium. An electric discharge—in fact, an explosion in the aqueous phase—causes complex physicochemical processes in it, which lead to the acceleration of the coagulation of colloidal and suspended substances, as well as the precipitation of suspensions and chemical compounds. A schematic diagram of the discharge–pulse treatment of the liquid is shown in Figure 1. In practice, the electrode system can be placed directly in the pipelines through which industrial effluents are pumped. The electric discharge occurs sequentially from one electrode pair to another. The processing model is selected so that after the operation of the last pair of electrodes, work was ready for the first pair. Water treatment is continuous. The mode of processing depends on the pipe section, a flow speed and necessary sanitary indicators of treatment. All purified water has passed through the zone of high-impulse activation.

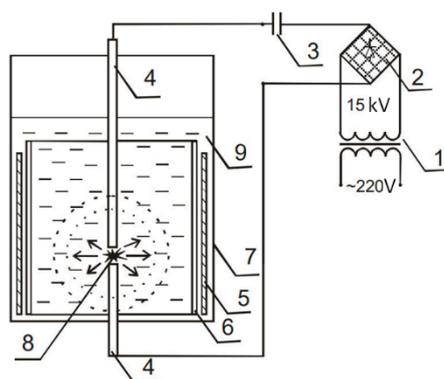


Figure 1. A schematic diagram of the discharge-pulse treatment of the liquid. 1—step-up transformer; 2—diode bridge; 3—capacitor; 4—electrodes; 5—treated fabric; 6—cylindrical mesh; 7—reactor vessel; 8—discharge zone; 9—liquid.

The plant for the electric blasting of wastewater is not characterized by high energy consumption, does not require excess costs to ensure the safety of service, and has a relatively small size. The method can accelerate the deposition by almost 7–8 times and significantly reduce the processing time. The positive effect of the method on the deposition rate of solid suspensions is explained by the increased coagulation of mineral particles due to the squeeze of the electric double layer under the action of the high-voltage electric discharge as a result of two opposing forces: electrostatic repulsion and van der Waals gravity.

Electrospark discharge in metal-containing reactors is an effective method for producing coagulative active metal oxides and hydroxides [45–48]. The method is proposed as an alternative to existing methods for the cleaning of galvanic wastewater. It was shown that it is possible in principle to purify multicomponent wastewater from heavy metal ions, namely Cr^{6+} , Ni^{2+} , Cu^{2+} , and Zn^{2+} [44]. In this case, attention is directed to expanding the capabilities of the method, which is aimed primarily at the component treatment of galvanic wastewater, by increasing the operating voltage from 300–600 V to 3–15 kV and by using monometallic metal loading (granules of one metal) [14]. This allowed the treatment of concentrated galvanic wastewater containing Cr^{6+} to 1000 mg/dm^3 . However, the further implementation of this method turned out to be economically inexpedient due to the high cost and limited resource of high-voltage equipment, its increased danger, and its low process productivity.

The objective of the work is to study the influence of such technological parameters (specific energy, characteristics of the electric pulses and its frequency, schemes of a channel of purified water) on the efficiency of the treatment process of multicomponent galvanic wastewater in reactors with metallic combined loading using low-voltage (up to 1000 V) electrical equipment.

2. Materials and Methods

The essence of the electrospark method is to pass through wastewater short-term electrical pulses with electrodes immersed in the solution (Figure 2). Pulsed electric discharge in a liquid is accompanied by a sharp increase of pressure (up to 100–200 MPa), exposure to strong electromagnetic and acoustic fields, cavitation, which creates a powerful flow of liquid that converges and diverges, a sharp rise in temperature, and so on. In this case, the discharge gap is practically a low-temperature plasma, which transmits energy to the treated medium.



Figure 2. A typical type of single electrospark.

Electric discharge—in fact, an explosion in the aqueous phase—causes complex physicochemical processes that lead to the decomposition of organic impurities present in wastewater, improving the coagulation of colloidal and suspended solids, as well as the precipitation of suspensions and chemical compounds.

The raw material for the treatment is real wastewater after various galvanic production operations, which is supplied to the treatment facilities of a machine-building enterprise. Galvanic wastewater is multicomponent composition containing ions Cr^{6+} , Ni^{2+} , Cu^{2+} , and Zn^{2+} .

A mixture of metals such as aluminum and iron granules with diameters from 4 to 6 mm is selected as the material for metal loading (Figure 3). This choice is due to the following reasons:

- the positive result of complex water purification from heavy metal ions during high-voltage electric discharges in reactors, granular metal loading, and the use of these materials [46];
- the traditional use of iron or aluminum electrolytic soluble anodes during the implementation of the electrocoagulation method for the treatment of galvanic wastewater [15];
- experience in stabilizing spatially distributed discharges in a layer of aluminum and iron granules using low-voltage (up to 1000 V) electrical equipment [49,50].

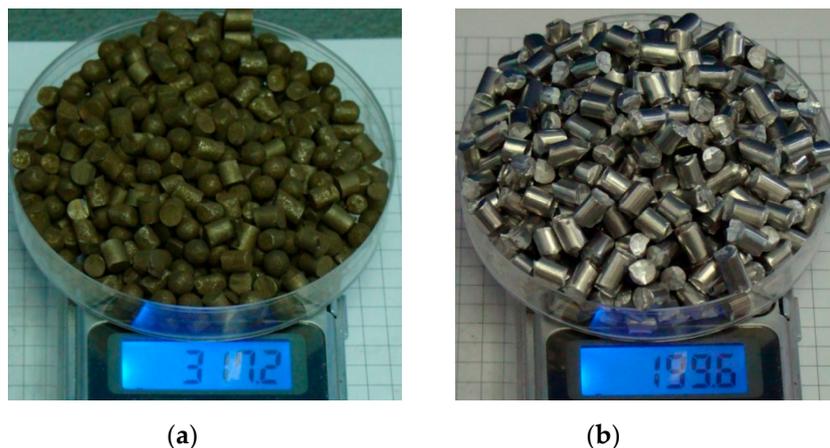


Figure 3. The appearance of metal-loading granules: (a) iron granules; (b) aluminum granules.

The layer of metal-loading granules in the form of a rectangular parallelepiped is characterized by the following sizes: length (l)—the distance between the electrodes; width (b), which is equal to the width of the electrodes, and height (h), which varied depending on the scheme of implementation of the fluid flow. The distance between the electrodes is chosen in such a way as to ensure a stable breakdown along the shortest chain of contacts between the granules from one electrode to another at a given capacitance of the capacitor bank in order to optimize the phase composition of electro erosion particles [49–51].

The discharge current and voltage at the inter-electrode gap are recorded with an OWON XDS 3202E oscilloscope, using a divider and shunt of our own manufacture. There are many variants of circuit solutions of sources of electric discharge pulses based on semiconductor switches. To solve the problems of this work, the basic scheme was chosen without the use of energy efficiency, feedback control, etc. This scheme eliminates any effects on the cleaning results, which is very important. The electric circuit based on semiconductor switches (a push–pull charge/discharge) was chosen to implement low-voltage electric discharges between the metal loading granules (Figure 4). The facts were formed by the signals of the rectangular pulse generators (PG1, PG2), which were connected by the output/input of synchronization, either with a preset frequency of the master oscillator (PG1) or external launching (S). Pulse isolation transformers (IT) were used to decouple the power and control circuits.

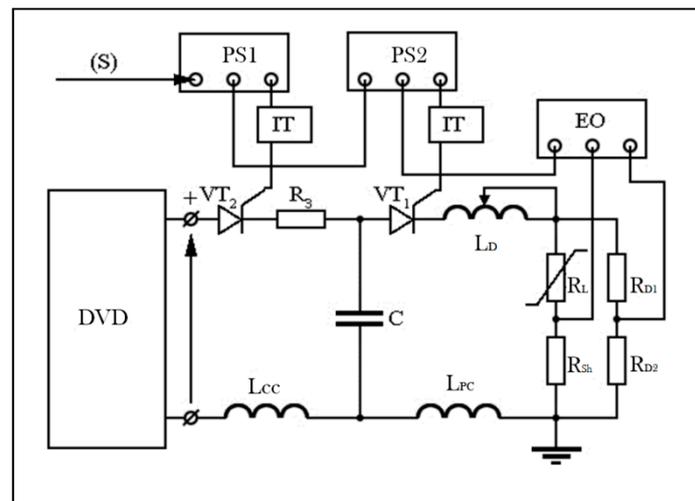


Figure 4. The electrical circuit of the experimental low-voltage source of discharge currents.

The experimental reactor (Figure 5a, position 4) is made in the form of a rectangular hollow parallelepiped with flat steel electrodes (position 7), a perforated bottom (position 9), and a prism-shaped cavity under it. The tank (position 1) was filled with galvanic wastewater. The shut-off valve (position 6) was set to the turned-off position. When the pump (position 2) was turned on by a valve (position 3), the required volumetric flow rate of the liquid was established. The volume of the reactor is about 20 dm³, and the tested hydraulic retention times is about 300 s.

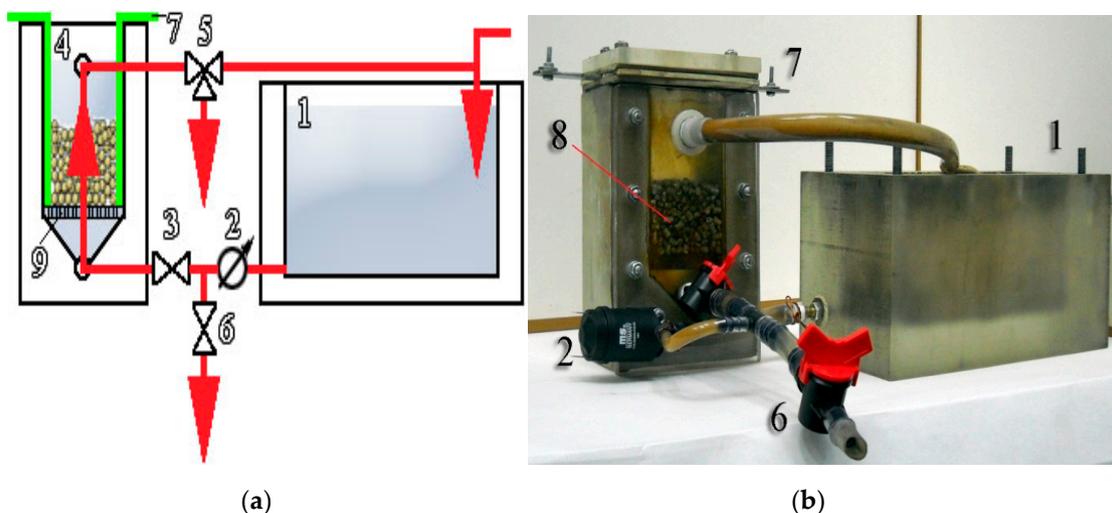


Figure 5. (a) The hydraulic scheme and (b) the appearance of the reactor.

The galvanic wastewater entered the reactor passing through the holes of the perforated bottom, then through the metal loading layer (Figure 5b, position 8), in which multichannel spark discharges between metal granules formed at a given frequency. After that, through the nozzle, depending on the position of the valve (Figure 5a, position 5), the treated galvanic wastewater was poured into a container for the next analysis or returned to a repeated treatment cycle.

The determination of the content of heavy metals in the start and treated water was carried out in accordance with the current regulatory documents [52–54]. The hydrogen index (pH) of the start galvanic wastewaters and the treated liquid was measured by an Ionomer I-160 M.

The efficiency of the galvanic wastewaters treatment process was studied by varying the specific processing energy, the amount of stored energy, the pulse parameters, and the height of the metal load.

3. Results

The peculiarity of the experiment was that the electro erosion powder, which is formed during the electrospark process, is a coagulant. At volumetric fluid flow rates of 50 dm³/h, the system is in a suspended state. Auto sedimentation is observed (Figure 6) immediately after sampling (order of time: min). The color of the liquid was changed from light yellow to transparent. To visualize the effect of self-sedimentation, i.e., the formation of a large amount of electro erosion powder, the treatment was performed for a long time: about 3 h with looping of the fluid flow.

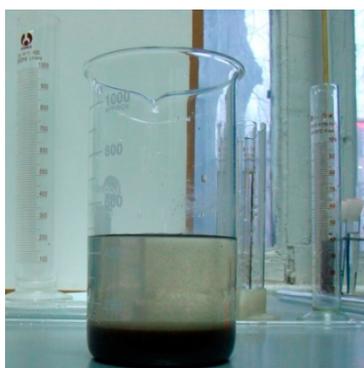


Figure 6. Deposition of electro erosion powder after sampling.

A sampling of wastewater from the reactor was carried out immediately after the end of each treatment. The wastewater was filtered using F-type filter paper. The volume of the sample filtrate for chemical analysis was 1.5 dm³.

The content of heavy metal ions in wastewater generated by the enterprise is not constant. Therefore, for all through treatments, one source material was used: sewage selected at treatment plants (Table 1).

Table 1. The content of heavy metal ions in the source wastewater (basic galvanic discharge).

pH	Color	Zn ²⁺ , mg/dm ³	Cr ³⁺ + Cr ⁶⁺ , mg/dm ³	Cu ²⁺ , mg/dm ³
7.45	light yellow	0.26	1.27	0.06
6.00	light yellow	0.06	4.69	5.28

The study also used another concentrated content of harmful substances source material (Table 1, second line) of the same galvanic origin, which was selected at treatment plants at other times. So, the source material for treatment is natural sewage of galvanic production from different streams of a machine-building enterprise.

The choice of the range of variation of parameters and processing schemes is based on the following assumptions. The specific energy is varied taking into account the data given in paper [17], which relates

to the purification from highly concentrated solutions of heavy metal ions (from 8500 mg/dm³—total content of heavy metals and up to 600 mg/dm³ Cr⁶⁺, respectively) with high-voltage electric discharges in reactors with granular metal loading in a column electrocoagulator.

We used data on the electrospray method for producing highly dispersed powders of metals and alloys to select the value of the pulse energy (W_p) [50]. This process can be implemented with pulse frequencies (f) up to several kHz using capacitor banks with capacities from 10 to 120 μ F. For research, we chose a capacitance corresponding to the middle of the range: 65 μ F. The charging voltage was determined experimentally. To do this, we first set the charging voltage (U_0), which corresponds to the extremum of the relative energy release in the interelectrode gap of the dispersion reactor to the stored energy of the capacitor bank.

$$\eta_W = \frac{W_p}{W_0} = \frac{\int_0^{\tau_1} i(t)u(t)dt}{W_0} \quad (1)$$

where W_p is the energy that is released in the interelectrode gap of the reactor during one discharge pulse, J; $W_0 = CU_0^2/2$ is the energy stored by the capacitor bank to the beginning of the discharge, J; and τ_1 , $i(t)$, and $u(t)$ are the discharge time, discharge current (time dependence), and the voltage on the electrode gap (time dependence), respectively, which are calculated from the results of oscillography (Figure 7).

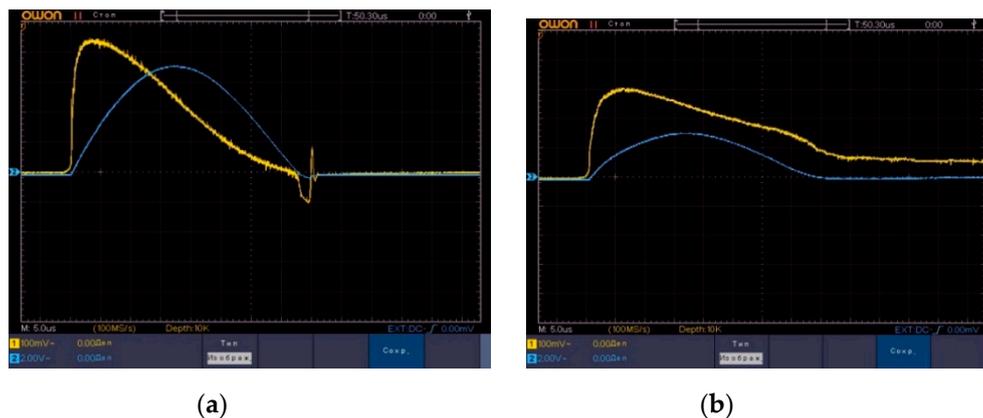


Figure 7. Oscillograms of the discharge current (blue curve) and voltage on the interelectrode gap (yellow curve) for $\eta_W \sim 0.95$ (a) and $\eta_W \sim 0.8$ (b).

Further increase of the charging voltage translates the discharge into the oscillating phase, which is very rarely used in the implementation of the electro spark method, both for fundamental reasons and for technical reasons, as there is a need to use a high-frequency diode connected to the switch. The maximum value of η_W can be equal to 0.9–0.95 (Figure 7a). However, this situation is idealized, and its practical implementation requires constant adaptive regulation of the charge voltage level. As part of the study, this does not allow adequately controlling the energy losses in the elements of the discharge circuit, as well as the specific energy consumption for galvanic purification. To reliably assess the effectiveness of galvanic purification cleaning, the value of η_W was brought to the values of 0.8–0.85 (Figure 7b) due to the gradual decrease of the charging voltage. The conditions η_W approximately 0.8–0.85 corresponded to the values of $W_p = 3.6$ J and $W_0 = 4.5$ J, which were chosen for experimental treatments of galvanic discharges. The efficiency of galvanic purification in the process of changing the specific processing energy is presented in Table 2. The concentration of heavy metals in the initial solution is less than the maximal permissible concentrations (MPC) for the region (Ukraine). So, the concentration of Zn²⁺, Cr⁶⁺ + Cr³⁺, and Cu²⁺ ions are 0.26 mg/dm³, 1.27 mg/dm³, and 0.06 mg/dm³ (MPC are 1 mg/dm³, 2.5 mg/dm³, and 2.5 mg/dm³), respectively. A comparative analysis of the treatment results with the specific treatment energy change is given in Table 3, where Δ_n is the decrease

in the concentration of metal ions after electrospark treatment relative to the initial concentration in the source wastewater, in absolute units, mg/dm^3 ; n is the number of the processing option; Kr_n is a multiplicity of purification, i.e., the ratio of the initial concentration of heavy metal ions to the concentration after treatment.

Table 2. The efficiency of galvanic purification in the process of changing the specific energy.

Specific Energy, kJ/dm^3	Zn^{2+} , mg/dm^3	$\text{Cr}^{3+} + \text{Cr}^{6+}$, mg/dm^3	Cu^{2+} , mg/dm^3	pH	Color
-	0.26	1.27	0.06	7.45	light yellow
130	0	0.0002	0.003	7.34	colorless
65	0.028	0.0023	0.010	8.19	colorless

Table 3. Comparison of purification results with changing the specific processing energy.

Value	Zn^{2+}	$\text{Cr}^{3+} + \text{Cr}^{6+}$	Cu^{2+}
Δ_1 mg/dm^3	0.26	1.27	0.06
Δ_1 mg/dm^3	0.23	1.27	0.05
Δ_1/Δ_2	1.12	1.00	1.14
Kr_1	-	6350	20
Kr_2	9.29	552	6

Analysis of the purification results showed that for all metals, their concentration was reduced to values below the MPC.

During the study of the galvanic purification effectiveness, when changing the pulse processing parameters, experiments were performed with long and short-term pulses with different power levels. Pulse parameters are the duration and maximum values of the power of the bit pulse. For high-voltage discharges in water, the approach of dividing them into two groups is widespread, each of which is characterized by a set of common features of the introduction of electrical energy into the spark load. These are short-term and long-term discharges.

The condition of division is the duration of the first half-cycle of the discharge current: up to 40 μs and more than 40 μs , respectively. Changing the pulse processing parameters under the condition of fixing the energy of a single discharge pulse leads to redistribution between the granules' material. As a result of heating under the action of the discharge current, the material of the granules passes into the gas and liquid phases with subsequent condensation. There is a redistribution of the micro- and nanopowder of the metal formed in the liquid, by dispersion, morphology, and other features, which leads to a change of its coagulation properties.

The characteristics of the electric discharge plasma formed between the granules also change. Fixation of the total galvanic processing energy when changing the pulse parameters of the discharge allows you to set more efficient parameters for purification efficiency, namely: short-term discharge pulses with a higher maximum power, or longer with a lower maximum power.

The pulse processing parameters in the bit circuit were increased in 25 times in relation to its inductance. The values of W_p and W_0 have been left as above (3.6 J and 4.5 J, respectively). So, the discharge duration is increased from 38 to 200 μs .

The effectiveness of galvanic purification when changing the pulse processing parameters is given in Table 4. As can be seen from the data on the concentrations of heavy metal ions after treatment (Table 4), changes in the efficiency of purification with a significant change in the pulse parameters did not occur.

Table 4. The efficiency of galvanic purification in the process of changing the duration of pulse discharge.

Discharge Duration τ_1 , μs	Zn^{2+} , mg/dm^3	$\text{Cr}^{3+} + \text{Cr}^{6+}$, mg/dm^3	Cu^{2+} , mg/dm^3	pH	Color
-	0.26	1.27	0.06	7.45	light yellow
38	0	0.0002	0.003	7.34	colorless
200	0	0.0002	0.003	7.33	colorless

This conclusion has practical value. The change in the pulse parameters of the treatment due to the increase in inductance has almost no effect on the purification efficiency. There is a possibility of a serial (in the electrical sense) connection of several purification reactors to one source of discharge current pulses without any loss of purification efficiency. The “softening” of the working conditions of the electric equipment can promote an increase of its resource, reducing the intensity and regulation of the frequency spectrum of electromagnetic interference, etc.

Note that by visual signs, the change in the temperature of the discharge plasma between the granules occurred (the color temperature changed). This aspect requires further research using high-speed photo recording and may be useful in determining priority mechanisms for electro spark cleaning.

The effectiveness of processing when changing the frequency of discharge pulses was studied by fixing the volumetric speed of the fluid flow. To solve this problem, two galvanic treatments were performed. The volumetric flow rate of the liquid was recorded at 50 dm³ h. Two frequencies of discharge pulses were established, which were correlated as 1/2. The first frequency is the same at which the results described above are obtained. The specific processing energy was chosen between two values of 130 and 65 kJ/dm³ (namely, 90 kJ/dm³) and was also recorded. The energy released in the interelectrode gap of the reactor during one discharge pulse and the stored energy remained unchanged: $W_p = 3.6$ J and $W_0 = 4.5$ J (Tables 5 and 6).

Table 5. The effectiveness of galvanic purification on changing the discharge pulse frequency.

Discharge Pulses Frequency	Zn ²⁺ , mg/dm ³	Cr ³⁺ + Cr ⁶⁺ , mg/dm ³	Cu ²⁺ , mg/dm ³	pH	Color
-	0.26	1.27	0.06	7.45	light yellow
1×	0	0.0002	0.007	8.00	colorless
2×	0	0.0070	0.007	8.14	colorless

Table 6. Comparison of purification results when changing the pulse frequency.

Value	Zn ²⁺	Cr ³⁺ + Cr ⁶⁺	Cu ²⁺
Δ_1 mg/dm ³	0.24	1.27	0.05
Δ_1 mg/dm ³	0.19	1.27	0.05
Δ_1/Δ_2	1.25	1.00	1.00

The results of the experiments (Tables 5 and 6) indicate the possibility of increasing the productivity of galvanic discharge cleaning by the electrospark method by increasing the discharge pulse frequency. Such an increase is possible up to certain limit values and has certain limitations on the initial concentrations of the pollutant. Addressing these issues requires further research. It should be noted that some differences in performance are still present and relate to the deep purification of galvanic discharge from zinc ions in the region of low concentrations.

Next, we investigated the effectiveness of galvanic wastewater purification when changing the scheme of implementation of the fluid flow (longitudinal/transverse). To realize the longitudinal fluid flow, the condition $h > l$ was observed, i.e., the fluid flow was realized along with the larger size of the metal loading layer. To organize the transverse flow of the liquid, the height of the layer of granules was reduced to comply with the condition $h \leq l/2$ (Tables 7 and 8).

Table 7. The effectiveness of galvanic wastewater purification with changing the scheme of fluid flow implementation.

Fluid Flow	Zn ²⁺ , mg/dm ³	Cr ³⁺ + Cr ⁶⁺ , mg/dm ³	Cu ²⁺ , mg/dm ³	pH	Color
-	0.26	1.27	0.06	7.45	light yellow
$h > l$	0.00	0.0002	0.003	7.34	colorless
$h \leq l/2$	0.15	0.0026	0.015	7.84	colorless

Table 8. Comparison of purification results with changing the scheme of fluid flow implementation.

Value	Zn ²⁺	Cr ³⁺ + Cr ⁶⁺	Cu ²⁺
Δ_1 mg/dm ³	0.26	1.27	0.06
Δ_1 mg/dm ³	0.11	1.27	0.05
Δ_1/Δ_2	2.36	1.00	1.20

Analysis of the results (Tables 7 and 8) shows that the length of the liquid path through an active layer (the layer where the discharge plasma is formed between the granules and the processes phase transitions of the granule material occur) may be important (in this case, the length is h). That is, the presence of micro- and submicron-powder coagulants in the liquid is not the only purification mechanism. This circumstance is especially related to the processes of zinc and copper ions.

The conclusion about technological implementation is obvious. Increasing the height of the layer of granules arbitrarily is not possible. In the lower layers of granules, under the action of weight loading, spark channels cease to be formed, the welding of granules occurs more often, and energy losses increase. It is necessary to divide one reactor into several sections located one above the other. This is possible through the use of dielectric perforated jumpers mounted horizontally. In each section, the maximum possible height of a layer of granules has been provided.

The influence of the energy in a pulse on the degree of galvanic wastewater purification at a fixed specific energy ($W = 130$ kJ/dm³) and a slight change in the pulse duration (from 38 to 40 μ s) is presented in Table 9.

Table 9. Influence of energy in a pulse on the degree of purification of galvanic wastewater.

The Stored Energy in a Pulse, J	Zn ²⁺ , mg/dm ³	Cr ³⁺ + Cr ⁶⁺ , mg/dm ³	Cu ²⁺ , mg/dm ³	pH	Color
-	0.26	1.27	0.06	7.45	light yellow
4.5	0.00	0.0002	0.003	7.34	colorless
5.5	0.04	0.0017	0.005	7.96	colorless

As can be seen from Table 9, the increase in energy in the pulse only leads to deterioration in the purification of metal ions in the low concentration area. Since a multiple increase in the capacity of the capacitor bank leads to such problems, the increase in energy in the pulse in this way is impractical for solving the problems of galvanic purification.

4. Discussion

Analysis and comparison of the Table 10 data allow drawing the following conclusions. Flow-through treatment of galvanic wastewaters to MPC standards using the electrospark method, granular metal loading, and a low voltage (up to 1000 V) source of discharge currents is possible and technologically feasible. This electrospark method allows achieving high results of wastewater treatment from galvanic industries from heavy metals. The achieved degree of galvanic wastewaters purification in the case of moderate concentrations of heavy metal ions (Zn²⁺, Σ Cr, Cu²⁺) is higher, sometimes by several times in comparison with the MPC standards in different countries of the world.

Table 10. The maximal permissible concentrations (MPC) of the studied metals in galvanic wastewaters in different countries.

Country	Zn ²⁺ , mg/dm ³	Cr ³⁺ , mg/dm ³	Cu ²⁺ , mg/dm ³
USA	1.48	-	2.07
EU	0.50	0.50	0.50
Ukraine	1.00	2.50	2.50
Belarus	5.00	2.50	1.00
Russia	2.00	1.00	0.50

The main influence on the degree of galvanic purification, with the correct choice of the parameters of the discharge pulse, has specific processing energy. For moderate concentrations of pollutants, it may be less than 65 kJ/dm^3 . Other parameters are a tool for purification processes or a means of regulating the modes of operation of electrical equipment.

The issues of checking the effectiveness of galvanic purification at industrial frequencies of discharge pulses are promising, i.e., 1 kHz in the flow (single-flow) implementation to identify threshold, critical, undesirable, or positive effects. Such effects will occur at pulse frequencies above 100 Hz. The introduction of the method into the technological process at lower frequencies is impractical from the standpoint of productivity.

5. Conclusions

Research has been carried out on the purification of multicomponent galvanic wastewaters by the electric spark method using combined metal loading (Fe, Al) and low-voltage (up to 1000 V) equipment. It is shown that the degree of purification depends on the specific energy and the height of the metal loading of the reactor, and it weakly depends on the pulse energy and the speed of its input. The electrospark method gives positive results in relation to improving water quality. The main influence on the degree of galvanic wastewaters' purification under the conditions of choosing the parameters of the discharge pulse is the specific energy, which at moderate concentrations of pollutants can be less than 65 kJ/dm^3 , and metal loading height. The concentrations of heavy metals (Zn^{2+} , $\text{Cr}^{6+} + \text{Cr}^{3+}$, Cu^{2+}) in the treated water are significantly lower than their MPC values regulated in different countries. The electrospark method is effective in terms of accelerating the rate of wastewater treatment from heavy metals. The solution to the issues of checking the effectiveness of wastewater treatment by the electrospark method under the conditions of real production is promising.

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