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Coupled Photocatalysis and Microalgal–Bacterial Synergy System for Continuously Treating Aquaculture Wastewater Containing Real Phthalate Esters

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Abstract: We developed a system combining visible-light photocatalysis with biological treatment for the continuous removal of phthalate esters (PAEs) from both synthetic and real aquaculture wastewater. We investigated the effects of different operating factors, including the coexistence of glucose or PAEs, on individual PAE removal by using a photobiological system (PBS). In wastewater containing a mixture of PAEs, that is, containing di-(2-ethylhexyl)phthalate (DEHP), dibutyl phthalate (DBP), and dimethyl phthalate (DMP), a coimmobilized bioreactor system comprising the bacterium *Pseudomonas putida* and the microalga *Chlorella vulgaris* demonstrated a higher removal efficiency than immobilized *P. putida* alone or a coculture of immobilized *P. putida* and suspended *C. vulgaris* did. The PBS employed for the continuous treatment of real aquaculture wastewater containing DEHP (0.62 ± 0.05 mg/L), DBP (8.7 ± 0.9 mg/L), and DMP (17.4 ± 1.5 mg/L) achieved at least 99.5% PAE removal and 99.2% mineralization efficiency under optimal operating conditions. After 42 days of treatment, inoculated *Pseudomonas* (98.12%) remained the predominant genus in the bioreactor. The results reveal that the symbiotic microalgal–bacterial system is a feasible alternative to a pure *P. putida* immobilized bioreactor for reducing CO₂ emissions from mineralized PAEs through microalgal activity.

Keywords: visible-light photocatalysis; di-(2-ethylhexyl) phthalate; di-butyl phthalate; di-methyl phthalate; photobiological system; immobilized bioreactor



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1. Introduction

Phthalate esters (PAEs) are crucial industrial chemicals and commonly used as plasticizers to improve the flexibility and processability of polymer materials [1]. Furthermore, PAEs are extensively used as plasticizers in polymer production. However, they can be released from plastic products into the environment [2]. PAEs can be categorized as short alkane chain and long alkane chain. Short-alkane-chain PAEs are commonly used in personal care products, cosmetics, and plastic bags, whereas long-alkane-chain PAEs are mainly used in plastic polymers, building materials, furniture, and food contact materials [3].

Numerous countries currently list PAEs as priority pollutants and endocrine-disrupting compounds for assessing and controlling phthalate pollution because of their association with various human and animal diseases [4]. PAEs can bind to cellular targets in the human body and interfere with hormone reactions, leading to various disorders. Moreover, PAEs are suspected to interfere with biological processes in wildlife, causing teratogenicity, mutagenicity, and carcinogenicity [5]. PAEs comprise diverse compounds with different structures and properties. Among them, di-(2-ethylhexyl)phthalate (DEHP), dibutyl phthalate (DBP), and dimethyl phthalate (DMP) have been discovered to be the most prevalent in the environment, wastewater, and sludge [6,7].

Advanced oxidation processes (AOPs), such as photocatalysis, have been suggested for the removal of PAEs from the environment [1]. Photocatalysis is highly effective in eliminating PAEs from water because it generates potent, nonselective oxidants through light-driven reactions [8]. However, achieving complete mineralization of PAEs is energy-intensive, rendering photocatalysis inefficient if used alone [9]. Biodegradation facilitated by microbes was also reported to be a key method of initiating PAE degradation. Although biological degradation of PAEs is both cost-effective and environmentally friendly [10], it is time-consuming, requiring an extended period before the amount of PAE is reduced to harmless levels [11].

Simultaneous coupling of photocatalytic and microbial processes can serve as an exceptionally efficient system, combining the advantages of both processes for the effective removal of PAEs [12]. In our previous studies, we developed a system involving TiO₂ photocatalysis under visible-light irradiation [4]. This system uses the solar spectrum, incorporating the visible-light region into the TiO₂ matrix to broaden its photoresponsive capability [4]. We analyzed the optimal operating conditions for PAE removal by using a visible-light photoreactor. When combined with a packed-bed reactor (PBR), our visible-light photo-pretreatment method achieved removal efficiencies of over 95% for individual PAEs in synthetic wastewater [4].

The concept of algae–bacteria consortia was initially proposed in 1981 [13]. Since then, these consortia have been used for the treatment of wastewater and detoxification of environmental pollutants. During photosynthesis, algae produce O₂, which is used by bacteria. Subsequently, bacteria degrade organic pollutants, releasing CO₂ that is beneficial for algal growth [14]. However, few studies have successfully developed a symbiotic algae–bacteria system for wastewater treatment [15]. We modified our previously designed packed-bed reactor, using a microalgae–bacteria consortia bioreactor rather than a PAE-degrading bacterial strain [4].

In a real wastewater environment, PAEs often coexist with other organic pollutants. We analyzed ten aquaculture ponds and found that the concentrations of DEHP ranged from 0.18–0.89 mg/L. We selected one aquaculture pond as our research model. The concentrations of DEHP, DBP, and DMP were 0.62 ± 0.05 mg/L, 8.7 ± 0.9 mg/L, and 17.4 ± 1.5 mg/L, respectively. In the present study, we investigated the efficiency of PBS in removing PAEs from synthetic and real wastewater. In addition, we investigated the effects of the coexistence of organic pollutants or PAEs on the removal efficiencies of individual PAEs. Furthermore, we evaluated changes in the bacterial community in the immobilized bioreactor before and after PBS treatment. The results of this study can provide insight into strategies that can be used for PAE removal in a real wastewater environment and CO₂ reduction across various environments toward an environmentally friendly and sustainable future.

2. Materials and Methods

2.1. Materials

Analytical-grade DEHP, DBP, DMP, and titanium tetraisopropoxide (TTIP) were purchased from AccuStandard Chem. Co. (New Haven, CT, USA). To ensure a neutral pH in the biological system, we automatically adjusted the pH of the wastewater we used with 0.1 M HCl or 0.1 M NaOH in the storage tank. A PAE (DEHP, DBP, and DMP) stock solution (100 mg/L) was prepared as described in our previous studies [4]. We additionally used a mineral medium (g/L) containing 1.09 KH₂PO₄, 2.10 K₂HPO₄, 0.40 (NH₄)₂SO₄, 0.29 CaCl₂, 0.21 MgSO₄, 0.21 MnSO₄, and 0.02 FeSO₄. All culture media, biochemical reagents, and chemicals were purchased from Sigma–Aldrich (Saint Louis, MO, USA) unless stated otherwise.

2.2. Synthesis of I-Doped TiO₂ and Preparation of I-Doped-TiO₂-Coated Beads

We synthesized I-doped TiO₂ following the method reported by Štengl and Grygar [4] and Hung et al. [11] with some modifications. First, 0.89 mL TTIP was mixed with 10 mL

isopropanol solution (0.3 M). The mixture was gently stirred for 30 min, and distilled water and alcohol were gradually added until the hydrogel solution appeared white and cloudy. Next, 35% HCl was added, and the pH of the solution was adjusted to 3–4 until the white turbidity in the solution changed to that of a white transparent gel. The resulting 100 mL transparent gel was mixed with 100 mL of 30% H₂O₂ solution, which caused it to form into a yellow gelatinous mass. This mass was subsequently mixed with 0.7 g of KI and heated at 80 °C until a yellowish-white precipitate formed. After standing for 30 h, the color of the precipitate changed to white, resulting in the formation of I-doped TiO₂ powder.

I-doped-TiO₂-coated beads were prepared using the same procedure as described in our previous studies [4]. First, 0.5 g of I-doped TiO₂ was mixed with 1 mL of solution containing 0.1 mL acetylacetone. The mixture was gently stirred until a viscous paste was formed. Subsequently, the paste was combined with 1.7 mL distilled water and 0.05 mL Triton X-100 and then mixed with 15 g of silica glass beads (id = 2 cm). The beads were coated with I-doped TiO₂ and were then removed from the liquid, heated for 10 min at 80 °C, and further heated for 30 min at 450 °C in an oven to immobilize the I-doped TiO₂ on the beads. The concentration, specific surface area, and crystal size of the I-doped TiO₂ on the surface of the glass beads were 0.38%, 205 m²/g, and 29.8 nm, respectively.

2.3. Microalgae and Bacterial Culture

Chlorella, a microalgae species, was selected because of its widespread use in wastewater treatment and its prevalence in municipal wastewater treatment systems [16]. In our preliminary investigations, we analyzed some *Chlorella* species and determined that *Chlorella vulgaris* exhibited favorable mutualistic growth when cocultivated with the PAE-degrading bacterial strain *Pseudomonas putida* [4]. *C. vulgaris* was isolated from an aquaculture pond in Tainan City. It was cultivated in 1 L Erlenmeyer flasks containing BG-11 medium under sterile conditions, was maintained at 25 °C, was exposed to white fluorescent light illumination at 60 μmole/m²/s, and was subjected to a 12:12 h light/dark cycle. The culture medium was then removed through centrifugation for 10 min at 5000 rpm, and the *C. vulgaris* biomass was diluted before it was introduced into the bioreactor. *P. putida* was routinely cultured in Luria–Bertani (LB) broth at 30 °C prior to being used in PAE treatment. As with *C. vulgaris*, *P. putida* biomass was collected through centrifugation for 10 min at 5000 rpm.

The *C. vulgaris* and *P. putida* biomasses were washed three times with 0.8% sterilized NaCl solution. The concentrations of *C. vulgaris* and *P. putida* were 1.5×10^6 cells/mL and 2×10^8 CFU/mL in the prepared inflow solution, respectively. The inoculum ratio of immobilized microalgae to bacteria was determined by considering the findings of the preliminary study.

2.4. Coupled PBS design

The coupled PBS mainly consisted of a photoreactor, a storage tank, and a bioreactor, as described in our previous studies [4]. The cylindrical concentric glass photoreactor (length 50 cm) was composed of an inner cylinder (id = 5 cm) and an outer cylinder (id = 7 cm). A xenon lamp served as the light source and was placed on the inner cylinder. I-doped-TiO₂-coated beads were packed in the outer cylinder of the photoreactor (with a packing height of 30 cm and a packing volume of 565 mL). Synthetic wastewater (with a pH of 5.0) or real aquaculture wastewater containing different PAE concentrations was continuously introduced into the photoreactor using an upward flow mode through a peristaltic pump. The photolytic conditions were 30 °C, a liquid retention time (RT) of 5.5 min, and a light intensity of 300 W, and wavelength was 420–440 nm unless stated otherwise. The effluent's pH value was automatically adjusted to 7 in the storage tank, and the effluent was continuously piped to the PBR with a peristaltic pump.

The bioreactor was a cylindrical packed-bed reactor (length = 150 cm, id = 20 cm) constructed from acrylic material. It had two ports at the top for measuring pH and dissolved oxygen (DO). Wastewater from the photoreactor outlet was directed into the

storage tank and then continuously introduced into the PBR in an upward flow mode with a retention time of 4 h, unless stated otherwise.

Three types of microbiota consortia were used in the PBR: immobilized *P. putida*, a coimmobilized culture of *C. vulgaris* and *P. putida*, and a coculture of immobilized *P. putida* and suspended *C. vulgaris*. The inoculation methods were as follows: In the first consortium, 2.5 L packed volumes of plastic Raschig rings (rosette type; id = 2 cm) were placed in the PBR as packing material. LB broth containing *P. putida* (2×10^8 CFU/mL) was continuously introduced into the PBR at a retention time of 24 h for 2 weeks to achieve immobilization. In the second consortium, LB broth containing *P. putida* (2×10^8 CFU/mL) and *C. vulgaris* (1.5×10^6 cells/mL) was continuously introduced into the PBR at a retention time of 24 h for 2 weeks to achieve microalgae–bacteria coimmobilization. In the third consortium, *P. putida* was immobilized for 2 weeks, and precultured *C. vulgaris* (1.5×10^6 cells/mL) was then suspended in the PBR. In the preliminary test, we analyzed the survival rate of the test organisms (microalgae and bacteria) by I-doped TiO₂, and the survival rate was not significantly decreased before or after the operation process ($p > 0.05$).

2.5. Effect of Operation Parameters on PAE Removal Efficiency

To evaluate the effect of the coexistence of PAEs on the efficiency of their removal, synthetic wastewater containing individual PAEs (20 mg/L) or a mixture (20 mg/L each of DEHP, DBP, and DMP) was continuously introduced into the coupled photoimmobilized *P. putida* biological system. To evaluate the matrix effects of real aquaculture wastewater on PAE removal efficiency, synthetic wastewater containing a mixture of PAEs (20 mg/L each of DEHP, DBP, and DMP) was mixed with easily degraded organic compounds (glucose) at 0–20 mg/L and introduced continuously into the coupled photoimmobilized *P. putida* biological system. To evaluate the effect of the microbiota consortium (immobilized *P. putida*, a coimmobilized culture of *C. vulgaris* and *P. putida*, and a coculture of immobilized *P. putida* and suspended *C. vulgaris*) in the PBR on PAE removal efficiency, synthetic wastewater containing a mixture of PAEs (20 mg/L each of DEHP, DBP, and DMP) was continuously introduced into the coupled PBS. To investigate the effect of shock loading on PAE removal efficiency, real PAE-containing wastewater was obtained from an aquaculture pond located in Tainan City (Taiwan), filtered through two layers of gauze, and introduced continuously into the coupled photo-coimmobilized *C. vulgaris*–*P. putida* biological system. Real PAE-containing wastewater was introduced into the photoreactor at a retention time of 5.5 min for 14 days, 4.5 min for the subsequent 14 days, and 5.5 min for the subsequent 14 days. The bioreactor was constantly operated for 42 days at a retention time of 4 h. The concentrations of PAEs were determined once every 30 min, and the results (that is, the removal efficiency) are expressed as an average value over 4 h. Furthermore, we analyzed the bacterial communities in the real PAE-containing wastewater, the bioreactor before system startup, and the bioreactor after 42 days of operation.

2.6. Identification of Bacterial Communities

Bacterial communities in both the influent (real PAE-containing wastewater) and the biofilm of the bioreactor were analyzed using next-generation sequencing (NGS). Cell lysis, DNA extraction, polymerase chain reaction amplification, and 454 pyrosequencing were conducted following processes described by Wu et al. [17]. DNA was extracted using a Fast DNA SPIN Kit (MP Biomedicals). The PCR primers GAGTTTGATCNTGGCTCAG (forward) and GTNTTACNGCGGCKGCTG (reverse) were used to amplify the eubacterial 16S rRNA fragment. The PCR protocol involved an initial denaturation step at 95 °C for 10 min followed by 35 cycles of denaturation at 94 °C for 45 s, with annealing at 55 °C for 1 min, extension at 72 °C for 1 min, and a final extension at 72 °C for 10 min. All of the partial 16S rRNA gene sequences were preprocessed following methods described by Wu et al. [17]. Sequence analysis was performed using the QIIME software package (2020.2.0.). These analyzed sequences were clustered into operational taxonomic units (OTUs) with consideration of a 0.97 sequence similarity threshold by using the UCLUST algorithm.

Representative OTUs were selected with consideration of the most abundant sequences, and taxonomic assignment was performed using the ribosomal database project classifier.

2.7. Chemical Analysis

The concentrations of PAEs were analyzed using a high-performance liquid chromatography system (Hitachi, Japan) equipped with two Hitachi L-6000 pumps and one L-5000 LC controller. These concentrations were detected at 280 nm by using a Hitachi L-4200 UV/VIS detector. The HPLC analysis was performed with a C18 column (4.6 mm ID × 250 mm, 5 μm). The mobile phase was isocratic CHCl₃:C₆H₁₄ (3:7) and the flow rate was at 1 mL/min. The intermediate products of the PAEs generated through photocatalysis were obtained through solid-phase extraction. Subsequently, the extracted samples were evaporated into vials and injected into a gas chromatography (GC)–mass spectrometer (MS). The GC–MS system included an HP 5890 series II GC and a HP 5971 MS detector (Agilent, Santa Clara, CA, USA). GC separation was performed using an Ultra-2 fused silica capillary column (0.2 mm ID × 25 m), with temperature programming ranging from 100 °C to 280 °C. Helium was used as the carrier gas and the gas flow rate was 31 cm/s. The injector and detector temperatures were set at 250 and 280 °C, respectively. The analysis of intermediate products was carried out in EI mode, 70 eV, and full scan.

3. Results and Discussion

3.1. Effect of Coexisting PAEs on PAE Removal in PBS

In a real wastewater environment, PAEs typically coexist as a mixture of more than one pollutant [18]. To investigate the effect of these coexisting PAEs on individual PAE removal, we analyzed the removal efficiencies of DEHP, DBP, and DMP in a PAE mixture by using PBS. The removal efficiencies of DEHP, DBP, and DMP were slightly affected by the coexistence of PAEs (Figure 1). Furthermore, the removal efficiencies of DEHP (98.1% ± 0.15%), DBP (99.0% ± 0.08%), and DMP (99.8% ± 0.03%) in the mixture were slightly lower than those in the samples of individual PAEs (DEHP: 99.6% ± 0.02%; DBP: 99.9% ± 0.005%; DMP: 100.0% ± 0.004%) at the same concentration. When only the photocatalytic efficiency was evaluated, whether PAEs were alone or in a mixture had a minimal effect on the removal efficiency. Coexisting PAEs mainly had an effect on the removal efficiency in the biotreatment stage. The removal of recalcitrant PAEs was affected when the PAE mixture was present in the wastewater, with DEHP removal being the most significantly affected. Xie et al. [19] indicated that the coexistence of PAEs in the environment affects microbial degradation. Even when bacteria exhibit a preference for a certain PAE as substrate, the addition of other PAEs might lead to an inhibitory effect, which does not occur in the presence of only a single PAE.

Unlike in our previous studies, in the current study, the PBS achieved higher PAE removal efficiencies than photoreactor treatment alone did (86.5% for DEHP at 20 mg/L) [4]. Furthermore, our system achieved a higher DEHP removal efficiency than the oxidative Fenton reaction (H₂O₂/Fe²⁺) system (85.6% for DEHP at 20 mg/L) [20] and the photo-Fenton–biological system did (60% for DEHP at 20 mg/L) [21]. In addition, our coupled PBS system achieved a similar DEHP removal efficiency (99.6%), even when the DEHP concentration was as high as 50 mg/L in the sample of DEHP alone [4]. This is the first study to report on the removal efficiency of individual PAEs from a coexisting PAE mixture in synthetic wastewater by using PBS.

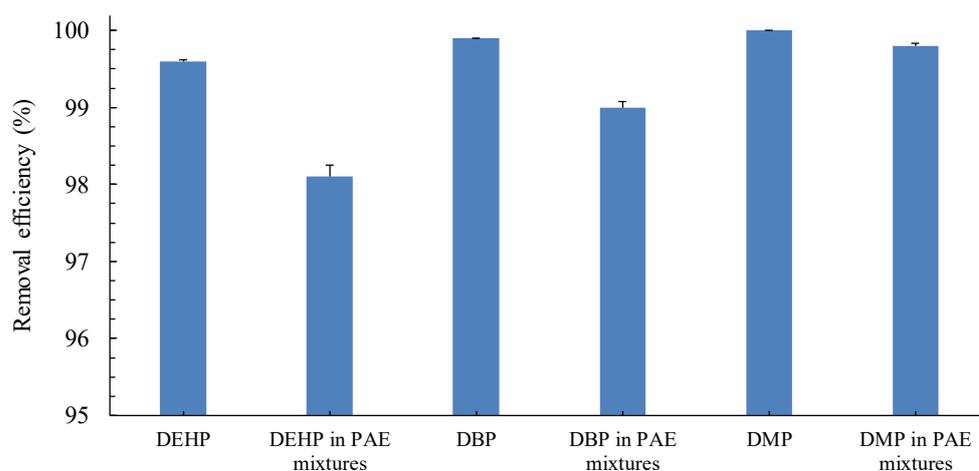


Figure 1. Effect of the coexistence of PAEs on continuous PAE removal in the coupled PBS. Individual PAEs and synthetic wastewater containing a PAE mixture (20 mg/L each of DEHP, DBP, and DMP) were introduced. The photolytic conditions were as follows: light intensity, 300 W; temperature, 30 °C; pH, 5.0; and RT, 5.5 min. The photoreactor effluent was continuously introduced into the immobilized *P. putida* PBS at an RT of 4 h.

3.2. Effects of Glucose on the Removal Efficiency of PAEs

Glucose is an easily degrading carbon source and is extensively used to induce bacterial growth [22]. In the present study, the removal efficiency of PAEs was evaluated under different glucose concentrations, which simulated the presence of coexisting organic compounds in real wastewater. When only photocatalysis was conducted, the coexistence of glucose did not exert any significant effect on PAE removal. However, the PAE removal efficiencies increased when the glucose concentration ranged from 0 to 10 mg/L and significantly decreased when the glucose concentration ranged from 10 to 20 mg/L in the immobilized *P. putida* PBR (Figure 2a). The coexistence of low glucose concentrations promoted *P. putida* growth (increase from 4.2×10^5 CFU/mL at 0 mg/L of glucose to 1.8×10^6 CFU/mL at 10 mg/L of glucose in the bioreactor), thus enhancing PAE removal. When the glucose concentration was >10 mg/L, *P. putida* preferentially degraded glucose instead of PAEs, resulting in a notable decrease in PAE removal. Correspondingly, the PAE removal efficiencies of the overall photobiological system were also decreased (Figure 2b). Short-chain DMP was more easily degraded than DEHP and DBP were (Figure 2a). Thus, their removal was not affected by the presence of coexisting glucose. Microorganisms can use glucose to metabolize or cometabolize refractory organic matter [23]. Hu and Wan [24] reported that when a mixture of PAEs and glucose serve as the carbon source, bacteria consume glucose first and then metabolize PAEs. However, the overall PAE removal efficiencies were maintained within the range of 99.6–100% in our PBS.

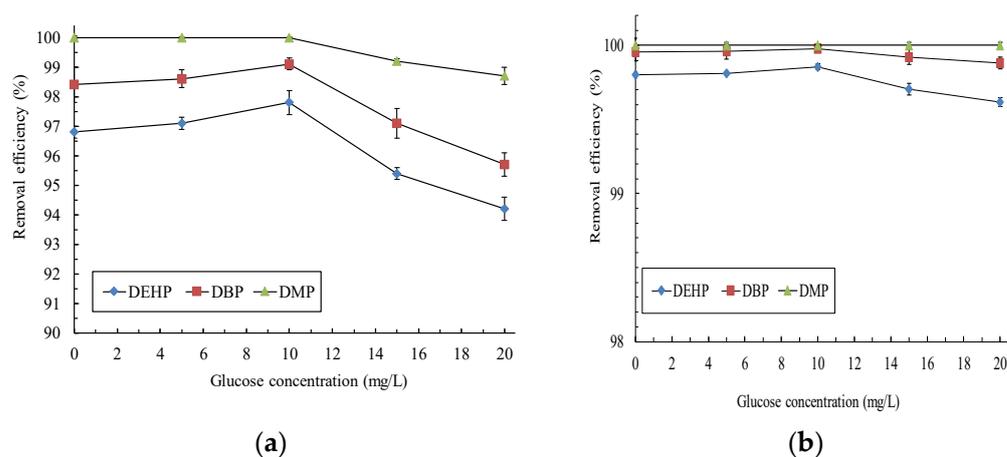


Figure 2. Effect of glucose on continuous PAE removal in (a) the immobilized *P. putida* PBR and (b) the coupled PBS. Synthetic wastewater containing a PAE mixture (20 mg/L each of DEHP, DBP, and DMP) and different glucose concentrations were introduced. The photolytic conditions were as follows: light intensity, 300 W; temperature, 30 °C; pH, 5.0; and RT, 5.5 min. The photoreactor effluent was continuously introduced into the immobilized *P. putida* PBR at a RT of 4 h.

3.3. Comparison of PAE Removal Efficiencies with Different Microbiota Consortia

The efficiencies of removing DEHP, DBP, and DMP from a coexisting PAE mixture (20 mg/L each of DEHP, DBP, and DMP) in PBS were analyzed. In the experiment, three types of microbiota consortia were used in the PBR. A coculture of immobilized *P. putida* and *C. vulgaris* exhibited a higher DEHP removal efficiency ($99.5\% \pm 0.08\%$) than did a pure culture of immobilized *P. putida* ($98.0\% \pm 0.06\%$) and a coculture of immobilized *P. putida* and suspended *C. vulgaris* ($96.8\% \pm 0.35\%$; Figure 3). Similar trends were observed for the removal of DBP and DMP (Figure 3). The results demonstrated that the PAEs were eliminated from wastewater more efficiently if microalgae coexisted in the system [16]. The findings further revealed that *C. vulgaris* preferred to remain immobilized in a matrix instead of being in free suspension during the PAE removal process. Moreover, the results indicated that *P. putida* might have a positive symbiotic relationship with *C. vulgaris* in a coimmobilized state. The adequate oxygen that is produced in the *C. vulgaris*–*P. putida* coimmobilized system is used as an electron acceptor for *P. putida*, which significantly enhances PAE degradation. Bahr et al. [25] demonstrated that a coimmobilized system completely degraded glucose. Furthermore, photosynthesis by *C. vulgaris* in the coimmobilized system can increase or balance the pH in the microenvironment, facilitating PAE biodegradation. In coimmobilized bacteria/microalgae systems, algal growth increases DO levels and pH values, leading to improved synergistic performance in pollutant removal [26].

Our results revealed that the coculture of immobilized *P. putida* and *C. vulgaris* exhibited a higher PAE removal efficiency than a pure culture of immobilized *P. putida* did. CO₂ generated from the mineralization of PAEs or other organic pollutants by *P. putida* can be absorbed by *C. vulgaris* for photosynthesis. Thus, the coimmobilized bioreactor system of *P. putida* and *C. vulgaris* is a feasible and environmentally friendly alternative to a pure *P. putida* immobilized bioreactor for carbon reduction.

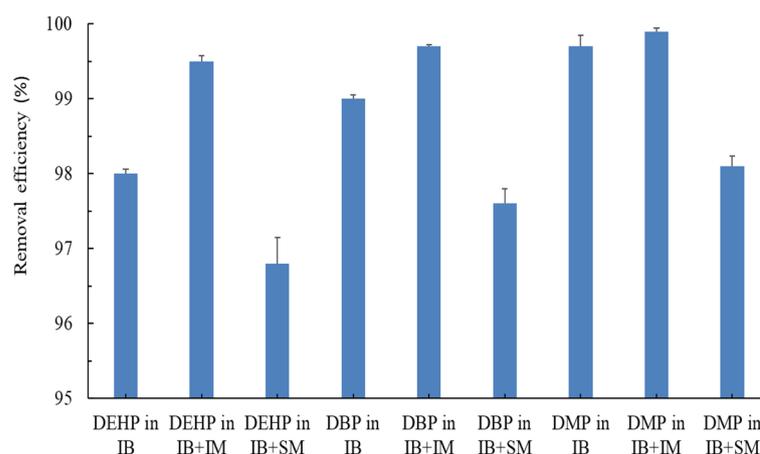


Figure 3. Removal efficiency of PAEs in the coupled PBS. Synthetic wastewater containing a PAE mixture (20 mg/L each of DEHP, DBP, and DMP) was introduced. The bioreactor included immobilized *P. putida* (IB), a coimmobilized culture of *P. putida* and *C. vulgaris* (IB + IM), and a coculture of immobilized *P. putida* and suspended *C. vulgaris* (IB + SM).

3.4. Effect of Shock Loading on the PBS

The water quality of the real aquaculture wastewater was as follows: total coliform, 3.2×10^2 CFU/mL; aerobic plate count, 6.5×10^5 CFU/mL; Cd^{2+} , 8×10^{-4} mg/L; Pb^{2+} , 2×10^{-2} mg/L; Cr^{6+} , 2×10^{-3} mg/L; Cu^{2+} , 6×10^{-4} mg/L; Zn^{2+} , 3×10^{-3} mg/L; As^{5+} , 7×10^{-4} mg/L; and Hg^{2+} , 2×10^{-4} mg/L. The concentrations of DEHP, DBP, and DMP were 0.62 ± 0.05 mg/L, 8.7 ± 0.9 mg/L, and 17.4 ± 1.5 mg/L, respectively. The total organic carbon content (TOC) from organic compounds was 22.3 mg/L and that from non-PAE organic compounds was 5.04 mg/L.

Real wastewater is prone to shock loading. Therefore, the continuous and shock-loading operation of the PBS for treating wastewater containing PAEs must be tested. Figure 4 presents the results regarding the effect of shock loading on the PAE removal efficiencies in the coupled photo-coimmobilized *C. vulgaris*–*P. putida* biological system. For an initial 14 days, the photoreactor was operated at a RT of 5.5 min, and the bioreactor was operated at a RT of 4 h. On day 7, a decline in the PAE removal efficiency and mineralization was noted. An increase was noted in the amount of suspended solids in the photoreactor, with this change being observable with the naked eye, and this increase may have caused scattering and reduced the photocatalytic efficiency. Thus, the system was temporarily shut down, and a filtration system was introduced at the inlet to remove suspended solids. Subsequently, the PAE removal efficiency increased suddenly on day 8. For instance, the DEHP removal efficiency increased from $96.9\% \pm 0.15\%$ to $99.6\% \pm 0.05\%$. From day 15 to 28, the photoreactor was operated at a RT of 4.5 min (shock loading), and the bioreactor was operated at a RT of 4 h, which had a minor effect on the PAE removal efficiencies but had a significant effect on mineralization (decrease from $99.9\% \pm 0.02\%$ to $96.2\% \pm 0.28\%$) (Figure 4). This finding indicates that some organic pollutants in the wastewater other than PAEs could not easily be completely degraded at a low RT. From day 29 to 42, the photoreactor's RT was restored to 5.5 min. During this period, the PAE removal efficiencies and mineralization were similar to those observed on days 8 to 14, indicating excellent PAE removal efficiency and mineralization ($>99.2\%$). Throughout this period, the pH and ORP in the coimmobilized *C. vulgaris*–*P. putida* biological system were maintained at 6.3–7.5 and 248–302 mV, respectively. These results indicate that our PBS can adapt to shock loading and that the effect of coexisting substances on PAE removal is limited. Pajoumshariati et al. [27] reported that an effective bioreactor process should be insensitive to shock loading or only transiently affected by it.

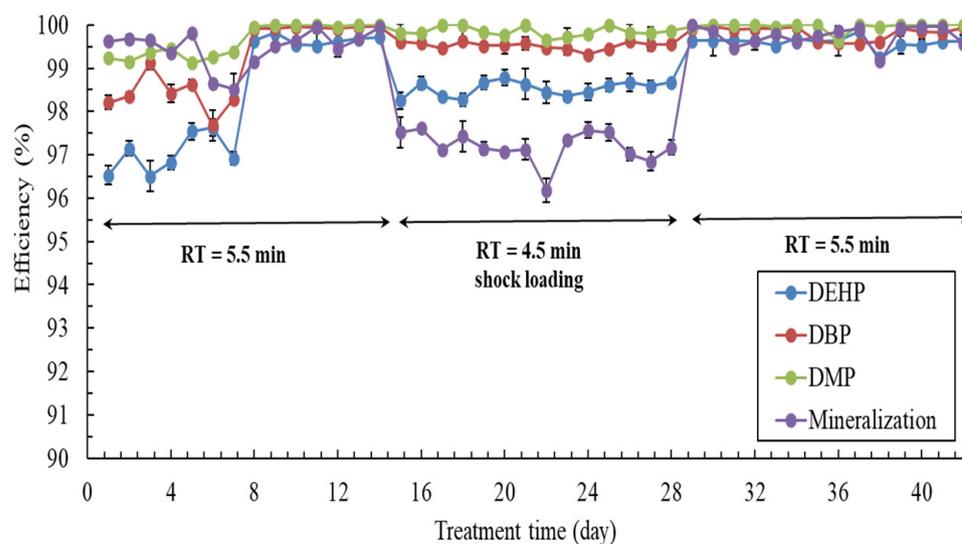


Figure 4. Effect of shock loading on PAE removal efficiencies in the coupled photo-coimmobilized *C. vulgaris*–*P. putida* biological system. Real aquaculture wastewater containing a PAE mixture was introduced. On days 1 to 14, the photoreactor was operated at a RT of 5.5 min. On days 15 to 28, the photoreactor was operated at a RT of 4.5 min (shock loading). On days 29 to 42, the photoreactor was operated at a RT of 5.5 min. The bioreactor was constantly operated at an RT of 4 h.

Regarding the presence of intermediate PAE products, we observed more complex aromatic intermediate compounds in the aquaculture wastewater in the photocatalysis system than those previously reported in synthetic wastewater [4]. This finding indicates that some aromatic intermediate compounds might originate from other PAE chemical structures that are present in real aquaculture wastewater. Yang et al. [28] observed the presence of additional PAEs in the sediments of the Dianbao River (Kaohsiung City, Taiwan), which is generally used for aquaculture, environmental conservation, and irrigation. Furthermore, Chang et al. [29] detected trace amounts of DEHP in Taiwanese aquafarm shrimps. Although no immediate health risks were discovered to be associated with consumption of these shrimps, the finding indicates that PAEs must be removed from real aquaculture wastewater. In future research, we will collect more data and think of using Spearman and Pearson correlation matrices [30] to analyze the correlation between parameters and phthalate esters.

3.5. Changes in Bacterial Communities during the PAE Treatment Process

To investigate changes in the bacterial community during the PAE treatment process, we analyzed bacterial communities through NGS. Figure 5 presents the relative abundances of bacterial 16S rRNA gene sequences at the genus level in different situations. At least 16 bacterial genera were identified in the real aquaculture wastewater, with the most abundant being *Flavobacterium* (20.64%), followed by *Edwardsiella* (12.27%), *Exiguobacterium* (9.04%), *Roseomonas* (8.12%), and *Mycobacterium* (7.38%). *Exiguobacterium* and *Roseomonas* are bacterial genera that are commonly found in freshwater culture ponds [31].

In the present study, before the PBS was used for wastewater treatment, bacterial community analysis conducted using the bioreactor revealed the presence of only three genera, with the dominant bacterial genus being *Pseudomonas* (99.68%, inoculated bacteria), followed by *Flavobacterium* (0.14%) and *Escherichia* (0.18%). Any miscellaneous bacteria beyond *Pseudomonas* that may have been detected may have resulted from contamination. *Escherichia* is commonly found in aquaculture ponds [32]. After we used the PBS to treat the real aquaculture wastewater, at least five bacteria genera were identified in the bioreactor, with *Pseudomonas* (98.12%) being the dominant genus, followed by *Exiguobacterium* (0.53%), *Roseomonas* (0.13%), *Flavobacterium* (0.26%), *Edwardsiella* (0.29%), and other genera (0.67%). These results indicate that most bacteria were killed during the photocatalytic

process, which is consistent with the notion that photocatalysis inactivates bacteria [33]. Furthermore, the relative abundance of *Roseomonas* significantly decreased in the wetland in the presence of DBP [34]. *Flavobacterium* exhibited the ability to degrade PAEs [35], and *Exiguobacterium* displayed the ability to degrade polyaromatic hydrocarbons [36]. *Edwardsiella* is a typical pathogen abundant in aquaculture environments and is known to infect some fish species, with such infection being associated with high mortality rates [37]. The findings of the present study indicate that the coupled system not only effectively removed pathogens from real wastewater but also maintained the dominance of inoculated bacteria in the bioreactor. Thus, the coupled system represents a feasible means of removing PAEs from aquaculture wastewater.

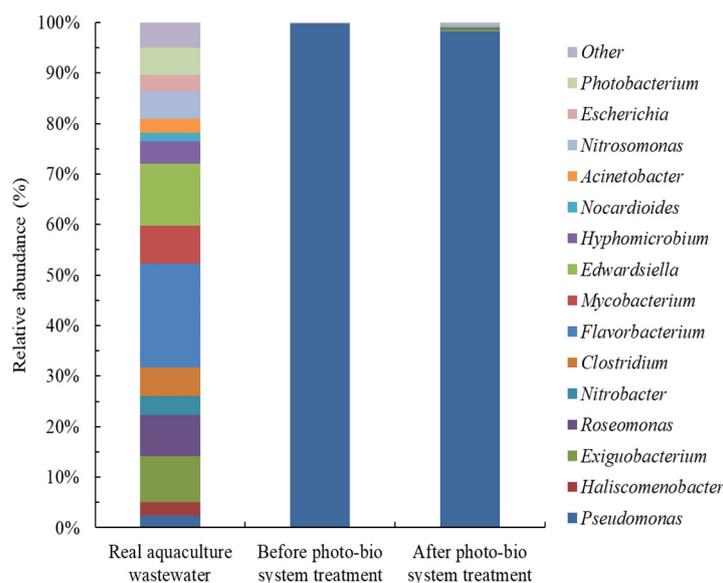


Figure 5. Bacterial communities in real aquaculture wastewater analyzed in the biofilm of the bioreactor before system startup and after 42 days of operation. The system was a coupled photocatalysis and coimmobilized *C. vulgaris*–*P. putida* biological system.

4. Conclusions

This is the first study to use a coupled visible-light PBS for the treatment of real aquaculture wastewater containing a PAE mixture. The findings reveal that the DEHP removal efficiency was the most influenced by the coexistence of multiple PAEs (DEHP, DBP, DMP) in the wastewater. The coimmobilization of the microalga *C. vulgaris* with the bacterium *P. putida* improved the PAE removal efficiencies relative to those achieved with only immobilization of *P. putida*. Analysis of the bacterial communities in the aquaculture wastewater in the bioreactor before and after PBS treatment indicated that most bacterial genera were removed through the photocatalysis process, and the inoculated bacteria remained dominant. These results indicate that application of the PBS for continuous treatment of PAE-containing real wastewater is feasible. However, additional research is required to identify the optimal parameters for the coupled visible-light PBS and to determine its cost-effectiveness to enable direct utilization of sunlight for PAE photocatalysis.

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