

Review

# The Potential of CO<sub>2</sub> Capture and Storage Technology in South Africa's Coal-Fired Thermal Power Plants

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**Abstract:** The global atmospheric concentration of anthropogenic gases, such as carbon dioxide, has increased substantially over the past few decades due to the high level of industrialization and urbanization that is occurring in developing countries, like South Africa. This has escalated the challenges of global warming. In South Africa, carbon capture and storage (CCS) from coal-fired power plants is attracting increasing attention as an alternative approach towards the mitigation of carbon dioxide emission. Therefore, innovative strategies and process optimization of CCS systems is essential in order to improve the process efficiency of this technology in South Africa. This review assesses the potential of CCS as an alternative approach to reducing the amount CO<sub>2</sub> emitted from the South African coal-fired power plants. It examines the various CCS processes that could be used for capturing the emitted CO<sub>2</sub>. Finally, it proposes the use of new adsorbents that could be incorporated towards the improvement of CCS technology.

**Keywords:** CO<sub>2</sub> capture and storage; climate change; coal-fired power plants; South Africa

## 1. Introduction

Over the past decade, global carbon dioxide emissions have significantly increased by approximately 2.7%, which is 60% more than that of the late 20th century [1]. South Africa is among the countries that are highly affected by carbon emissions; the country is the leading CO<sub>2</sub> emitter in Africa and is ranked amongst the top twelve emitters in the world [2]. The country's emissions are intensified by the energy and manufacturing sectors, which release huge amounts of CO<sub>2</sub> into the atmosphere. For instance, an estimated 367.6 million tons of CO<sub>2</sub> were emitted by South Africa in 2011; this value increased to 476 million tons in 2015. Most of the country's CO<sub>2</sub> emissions are derived from the burning of coal [3]. Thus, future projections show that carbon emissions will continue to increase unless there is acceleration in the formation of carbon-neutral technologies that will reduce this problem or incorporate CO<sub>2</sub> capture technologies from major emitting sources, such as the coal-fired thermal power plants.

Moreover, there has been a significant decline in the country's agricultural output due to low rainfall seasons and temperature rise, which is caused by climate change [4]. Many parts of South Africa are experiencing drought and are therefore no longer suitable for commercial farming. Studies have reported that carbon emissions if not curtailed will have the following devastating effects: (i) South Africa's coastal region is expected to have an atmospheric temperature rise of 2 °C by 2050 and 4 °C by 2100; (ii) the country's interior region is also expected to increase by 4 °C in 2050 and 7 °C in 2100; (iii) this will affect the country's food security; (iv) alien invasive plants might increase and negatively affect the country's water resources; (v) this will likely exacerbate health issues due to droughts and floods; diseases, such as malaria and cholera, have been linked to extreme weather

patterns; and (vi) bushlands and various commercial plantations will be vulnerable to wildfires [4]. It is estimated that in order to reduce global warming or limit global average temperatures by 2 °C in 2050, global CO<sub>2</sub> emissions should be reduced by at least 50% [5]. Currently, a range of options that could help to mitigate climate change are being considered worldwide, including carbon capture and storage technology (CCS) [6]. CCS technology can contribute towards the reduction of carbon emissions, thus allowing the continual use of coal-dependent energy markets, like South Africa. The aim of CCS is to capture carbon emissions from point sources, such as coal-fired power plants and industrial processes, to prevent it from being released into the atmosphere [7]. The captured CO<sub>2</sub> can be used for enhanced oil recovery; it can be utilized in chemical and beverage industries for the preservation of drinks. Alternatively, it can be stored in underground rocks or deep ocean waters [8]. Devilliers et al. [9] highlighted that South Africa's economy is primarily dependent on coal reserves for energy supply, and therefore, its utilization is envisaged to continue for the next three decades. In addition, 75% of the country's primary energy supply and 93% of the electricity are derived from coal reserves. The drawback about coal reserves is that they are escalating the country's CO<sub>2</sub> emissions and consequently contributing to environmental degradation, i.e., more than 80% of the country's carbon footprint is produced from the coal-fired power plants [10,11].

The integration of clean and sustainable energy technologies in South Africa requires solutions that deal with high CO<sub>2</sub>-emitting sources, such as coal-fired thermal power plants [12]. This implies that sustainability assessment of CCS technology is an important aspect of climate policy, especially in highly industrialized countries, like South Africa [13]. Nonetheless, CCS has some technical and economic barriers that must be addressed before it can be implemented on the industrial scale, which include high capital incentives and leakage problems. CCS is also hindered by economic, social and legal barriers [14]. Besides, some countries have limited geological storage capacity for CO<sub>2</sub> capture [15]. The development of CCS is still in its infancy in South Africa, implying that there are no frameworks for this technology [16]. Against this background, this review examines the potential of CCS technology for mitigating CO<sub>2</sub> emitted from coal-fired thermal power plants in South Africa. It investigates the various CCS methods that could be applied to capture the CO<sub>2</sub> generated from these coal-fired power plants. Lastly, it recommends the use of new adsorbents that could be utilized towards the implementation of CCS systems in South African coal-fired thermal power plants and also the retrofitting of capture devices into the existing coal-fired thermal power plants.

## 2. Technological Routes for CO<sub>2</sub> Capture

The efficient capture of anthropogenic CO<sub>2</sub> emitted from large point sources such as power plants, is seen as an important strategy that can be used to significantly reduce the level of atmospheric CO<sub>2</sub>. This is because the generation of CO<sub>2</sub> is inherent in the combustion of hydrocarbon fuels, which is a daily occurrence in South Africa's coal-fired thermal power plants [17–28]. Currently, pre-combustion, post-combustion and oxy-fuel combustion captures are the three basic technological routes used to capture CO<sub>2</sub> [29–36]. These technological routes are discussed below on a broader note and related to their possible implementation in South African coal-fired thermal power plants.

### 2.1. Post-Combustion

This capture technology involves the separation of CO<sub>2</sub> from waste gas streams after the conversion of the carbon source of CO<sub>2</sub> [37–40]. This method is very effective at capturing CO<sub>2</sub> from power plants. It is also known as post-conversion capture, but when applied in power plants, it is referred to as post-combustion capture [41]. The post-combustion method of CO<sub>2</sub> capture includes solvent absorption, solid sorbent adsorption, membranes and cryogenic separation [42,43]. Out of all of these options, CO<sub>2</sub> absorption by monoethanolamine is extensively used and referred to as a very mature technology [44]. The post-combustion capture is still considered as the most mature capture route, because it has a good reputation within many industrial applications and also a better operational flexibility [45–48]. The post-combustion capture technology is mostly used in power

plants because it has the possibility of retrofitting in existing power plants, such as the South African coal-fired thermal power plants. The South African energy sector is mainly driven by coal, and the sustainable use of coal in these power plants must continue in order to avoid escalating the price of electricity. On this note, retrofitting CO<sub>2</sub> capture devices in the already existing coal-fired power plants in South Africa becomes a viable option in order to curtail CO<sub>2</sub> emission to the atmosphere. Since the post-combustion technology allows for possible retrofitting, it becomes a promising technology that can be implemented in the South African coal-fired thermal power plants with no associated increase in the price of electricity, because coal will still remain the primary source of electricity in the country, and carbon emissions from this sector will be reduced drastically.

## 2.2. Pre-Combustion

The pre-combustion capture refers to capturing CO<sub>2</sub> generated as an undesired co-product of a conversion process [49–54]. In the pre-combustion capture, fuel from the power plant is reacted with oxygen to generate a syngas mixture, which is carried out in the gasification step [55–60]. Carbon dioxide is then reacted with steam in the second step to produce CO<sub>2</sub> and H<sub>2</sub> before the CO<sub>2</sub> is finally separated using a physical or chemical absorption process [61–65]. The pre-combustion capture technique incurs high costs for chemical solvent regeneration. However, for physical solvents, the costs are lower because they are regenerated by pressure reduction instead of using heat. Physical solvents are most suitable for use at high operating pressure and low temperatures, and it is more efficient when the CO<sub>2</sub> streams in the power plants are more concentrated [66–70]. In the context of CO<sub>2</sub> capture from the South African coal-fired power plants, the pre-combustion technology cannot be fully implemented because it has a high energy requirement with no option of retrofitting capture devices into existing power plants. This invariably means that the implementation of this technology will only be feasible in newly-built power plants and cannot be implemented in the already existing coal-fired thermal power plants in South Africa. This makes the pre-combustion CO<sub>2</sub> capture technology more expensive and difficult to implement in the South African power sector.

## 2.3. Oxy-Fuel

In the oxy-fuel combustion technological approach for CO<sub>2</sub> capture, flue gas consisting of pure oxygen is burnt. This technological route produces a flue gas stream that is highly saturated with CO<sub>2</sub> [71–76]. This technology also produces flame with an excessively high temperature because, theoretically, if fossil fuel (coal) is burnt in pure oxygen, much heat is produced [77–89]. The pure oxygen is produced by cryogenics. This technique is a modification of the pulverized coal-fired power plant in South Africa. It involves burning coal in nearly pure oxygen. The main advantage of the oxy-fuel CO<sub>2</sub> capture technique is that the flue gas is available at a high CO<sub>2</sub> concentration of approximately 75.7 mol%, thereby reducing compression costs and facilitating efficient CO<sub>2</sub> removal [90–104]. Although this technology appears promising if implemented for CO<sub>2</sub> capture in power plants, its possibility of implementation in the South African coal-fired power plants is quite slim because burning coal in pure oxygen instead of air on a large scale is very expensive. This will in turn increase the cost of electricity in South Africa. Therefore, it is not a suitable technological route for CO<sub>2</sub> capture in South Africa.

## 3. Separation Technologies during Post-Combustion CO<sub>2</sub> Capture

The preference of one technological route over others could be attributed to its ease of access, its possibility of the capture process, retrofitting to existing power plants, the maturity level of such a technological route and the period needed for the implementation of such technology [105]. Currently, there is a wide range of CO<sub>2</sub> capture and separation techniques from gas streams, which could be implemented in the South African coal-fired thermal power plants. They are based on physical and chemical processes, which include adsorption, absorption, cryogenic and membrane separation technologies. They are discussed below.

### 3.1. Cryogenic Separation

The cryogenic separation method for CO<sub>2</sub> capture is mainly based on the principle of condensation and cooling [106–110]. It is mostly applied in CO<sub>2</sub> capture systems where the gas streams contain a high concentration of CO<sub>2</sub>. The challenge about cryogenic separation is that it cannot be used in CO<sub>2</sub> capture from power plants because the power plants have a more dilute CO<sub>2</sub> stream [111,112]. Another setback is that this technology is energy intensive, i.e., it requires high amounts of energy for CO<sub>2</sub> separation. The concentration of CO<sub>2</sub> from South African coal-fired power plants is quite low, thereby rendering this CO<sub>2</sub> separation method difficult to implement in South Africa. Furthermore, cryogenic separation is best carried out at very low temperatures [113–119]. However, it is difficult to attain very low temperatures in coal-fired power plants that will be suitable for CO<sub>2</sub> capture using this technique. In most cryogenic separation processes, various components in gas mixtures are separated by a series of compression, refrigeration and separation steps [120]. Impurities lower the phase transition temperature of CO<sub>2</sub> in cryogenic separation processes to as low as  $-80$  °C. In this case, the refrigeration energy penalty increases substantially, and there is a huge possibility of CO<sub>2</sub> frost formation, which is a threat to equipment safety [120–123]. As a result, another technology that is economically viable and less energy intensive needs to be investigated.

### 3.2. Membrane Separation

Corti et al. [65] investigated CO<sub>2</sub> capture using membranes and concluded that the application of CO<sub>2</sub> capture from flue gases using membranes can only be competitive if the CO<sub>2</sub> concentration in the flue gas is higher than 10%. CO<sub>2</sub> capture using membranes operates on the principle of differences in the physical or chemical interaction between the CO<sub>2</sub> gas and the membrane for which the membrane is designed in such a way as to allow one gas to pass through faster than the other. The membrane modules can also be used as a gas absorption column or as a conventional membrane separation unit [124–128]. Although the membrane technology is relatively new, it requires high energy during separation, and it is widely known for its poor selectivity [129–135]. This poses a major disadvantage for CO<sub>2</sub> capture using membranes [136–138]. More so, this technology uses either inorganic ceramic membranes or organic polymeric membranes [139,140]. Ceramic membranes are quite expensive; however, it is very difficult to achieve a high degree of separation of CO<sub>2</sub> and a high purity of CO<sub>2</sub> at the same time with CO<sub>2</sub> in the flue gas through a single-stage ceramic or polymeric membrane. This is another major limitation of this CO<sub>2</sub> capture technology. This technology for post-combustion CO<sub>2</sub> capture is not suitable for implementation in the South African coal-fired power plants owing to its expensive nature if ceramic membranes are used and fouling in the case of polymeric membranes. Although the polymeric membranes have excellent selectivity and permeability for CO<sub>2</sub> capture, they have very low thermal stability and these membranes may be plasticized with the influence of CO<sub>2</sub> in the membrane. Therefore, application of the membrane technology for post-combustion CO<sub>2</sub> capture in power plants similar to the South African coal-fired thermal power plants is limited. Efficient capture technologies for CO<sub>2</sub> with low cost and high CO<sub>2</sub> capture potential, as well as selectivity need to be studied further as an alternative to the use of membranes for post-combustion CO<sub>2</sub> capture [141].

### 3.3. Absorption

The absorption technology involves the use of chemical solvents to capture CO<sub>2</sub>. It is a well-researched, robust, mature technology, and it is widely applied industrially. It is sub-divided into physical and chemical absorption. The former is temperature and pressure dependent, and the absorption of CO<sub>2</sub> from the flue gas occurs at high pressure and low temperature. Whereas in the latter, the absorption of CO<sub>2</sub> from the flue gas depends on the acid-base neutralization reaction using basic solvents [142–145]. The most commonly-used solvents for absorption of CO<sub>2</sub> from flue gases are basically amines [146], chilled methanol [147] and ammonia solution [148]. Even though the absorption technology is considered as a mature technology for CO<sub>2</sub> capture, the use of solvents for

this technology makes it corrosive and energy intensive due to high energy demands during solvent regeneration, and it is also expensive. The major limitation of this technique is that it uses liquid absorbents, which corrode piping in power plants; as such, it is not very suitable for adoption in the South African coal-fired power plants. Consequently, the adsorption technology that uses solid adsorbents for CO<sub>2</sub> capture is highly recommended for use in most South-African coal-fired power plants because it is not corrosive, the least expensive and has minimum energy requirements for the regeneration of the solid adsorbents [149]. Liquids, such as monoethanolamine, react readily with CO<sub>2</sub>, but because heat must be applied to remove CO<sub>2</sub> from the resulting liquid, the process is not economically viable for implementation in power plants. If the approach were applied to every power station in the South Africa, CO<sub>2</sub> capture could cost 30% of the country’s growth in gross domestic product each year [150]. Less expensive methods for capturing CO<sub>2</sub> and hydrocarbon emissions with minimal energy costs need to be investigated.

In order to reduce the high thermal energy consumption in the power plants, the concentration of monoethanolamine used during the post-combustion CO<sub>2</sub> capture process should be increased, and better corrosion inhibitors should be used to eliminate the high corrosive effect of monoethanolamine as a solvent for the CO<sub>2</sub> capture by absorption. Figure 1 shows a summary of various CO<sub>2</sub> capture and separation technologies for post-combustion CO<sub>2</sub> capture.

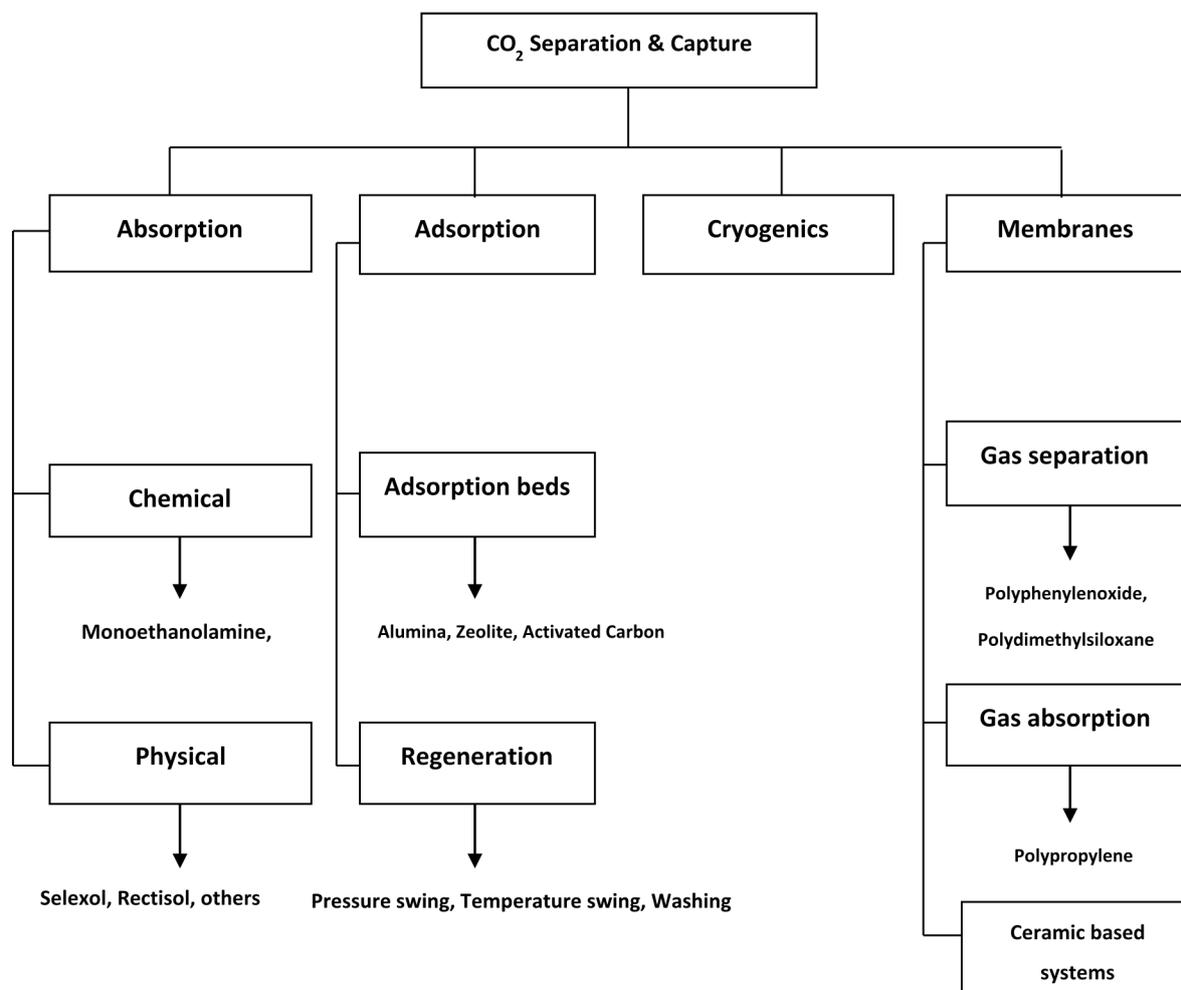


Figure 1. Different CO<sub>2</sub> separation and capture technologies for post-combustion CO<sub>2</sub> capture [82].

### 3.4. Adsorption

This technology is extensively used in chemical and environmental processes. It uses various adsorbents such as zeolites, activated carbon, polyaspartamide, metal oxides; porous silicates, metal organic frameworks and chitosan for CO<sub>2</sub> capture [151]. However, CO<sub>2</sub> capture by adsorption using activated carbon fibers and a carbon fiber component is regarded as an efficient approach when used in power plants [152]. Adsorption technology is attracting increasing attention due to its characteristics, which include minimum energy requirements, easy maintenance, simple operation and flexibility [153]. Amongst the adsorption processes reported in literature, temperature swing adsorption (TSA) is an advantageous process because it is inexpensive and uses less thermal energy. Therefore, it can reduce the operating costs if it is incorporated into coal-fired plants [154]. However, it requires longer cooling and heating times for CO<sub>2</sub> capture [155]. Meanwhile, vacuum swing adsorption (VSA) is more economically viable than pressure swing adsorption (PSA) in post-combustion for CO<sub>2</sub> capture [156]. Nevertheless, it has its own drawbacks, such as its sensitivity to feed gas temperature. More heat treatment might be needed to condition the flue gas before injecting it to the VSA plant; this affects the separation efficiency and process economics. PSA has been shown to be a promising technology in recent years because it can use a wide range of temperatures and pressures and requires minimum energy. Another advantage is that it requires low investment costs [157]. The adsorption technology also has its disadvantages, such as poor heat transfer, especially in packed beds, and slow kinetics, but the advantages of this technology far out-weigh its disadvantages [158]. There is potential in the implementation of this technology in the South African coal-fired power plants because of its ease of regeneration of the adsorbent using pressure modulation with reduced energy requirements.

## 4. The South African Power Sector

### 4.1. Power Generation in South Africa

South Africa has different options for power generation, which include nuclear energy, hydroelectric energy and wind energy [143]. South Africa is a main supplier of almost two-thirds of the electricity used in the African continent, and it falls among the top four least expensive electricity-producing nations globally. Over 90% of South Africa's electricity is generated from its coal-fired thermal power stations; 5% is generated from nuclear power plants, i.e., the Koeberg nuclear power station in Cape Town; and a further 5% of electricity is generated in hydroelectric power stations. However, there are only a few economic hydro sites that could be used for significant power generation in South Africa [147]. Approximately 52,017 MW of electricity are generated in South Africa, out of which 42,691 MW are generated from the combustion of fossil fuels, like coal. The remaining 9326 MW of electricity are generated from renewable, nuclear and hydro-electric stations, which are low CO<sub>2</sub>-emitting power generation sources [16].

### 4.2. An Outlook for the South African Coal-Fired Power Plants

The major CO<sub>2</sub>-emitting industries in South Africa are situated in the provinces of Gauteng, Mpumalanga and Free State. These regions form South Africa's coal mining sector, and most coal-fired powered plants are situated in these provinces, as well [17]. The electricity sector is predominantly dependent on coal energy, thereby making South Africa's coal-fired thermal power plants the largest CO<sub>2</sub> emitters in the country. Coal-fired power plants generate more than 90% of South Africa's electricity through the country's power parastatal, i.e., Electricity Supply Commission (ESKOM). Since 2008, new coal-fired power plants have been established in the coal-rich provinces of Mpumalanga and Limpopo. The Camden Power Station, which is located in Mpumalanga, generates about 156 megawatts of electricity, and it was established in 2008. The Grootveli Station was established in 2011 and has a production capacity of 1180 megawatts; it is also situated in Mpumalanga. Currently, two major coal-fired power plants are under construction, these include the Kusile and Medupi

power plants, which are expected to generate about 794–4764 megawatts of electricity supply in 2015–2020 [18].

The utilization of coal energy is expected to continue for the next decades because the country has enormous coal reserves, and this source of energy is inexpensive compared to other hydrocarbon fuels [19,20]. The country's power utility, Electricity Supply Commission (ESKOM) is listed amongst the highest CO<sub>2</sub>-emitting companies in the world due to its use of pulverized coal combustion plants for power generation [21]. In 2010, South African coal-fired thermal power plants were among the highest CO<sub>2</sub> emitters in the world, as depicted in Table 1, i.e., South Africa was ranked ninth and generated 218 million tons of CO<sub>2</sub>, with a total energy production of 215,000 GWh, out of which 93.4% was derived from coal. Therefore, mitigation strategies are highly emphasized by the South African government as a result of its heavy reliance on coal for electricity generation [21]. Consequently, the implementation of CCS technology is mandatory in South Africa's coal-intensive energy-grid in order to address the challenges of carbon emissions.

**Table 1.** World's largest CO<sub>2</sub> emitting coal-fired power plants by country.

| Rank | Country      | CO <sub>2</sub> Emitted (Megatons) | Energy Produced (GWh) | Fossil Fuel Power (%) | Reference |
|------|--------------|------------------------------------|-----------------------|-----------------------|-----------|
| 1    | China        | 3120                               | 3,620,000             | 82.5                  | [22]      |
| 2    | USA          | 2820                               | 4,190,000             | 68.8                  | [23]      |
| 3    | India        | 638                                | 719,000               | 76.3                  | [24]      |
| 4    | Russia       | 478                                | 896,000               | 63.4                  | [25]      |
| 5    | Germany      | 429                                | 636,000               | 62.1                  | [26]      |
| 6    | Japan        | 414                                | 1,030,000             | 33.2                  | [27]      |
| 7    | U.K.         | 227                                | 370,000               | 71.4                  | [28]      |
| 8    | Australia    | 224                                | 228,000               | 90.1                  | [29]      |
| 9    | South Africa | 218                                | 215,000               | 93.4                  | [30]      |
| 10   | South Korea  | 192                                | 392,000               | 44.3                  | [31]      |

## 5. The Potential of CO<sub>2</sub> Capture and Storage in South Africa

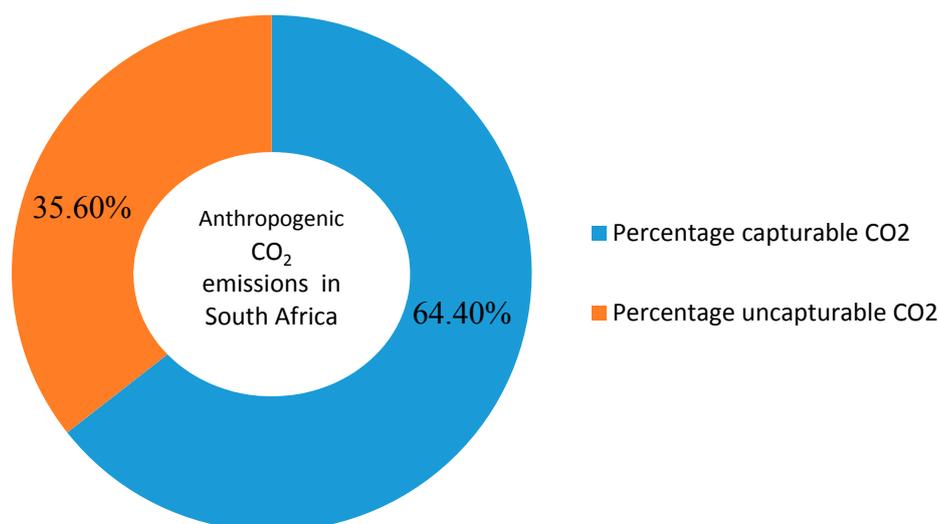
South Africa is amongst the fast developing nations in the world and has a power sector that is mostly dependent on coal, i.e., the country generates up to 224 million tons of coal per annum. Owing to the country's strong commitment to sustainable energy development, it is necessary to understand the need for climate change mitigation options in the country's economic, social and environmental dimensions. With South Africa's high dependence on coal energy and the presence of streams of pure carbon dioxide in its coal-fired power plants, the application of CCS systems will be an attractive option to curtail the unfettered release of CO<sub>2</sub> into the atmosphere by the South African power sector [32]. The country's climate policy is deeply rooted in a strong commitment to a multilateral process under the Kyoto Protocol and the United Nation's Framework Convention on Climate Change (UNFCCC). South Africa is also a signatory to both the Kyoto Protocol and the United Nation's Framework on Climate Change; the country is committed to introducing measures to mitigate climate change, albeit it does not have quantifiable emission reduction targets under the Kyoto Protocol. Therefore, the country can benefit immensely by switching to a clean and sustainable energy development path through the CCS approach [33]. It can offer an environmentally-benign alternative in the utilization of coal energy in coal-fired power plants. Coal can still be used to fuel the power plants and yet reduce the emission of greenhouse gases like CO<sub>2</sub>, instead of the so-called "business-as-usual" approach in which it is released into the atmosphere.

The theoretical maximum amount of capturable CO<sub>2</sub> in South Africa is approximately 64% of all anthropogenic CO<sub>2</sub> released [34–36]. Table 2 presents a breakdown of CO<sub>2</sub> contributing sources in South Africa and the amounts of CO<sub>2</sub> that are likely and unlikely to be captured if CCS technology were employed. It can be observed from Figure 2 that a higher percentage of CO<sub>2</sub> emitted in South Africa is capturable, and the majority of CO<sub>2</sub> emissions are generated by the power sector. Therefore, CCS technology would play a pivotal role in curbing the environmental pollution and health hazards caused by anthropogenic greenhouse gases, such as CO<sub>2</sub>. A report from Engelbrecht et al. [35] indicated

that CCS systems can significantly reduce South Africa's CO<sub>2</sub> emissions if they are incorporated in coal-fired electricity-generating power plants [37]. The realization of CCS has been hampered by economic constraints, and its implementation has been discouraged in most developing countries due to high costs. Other barriers include lack of a framework, legislation and regulation from governments. Nonetheless, South Africa is a fast developing nation with sound economic policies that can fully implement CCS technology in these power plants, which is the country's major CO<sub>2</sub> emitter [14]. Furthermore, the implementation of CCS is economically feasible in South Africa, because it will primarily focus on coal-fired power plants, which will be less expensive than incorporating it in all sectors. South Africa can acquire skills from countries where the CCS technology is already functional and from sources like the European Directive on the Geological Storage of Carbon Dioxide (CCS Directive 2009/31/EC), which focuses on the geological storage of CO<sub>2</sub>.

**Table 2.** Sources of CO<sub>2</sub> emissions in South Africa [35–37].

| Source of Likely Capturable CO <sub>2</sub>       | Amount of CO <sub>2</sub> (Mt/a) | Source of Unlikely to Be Capturable | Amount of CO <sub>2</sub> (Mt/a) |
|---|----------------------------------|-------------------------------------|----------------------------------|
| Electricity generation                            | 137                              | Municipal wastes                    | 9                                |
| Process industries                                | 24                               | Agricultural wastes                 | 41                               |
| Other energy production companies                 | 26                               | Other wastes                        | 36                               |
| Manufacturing companies                           | 26                               | Thermal energy production           | 32                               |
| Total capturable CO <sub>2</sub>                  | 213                              | Total uncapturable CO <sub>2</sub>  | 118                              |
| Total capturable and uncapturable CO <sub>2</sub> | 331                              |                                     |                                  |
| Percentage capturable CO <sub>2</sub>             | 64.40%                           |                                     |                                  |
| Percentage uncapturable CO <sub>2</sub>           | 35.60%                           |                                     |                                  |



**Figure 2.** Percentage of capturable and uncapturable CO<sub>2</sub> in South Africa.

## 6. Geological Storage of CO<sub>2</sub>

When CO<sub>2</sub> is successfully captured from these coal-fired power plants, it can be stored in natural areas, like geological formations, where it is trapped below impermeable rocks and retained in pore spaces after being dissolved by underground water [159,160]. This method of storing CO<sub>2</sub> has a long residence time. It can also be stored in geological formations, such as unused deep saline aquifers. According to literature reports, the geological storage of CO<sub>2</sub> is currently considered as the most viable option for storing captured CO<sub>2</sub> in large quantities [161,162]. Geological storage formations can store up to 10 million tons of CO<sub>2</sub> for a long period of time [163]. However, good geological sites for CO<sub>2</sub> storage must have: (i) appropriate thickness and porosity; (ii) the reservoir rock must be permeable and (iii) the cap-rock must be in a stable geological environment, as well as having a good sealing capability. Depleted or almost depleted oil and gas reservoirs, saline aquifers and un-mineable coal beds are the three major geological formations commonly considered for CO<sub>2</sub> storage [164]. Storing

CO<sub>2</sub> in deep oceans is another option for CO<sub>2</sub> storage; however, it poses environmental concerns, such as eutrophication and ocean acidification. Captured CO<sub>2</sub> could be stored in oceans by releasing it into deep ocean waters of a minimum depth of 1000 m below sea level. This form of CO<sub>2</sub> storage is feasible because cold-deep sea waters are unsaturated with CO<sub>2</sub> and subsequently have a significant potential of dissolving it. This is based on the principle that CO<sub>2</sub> becomes super critical below certain depths with a liquid-like density; and also, it is less buoyant than water [165]. However, as stated earlier, the major disadvantages of this option are the environmental challenges attributed to it.

South Africa has more geological formations than deep waters; therefore, the suitable option of storing the captured CO<sub>2</sub> from coal-fired power plants is by using geological formations, like deep saline aquifers at 700–1000 m below ground level. Carbon dioxide is soluble in water; there are natural exchanges of CO<sub>2</sub> between the atmosphere and waters at the ocean surface that occur until equilibrium is reached. If the atmospheric concentration of CO<sub>2</sub> increases, the ocean gradually takes up additional CO<sub>2</sub>. In this way, the oceans have absorbed about 500 Gt CO<sub>2</sub> of the total 1300 Gt CO<sub>2</sub> of anthropogenic emissions released to the atmosphere over the past 200 years [166]. As a result of the increased atmospheric CO<sub>2</sub> concentrations from human activities relative to pre-industrial levels, the oceans are currently absorbing CO<sub>2</sub> at a rate of 7 Gt CO<sub>2</sub> per year. Most of this carbon dioxide now resides in the upper ocean and thus far, has resulted in a decrease in pH of about 0.1 at the ocean surface because of the acidic nature of CO<sub>2</sub> in water. To date, there has been virtually no change in pH in the deep ocean. Models predict that over the next several centuries, the oceans will eventually take up most of the CO<sub>2</sub> released to the atmosphere as CO<sub>2</sub> is dissolved at the ocean surface and subsequently mixed with deep ocean waters [167]. South Africa has various locations with great potential for CO<sub>2</sub> storage. For instance, the Karoo basin, which covers the Eastern Cape, Northern Cape, Free State, KwaZulu-Natal and the Mpumalanga provinces of South Africa, are very promising geological storage sites for the captured CO<sub>2</sub>. The orange basin of Western South Africa around Durban and Zululand is another storage site available for the captured CO<sub>2</sub> from these power plants.

## 7. An Overview of CO<sub>2</sub> Capture Using Solid Adsorbents

CO<sub>2</sub> emissions from coal-fired power plants can be captured using solid adsorbents. Even though it is less mature than the absorption method, it is inexpensive, has minimum energy requirements and uses non-corrosive materials. Adsorption of CO<sub>2</sub> can be achieved by using various solid support systems, such as activated carbon, zeolites, carbon molecular sieves and polymeric adsorbents like amine-grafted polyaspartamide [168]. According to Chaffee et al. [165], physical adsorption of CO<sub>2</sub> using solid adsorbents require less energy as compared to other CO<sub>2</sub> capture systems. Physical adsorption of CO<sub>2</sub> requires about 0.09 KWh/kg CO<sub>2</sub> with equal pressure in the feed and product streams, which is by far smaller than the chemical adsorption, which requires about 0.34 KWh/kg CO<sub>2</sub>. Yang et al. [166] conducted a study on modeling the physical adsorption of CO<sub>2</sub> using solid physical adsorbents and investigated CO<sub>2</sub> capture via the pressure swing adsorption methods using activated carbon, zeolite13X, and concluded that the adsorption technology is less expensive and less energy intensive for capturing CO<sub>2</sub>. Similar findings were also confirmed by Othman et al. [167] when using molecular sieves and activated carbon materials. Rivas et al. [168] indicated that solid adsorbents are more efficient than liquid systems. For example, solid adsorbents exhibit better performance at partial pressures greater than 50 KPa of CO<sub>2</sub> [169–172]. However, liquid absorbents stabilize when coupled to chemical absorbents. Since the adsorption of gases is favored by higher pressures and lower temperatures, CO<sub>2</sub> capture from these power plants need to be carried out at high pressures; therefore, the adsorption technology will be ideal for effective CO<sub>2</sub> capture.

Physical adsorbents have also been proven to capture CO<sub>2</sub>; they have a high affinity for CO<sub>2</sub>. However, the purity of the gas decreases during the downstream process [173]. It was indicated that activated carbon and polymer-based adsorbents are the best type of physical adsorbents to be used for CO<sub>2</sub> capture. They produce about a 75%–80% pure CO<sub>2</sub> stream at a recovery of 90% [174]. Adsorption systems do not use high energy, and the recovery is far less than the chemical absorption methods [175].

Furthermore, polymer adsorption systems have been shown to bind CO<sub>2</sub>. A study conducted by Diaf and Beckman [176] assessed the effects of polymers on CO<sub>2</sub> capture using primary, secondary and tertiary amine-based polymers, concluded that CO<sub>2</sub> binds strongly on basic amines and proposed ethylene diamine (EDA) as the most efficient amine compound for polymer system. Similar findings were also confirmed by Seckin et al. [177]; the authors used 1, 4, 5, 6-tetrahydropyrimidine polymer compound to capture CO<sub>2</sub> and concluded that this method was more feasible compared to other CO<sub>2</sub> capture methods. The effectiveness of CO<sub>2</sub> binding was due to the 1:1 nature of amidine groups in the 1, 4, 5, 6-tetrahydropyrimidine [174]. These findings could pave the way for the use of carbon dioxide capture technologies via amidine systems [175]. Recently, a novel polymer-based adsorbent “polyaspartamide” from polysuccinimide was identified as a promising adsorbent for CO<sub>2</sub> capture because of its ability to selectively adsorb gases; this is due to its molecular sieving characteristics [176]. The adsorbent was suggested in this study in order to address the limitations of conventional wet solvent processes for CO<sub>2</sub> capture at the pilot scale, such as high costs, high energy requirements and the generation of large quantities of water and sludge from the process [177]. Thus, the application of adsorption technology for CO<sub>2</sub> capture using amine-grafted polymer-based adsorbents is highly encouraged because it is a dry process and has fewer challenges as compared to the conventional process, which uses solvents for CO<sub>2</sub> capture.

## 8. Challenges Facing CO<sub>2</sub> Capture and Storage in South Africa

### 8.1. Economic Challenges

The implementation of CCS technology has been hindered mainly by financial constraints. The prices of incorporating CCS in power systems ranges between 30% and 70% depending on the method of CO<sub>2</sub> capture used [178,179]. Maver [180] showed that the challenges facing the implementation of CCS globally centers on economic, social and legal barriers; economic barriers in the sense that CCS is expensive and cannot be implemented by most developing countries. Nonetheless, South Africa is amongst the fast developing nations that have good economic frameworks and policies for successful implementation of CCS in its coal-fired power plants. There has also been some skepticism with regards to the deployment of CCS technology in South Africa; it has been debated that its implementation will threaten the country's efforts of developing renewable and sustainable energy resources because they also require huge financial incentives from the government [180]. Nevertheless, the CO<sub>2</sub> generated from the country's coal-fired thermal power plants is causing many challenges associated with environmental pollution and health hazards. It is essential to establish regulatory frameworks that will oversee this technology in South Africa [100]. Moreover, some of the economic barriers could be overcome by creating CCS financing mechanisms, whereby CO<sub>2</sub>-emitting industries, e.g., Electricity Supply Commission (ESKOM) could contribute towards its financial development. A collaborative effort between various stakeholders can also accelerate its implementation [181].

### 8.2. Environmental Challenges

There are many environmental concerns associated with CCS; these include contamination of groundwater as a result of CO<sub>2</sub> leakage and the occurrence of earthquakes that might be caused by the sequestered CO<sub>2</sub> due to pressure build-up [182]. The sequestered CO<sub>2</sub> might be leaked into the atmosphere if it is stored in underground rocks and therefore escalates the problems of climate change. In addition, leakage could negatively affect soil quality; trees and other vegetation if stored underground [183]. In South Africa, this challenge could be surmounted because apart from storing the captured CO<sub>2</sub> in underground rocks, it can also be stored in the available basins listed in the previous chapters in this study. South Africa has abundant geological formations and un-mineable coal fields where captured CO<sub>2</sub> can be stored without infringing on environmental safety [184].

### 8.3. Social Challenges

The implementation of CCS may invigorate public debate because this technology is relatively new in South Africa and thus requires extensive research. Its long-term effects on the environment and people are not yet fully known. However, public awareness is essential in order to highlight its advantages, such as mitigation of CO<sub>2</sub> emissions and environmental degradation. This might in turn stimulate the interests of various stakeholders, which might contribute towards its implementation in South Africa [185]. South Africa through the South African Center for Carbon Capture and Storage (SACCCS) is creating public awareness on the need to curtail the indiscriminate emission of CO<sub>2</sub> in this region.

## 9. Conclusions and Recommendations

South Africa is a fast-developing nation with an energy economy that is highly dependent on coal, and it is apparent that the country has the potential for the implementation of CCS in the power sector. The potential for CO<sub>2</sub> capture lies in the major emitting sources, such as the electricity-generating coal-fired power plants, which are a major emitting source, as pointed out in this study. The establishment of the South African Center for Carbon Capture and Storage (SACCCS) illustrates the potential of the implementation of this technology in South Africa's power sector. There are various barriers facing the implementation of CCS globally. Nonetheless, it can be inferred that South Africa is a country with a strong commitment to sustainable and renewable energy and also a signatory to the Kyoto Protocol, as highlighted earlier in this review. This nation is working towards curtailing its carbon footprint by shifting its focus to major sources of CO<sub>2</sub> emission, such as the country's coal-fired thermal power plants. More so, it has included CCS policies into its legislation and has mandated SACCCS to oversee its implementation. This clearly brings to light that there is a huge potential of implementing CCS in the country's coal-fired thermal power plants. Thus, this review presented the potential of CCS technology in South African coal-fired power plants. The pressing challenges related to CO<sub>2</sub> emissions necessitate the search for clean and sustainable energy technologies, such as CCS in South Africa. The potential for CO<sub>2</sub> capture lies in the major emitting sources, which are the electricity-generating coal-fired power plants. The most suitable CO<sub>2</sub> capture route for the South African coal-fired power plants is post-combustion CO<sub>2</sub> capture, because it allows for easy retrofitting of capture devices in the existing coal-fired power plants. Adsorption technology using solid polymer-based adsorbents will be ideal and more economically viable for CO<sub>2</sub> capture in the South African coal-fired power plants.

The following recommendations are proposed for the implementation of CCS in South Africa's coal-fired power plants:

- ❖ The implementation of CCS has been stagnant in South African coal-fired power plants due to financial barriers, the lack of frameworks and the lack of technical expertise. Nonetheless, this challenge can be overcome by using solid inexpensive composite adsorbents, which have been shown in recent years to be economically viable, towards the improvement of CCS processes.
- ❖ Chemical absorbents, such as monoethanolamine, are extensively used in CO<sub>2</sub> capture. However, they have some limitations in terms of solvent capacity; it is therefore recommended that if the absorption technology must be used in post-combustion CO<sub>2</sub> capture from these South African power plants, a chemical absorbent with higher loading capacity, such as amine 2-amino-2-methyl-1-propanol (AMP) should be employed. Alternatively, the monoethanolamine can be coupled with activators, such as piperazine (PZ), to improve its efficiency, but if the adsorbents will be used as suggested by this study, these adsorbents should be impregnated with amine-rich materials, such as chitosan and polysuccinimide, because they increase the adsorbent's affinity for CO<sub>2</sub>. Possible solid sorbents that could be used for CO<sub>2</sub> capture in the South African power plants include carbon nanotubes with chitosan impregnation, amine-grafted polyaspartamide, Sodalite-Zeolite Metal Organic Framework/chitosan composite materials, etc.

- ❖ Given the fact that the post-combustion CO<sub>2</sub> capture technology is highly embraced, its overall system performance with regards to South Africa's coal-fired power plants should be assessed by using pilot-plant experimental results from these power plants, and these results should be validated for their accuracy.

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## References

1. Lim, Y.; Kim, J.; Jung, J.; Lee, C.S.; Han, C. Modeling and simulation of CO<sub>2</sub> capture process for coal-based power plant using amine solvent in South Korea. *Energy Procedia* **2013**, *37*, 1855–1862. [CrossRef]
2. Sekoai, P.T.; Daramola, M.O. Biohydrogen as a potential energy fuel in South Africa. *Biofuel Res. J.* **2015**. [CrossRef]
3. Sekoai, P.T.; Yoro, K.O. Biofuel development initiatives in Sub-Saharan Africa: Opportunities and challenges. *Climate* **2016**, *4*, 33. [CrossRef]
4. Pegels, A. Renewable energy in South Africa: Potentials, barriers and options for support. *Energy Policy* **2010**, *38*, 4945–4954. [CrossRef]
5. Intergovernmental Panel on Climate Change. The Physical Science Basis. Available online: <http://www.ipcc.ch/report/ar5/wg1/> (accessed on 5 June 2016).
6. CCS Roadmap Storage Strategy. Department of Energy and Climate Change. Available online: [https://www.gov.uk/government/uploads/system/uploads/attachment\\_data/file/48320/4904-ccs-roadmap-storage-strategy.pdf](https://www.gov.uk/government/uploads/system/uploads/attachment_data/file/48320/4904-ccs-roadmap-storage-strategy.pdf) (accessed on 5 June 2016).
7. Khoo, H.H.; Bu, J.; Wong, R.L.; Kuan, S.Y.; Sharratt, P.N. Carbon capture and utilization: Preliminary life cycle CO<sub>2</sub>, energy, and cost results of potential mineral carbonation. *Energy Proc.* **2011**, *4*, 2494–2501. [CrossRef]
8. Intergovernmental Panel on Climate Change. Carbon Dioxide Capture and Storage. Cambridge University Press. Available online: [https://www.ipcc.ch/pdf/special-reports/srccs/srccs\\_wholereport.pdf](https://www.ipcc.ch/pdf/special-reports/srccs/srccs_wholereport.pdf) (accessed on 5 June 2016).
9. De Villiers, M.; Howells, M.; Kenny, A. *Sustainable Energy for South Africa: Energy Scenarios from 1995 to 2025*; Report for Eskom and National Research Foundation; University of Cape Town: Cape Town, South Africa, 2009.
10. The Third South African Carbon Capture and Storage Conference 2013. Available online: <http://www.saccs.org.za/wp> (accessed on 5 June 2016).
11. Van der Merwe, M.R.; Scholes, R.J. *South African Greenhouse Gas Emissions Inventory for the Years 2000 and 2004*; National Committee on Climate Change: Pretoria, South Africa, 2008.
12. Banks, D.; Schäffler, J.L. *The Potential Contribution of Renewable Energy in South Africa: Prepared for the Sustainable Energy & Climate Change Partnership, Earth Life Africa*; RAPS Consulting & Nano Energy: Pretoria, South Africa, 2010.
13. Bolland, O.; Undrum, H. Removal of CO<sub>2</sub> from gas turbine power plants: Evaluation of pre- and post-combustion methods. In Proceedings of the 4th Conference on Greenhouse Gas Technologies, Interlaken, Switzerland, 30 August–2 September 1998.
14. Lilliestam, J.; Bielicki, J.M.; Anthony, G.P. Comparing carbon capture and storage (CCS) with concentrating solar power (CSP): Potentials, costs, risks, and barriers. *Energy Policy* **2012**, *47*, 447–455. [CrossRef]
15. Carbon Capture and Utilisation in the Green Economy. Available online: <http://co2chem.co.uk/carbon-capture-and-utilisation-in-the-green-economy> (accessed on 5 June 2016).
16. International Energy Agency. Technology Roadmap Carbon Capture and Storage, Organization for Economic Development & International Energy Agency. Available online: <http://www.iea.org/publications/freepublications/publication/TechnologyRoadmapCarbonCaptureandStorage.pdf> (accessed on 5 June 2016).

17. Figueroa, J.D.; Fout, T.; Plasynski, S.; McIlvried, H.; Srivastava, R.D. Advances in CO<sub>2</sub> capture technology—The US department of energy and carbon sequestration programme. *Int. J. Greenh. Gas Control* **2008**, *2*, 9–20. [[CrossRef](#)]
18. Carbon Monitoring for Action. The Ten Largest CO<sub>2</sub> Emitting Power Sectors in the World by Country. Available online: <http://www.carma.org> (accessed on 5 June 2016).
19. Eskom Power Stations. Available online: [http://www.eskom.co.za/OurCompany/PhotoGallery/Pages/Eskom\\_Power\\_Stations.aspx](http://www.eskom.co.za/OurCompany/PhotoGallery/Pages/Eskom_Power_Stations.aspx) (accessed on 5 June 2016).
20. Zheng, B.; Xu, J. Carbon capture and storage development trends from a techno-paradigm perspective. *Energies* **2014**, *7*, 5221–5250. [[CrossRef](#)]
21. Department of Minerals & Energy. Sustainable Development Criteria for Approval of Clean Development Mechanism Projects by the Designated National Authority of the CDM. Available online: <http://www.energy.gov.za/files/esources/kyoto/Web%20info/Annex%203%20SA%20Sustainable%20Development%20Criteria.pdf> (accessed on 5 June 2016).
22. Ian, B. Upgrading the Efficiency of the World's Coal Fleet to Reduce CO<sub>2</sub> Emissions. Available online: <http://www.cornerstonemag.net/upgrading-the-efficiency-of-the-worlds-coal-fleet-to-reduce-co2-emissions> (accessed on 5 June 2016).
23. Schneider, J.; Madsen, T. America's Dirtiest Power Plants: Their Oversized Contribution to Global Warming and What We Can Do About It. Available online: <http://www.environmentamericacenter.org/sites/environment/files/reports/Dirty%20Power%20Plants.pdf> (accessed on 5 June 2016).
24. Chaudhary, J. Indian Coal Power Plants World's Most Polluting. Available online: <http://www.indiaclimatedialogue.net/2015/02/24/indian-coal-power-plants-worlds-most-polluting/> (accessed on 5 June 2016).
25. Capiello, D. These 6 Countries Are Responsible for 60% Of CO<sub>2</sub> Emissions. Available online: <http://www.businessinsider.com/these-6-countries-are-responsible-for-60-of-co2-emissions-2014-12> (accessed on 5 June 2016).
26. Homewood, P. Germany Opens Another New Coal Plant. Available online: <https://www.notalotofpeopleknowthat.wordpress.com/2015/11/20/germany-opens-another-new-coal-plant/> (accessed on 5 June 2016).
27. Obayashi, Y. Japan to Get More Coal-Fired Power Plants Thanks to Environment Ministry Policy Reversal'. Available online: <http://www.reuters.com/article/us-japan-emissions-iduskcn0vw0ev> (accessed on 5 June 2016).
28. Cebrucean, D.; Cebrucean, V.; Ionel, I. CO<sub>2</sub> capture and storage from fossil fuel power plants. *Energy Procedia* **2014**, *63*, 18–26. [[CrossRef](#)]
29. Bui, M.; Gunawan, I.; Verheyen, T.V.; Meuleman, E.; Feron, P. Dynamic operation of post-combustion CO<sub>2</sub> capture in Australian coal-fired power plants. *Energy Procedia* **2014**, *63*, 1368–1375. [[CrossRef](#)]
30. Mabuza, M.; Premlall, K. Assessing impure CO<sub>2</sub> adsorption capacity on selected South African coals: Comparative study using low and high concentrated simulated flue gases. *Energy Procedia* **2014**, *51*, 308–315. [[CrossRef](#)]
31. Carbon Monitoring for Action. Centre for Global Development. Available online: <http://www.cgdev.org/files/14846fileCARMAPR.pdf> (accessed on 5 June 2016).
32. Ahn, Y.; Bae, S.J.; Kim, M.; Cho, S.K.; Baik, S.; Lee, J.I.; Cha, J.E. Review of supercritical CO<sub>2</sub> power cycle technology and current status of research and development. *Nucl. Eng. Technol.* **2015**, *47*, 647–661. [[CrossRef](#)]
33. Fine, B.; Rustomjee, Z. *The Political Economy of South Africa: From Minerals Energy Complex to Industrialization: 1996*; Westview Publishing Press: Boulder, CO, USA; Volume 1, pp. 60–288.
34. Department of Minerals and Energy. South Africa National Energy Balance. Available online: [http://www.erc.uct.ac.za/sites/default/files/imagetool/images/119/Papers2004/04ERCenergysustainable\\_developmentphase1.pdf](http://www.erc.uct.ac.za/sites/default/files/imagetool/images/119/Papers2004/04ERCenergysustainable_developmentphase1.pdf) (accessed on 5 June 2016).
35. Engelbrecht, A.; Golding, A.; Hietkamp, S.; Scholes, R.J. *The Potential for Sequestration of Carbon Dioxide in South Africa*; Report for the Department of Minerals & Energy: Pretoria, South Africa, 2004.
36. Lloyd, P.J.D. *Carbon Capture and Storage in South Africa: Development and Climate Change*; University of Cape Town: Cape Town, South Africa, 2014.
37. Carbon Sequestration Leadership Forum. Available online: <https://hub.globalccsinstitute.com/category/organisation/carbon-sequestration-leadership-forum-cslf?page=7> (accessed on 27 August 2004).

38. Wall, T. Combustion processes for carbon capture. *Proc. Combust. Inst.* **2007**, *31*, 31–47. [[CrossRef](#)]
39. International Energy Agency. Greenhouse Gas R & D Programme, 2004. Impact of Impurities on CO<sub>2</sub> Capture, Transport and Storage, Report No. PH4/32. 2004. Available online: [http://www.ieaghg.org/docs/General\\_Docs/Reports/Ph4-32%20Impurities.pdf](http://www.ieaghg.org/docs/General_Docs/Reports/Ph4-32%20Impurities.pdf) (accessed on 5 June 2016).
40. International Energy Agency. Greenhouse Gas R & D Programme, 2005. Near Zero Emission Coal-Fired Power Plants. Clean Coal centre, Report No. CCC/101. Available online: [http://www.ieaghg.org/docs/General\\_Docs/Reports/2006-13%20Near%20zero%20emissions.pdf](http://www.ieaghg.org/docs/General_Docs/Reports/2006-13%20Near%20zero%20emissions.pdf) (accessed on 5 June 2016).
41. Technology Benchmarking Studies in Oxy-Fuel Combustion. Presentation to IEA Oxy-Fuel Combustion Research Network, Cottbus, Germany. Available online: <http://www.ieaghg.org/docs/oxyfuel/w1/1stOxyCombustionWorkshopReport.pdf> (accessed on 5 June 2016).
42. Cuellar-Franca, R.S.; Azapagic, A. Carbon capture, storage and utilisation technologies: A critical analysis and comparison of their life cycle environmental impacts. *J. CO<sub>2</sub> Util.* **2015**, *9*, 82–102. [[CrossRef](#)]
43. Singh, B.; Strømman, A.H.; Hertwich, E.G. Life cycle assessment of natural gas combined cycle power plant with post-combustion carbon capture, transport and storage. *Int. J. Greenh. Gas Control* **2011**, *5*, 911–921. [[CrossRef](#)]
44. Otto, A.; Grube, T.; Schiebahna, S.; Stoltena, D. Closing the loop: Captured CO<sub>2</sub> as a feedstock in the chemical industry. *Energy Environ. Sci.* **2015**, *8*, 3283–3297. [[CrossRef](#)]
45. Schakel, W.; Meerman, H.; Talaei, A.; Ramirez, A.; Faaij, A. Comparative life cycle assessment of biomass co-firing plants with carbon capture and storage. *Appl. Energy* **2014**, *131*, 441–467. [[CrossRef](#)]
46. Technology Roadmap. Carbon Capture and Storage in Industrial Applications. Available online: [https://www.iea.org/publications/freepublications/publication/ccs\\_industry.pdf](https://www.iea.org/publications/freepublications/publication/ccs_industry.pdf) (accessed on 5 June 2016).
47. Roman, M. Carbon capture and storage in developing countries: A comparison of Brazil, South Africa and India. *Glob. Environ. Chang.* **2011**, *21*, 391–401. [[CrossRef](#)]
48. Arranz, A.M. Carbon capture and storage: Frames and blind spots. *Appl. Policy* **2015**, *82*, 249–259.
49. Liu, L.; Qiu, W.; Sanders, E.S.; Ma, C.; Koros, W.J. Post-combustion carbon dioxide capture via 6FDA/BPDA-DAM hollow fiber membranes at sub-ambient temperatures. *J. Membr. Sci.* **2016**, *510*, 447–454. [[CrossRef](#)]
50. Liu, L.; Sanders, E.S.; Kulkarni, S.S.; Hasse, D.J.; Koros, W.J. Sub-ambient temperature flue gas carbon dioxide capture via Matrimids hollow fiber membranes. *J. Membr. Sci.* **2014**, *465*, 49–55. [[CrossRef](#)]
51. Kumar, A.; Bhattacharjee, G.; Barmecha, V.; Diwan, S.; Kushwaha, O.S. Influence of kinetic and thermodynamic promoters on post-combustion carbon dioxide capture through gas hydrate crystallization. *Environ. Chem. Eng.* **2016**, *4*, 1955–1961. [[CrossRef](#)]
52. Goetheer, E.; Abu-Zahra, M. Overview of Post Combustion Capture Technology. Available online: [http://www.fossiltransition.org/pages/post\\_combustion\\_capture\\_/128.php](http://www.fossiltransition.org/pages/post_combustion_capture_/128.php) (accessed on 5 June 2016).
53. Davison, J. Performance and costs of power plants with capture and storage of CO<sub>2</sub>. *Energy* **2007**, *32*, 1163–1176. [[CrossRef](#)]
54. Singto, S.; Supap, T.; Raphael, I.; Tontiwachwuthikul, P.; Tantayanon, S.; Al-Marri, M.J.; Benamor, A. Synthesis of new amines for enhanced carbon dioxide (CO<sub>2</sub>) capture performance: The effect of chemical structure on equilibrium solubility, cyclic capacity, kinetics of absorption and regeneration, and heats of absorption and regeneration. *Sep. Purif. Technol.* **2016**, *167*, 97–107. [[CrossRef](#)]
55. The European Union Technology Platform for Zero Emission Fossil Fuel Power Plant (ZEP), Strategic Research Agenda, 2006. Available online: <http://www.zeroemissionsplatform.eu/> (accessed on 5 June 2016).
56. Tontiwachwuthikul, P.; Idem, R.; Gelowitz, D. Recent progress and new development in post-combustion carbon-capture technology with reactive solvents. *Carbon Manag.* **2013**, *2*, 261–263. [[CrossRef](#)]
57. Rao, A.B.; Rubin, E.S. A technical, economic, and environmental assessment of amine-based CO<sub>2</sub> capture technology for power plant greenhouse gas control. *Environ. Sci. Technol.* **2012**, *36*, 4467–4475.
58. Liu, H.; Sema, T.; Liang, Z.; Fu, K.; Idem, R.; Na, Y. CO<sub>2</sub> absorption kinetics of 4-diethylamine-2-butanol solvent using stopped-flow technique. *Sep. Purif. Technol.* **2014**, *136*, 81–87. [[CrossRef](#)]
59. Xu, G.; Liang, F.; Yang, Y.; Hu, Y.; Zhang, K.; Liu, W. An improved CO<sub>2</sub> separation and purification system based on cryogenic separation and distillation theory. *Energies* **2014**, *7*, 3484–3502. [[CrossRef](#)]
60. Li, X.; Jiageng, L.; Bolun, Y. Design and control of the cryogenic distillation process for purification of synthetic natural gas from methanation of coke oven gas. *Ind. Eng. Chem. Res.* **2012**, *51*, 1438–1463. [[CrossRef](#)]

61. Scholes, C.A.; Ho, M.T.; Wiley, D.E. Membrane-cryogenic post-combustion carbon capture of flue gases from NGCC. *Technologies* **2016**, *4*, 14. [[CrossRef](#)]
62. Song, G.; Zhu, X.; Chen, R.; Liao, Q.; Ding, Y.-D.; Chen, L. An investigation of CO<sub>2</sub> adsorption kinetics on porous magnesium oxide. *Chem. Eng. J.* **2016**, *283*, 175–183. [[CrossRef](#)]
63. Fu, Q.; Kansha, Y.; Song, C.; Liu, Y.; Ishizuka, M.; Tsutsumi, A. A cryogenic air separation process based on self-heat recuperation for oxy-combustion plants. *Appl. Energy* **2016**, *162*, 1114–1121. [[CrossRef](#)]
64. Shi, H.; Naami, A.; Idem, R.; Tontiwachwuthikul, P. Catalytic and non catalytic solvent regeneration during absorption-based CO<sub>2</sub> capture with single and blended reactive amine solvents. *Int. J. Greenh. Gas Control* **2016**, *26*, 39–50. [[CrossRef](#)]
65. Corti, A.; Lombardi, L. Reduction of carbon dioxide emissions from a SCGT/CC by ammonia solution absorption—Preliminary results. *Int. J. Thermodyn.* **2004**, *4*, 173–181.
66. Madden, D.; Curtin, T. Carbon dioxide capture with amino-functionalised zeolite-b: A temperature programmed desorption study under dry and humid conditions. *Microporous Mesoporous Mater.* **2014**, *228*, 310–317. [[CrossRef](#)]
67. Center for Global Development. Carbon Dioxide Emissions From Power Plants Rated Worldwide. Available online: <https://www.sciencedaily.com/releases/2007/11/071114163448.htm> (accessed on 5 June 2016).
68. Abbas, Z.; Mezher, T.; Abu-Zahra, M.R.M. Evaluation of CO<sub>2</sub> purification requirements and the selection of processes for impurities deep removal from the CO<sub>2</sub> product stream. *Energy Proc.* **2013**, *37*, 2389–2396. [[CrossRef](#)]
69. Zhao, L.; Dong, H.; Tang, J.; Ca, J. Cold energy utilization of liquefied natural gas for capturing carbon dioxide in the flue gas from the magnesite processing industry. *Energy* **2016**, *105*, 45–56. [[CrossRef](#)]
70. Almahdi, M.; Dincer, I.; Rosen, M.A. Analysis and assessment of methanol production by integration of carbon capture and photocatalytic hydrogen production. *Int. J. Greenh. Gas. Control* **2016**, *5*, 56–70. [[CrossRef](#)]
71. Diego, M.E.; Arias, B.; Grasa, G.; Abanades, J. Design of a novel fluidized bed reactor to enhance sorbent performance in CO<sub>2</sub> capture systems using CO<sub>2</sub>. *Ind. Eng. Chem. Res.* **2014**, *53*, 10059–10071. [[CrossRef](#)]
72. Briz-López, E.M.; Ramírez-Moreno, M.J.; Romero-Ibarrac, I.C.; Gómez-Yáñez, C.; Pfeiffer, H.; Ortiz-Landeros, J. First assessment of Li<sub>2</sub>O-Bi<sub>2</sub>O<sub>3</sub> ceramic oxides for high temperature carbon dioxide capture. *J. Energy Chem.* **2016**. [[CrossRef](#)]
73. Ortiz, A.L.; Escobedo Bretado, M.A.; Velderrain, V.G.; Zaragoza, M.M.; Gutiérrez, J.S.; Gutiérrez, D.L.; Collins-Martínez, V. Experimental and modeling kinetic study of the CO<sub>2</sub> absorption by Li<sub>4</sub>SiO<sub>4</sub>. *Int. J. Hydrog. Energy* **2014**, *39*, 16656–16666. [[CrossRef](#)]
74. Mejia-Trejo, V.L.; Fregoso-Israel, E.; Pfeiffer, H. Textural, structural, and CO<sub>2</sub> chemisorption effects produced on the lithium orthosilicate by its doping with sodium (Li<sub>4-x</sub>Na<sub>x</sub>SiO<sub>4</sub>). *Chem. Mater.* **2008**, *20*, 7171–7176. [[CrossRef](#)]
75. Vieille, L.; Govin, A.; Grosseau, P. Improvements of calcium oxide based sorbents for multiple CO<sub>2</sub> capture cycles. *Powder Technol.* **2012**, *228*, 319–323. [[CrossRef](#)]
76. Shan, S.Y.; Jia, Q.M.; Jiang, L.H.; Li, Q.C.; Wang, Y.M.; Peng, J.H. Preparation and kinetic analysis of Li<sub>4</sub>SiO<sub>4</sub> sorbents with different silicon sources for high temperature CO<sub>2</sub> capture. *Chin. Sci. Bull.* **2012**, *57*, 2475–2479. [[CrossRef](#)]
77. Shan, S.Y.; Jia, Q.M.; Jiang, L.H.; Li, Q.C.; Wang, Y.M.; Peng, J.H. Impregnation precipitation preparation and kinetic analysis of Li<sub>4</sub>SiO<sub>4</sub>-based sorbents with fast CO<sub>2</sub> adsorption rate. *Ind. Eng. Chem. Res.* **2013**, *52*, 6941–6945. [[CrossRef](#)]
78. Blackforda, J.; Bull, J.M.; Cevatoglu, M.; Connelly, D.; Hauton, C.; James, R.H.; Lichtschlag, A.; Stahl, H.; Widdicombe, S.; Wright, I.C. Marine baseline and monitoring strategies for carbon dioxide capture and storage (CCS). *Int. J. Greenh. Gas Control* **2015**, *38*, 221–229. [[CrossRef](#)]
79. Yu, C.H.; Huang, C.H.; Tan, C.S. A review of CO<sub>2</sub> capture by absorption and adsorption. *Aerosol Air Qual. Res.* **2012**, *12*, 745–769. [[CrossRef](#)]
80. Webley, P.A. Adsorption technology for CO<sub>2</sub> separation and capture: A perspective. *Adsorption* **2014**, *20*, 225–231. [[CrossRef](#)]
81. Sholl, D.S.; Lively, R.P. Seven chemical separations to change the world. *Nature* **2016**, *532*, 435–437. [[CrossRef](#)] [[PubMed](#)]
82. Siriwardane, R.V.; Shen, M.S.; Fisher, E.P.; Poston, J.A. Adsorption of CO<sub>2</sub> on molecular sieves and activated carbon. *Energy Fuels* **2001**, *15*, 279–284. [[CrossRef](#)]

83. Ben-Mansour, R.; Habib, M.A.; Bamidele, O.E.; Basha, M.; Qasem, N.A.A.; Peedikakkal, A.; Laoui, T.; Ali, M. Carbon capture by physical adsorption: Materials, experimental investigations and numerical modeling and simulations—A review. *Appl. Energy* **2016**, *161*, 225–255. [[CrossRef](#)]
84. Arachchige, U.S.P.R.; Melaaen, M.C. Aspen plus simulation of CO<sub>2</sub> removal from coal and gas fired power plants. *Energy Procedia* **2012**, *23*, 391–399. [[CrossRef](#)]
85. Gatti, L.V.; Miller, J.B.; D’amelio, M.T.S.; Martinewski, A.; Basso, L.S.; Gloor, M.E.; Wofsy, S.; Tans, P. Vertical profiles of CO<sub>2</sub> above eastern Amazonia suggest a net carbon flux to the atmosphere and balanced biosphere between 2000 and 2009. *Tellus B* **2010**, *62*, 581–594. [[CrossRef](#)]
86. Ngoy, J.M.; Wagner, N.; Riboldi, L.; Bolland, O. A CO<sub>2</sub> capture technology using multi-walled carbon nanotubes with polyaspartamide surfactant. *Energy Proc.* **2014**, *63*, 2230–2248. [[CrossRef](#)]
87. Zanganeh, K.; Shafeen, A. A novel process integration, optimization, and design approach for large-scale implementation of oxy-fired coal power plant with CO<sub>2</sub> capture. *Int. J. Greenh. Gas Control* **2007**, *1*, 47–54. [[CrossRef](#)]
88. Zahid, U.; Lim, Y.; Jung, J.; Han, C. CO<sub>2</sub> geological storage: A review on present and future prospects. *Korean J. Chem. Eng.* **2011**, *28*, 674–685. [[CrossRef](#)]
89. Celia, M.A.; Nordbottena, J.M. Practical modeling approaches for geological storage of carbon dioxide. *Ground Water* **2009**, *47*, 627–638. [[CrossRef](#)] [[PubMed](#)]
90. Van der Zwaan, B.; Smekens, K. CO<sub>2</sub> capture and storage with leakage in an energy-climate model. *Environ. Model. Assess.* **2009**, *14*, 135–148. [[CrossRef](#)]
91. Yang, F.; Bai, B.J.; Tang, D.Z.; Dunn-Norman, S.; Wronkiewicz, D. Characteristics of CO<sub>2</sub> sequestration in saline aquifers. *Pet. Sci.* **2010**, *7*, 83–92. [[CrossRef](#)]
92. Myer, L. Global Status of Geologic CO<sub>2</sub> Storage Technology Development United States Carbon Sequestration Council Report. Available online: <http://www.iea-coal.org.uk/documents/82579/7892/Global-status-of-geologic-CO2-storage-technology-development> (accessed on 5 June 2016).
93. Oh, T.H. Carbon capture and storage potential in coal-fired plant in Malaysia – A Review. *Renew. Sustain. Energy Rev.* **2010**, *14*, 2697–2709. [[CrossRef](#)]
94. Svensson, R.; Odenberger, M.; Johnsson, F.; Stromberg, L. Transportation systems for CO<sub>2</sub>—Application to carbon capture and storage. *Energy Convers. Manag.* **2004**, *45*, 2343–2353. [[CrossRef](#)]
95. Norisor, M.; Badea, A.; Dinca, C. Economical and technical analysis of CO<sub>2</sub> transport ways. *UPB Sci. Bull. Ser. C* **2012**, *74*, 127–138.
96. Gao, L.; Fang, M.; Li, H.; Hetland, J. Cost analysis of CO<sub>2</sub> transportation: Case study in China. *Energy Procedia* **2011**, *4*, 5974–5981. [[CrossRef](#)]
97. Johnsen, K.; Helle, K.; Roneid, S.; Holt, H. DNV recommended practice: Design and operation of CO<sub>2</sub> pipelines. *Energy Proc.* **2011**, *4*, 3032–3039. [[CrossRef](#)]
98. Kikkinides, E.S.; Yang, R.T.; Cho, S.H. Concentration and recovery of carbon dioxide from flue gas by pressure swing adsorption. *Ind. Eng. Chem. Res.* **1993**, *32*, 2714–2720. [[CrossRef](#)]
99. Songolzadeh, M.; Soleimani, M.; Ravanchi, M.T.; Songolzadeh, R. Carbon dioxide separation from flue gases: A technological review emphasizing reduction in greenhouse gas emissions. *Sci. World J.* **2014**, *2014*, 828131. [[CrossRef](#)] [[PubMed](#)]
100. Voleno, A.; Romano, M.C.; Turi, D.M.; Chiesa, P.; Ho, M.T.; Wiley, D.E. Post-combustion CO<sub>2</sub> capture from natural gas combined cycles by solvent supported membranes. *Energy Procedia* **2014**, *63*, 7389–7397. [[CrossRef](#)]
101. Barkakaty, B.; Browning, K.L.; Sumpter, B.; Uhrig, D.; Karpisova, I.; Harman, K.W.; Ivanov, I.; Hensley, D.K.; Messman, J.M.; Kilbey, S.M.; et al. Amidine-Functionalized Poly (2-vinyl-4,4-dimethylazlactone) for Selective and Efficient CO<sub>2</sub> Fixing. *Macromolecules* **2016**, *49*, 1523–1531. [[CrossRef](#)]
102. Heldebrant, D.J.; Koech, P.K.; Rainbolt, J.E.; Zheng, F.; Smurthwaite, T.; Freeman, C.J.; Oss, M.; Leito, I. Performance of single-component CO<sub>2</sub>-binding organic liquids (CO<sub>2</sub>BOLs) for post combustion CO<sub>2</sub> capture. *Chem. Eng. J.* **2011**, *171*, 794–800. [[CrossRef](#)]
103. Kim, H.; Kim, Y.H.; Kang, S.G.; Park, Y.-G. Development of environmental impact monitoring protocol for offshore carbon capture and storage (CCS): A biological perspective. *Environ. Impact Assess. Rev.* **2016**, *57*, 139–150. [[CrossRef](#)]
104. Smit, B.; Park, A.H.A.; Gadikota, G. The grand challenges in carbon capture, utilization, and storage. *Front. Energy Res.* **2014**. [[CrossRef](#)]

105. Pehnat, M.; Henkel, J. Life cycle assessment of carbon dioxide capture and storage from lignite power plants. *Int. J. Greenh. Gas Control* **2009**, *3*, 49–66. [[CrossRef](#)]
106. Tan, Y.; Nookuea, W.; Li, H.; Thorin, E.; Yan, J. Property impacts on carbon capture and storage (CCS) processes: A review. *Energy Convers. Manag.* **2016**, *118*, 204–222. [[CrossRef](#)]
107. Raza, A.; Rezaee, R.; Bing, C.H.; Gholami, R.; Hamid, M.A.; Nagarajan, R. Carbon dioxide storage in subsurface geologic medium: A review on capillary trapping mechanism. *Egypt. J. Pet.* **2015**. [[CrossRef](#)]
108. Lake, A.J.; Johnson, I.; Cameron, D.D. Carbon capture and storage (CCS) pipeline operating temperature effects on UK soils: The first empirical Data. *Int. J. Greenh. Gas Control* **2016**, *53*, 11–17. [[CrossRef](#)]
109. Leung, D.Y.C.; Caramanna, G.; Maroto-Valer, M.M. An overview of current status of carbon dioxide capture and storage technologies. *Renew. Sustain. Energy Rev.* **2014**, *39*, 426–443. [[CrossRef](#)]
110. Chu, F.; Jon, C.; Yang, L.; Du, X.; Yang, Y. CO<sub>2</sub> absorption characteristics in ammonia solution inside the structured packed column. *Ind. Eng. Chem. Res.* **2016**, *55*, 3696–3709. [[CrossRef](#)]
111. Hu, G.; Nicholas, N.J.; Smith, K.H.; Mumford, K.A.; Kentish, S.E.; Stevens, G.W. Carbon dioxide absorption into promoted potassium carbonate solutions: A review. *Int. J. Greenh. Gas Control* **2016**, *53*, 28–40. [[CrossRef](#)]
112. Kwak, K.O.; Jung, S.J.; Chung, S.Y.; Kang, C.M.; Huh, Y.I.; Bae, S.O. Optimization of culture conditions for CO<sub>2</sub> fixation by a chemoautotrophic microorganism, strain YN-1 using factorial design. *Biochem. Eng. J.* **2006**, *31*, 1–26. [[CrossRef](#)]
113. Rochelle, G.T. Amine scrubbing for CO<sub>2</sub> capture. *Science* **2009**, *325*, 1652–1654. [[CrossRef](#)] [[PubMed](#)]
114. Kim, S.; Park, C.B. Bio-inspired synthesis of minerals for energy, environment, and medicinal applications. *Adv. Funct. Mater.* **2013**, *23*, 10–25. [[CrossRef](#)]
115. Wang, S.; Liu, K.; Yao, X.; Jiang, L. Bioinspired surfaces with superwettability: New insight on theory, design, and applications. *Chem. Rev.* **2015**, *115*, 8230–8293. [[CrossRef](#)] [[PubMed](#)]
116. Quan, S.; Li, S.; Wang, Z.; Yan, X.; Guo, Z.; Shao, L. A bio-inspired CO<sub>2</sub>-philic network membrane for enhanced sustainable gas separation. *J. Mater. Chem.* **2015**, *3*, 13758–13766. [[CrossRef](#)]
117. Wegst, U.G.; Bai, H.; Saiz, E.; Tomsia, A.P.; Ritchie, R.O. Bioinspired structural materials. *Nat. Mater.* **2014**, *14*, 23–26. [[CrossRef](#)] [[PubMed](#)]
118. Lau, C.H.; Li, P.; Li, F.Y.; Chung, T.S.; Paul, D.R. Reverse-selective polymeric membranes for gas separations. *Prog. Polym. Sci.* **2013**, *38*, 740–766. [[CrossRef](#)]
119. Su, J.C.; Ong, R.C.; Wang, P.; Chung, T.S.; Helmer, B.J.; de Wit, J.S. Advanced FO membranes from newly synthesized CAP polymer for wastewater reclamation through an integrated FO-MD hybrid system. *AIChE J.* **2013**, *59*, 1245–1254. [[CrossRef](#)]
120. Mangindaan, D.W.; Woon, N.M.; Shi, G.M.; Chung, T.S. P84 polyimide membranes modified by a tripodal amine for enhanced pervaporation dehydration of acetone. *Chem. Eng. Sci.* **2015**, *122*, 14–23. [[CrossRef](#)]
121. Xu, A.W.; Ma, Y.; Cölfen, H. Biomimetic mineralization. *J. Mater. Chem.* **2007**, *17*, 415–449. [[CrossRef](#)]
122. Cai, Y.; Yao, J. Effect of proteins on the synthesis and assembly of calcium phosphate nanomaterials. *Nanoscale* **2010**, *20*, 1842–1848. [[CrossRef](#)] [[PubMed](#)]
123. Mondal, B.; Song, J.; Neese, F.; Ye, S. Bio-inspired mechanistic insights into CO<sub>2</sub> reduction. *Curr. Opin. Chem. Biol.* **2015**, *25*, 103–109. [[CrossRef](#)] [[PubMed](#)]
124. Seoane, B.; Coronas, J.; Gascon, I.; Benavides, M.E.; Karvan, O.; Caro, J. Metal-organic framework based mixed matrix membranes: A solution for highly efficient CO<sub>2</sub> capture? *Chem. Soc. Rev.* **2015**, *44*, 2421–2444. [[CrossRef](#)] [[PubMed](#)]
125. Feng, H.; Wu, S.; Huang, S.; Wu, Y.; Gao, J. Regenerable magnesium-based sorbent for high-pressure and moderate-temperature CO<sub>2</sub> capture: Physicochemical structures and capture performances. *Fuel* **2015**, *159*, 559–569. [[CrossRef](#)]
126. Alaswad, A.; Dassisti, M.; Prescott, T.; Olabi, A. Technologies and developments of third generation biofuel production. *Renew. Sustain. Energy Rev.* **2015**, *51*, 1446–1460. [[CrossRef](#)]
127. Alshehry, A.S.; Belloumi, M. Energy consumption, carbon dioxide emissions and economic growth: The case of Saudi Arabia. *Renew. Sustain. Energy Rev.* **2015**, *41*, 237–247. [[CrossRef](#)]
128. Ampelli, C.; Perathoner, S.; Centi, G. CO<sub>2</sub> utilization: An enabling element to move to a resource- and energy-efficient chemical and fuel production. *Philos. Trans. R. Soc. A* **2015**, *373*, 1–35. [[CrossRef](#)] [[PubMed](#)]
129. Ang, R.R.; Sin, L.T.; Bee, S.T.; Tee, T.T.; Kadhum, A.; Rahmat, A.; Wasmi, B.A. A review of copolymerization of greenhouse gas carbon dioxide and oxiranes to produce polycarbonate. *J. Clean. Prod.* **2015**, *102*, 1–17. [[CrossRef](#)]

130. Anjos, M.; Fernandes, B.D.; Vicente, A.A.; Teixeira, J.A.; Dragone, G. Optimization of CO<sub>2</sub> bio-mitigation by *Chlorella vulgaris*. *Bioresour. Technol.* **2013**, *139*, 149–154. [[CrossRef](#)] [[PubMed](#)]
131. Babu, P.; Linga, P.; Kumar, R.; Englezos, P. A review of the hydrate based gas separation (HBGS) process for carbon dioxide pre-combustion capture. *Energy* **2015**, *85*, 261–279. [[CrossRef](#)]
132. Bacik, D.B.; Yuan, W.; Roberts, C.B.; Eden, M.R. Systems analysis of benign hydrogen peroxide synthesis in supercritical CO<sub>2</sub>. *Comput. Aided Chem. Eng.* **2011**, *29*, 392–396.
133. Berg, I.A. Ecological aspects of the distribution of different autotrophic CO<sub>2</sub> fixation pathways. *Appl. Environ. Microbiol.* **2011**, *77*, 1925–1936. [[CrossRef](#)] [[PubMed](#)]
134. Centi, G.; Perathoner, S. Opportunities and prospects in the chemical recycling of carbon dioxide to fuels. *Catal. Today* **2009**, *148*, 191–205. [[CrossRef](#)]
135. Cheah, W.Y.; Show, P.L.; Chang, J.S.; Ling, T.C.; Juan, J.C. Biosequestration of atmospheric CO<sub>2</sub> and flue gas-containing CO<sub>2</sub> by microalgae. *Bioresour. Technol.* **2015**, *184*, 190–201. [[CrossRef](#)] [[PubMed](#)]
136. Chen, C.Y.; Zhao, X.Q.; Yen, H.W.; Ho, S.H.; Cheng, C.L.; Lee, D.J.; Bai, F.W.; Chang, J.S. Microalgae-based carbohydrates for biofuel production. *Biochem. Eng. J.* **2013**, *78*, 1–10. [[CrossRef](#)]
137. Cheng, J.; Huang, Y.; Feng, J.; Sun, J.; Zhou, J.; Cen, K. Improving CO<sub>2</sub> fixation efficiency by optimizing *Chlorella* PY-ZU1 culture conditions in sequential bioreactors. *Bioresour. Technol.* **2013**, *144*, 321–327. [[CrossRef](#)] [[PubMed](#)]
138. Cheng, J.; Huang, Y.; Feng, J.; Sun, J.; Zhou, J.; Cen, K. Mutate *Chlorella* sp. by nuclear irradiation to fix high concentrations of CO<sub>2</sub>. *Bioresour. Technol.* **2013**, *136*, 496–501. [[CrossRef](#)] [[PubMed](#)]
139. Cheng, H.H.; Whang, L.M.; Chan, K.C.; Chung, M.C.; Wu, S.H.; Liu, C.P.; Tien, S.Y.; Chen, S.Y.; Chang, J.S.; Lee, W.J. Biological butanol production from microalgae-based biodiesel residues by *Clostridium acetobutylicum*. *Bioresour. Technol.* **2015**, *184*, 379–385. [[CrossRef](#)] [[PubMed](#)]
140. Chiang, C.L.; Lee, C.M.; Chen, P.C. Utilization of the cyanobacteria *Anabaena* sp. CH1 in biological carbon dioxide mitigation processes. *Bioresour. Technol.* **2011**, *102*, 5400–5405. [[CrossRef](#)] [[PubMed](#)]
141. Fulke, A.B.; Krishnamurthi, K.; Giripunje, M.D.; Devi, S.S.; Chakrabarti, T. Biosequestration of carbon dioxide, biomass, calorific value and biodiesel precursors production using a novel flask culture photobioreactor. *Biomass Bioenergy* **2015**, *72*, 136–142. [[CrossRef](#)]
142. Corsten, M.; Ramírez, A.; Shen, L.; Koornneef, J.; Faaij, A. Environmental impact assessment of CCS chains—Lessons learned and limitations from LCA literature. *Int. J. Greenh. Gas Control* **2013**, *13*, 59–71. [[CrossRef](#)]
143. Nykvist, B. Ten times more difficult: Quantifying the carbon capture and storage challenge. *Energy Policy* **2013**, *55*, 683–689. [[CrossRef](#)]
144. Sovacool, B.K.; Brossmann, B. Symbolic convergence and the hydrogen economy. *Energy Policy* **2010**, *38*, 1999–2012. [[CrossRef](#)]
145. Sovacool, B.K.; Ramana, M.V. Back to the future: Small modular reactors, nuclear fantasies, and symbolic convergence. *Sci. Technol. Hum. Values* **2015**, *40*, 96–125. [[CrossRef](#)]
146. Verdon, J.P. Significance for secure CO<sub>2</sub> storage of earthquakes induced by fluid injection. *Environ. Res. Lett.* **2014**, *9*, 1–10. [[CrossRef](#)]
147. Vesnic-Alujevic, L.; Breitegger, M.; Guimarães Pereira, A. What smart grids tell about innovation narratives in the European Union: Hopes, imaginaries and policy. *Energy Res. Soc. Sci.* **2016**, *12*, 16–26. [[CrossRef](#)]
148. Lisjak, M.; Lee, A.Y.; Gardner, W.L. When a threat to the brand is a threat to the self: The importance of brand identification and implicit self-esteem in predicting defensiveness. *Personal. Soc. Psychol. Bull.* **2012**, *38*, 1120–1132. [[CrossRef](#)] [[PubMed](#)]
149. Little, M.G.; Jackson, R.B. Potential impacts of leakage from deep CO<sub>2</sub> gas sequestration on overlying freshwater aquifers. *Environ. Sci. Technol.* **2010**, *44*, 9225–9232. [[CrossRef](#)] [[PubMed](#)]
150. Hoggett, P. Government and the perverse social defence. *Br. J. Psychiatry* **2010**, *26*, 202–212. [[CrossRef](#)]
151. Mondal, M.K.; Balsora, H.K.; Varshney, P. Progress and trends in CO<sub>2</sub> capture/ separation technologies: A review. *Energy* **2012**, *46*, 431–441. [[CrossRef](#)]
152. Rubin, E.S.; Chen, C.; Rao, A.B. Cost and performance of fossil fuel power plants with CO<sub>2</sub> capture and storage. *Energy Policy* **2007**, *35*, 4444–4454. [[CrossRef](#)]
153. Cau, G.; Tola, V.; Deiana, P. Comparative performance assessment of USC and IGCC power plants integrated with CO<sub>2</sub> capture systems. *Fuel* **2014**, *116*, 820–833. [[CrossRef](#)]
154. Wang, M.; Lawal, A.; Stephenson, P.; Sidders, J.; Ramshaw, C. Post-combustion CO<sub>2</sub> capture with chemical absorption: A state-of-the-art review. *Chem. Eng. Res. Des.* **2011**, *89*, 1609–1624. [[CrossRef](#)]

155. Scheffknecht, G.; Al-Makhadmeh, L.; Schnell, U.; Maier, J. Oxy-fuel coal combustion—A review of the current state-of-the-art. *Int. J. Greenh. Gas Control* **2011**, *5*, 16–35. [[CrossRef](#)]
156. Kundu, P.K.; Chakma, A.; Feng, X. Effectiveness of membranes and hybrid membrane processes in comparison with absorption using amines for post combustion CO<sub>2</sub> capture. *Int. J. Greenh. Gas Control* **2014**, *28*, 248–256. [[CrossRef](#)]
157. Rehfeldt, S.; Kuhr, C.; Schiffer, F.P.; Weckes, P.; Bergins, C. First test results of oxyfuel combustion with Hitachi's DST-burner at Vattenfall's 30 MWth pilot plant at schwarze pumpe. *Energy Procedia* **2011**, *4*, 1002–1009. [[CrossRef](#)]
158. Cormos, C.C.; Vatopoulos, K.; Tzimas, E. Assessment of the consumption of water and construction materials in state-of-the-art fossil fuel power generation technologies involving CO<sub>2</sub> capture. *Energy* **2013**, *51*, 37–49. [[CrossRef](#)]
159. De Visser, E.; Hendriks, C.; Barrio, M.; Mølnvik, M.J.; de Koeijer, G.; Liljemark, S. Dynamics CO<sub>2</sub> quality recommendations. *Int. J. Greenh. Gas Control* **2008**, *2*, 478–484. [[CrossRef](#)]
160. Skorek-Osikowska, A.; Bartela, L.; Kotowicz, J. A comparative thermodynamic, economic and risk analysis concerning implementation of oxy-combustion power plants integrated with cryogenic and hybrid air separation units. *Energy Convers. Manag.* **2015**, *92*, 421–430. [[CrossRef](#)]
161. Cormos, C.C. Integrated assessment of IGCC power generation technology with carbon capture and storage (CCS). *Energy* **2012**, *42*, 434–445. [[CrossRef](#)]
162. Roy, B.; Bhattacharya, S. Oxy-fuel fluidized bed combustion using Victorian brown coal: An experimental investigation. *Fuel Process Technol.* **2014**, *117*, 23–29. [[CrossRef](#)]
163. Riaza, J.; Gil, M.V.; Álvarez, L.; Pevida, C.; Pis, J.J.; Rubiera, F. Oxy-fuel combustion of coal and biomass blends. *Energy* **2012**, *41*, 429–435. [[CrossRef](#)]
164. Al-Abbas, A.H.; Naser, J.; Hussein, E.K. Numerical simulation of brown coal combustion in a 550 MW tangentially-fired furnace under different operating conditions. *Fuel* **2013**, *107*, 688–698. [[CrossRef](#)]
165. Chaffee, A.L.; Knowles, G.P.; Liang, Z.; Zhang, J.; Xiao, P.; Webley, P.A. CO<sub>2</sub> capture by adsorption: Materials and process development. *Int. J. Greenh. Gas Control* **2007**, *1*, 11–18. [[CrossRef](#)]
166. Yang, H.; Xu, Z.; Fan, M.; Gupta, R.; Slimane, R.B.; Bland, A.E.; Wright, I. Progress in carbon dioxide separation and capture: A review. *J. Environ. Sci.* **2008**, *20*, 14–27. [[CrossRef](#)]
167. Othman, M.R.; Zakaria, M.R.; Fernando, W.J.N. Strategic planning on carbon capture from coal fired plants in Malaysia and Indonesia: A review. *Energy Policy* **2009**, *37*, 1718–1735. [[CrossRef](#)]
168. Rivas, O.R.; Prausnitz, J.M. Sweetening of sour natural gases by mixed-solvent absorption: Solubilities of ethane, carbon dioxide, and hydrogen sulfide in mixtures of physical and chemical solvents. *AIChE J.* **1979**, *25*, 975–984. [[CrossRef](#)]
169. Álvarez, L.; Yin, C.; Riaza, J.; Pevida, C.; Pis, J.J.; Rubiera, F. Biomass co-firing under oxyfuel conditions: A computational fluid dynamics modelling study and experimental validation. *Fuel Process Technol.* **2014**, *120*, 22–33. [[CrossRef](#)]
170. Cormos, C.C. Evaluation of energy integration aspects for IGCC-based hydrogen and electricity co-production with carbon capture and storage. *Int. J. Hydrog. Energy* **2010**, *35*, 7485–7497. [[CrossRef](#)]
171. Bade, M.H.; Bandyopadhyay, S. Analysis of gas turbine integrated cogeneration plant: Process integration approach. *Appl. Therm. Eng.* **2015**, *78*, 118–128. [[CrossRef](#)]
172. Dinca, C.; Badea, A. The parameters optimization for a CFBC pilot plant experimental study of post-combustion CO<sub>2</sub> capture by reactive absorption with MEA. *Int. J. Greenh. Gas Control* **2013**, *12*, 269–279. [[CrossRef](#)]
173. Domenichini, R.; Arienti, S.; Cotone, P.; Santos, S. Evaluation and analysis of water usage and loss of power in plants with CO<sub>2</sub> capture. *Energy Procedia* **2011**, *4*, 1925–1932. [[CrossRef](#)]
174. Tola, V.; Pettinau, A. Power generation plants with carbon capture and storage: A techno-economic comparison between coal combustion and gasification technologies. *Appl. Energy* **2014**, *113*, 1461–1474. [[CrossRef](#)]
175. Oehlert, A.M.; Lamb-Wozniak, K.A.; Devlin, Q.B.; Mackenzie, G.J.; Reijmer, J.J.G.; Swart, P.K. The stable carbon isotopic composition of organic material in platform derived sediments: Implications for reconstructing the global carbon cycle. *Sedimentology* **2012**, *59*, 319–335. [[CrossRef](#)]
176. Diaf, A.; Beckman, E. Thermally reversible polymeric sorbents for acid gases. III. CO<sub>2</sub>-Sorption enhancement in polymer-anchored amines. *React. Funct. Polym.* **1995**, *27*, 45–51. [[CrossRef](#)]

177. Seckin, T.; Alici, B.; Çetinkaya, E.; Özdemir, I. Synthesis and characterization of N-substituted 1,4,5,6-tetrahydropyrimidine containing functional polymers as SO<sub>2</sub> and CO<sub>2</sub> sorbents. *J. Polym. Sci. A Polym. Chem.* **1997**, *35*, 2411–2420. [[CrossRef](#)]
178. Schacht, U.; Jenkins, C. Soil gas monitoring of the Otway project demonstration site in SE Victoria, Australia. *Int. J. Greenh. Gas Control* **2014**, *24*, 14–29. [[CrossRef](#)]
179. Beaubien, S.E.; Jones, D.G.; Gal, F.; Barkwith, A.K.A.P.; Braibant, G.; Baubron, J.C.; Ciotoli, G.; Graziani, S.; Lister, T.R.; Lombardi, S.; et al. Monitoring of near-surface gas geochemistry at the Weyburn, Canada, CO<sub>2</sub>-EOR site, 2001–2011. *Int. J. Greenh. Gas Control* **2013**, *16*, 236–240. [[CrossRef](#)]
180. Maver, M. Barriers to Carbon Capture and Storage. Available online: <http://ehsjournal.org/marko-maver/barriers-to-carbon-capture-and-storage-ccs/2012/> (accessed on 5 June 2016).
181. Zhang, C.; Zhou, D.; Li, P.; Li, F.; Zhang, Y.; Sun, Z.; Zhao, Z. CO<sub>2</sub> storage potential of the Qiongdongnan Basin, north western South China Sea. *Greenh. Gases Sci. Technol.* **2014**, *4*, 1–16.
182. Lee, M.Y.; Hashim, H. Modelling and optimization of CO<sub>2</sub> abatement strategies. *J. Clean. Prod.* **2014**, *71*, 40–47. [[CrossRef](#)]
183. Leion, H.; Jerndal, E.; Steenari, B.M.; Hermansson, S.; Israelsson, M.; Jansson, E.; Johnsson, M.; Thunberg, R.; Vadenbo, A.; Mattisson, T.; et al. Solid fuels in chemical-looping combustion using oxide scale and unprocessed iron ore as oxygen carriers. *Fuel* **2009**, *88*, 1945–1954. [[CrossRef](#)]
184. Man, Y.; Yang, S.; Xiang, D.; Li, X.; Quian, Y. Environmental impact and techno economic analysis of the coal gasification process with/without CO<sub>2</sub> capture. *J. Clean. Prod.* **2014**, *71*, 59–66. [[CrossRef](#)]
185. Mores, P.; Rodríguez, N.; Scenna, N.; Mussati, S. CO<sub>2</sub> capture in power plants: Minimization of the investment and operating cost of the post-combustion process using MEA aqueous solution. *Int. J. Greenh. Gas Control* **2012**, *10*, 148–163. [[CrossRef](#)]



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