



Article Thermodynamic and Experimental Study on Migration Characteristics of Heavy Metals during the Melting Process of Incineration Fly Ash

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Abstract: The migration characteristics of heavy metals during the melting process were one of the key factors for safe treatment and resource utilization of incineration fly ash (IFA). In this paper, the material variation of heavy metal elements of Pb, Zn, Cu, and Fe during the IFA melting process was simulated by HSC 6.0 chemistry software. The effects of melting temperature, alkalinity, atmosphere, chlorine content of raw materials, and an iron bath added to the migration characteristics, and phase transformation of selected heavy metal elements was investigated. The simulation results were also verified by experimental results. The results showed that, with the increase in temperature, the gas phase proportion of Pb, Zn, Cu, and Fe gradually increased. The alkalinity had little effect on the proportion of elements Fe and Cu in the liquid slag (LS) phase and the element Pb in the gas phase, but the increase in alkalinity could inhibit the proportion of element Zn in the gas phase. Zn mainly existed in the gas phase, and the atmosphere had little influence on the distribution of Zn. In reducing atmosphere (RA), elements Fe and Cu, which entered the liquid metal (LM) phase, were promoted, while the volatilization of Pb was restrained, which was conducive to the recovery of heavy metals. The melting process of IFA with water-washing and dechlorination had an inhibitory effect on the volatilization of Zn and Pb, but had little effect on Fe and Cu. The proportion of element Zn in the gas phase reduced from 85.84% to 9.89%. With the iron bath added in the IFA melting process, 98.42% of Cu and 82.28% of Pb entered the LM phase as metal simple substances, and 76.3% of Zn entered the gas phase as Zn(g) and $ZnCl_2(g)$. In the experimental verification, the distribution proportions of the four heavy metals in the gas phase, LS phase, and LM phase were consistent with the simulation results.

Keywords: incineration fly ash; melting process; thermodynamic modeling; heavy metal; migration distribution

1. Introduction

The method of semidry or dry deacidification-activated carbon adsorption-bag filter dust removal is widely adopted in the present flue gas treatment process. The heavy metal dioxin, as well as some toxic substances in flue gas, are adsorbed by activated carbon [1–4]. Furthermore, the particles generated in the process of deacidification and adsorption are captured by a bag filter. Therefore, the incineration fly ash (IFA) is formed. The IFA, containing massive harmful heavy metals and dioxins, is clearly classified as hazardous waste [5–9]. The high-temperature melting process by the electric arc furnace of IFA is helpful for eliminating dioxins and solidifying heavy metal elements. This has several advantages, including volume reduction, weight decline, and completely safe treatment. Furthermore, the molten products can be used to gain high-value-added products for resource utilization, such as cement additives, thermal insulation cotton, glass ceramics,



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Copyright: © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). and so on. Therefore, the high-temperature melting process is considered as one of the most effective means for treating IFA [10–16].

The IFA contains the major Inorganic components of CaO, SiO₂, Al₂O₃, and MgO, plentiful chloride salts of NaCl, CaCl₂, and KCl, as well as small amounts of organic components of C, H, N, S, and Cl. In addition, there are also metal components such as Fe, Cu, Pb, Zn, Cr, and Cd. The complex reaction system is constituted by the various components mentioned above and melting additives in the coupled treatment process of IFA. To effectively solidify and utilize heavy metal elements, it is necessary to study the thermodynamic behavior of heavy metal elements in the above reaction system of IFA. Many researchers have conducted studies on the distribution of metal elements in the melting process of IFA [17,18]. M.Takaoka [19] and X.T Wang [20] studied the effect of atmosphere on the behavior of heavy metals in the melting process of IFA and found that the volatilization rate of low-boiling heavy metals in a reduction atmosphere was higher than that in an oxidation condition. Under the reducing atmosphere, the compounds of heavy metals were reduced to metal elements, which had a higher vapor pressure than oxides. A Jakob [21] investigated the influence on chemical reactions of various heavy metals under temperatures ranging from 670 °C to 1300 °C. B. Nowak [22] researched the existence of the formation law of heavy metal chlorides at high temperature in an IFA. X.L Lu [23] and J.Y Liu [24] explored the volatilization and chlorination transformation characteristics of heavy metals in the high-temperature melting process of IFA. Chloride helped to convert heavy metals in fly ash into heavy metal chloride with a low boiling point and promoted the volatilization of heavy metals. H.K Li [25] and J. Wen [26] conducted a study on the migration and distribution laws of heavy metals in IFA using the iron bath method. The iron bath melting system created a reduction environment for fly ash melting and promoted the reduction of heavy metal compounds to metal elements. The metals with a high boiling point were enriched in the iron phase, while the metals with a low boiling point were volatilized. The above research mainly focused on the solidification and volatilization distribution laws of toxic heavy metals in the melting process, and there is still a lack of systematic expositions on the quantification and mechanism analysis of the influence degree of various factors.

In this study, the household IFA was selected as the research object. The effects of melting temperature, alkalinity, atmosphere, chloride content of raw materials, and an iron bath added to the thermodynamic behavior of four heavy metal elements (Fe, Pb, Zn, and Cu) with high content (except alkali metal compounds) in the IFA during the melting process were systematically investigated by HSC 6.0 chemistry software (developed by Outokumpu Research Center, Finland). The reference and guidance of the solidification and resource utilization of metal elements in the melting process of IFA were provided.

2. Raw Material Properties and Research Methods

2.1. *Raw Material Properties*

In this study, the two types of raw materials were selected, which were produced by the grate incineration line of a waste incineration power plant in the Jiangsu Province. The raw IFA (R—IFA) samples were taken from the bag dust collector of the incineration line. Considering the composition fluctuation of the R—IFA, 10 samples were taken every 3 days in 1 month. Then, the samples were mixed evenly. To research the influence of chloride content of raw materials, the water-washing IFA (WW—IFA) samples were chosen. Half of the R—IFA samples were washed by three levels of counter-current water. The mass ratio of the R—IFA and water was 1:3 in each level of the water-washing process. After that, the mixture was filtered and separated by a vacuum filter extractor. The products were then dried in a drying oven. The moisture content of the final products was controlled by 5%. The final products were also called WW—IFA samples. The main chemical constituents of XRF and XRD patterns of R—IFA and WW—IFA are shown in Table 1 and Figure 1, respectively. From Table 1, the main components of R—IFA and WW—IFA were CaO, SiO₂, Al₂O₃, Na₂O, K₂O, SO₃, and Cl. Additionally, a small amount of heavy metals, such as

ZnO, PbO, CuO, and Fe_2O_3 also existed. From Figure 1, the major phases of the R—IFA were NaCl, KCl, CaClOH, CaCO₃, CaSO₄, and Ca(OH)₂, while the major phases of the WW—IFA were CaCO₃, CaSO₄, and Ca(OH)₂. Compared with the R—IFA, more than 95% of the chlorine salt in the WW—IFA, such as NaCl, KCl, and CaClOH, was effectively removed. So the chloride content of the WW—IFA was quite lower than that in the R—IFA.

Table 1. Chemical constituents of R—IFA and WW—IFA. (Mass percent, %).

Chemical Constituents	CaO	SiO ₂	Al_2O_3	MgO	Na ₂ O	K ₂ O	Fe ₂ O ₃	SO ₃
R—IFA	44.25	3.74	1.48	1.17	7.36	5.81	1.25	6.48
WW—IFA	64.87	5.48	2.17	1.72	0.54	0.43	1.83	9.50
	Cl	С	H ₂ O	ZnO	PbO	CuO	Others	
R—IFA	20.81	2.51	2.71	0.551	0.155	0.049	1.67	
WW—IFA	1.22	3.68	5.0	0.808	0.228	0.072	2.45	



Figure 1. XRD patterns of R—IFA (left) and WW—IFA (right).

2.2. Research Method

The thermodynamic calculation software HSC 6.0 chemistry includes an abundant and comprehensive thermodynamic database, which can determine 22 calculation modules for different applications [27]. The equilibrium composition module in the HSC 6.0 chemistry thermodynamic software was applied. The equilibrium phase composition of the reaction system was obtained based on the condition of mass balance and the lowest Gibbs free energy of constant pressure and temperature [28]. The heavy metal elements in the R—IFA and WW—IFA were considered in the form of oxides for process analysis. By adjusting the melting temperature, total pressure, chemical composition and proportion of raw materials, and the state of the input reaction system, as well as the stable phase that appeared in the subsequent process, the distribution coefficients of four heavy metal elements in the liquid metal (LM)phase, liquid slag (LS) phase, and gas phase were simulated and calculated.

The R—IFA was characterized by a high content of Ca and low content of Si and Al. The ternary phase diagram of CaO-SiO₂-Al₂O₃ was drawn by the FactSage 8.0 software (developed by Thermfact/CRCT, Montreal, Canada, and GTT-Technologies, Aachen, German), shown in Figure 2. Based on the chemical composition, the R—IFA was located in point 2, where the melting temperature was higher than 1700 °C. The high melting temperature was quite disadvantageous for the actual IFA melting process. To reduce the melting temperature, the proportions of CaO, SiO₂, and Al₂O₃ in the R—IFA were adjusted by charging SiO₂, Al₂O₃, and other flux, which aimed to decrease the melting temperature from point 2 to the lower temperature region of area 2. Under the base condition of a binary alkalinity of 1 (mass ratio of CaO to SiO₂) and Al₂O₃ content of 15%, the mass ratio of the R—IFA and additives was selected as fly ash:SiO₂:Al₂O₃ = 65:26:9. Then, the influence of other variables was further studied. Additionally, the melting atmosphere was also considered based on the actual IFA melting process. The excess air coefficient (EAC) was introduced according to the reference [28]. Some organic components in IFA would combine with oxygen to form gaseous oxides and left the system. The amount of oxygen consumed was fixed according to the steady composition of IFA. The EAC was defined as the ratio of actual oxygen consumption to the above oxygen consumption. While the amount of oxygen was more than the consumed value, the oxidizing atmosphere (OA) formed. The atmosphere included reducing atmosphere (RA), direct melting atmosphere (DMA), and OA, where DMA referred to the atmosphere under the condition that EAC was chosen as 0. This meant that, in the R—IFA melting process, the inner region of the furnace was sealed in good condition, and there was no air infiltration. Likewise, the OA represented that the EAC was 1.2. Furthermore, RA was obtained by adding 5% of C of the total mass of IFA. The calculation schemas are shown in Figure 3.



Figure 2. Ternary phase diagram of CaO-SiO₂-Al₂O₃.



Figure 3. Framework of the research schemes.

2.3. Experimental Procedure and Detection Methods

To verify the theoretical calculation results of the HSC 6.0 software, physical experiments were conducted. The experimental facilities are shown in Figure 4. These included a power supply system, a plasma melting furnace, a gas supply unit, a tail gas purification unit, and a slag cooling device. The plasma melting furnace was heated by a DC plasma arc with 50 KW of power [29,30]. The results of the R—IFA melting experiment under the conditions of different temperatures, atmospheres, and iron baths were collected. The experimental procedure was as follows:

- (1) The melting experiments were carried out by adjusting the melting electrical power of the plasma furnace. The melting temperature was changed and maintained in the range of 1100–1600 °C, while other conditions remained unchanged.
- (2) Under the conditions of a temperature of 1300 °C and alkalinity of 0.8, the melting state in the furnace variated by iron bath added. The atmosphere in the furnace was changed by connecting the external gas supply unit and carbon charged. The sampling analysis was conducted after the melting experiments. The detailed conditions are shown in Table 2.

Table 2. Conditions of melting experiments in R—IFA melting process under different atmosphere and iron bath charged.

Conditions	Temperature	Alkalinity	Atmosphere	Raw Materials	Iron Bath
А	1300 °C	0.8	DMA	R—IFA	No
В	1300 °C	0.8	DMA	R—IFA	Yes
С	1300 °C	0.8	OA	R—IFA	No
D	1300 °C	0.8	RA	R—IFA	No



Figure 4. Diagram of experimental facilities in IFA melting process.

An X-ray fluorescence spectrometer and a direct-reading inductively coupled plasma spectrometer were adopted in the performance detection. The total content and distribution of Fe, Pb, Zn, and Cu in the glass slag and alloy were estimated, and the test results were compared with the calculation results.

3. Results Analysis

3.1. Effect of Melting Temperature on Selected Heavy Metal Elements Distribution in R—IFA Melting Process

Figures 5 and 6, and Tables A1–A4 show the calculation results of the distribution forms of Fe, Pb, Zn, and Cu in the temperature range of 1100–1600 °C. It could be concluded in Figures 5a and 6a that Fe mainly existed in the slag phase in the form of oxide and silicate, while a small amount of Fe volatilized into the gas phase in the form of FeCl₂ (g). With the temperature increased from 1100 to 1600 °C, the proportion of FeCl₂ (g) increased from 0.29% to 5.43%.

The variation of the process products of Pb with temperature is shown in Figures 5b and 6b. Within the melting temperature range of $1100-1600 \,^{\circ}$ C, Pb volatilized into a gas phase, mainly in the form of gaseous products, such as PbS (g), PbCl₂ (g), PbCl (g), and PbCl₄ (g). As the temperature increased, the proportion of Pb into the gas phase increased from 73.65% to 99.6%, and the proportion of PbS (g) decreased, while the proportion of PbCl₂ (g) and PbCl₂ (g) increased.





Figure 5. Cont.



Figure 5. Effect of melting temperature on distribution forms of selected heavy metal elements in R—IFA melting process. (**a**) element Fe; (**b**) element Pb; (**c**) element Zn; (**d**) element Cu.



Figure 6. Effect of melting temperature on proportion of selected heavy metal elements in gas, LS, and LM phase in R—IFA melting process. (**a**) element Fe; (**b**) element Pb; (**c**) element Zn; (**d**) element Cu.

The variation of the process products of Zn with temperature is shown in Figures 5c and 6c. The proportion of ZnS and ZnO in solid products gradually decreased, and the proportion of $ZnCl_2$ (g) in gaseous products significantly increased. Furthermore, the proportion of gaseous products increased from 12.57% to 98%.

The variation of process products of Cu with temperature is shown in Figures 5d and 6d. When the melting temperature was below 1300 °C, Cu mainly existed in nonvolatile sulfide, aluminate, and CuCl. When the temperature was above 1300 °C, the proportion of gaseous product of CuCl (g) increased significantly, reaching 58.96% at 1600 °C.

In conclusion, a large amount of chloride salts, such as NaCl, KCl, and CaCl₂, accounted for about 30% of the total amount of IFA, which promoted the conversion of heavy metals into metal chlorides with a low boiling point, especially for Pb, Zn, and Cu, in IFA melting. The phenomenon was consistent with the experimental research results of reference [23]. When the temperature was above 1300 °C, Pb and Zn mainly volatilized into a gas phase, while Fe and Cu solidified mainly in a slag phase in a nonvolatile state. From the perspective of enrichment of metals and energy consumption reduction of the IFA melting process, 1300 °C was selected as the suitable melting temperature.

3.2. Effect of Alkalinity on Selected Heavy Metal Elements Distribution in R—IFA Melting Process

Under the melting temperature of 1300 °C, the influence of alkalinity on the heavy metal morphology distribution in the IFA melting process was investigated. The results are shown in Figures 7 and 8, and Tables A5–A8.

It could be seen from Figures 7a and 8a that Fe mainly existed in the form of silicate and oxide. A small amount of Fe volatilized into the gas phase in the form of FeCl₂ (g), and the increase in alkalinity significantly inhibited the process of Fe volatilization. When the alkalinity increased from 0.4 to 1.4, the component of FeCl₂ (g) decreased from 6.4% to 1%, the proportion of iron containing silicate decreased significantly, and the proportion of iron oxide increased gradually. The phenomenon was mainly related to the decrease in silicon content in complex compounds formed by combining with iron in the melting process.

The Pb mainly formed the gaseous products of PbCl (g), PbCl₂ (g), PbCl₄ (g), and PbS (g), shown in Figures 7b and 8b. With the increase in alkalinity, the proportion of chloride in Pb decreased, while the proportion of sulfide increased. The proportion of the gas-phase product of Pb was more than 96%, reaching up to 99.26%. Therefore, there was little effect of alkalinity on the volatilization rate of Pb.



Figure 7. Cont.



Figure 7. Effect of alkalinity on distribution forms of selected heavy metal elements in R—IFA melting process. (a) element Fe; (b) element Pb; (c) element Zn; (d) element Cu.



Figure 8. Effect of alkalinity on proportion of selected heavy metal elements in gas, LS, and LM phase in R—IFA melting process. (**a**) element Fe; (**b**) element Pb; (**c**) element Zn; (**d**) element Cu.

As shown in Figures 7c and 8c, with the increase in alkalinity, the proportion of the gaseous product of $ZnCl_2$ (g) decreased, especially when the basicity was greater than 0.8. The proportion of non-volatile ZnO and ZnO·Al₂O₃ increased significantly. It could be concluded that the increase in alkalinity inhibited the volatilization of Zn.

Cu was mainly distributed in the slag phase as nonvolatile CuCl and CuO·Al₂O₃, and the gaseous product CuCl (g) accounted for about 5%. The content of CuCl in the slag phase decreased from more than 90% to 41.73%, and the proportion of the CuO·Al₂O₃ phase increased to about 54%. The increase in alkalinity had little effect on the volatilization of Cu.

In conclusion, when the alkalinity changed in the range of 0.4–1.4, Pb mainly existed in a gaseous phase, and Fe and Cu mainly solidified in a slag phase as a nonvolatile phase. The proportion of Zn volatilized into the gas phase decreased significantly when the alkalinity was higher than 0.8. This could explain why the lower alkalinity led to the high slag viscosity. To ensure the smooth smelting process of IFA and enrichment of metals, the alkalinity of 0.8 was recommended, and increased the melting temperature [31].

3.3. Effect of Atmosphere on Selected Heavy Metal Elements Distribution in R—IFA Melting Process

The effect of redox atmosphere on the heavy metal distribution in the IFA melting process was investigated under the conditions of a melting temperature of 1300 °C and alkalinity of 0.8. The research results are shown in Figures 9 and 10, and Tables A9–A12. In the reducing conditions, the products of Fe, Pb, Zn, and Cu mainly existed in the form of metal elements, and the mass proportions of the four elements were 62.51%, 71.28%, 91.76%, and 98.39%, respectively. Due to the low boiling point, about 90% of Zn entered the gas phase. About 50% of Pb entered the gas phase as Pb (g), PbCl (g), and PbS (g), while the rest existed in the form of a metal element. Fe and Cu existed in the forms of metal elementals or metal sulfide. Due to the high boiling point, the proportion of them entering the gas phase was small, and most of them formed alloys.

Under the oxidizing atmosphere, the products of Fe mainly existed in the slag phase in the forms of oxide and composite silicate. About 20% of the products of Cu volatilized into the gas phase in the forms of CuCl₂ (g) and CuCl (g), and the remaining existed in the slag phase in the forms of CuO and CuO·Al₂O₃. Almost all Pb and Zn entered the gas phase in the forms of chloride with a low boiling point.

In summary, Zn would enter the gas phase as a volatile product with a low boiling point under oxidation or reduction atmosphere. The volatilization of Pb was inhibited in the reducing atmosphere, which was in line with the research results of the literature [32]. Fe and Cu existed in the slag phase in the forms of oxide, silicate, and aluminate in the oxidizing atmosphere, while in the reducing conditions, they were reduced to metal elements to form an alloy phase.

3.4. Effect of Chlorine Content in Raw Materials on Selected Heavy Metal Elements Distribution in IFA Melting Process

The effect of chlorine on the heavy metal distribution in raw IFA and water-washing IFA melting processes was investigated under the conditions of a melting temperature of 1300 °C and alkalinity of 0.8. The water-washing process was helpful for removing soluble chlorine salt. The research results are shown in Figures 11 and 12, and Tables A13–A16. In the raw IFA melting process, the products of Pb, Zn, and Cu mainly existed in the form of chloride, while only 4% of the products of Fe existed in the form of chloride, and the rest were oxides and silicates. The proportion of Pb, Zn, Cu, and Fe entering the gas phase was 97.15%, 85.84%, 4.68%, and 4.00%, respectively. In the water-washing IFA melting processes, the products of each metal element were mainly metal sulfide, and the proportion of Pb, Zn, Cu, and Fe entering the gas phase was 75.42%, 9.89%, 0.66%, and 0.61%, respectively. It could be concluded that the pretreatment of IFA with water washing had a significant inhibition effect on the volatilization of Zn and Pb, but the effect was limited, while the effect on Fe and Cu was not significant.



Figure 9. Effect of atmosphere on distribution forms of selected heavy metal elements in R—IFA melting process. (**a**) element Fe; (**b**) element Pb; (**c**) element Zn; (**d**) element Cu.





Figure 10. Cont.







Figure 11. Effect of chlorine content in raw materials on distribution forms of selected heavy metal elements in IFA melting process. (**a**) element Fe; (**b**) element Pb; (**c**) element Zn; (**d**) element Cu.





3.5. Effect of Iron Bath Charged on Selected Heavy Metal Elements Distribution in R—IFA Melting Process

In the actual plasma melting process of IFA, the iron bath was usually arranged at the bottom of the furnace to promote the heat transfer and the chemical reaction [33,34]. The effect of the iron bath on the heavy metal distribution in raw IFA and water-washing IFA melting processes was investigated under the conditions of a melting temperature of 1300 °C and alkalinity of 0.8. The research results are shown in Figures 13 and 14, and Tables A17–A19.



Figure 13. Effect of iron bath charged on distribution forms of selected heavy metal elements in R—IFA melting process. (**a**) element Pb; (**b**) element Zn; (**c**) element Cu.







In the IFA melting process without pig iron added, the main products of Pb were PbCl (g), PbCl₂ (g), PbCl₄ (g), and PbS (g), and the gas products accounted for 97.15%. The main products of Zn were ZnCl₂ (g) and ZnO, and the gas products accounted for 76.35%. The main products of Cu were CuCl (g) and CuO·Al₂O₃, and the gas products accounted for 4.68%, while the rest entered the slag phase. When the pig iron was added in the IFA melting process, 98.42% of Cu, 82.28% of Pb, and 5% of Zn entered the iron phase as metallic elements. A total of 76.3% of Zn entered the gas phase as Zn (g) and ZnCl₂ (g). In the IFA melting process, the heavy metal compounds were reduced to elemental compounds by the reducing agent of carbon in pig iron. The Zn with a low boiling point volatilized in the forms of elemental and chloride. The heavy metals of Cu and Pb with a high boiling point were captured by the iron bath, which could realize the classification and enrichment of heavy metals.

4. Comparison of Experimental and Theoretical Results in R—IFA Melting Process *4.1. Comparison of Experimental and Theoretical Results on Melting Temperature in R—IFA Melting Process*

The elements in the slag phase and alloy phase obtained at different melting temperatures were detected. The proportion of Fe, Pb, Cu, and Zn was compared with the above simulation results, as shown in Figure 15 and Table A20.

In the experimental results, the proportion of Fe, Pb, Zn, and Cu elements in the slag phase decreased gradually with the increase in temperature. The trend of proportions of the four heavy metals in the slag phase in experimental results was close to the calculated results, but the values of experimental results were slightly lower than the calculated results. Despite the uncontrollable factors in the experiment, the simulated data was calculated under the reaction equilibrium state in the HSC 6.0 software (developed by Outokumpu Research Center, Finland), which was different from the situation of the actual smelting process. Lowering the concentration of the product allowed the reaction to proceed in the direction of the product.



Figure 15. Comparison between experimental and theoretical results of proportion of selected heavy metal elements in LS phase under different melting temperature in R—IFA melting process. (a) element Fe; (b) element Pb; (c) element Zn; (d) element Cu.

4.2. Comparison of Experimental and Theoretical Results on Atmosphere and Iron Bath Charged in *R*—IFA Melting Process

The experimental results of the distribution of Fe, Pb, Zn, and Cu elements in each phase under four conditions in Table 2 were compared with the simulation results, shown in Figure 16 and Tables A21–A24.

In Figure 16, the trend of the distribution of four heavy metals in three phases in experimental results was basically consistent with the simulated values. Under the conditions of A and C in Table 2, the products of IFA melting were the gas phase and the slag phase, without an alloy phase. Most of Pb and Zn entered the gas phase, while most of Fe and Cu entered the slag phase. Under the conditions of B and D, the products of IFA melting were the gas phase, slag phase, and alloy phase, with the heavy metals mainly distributed in the gas phase, slag phase, and alloy phase. Cu and Pb were mostly enriched in the alloy phase, while most of Zn entered the gas phase. Under the reductive atmosphere, most of Cu and Zn entered the alloy phase. The proportion of Fe in the slag phase and alloy phase was about half, and the proportion of Pb in the alloy phase and gas phase was about 50%, respectively. The experimental results were slightly different from the simulation results, but the trend was consistent with Section 4.1. This was mainly because the kinetic factors such as melting time and temperature rise rate were not considered in the thermodynamic equilibrium calculation and analysis in the HSC 6.0 software.



Figure 16. Comparison between experimental and theoretical results. (**a**) condition A; (**b**) condition B; (**c**) condition C; (**d**) condition D.

5. Conclusions

In this research, the physicochemical properties of household IFA in the Jiangsu Provence were studied by thermodynamic analysis in the HSC 6.0 software. The effects of melting temperature, alkalinity, atmosphere, chlorine content of raw materials, and an iron bath added to the migration characteristics of four heavy metal elements in three phases in the IFA melting process were systematically investigated. The main conclusions are as follows:

- (1) Within the temperature range of 1100–1600 °C, Fe mainly entered the slag phase as oxides and silicates, Pb mainly entered the gas phase as gaseous products of PbS (g), PbCl₂ (g), PbCl (g), and PbCl₄ (g). When the temperature was higher than 1300 °C, most of Zn entered the gas phase in the form of ZnCl₂ (g). CuCl (g) appeared in the Cu products, and the proportion of CuCl (g) increased significantly with the increase in temperature.
- (2) With the increase in alkalinity from 0.4 to 1.4, the proportion of oxide in Fe products increased, and the proportion of silicate decreased, but the proportion of the slag phase was almost unchanged. As for Pb products, the proportion of PbCl₂ (g) and PbCl₄ (g) decreased, the proportion of PbS (g) increased, and the proportion of the gas phase increased slightly. The proportion of Zn volatilization into the gas phase

could be inhibited with the increase in alkalinity, while the proportion of Cu into the slag phase remained unchanged.

- (3) In the oxidation or reduction atmosphere, Zn would enter the gas phase with low boiling point volatile products. The reducing atmosphere had an inhibitory effect on the volatilization of Pb. In the oxidation atmosphere, Fe and Cu existed in the forms of oxide, silicate, and aluminate in the slag phase, while in reduction conditions, Fe and Cu were reduced to metal elementals in the alloy phase.
- (4) Compared with the raw IFA, the volatilization of Zn in the water-washing IFA was inhibited effectively. The proportion of Zn entering the gas phase decreased from 85.84% to 9.89%. The volatilization of Pb was inhibited slightly, and there was little effect on the volatilization of Fe and Cu.
- (5) In the IFA melting process with an iron bath, 98.42% of Cu and 82.28% of Pb entered the iron phase in the form of metallic elements, respectively. A total of 76.3% of Zn entered the gas phase as gaseous products of Zn (g) and ZnCl₂ (g), and only 5% of Zn entered the iron phase. The classification and enrichment of heavy metals was realized by carbon in pig iron of the reducing agent and Fe of heavy metals collector.
- (6) Under the same technological conditions, the calculated results of Fe, Pb, Zn, and Cu were consistent with the experimental results in the proportion of the gas phase, slag phase, and alloy phase.
- (7) From the perspective of metal recovery, the reduction condition or addition of an iron bath were recommended for the IFA melting process. Fe, Cu, Pb, and Zn in IFA could be enriched in the gas phase and alloy phase to achieve the classification and enrichment of metal resources.

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Conflicts of Interest: The authors declare no conflict of interest.

Appendix A

Table A1. Calculation results of distribution forms and proportion of three phases of element Fe in R—IFA melting process under different melting temperature (Molar percentage, %).

	Gas Phase			LS	LS Phase			
Temperature	FeCl ₂	Fe ₂ O ₃	FeO	Other Iron Oxides	Iron-Bearing Silicate	Iron-Bearing Sulfide		
1100 °C	0.3	1.8	10.55	42.91	21.5	22.93		
1200 °C	1.05	6.73	11.99	47.47	23.47	9.29		
1300 °C	2.56	21.5	10.54	41.7	23.7	0		
1400 °C	4.16	45.4	6.03	24.45	19.95	0		
1500 °C	5.49	66.54	2.72	11.12	14.13	0		
1600 °C	4.78	81.72	0.98	4.11	8.41	0		

							LODI	
	Gas Phase						LS Phase	
Temperature	PbS	PbCl ₂	PbC1	PbCl ₄	Pb	PbS	PbCl ₂	РЬО
1100 °C	48.38	16.11	7.27	1.8	0.09	20.02	5.93	0.4
1200 °C	64.64	16.34	10.91	0.82	0.21	4.04	2.78	0.26
1300 °C	58.19	20.94	17.88	0.63	0.45	0	1.69	0.22
1400 °C	24.17	38.88	33.27	1.16	0.87	0	1.41	0.24
1500 °C	6.3	50.45	39.63	1.78	0.99	0	0.7	0.15
1600 °C	1.71	54.5	40.23	2.19	0.97	0	0.3	0.1

Table A2. Calculation results of distribution forms and proportion of three phases of element Pb in R—IFA melting process under different melting temperature (Molar percentage, %).

Table A3. Calculation results of distribution forms and proportion of three phases of element Zn in R—IFA melting process under different melting temperature (Molar percentage, %).

	Gas Pl	nase		LS Phase				
Temperature	ZnCl ₂	Zn	ZnS	ZnO	$ZnO \cdot Al_2O_3$	ZnSiO ₃		
1100 °C	12.47	0.1	66.55	19.01	1.3	0.57		
1200 °C	40.27	0.85	30.03	25.89	2.09	0.87		
1300 °C	73.48	2.99	0	20.81	1.93	0.79		
1400°C	84.76	4.02	0	9.8	0.99	0.43		
1500 °C	91.43	4.15	0	3.82	0.41	0.19		
1600 °C	93.8	4.21	0	1.7	0.2	0.09		

Table A4. Calculation results of distribution forms and proportion of three phases of element Cu in R—IFA melting process under different melting temperature (Molar percentage, %).

	Gas	Phase			LS Phase			
Temperature	CuCl	CuCl ₂	CuCl	CuFeS ₂	CuS	Cu ₂ S	$CuO \cdot Al_2O_3$	
1100 °C	0.14	0	31.27	34.33	16.23	13.9	4.13	
1200 °C	0.86	0.01	55.5	16.54	8.41	11.97	6.71	
1300 °C	4.19	0.08	85.06	0	0	0	10.67	
1400 °C	12.12	0.29	75.87	0	0	0	11.72	
1500 °C	32.4	1.11	55	0	0	0	11.49	
1600 °C	58.96	2.72	28.88	0	0	0	9.44	

Table A5. Calculation results of distribution forms and proportion of three phases of element Fe in R—IFA melting process under different alkalinity (Molar percentage, %).

	C Dh			I C Dhasa	
	Gas Phase			LS Phase	
Alkalinity	FeCl ₂	Fe ₂ O ₃	FeO	Other Iron Oxides	Iron-Bearing Silicate
0.4	6.53	2.59	4.99	21.19	64.69
0.6	5.39	6.18	6.36	26.51	55.58
0.8	4.05	12.18	8.15	33.49	42.12
1	2.51	21.07	10.33	41.92	24.17
1.2	1.34	28.17	11.82	47.64	11.04
1.4	0.9	31.13	12.24	49.33	6.4

		Gas	LS Phase				
Alkalinity	PbCl ₂	PbS	PbCl ₄	PbC1	PbS	PbCl ₂	PbSiO ₃
0.4	50.76	13.94	19.29	12.21	0	3.49	0.31
0.6	47.18	24.01	8.26	16.72	0	3.56	0.27
0.8	36.11	38.91	2.83	19.13	0	2.84	0.17
1	21.07	58.53	0.64	17.99	0	1.7	0.07
1.2	10.54	73.37	0.13	14.24	0	0.86	0.86
1.4	7.33	79.23	0.05	12.64	0.13	0.61	0.01

Table A6. Calculation results of distribution forms and proportion of three phases of element Pb in R—IFA melting process under different alkalinity (Molar percentage, %).

Table A7. Calculation results of distribution forms and proportion of three phases of element Zn in R—IFA melting process under different alkalinity (Molar percentage, %).

	Gas I	Phase					
Alkalinity	ZnCl ₂	Zn	ZnS	ZnO	ZnSiO ₃	ZnCl ₂	$ZnO \cdot Al_2O_3$
0.4	92.18	0.3	0	4.83	1.86	0.81	0.02
0.6	89.49	0.63	0	7.26	1.69	0.87	0.06
0.8	84.51	1.33	0	11.68	1.34	0.85	0.29
1	72.93	2.97	0	20.65	0.79	0.75	1.91
1.2	50.78	7.48	0	30.79	0.22	0.35	10.38
1.4	36.76	6.12	1.34	34.26	0.16	0.39	20.97

Table A8. Calculation results of distribution forms and proportion of three phases of element Cu in R—IFA melting process under different alkalinity (Molar percentage, %).

	Gas	Phase					
Alkalinity	CuCl	CuCl ₂	CuCl	CuFeS ₂	CuS	Cu ₂ S	CuO·Al ₂ O ₃
0.4	5.42	0.35	93.92	0	0	0	0.31
0.6	4.95	0.22	94.02	0	0	0	0.81
0.8	4.68	0.14	92.7	0	0	0	2.48
1	4.19	0.08	85.06	0	0	0	10.67
1.2	2.93	0.03	60.36	0	0	0	36.68
1.4	2	0.02	41.73	0.29	0.34	0.73	54.89

Table A9. Calculation results of distribution forms and proportion of three phases of element Fe in R—IFA melting process under different atmosphere (Molar percentage, %).

	Gas Phase			LS Phase	LM Phase		
Atmosphere	FeCl ₂	Fe ₂ O ₃	FeO	Other Iron Oxides	Iron-Bearing Silicate	Iron-Bearing Sulfide	Fe
RA	0	0	0	0	10.54	26.96	62.5
DMA	4.09	12.29	8.22	32.93	42.47	0	0
OA	0	84.7	0	5.03	10.27	0	0

			Gas Phase			LM Phase
Atmosphere	Pb	PbCl	PbS	PbCl ₂	PbCl ₄	Pb
RA	20.65	19.83	8.89	0	0	50.63
DMA	0	19.72	40.12	37.24	2.92	0
OA	0	0	0	0.19	99.81	0

Table A10. Calculation results of distribution forms and proportion of three phases of element Pb in R—IFA melting process under different atmosphere (Molar percentage, %).

Table A11. Calculation results of distribution forms and proportion of three phases of element Zn in R—IFA melting process under different atmosphere (Molar percentage, %).

	Gas Phase			LS Phase			
Atmosphere	Zn	ZnCl ₂	ZnS	ZnO	ZnSiO ₃		
RA	91.76	1.33	6.91	0	0		
DMA	1.34	85.49	0	11.82	1.35		
OA	0	96.67	0	3.02	0.31		

Table A12. Calculation results of distribution forms and proportion of three phases of element Cu in R—IFA melting process under different atmosphere (Molar percentage, %).

Gas Phase				LS Phase		LM Phase
Atmosphere	CuCl	CuCl ₂	CuCl	$CuO \cdot Al_2O_3$	CuO	Cu
RA	0	0	1.61	0	0	98.39
DMA	4.68	0	92.83	2.49	0	0
OA	6.46	15.64	7.23	66.72	3.95	0

Table A13. Calculation results of distribution forms and proportion of three phases of element Fe in R—IFA melting process under different raw materials (Molar percentage, %).

Gas Phase				LS		
Raw Materials	laterials FeCl ₂ Fe ₂ O ₃ Fe		FeO	Other Iron Oxides	Iron-Bearing Sulfide	
R—IFA	4.09	12.28	8.22	32.94	42.47	0
WW—IFA	0.61	0.06	2.03	7.5	17.77	72.03

Table A14. Calculation results of distribution forms and proportion of three phases of element Pb in R—IFA melting process under different raw materials (Molar percentage, %).

	LS P	hase					
Raw Materials	PbCl ₂	PbS	PbCl ₄	PbCl	Pb	PbCl ₂	PbS
R—IFA	36.18	38.97	2.84	19.16	0	2.85	0
WW—IFA	4.64	60.09	0.02	10.03	0.64	0.01	24.57

Table A15. Calculation results of distribution forms and proportion of three phases of element Zn in R—IFA melting process under different raw materials (Molar percentage, %).

Raw Materials	ZnCl ₂	Zn	ZnS	ZnO	ZnSiO ₃	ZnCl ₂	$ZnO \cdot Al_2O_3$
R—IFA	84.52	1.33	0	11.67	1.34	0.85	0.29
WW—IFA	7.85	2.05	88.15	1.78	0.17	0	0

Gas Phase						
Raw Materials	CuCl	$CuO \cdot Al_2O_3$	CuS	CuFeS ₂	Cu ₂ S	CuCl
R—IFA	4.68	2.49	0	0	0	92.83
WW—IFA	0.66	0.17	27.88	43.94	27.13	0.22

Table A16. Calculation results of distribution forms and proportion of three phases of element Cu in R—IFA melting process under different raw materials (Molar percentage, %).

Table A17. Calculation results of distribution forms and proportion of three phases of element Pb in R—IFA melting process under different melting mode (Molar percentage, %).

Gas Phase						LS Phase	LM Phase
Melting Mode	PbCl ₂	PbS	PbCl ₄	PbCl	Pb	PbCl ₂	Pb
DM	36.17	38.98	2.84	19.16	0	2.85	0
IBM	1.83	1.92	0	11.65	2.2	0.12	82.28

Table A18. Calculation results of distribution forms and proportion of three phases of element Zn in R—IFA melting process under different melting mode (Molar percentage, %).

	LS Phase				LM Phase			
Melting Mode	ZnCl ₂	Zn	ZnS	ZnO	ZnSiO ₃	ZnCl ₂	$ZnO \cdot Al_2O_3$	Zn
DM	84.52	1.33	0	11.67	1.34	0.85	0.29	0
IBM	23.29	53.06	13.98	3.8	0.33	0.19	0.11	5.24

Table A19. Calculation results of distribution forms and proportion of three phases of element Cu in R—IFA melting process under different melting mode (Molar percentage, %).

	Gas Phase		LS Phase			
Melting Mode	CuCl	$CuO{\cdot}Al_2O_3$	CuFeS ₂	CuCl	Cu	
DM	4.68	2.49	0	92.83	0	
IBM	0.06	0	0.48	1.05	98.41	

Table A20. Theoretical and experimental results of distribution forms and proportion of three phases of selected four heavy metal elements in R—IFA melting process under different melting temperatures (Molar percentage, %).

	Fe		Р	Pb		Zn		Cu	
Temperature	TR	ER	TR	ER	TR	ER	TR	ER	
1100 °C	99.71	85.01	26.35	20.8	87.43	80.71	99.86	89.52	
1200 °C	99	86.7	7.08	4.88	58.88	53.28	99.13	85.26	
1300 °C	97.54	80.64	1.91	1.55	23.53	20.13	95.73	75.2	
1400 °C	95.94	76.98	1.65	1.31	11.22	8.92	87.59	70.84	
1500 °C	94.57	72.27	0.86	0.73	4.42	3.35	66.48	50.95	
1600 °C	95.24	68.94	0.4	0.32	1.99	1.61	38.32	21.48	

	Gas	Gas Phase		hase	LM Phase	
	TR	ER	TR	ER	TR	ER
Pb	97.15	98.61	2.85	1.39	0	0
Zn	85.84	93.41	14.16	6.59	0	0
Cu	4.68	16.85	95.32	83.15	0	0

Table A21. Theoretical and experimental results of proportion of three phases of selected elements Pb, Zn, and Cu in R—IFA melting process without iron bath added (Molar percentage, %).

Table A22. Theoretical and experimental results of proportion of three phases of selected elements Pb, Zn, and Cu in R—IFA melting process with iron bath added (Molar percentage, %).

	Gas Phase		LS P	hase	LM Phase	
	TR	ER	TR	ER	TR	ER
Pb	17.6	17.48	0.12	5.1	82.28	77.42
Zn	76.35	77.12	18.41	12.53	5.24	10.35
Cu	0.06	4.15	1.52	6.31	98.42	89.54

Table A23. Theoretical and experimental results of proportion of three phases of selected four heavy metal elements in R—IFA melting process under OA (Molar percentage, %).

	Gas Phase		LS Phase		LM Phase	
	TR	ER	TR	ER	TR	ER
Fe	0	5.27	100	94.73	0	0
Pb	100	98.17	0	1.83	0	0
Zn	96.67	93.35	3.33	6.65	0	0
Cu	22.1	25.15	77.9	74.85	0	0

Table A24. Theoretical and experimental results of proportion of three phases of selected four heavy metal elements in R—IFA melting process under RA (Molar percentage, %).

	Gas Phase		LS Phase		LM Phase	
	TR	ER	TR	ER	TR	ER
Fe	0	3.26	37.49	43.15	62.51	53.59
Pb	49.37	60.32	0	4.48	50.63	35.2
Zn	93.09	85.99	6.91	5.69	0	8.32
Cu	0	7.39	1.61	3.07	98.39	89.54

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