

Table S1: Physical, Chemical, and Biological Parameters. Default simulation parameters are used in all simulations unless otherwise stated.

Parameter	Symbol	Value	Units	Description	Ref.
Simulation Physical Properties					
Simulation Dimensions		300 x 100 x 300	μm	Radial and azimuthal periodic boundary conditions. Zero-gradient boundary conditions elsewhere	
Parcel Dimensions		5 x 20 x 5	μm	Fluid parcel size	
Simulation Volume	V	$9 (10)^6$	μm^3		
Simulation Radius from HARV	r	$(10)^5$	μm	Maximum distance of simulation box to radius of rotation	
Fluid Density	ρ_f	1.00	$\frac{\text{pg}}{\mu\text{m}^3}$	Density of media	[54]
Fluid Kinematic Viscosity	ν	0.9	$\frac{\mu\text{m}^2}{\mu\text{s}}$	Constant viscosity of media	[54]
HARV Rotation Rate		10	R.P.M.		
Gravitational Field Strength	g	$9.81 (10)^{-6}$	$\frac{\text{pg}}{\mu\text{s}^2}$		
Integration					
Timesteps:			μs		
Particle Timestep	dt	150-250	μs		
Fluid Timestep	dt	150-250	μs		
Chemical Timestep	dt	150-250	μs	Higher diffusion requires a smaller timestep	
Biological Timestep	dt	150-250	μs		
Temperature	T	310.15	K	Constant	[20]

Simulation Chemical Properties

Mass Transfer Coefficient	h_s	variable	$\frac{\mu\text{m}}{\mu\text{s}}$		
Methionine Diffusivity	$D_{e,m}$	Low: 3.1 (10) ⁻⁴ Mid: 5.0 (10) ⁻⁴ High: 7.6 (10) ⁻⁴	$\frac{\mu\text{m}^2}{\mu\text{s}}$	Fick's Law diffusion constant	[51, 55]
Acetate Diffusivity	$D_{e,a}$	Low: 4.9 (10) ⁻⁴ Mid: 5.0 (10) ⁻⁴ High: 12. (10) ⁻⁴ 4	$\frac{\mu\text{m}^2}{\mu\text{s}}$	Fick's Law diffusion constant	[51, 55]
Bulk Media Diffusivity	$D_{e,l}$	Low: 2.1 (10) ⁻⁴ Mid: 5.0 (10) ⁻⁴ High: 5.1 (10) ⁻⁴	$\frac{\mu\text{m}^2}{\mu\text{s}}$	Fick's Law diffusion constant	[56]
Starting Methionine Quantity		0.00001/Y _{ES}	$\frac{\text{pg}}{\mu\text{m}^3}$	To kickstart metabolism, total Simulation Starting Quantity Distributed Equally among all Cells, in terms of Biomass Equivalents of <i>E</i> .	
Starting Acetate Quantity		0.00001/Y _{SS}	$\frac{\text{pg}}{\mu\text{m}^3}$	Starting Quantity in terms of Biomass Equivalents of <i>S</i> .	
Acetate Coefficient of Solutal Specific Gravity	β_1	0.85		Linearly interpolated coefficient that converts acetate concentration (cell equivalent) to fluid density	[57]
Methionine Coefficient of Solutal Specific Gravity	β_2	0.003		Linearly interpolated coefficient that converts methionine concentration (cell equivalent) to fluid density	[58]
Bulk Media Coefficient of Solutal Specific Gravity	β_3	0.39		Linearly interpolated coefficient that converts lactose concentration (cell equivalent) to fluid density	[59]

Bacterial Cell Physical/Mechanical Properties

Cell size	d	1.12	pg	Diameter, based on effective volume of a rod shaped <i>E. coli</i> [60]	
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Cell Volumetric density	ρ_s	1.08	$\frac{\text{pg}}{\mu\text{m}^3}$	Needed for Bouyancy	[60]
Young's Modulus of Elasticity	E	50,000	$\frac{\text{pg}}{\mu\text{m}\mu\text{s}^2}$	Required LIGGGHTS® parameter	[46]
Coefficient of Restitution	e	0.05		Minimum Required LIGGGHTS® collision parameter	
Poisson Ratio	ν	0.4		Required LIGGGHTS® parameter	[46]
Surface Energy Intensity	γ	0	$\frac{\text{pg}}{\mu\text{s}^2}$	Cell – cell Adhesion Energy	
Coefficient of Friction	μ_f	0		Cell – cell Sliding Friction Coefficient	

E. coli Biological Properties

Population Density		$1.11 (10)^{-10}$	$\frac{\text{cells}}{\mu\text{m}^3}$	Starting Density of Coculture	[20]
Maximal growth-rate	$\mu_{max,E}$	$1.82 (10)^{-11}$	μs^{-1}	Monod Kinetic Maximal Growth Rate	[29, 61]
Biomass Yield (Methionine)	Y_{ES}	70.2	$\frac{\text{pg}}{\text{pg}}$	Biomass/Methionine Mass	[17, 48]
Biomass Yield (Lactose)	Y_{ES}	1.5	$\frac{\text{pg}}{\text{pg}}$	Biomass/Lactose Mass	[61, 62]
Product Yield	Y_{PS}	31.9	$\frac{\text{pg}}{\text{pg}}$	Acetate/Methionine Mass	[29, 63]
Half-saturation constant	K_S	variable	$\frac{\text{pg}}{\mu\text{m}^3}$	Monod Kinetic Substrate Concentration of Half-maximal Growth Rate	[48]

S. enterica Biological Properties

Population Density		$1.11 (10)^{-10}$	$\frac{\text{cells}}{\mu\text{m}^3}$	Starting Density of Coculture	[20]
Maximal growth-rate	$\mu_{max,S}$	$9.09 (10)^{-12}$	μs^{-1}	Monod Kinetic Maximal Growth Rate	[61]
Biomass Yield	Y_{SS}		$\frac{\text{pg}}{\text{pg}}$	Biomass/Acetate Mass	[61]

0.46				
Product Yield	Y_{PS}	0.058	$\frac{\text{pg}}{\text{pg}}$	Methionine/Acetate Mass [29, 61]
Half-saturation constant	K_s	variable	$\frac{\text{pg}}{\mu\text{m}^3}$	Monod Kinetic Substrate Concentration of Half Maximal Growth Rate [48]
Non-dimensional Numbers				
Reynolds Number	Re	$\frac{u_f d}{\nu}$	Ratio of Inertial to Viscous Forces	
Schmidt Number	Sc	$\frac{\nu}{D_m}$	Ratio of Momentum Diffusivity to Mass Diffusivity	
Sherwood Number	Sh	$\frac{h}{D_m/d}$	Ratio of Convective to Diffusive Mass Transport	

Table S2: Simulation Details and Results. Simulation input files can be found in File S1.

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File Names	Spatial Structure & Diffusivity	Population Size & E:S Ratio	Notes	Steady % Growth Rate
3.1.1a-c	Manually Placed, Intermediate Diffusion	2 cells, 1 E : 1 S	0.01_starting metabolites	
			a. (1 µm distance)	4.7
			b. (50 µm distance)	4.6
			c. (218 µm distance)	4.4
3.1.1d, 3.1.1e/3.1.2a/3.1.3f	Manually Placed, High Diffusion	3 cells, 2:1	0.00001_starting metabolites	
			d. (207 µm distance)	0.8
			e. (1 µm distance)	4.9
3.1.2b-c,	Randomly Distributed High Diffusion	b. 2000 cells		27.2
		1.86:1		
		c. 283 cells		
		1.86:1		29.4
3.1.2c2, 3.1.2e	Spherical gaussian distributed High Diffusion	C2. 283 cells		
		1.86:1		27.8
		E. 100 cells		
		1.86:1		24.5
3.1.2d/3.1.3a/3.2.3e 3.1.3b-e	Tightly packed Sphere, High diffusion	1:86:1		
		a. 2000 cells		35.4
		b. 1000 cells		29.3
		c. 500 cells		28.8
		d. 283 cells		
		e. 99 cells		26
		f. See above		23.4

		1:86:1		29.4
3.1.3g/3.2.3c 3.1.3h-l	Tightly packed Sphere, Low diffusion	g. 2000 cells		29.0
		h. 1000 cells		28.6
		i. 500 cells		27.8
		j. 283 cells		
		k. 99 cells		24.5
		l. 3 cells		
				6.6
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3.1.4a/3.2.3a 3.1.4b	Intermediate diffusion	2000 cells, 44 E : 1 S	0.00000001 starting metabolites 190% λ_E and 333% λ_S Measured S. Growth	50
	a. Gaussian Distributed Sphere b. Randomly distributed			~0
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3.2.1/3.2.3b			Same conditions as 3.1.4a plus RWV hydrodynamics	7.6
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3.2.2a-b	Gaussian Spheres	2000 cells, 18 E : 1 S	0.00001 starting metabolites 190% λ_E and 333% λ_S Measured S. Growth (218 μm distance)	not steady (Figure 8b)
	Distributed Intermediate diffusion		a. Microgravity b. RWV	not steady (Figure 8b)

3.2.3c-g	Tightly packed spheres, c-e. Low Diffusion f-g. High Diffusion	2000 cells, 1.86 E : 1 S	b. RWV Liquid colony c. RWV Solid colony d. Microgravity e. RWV Solid Colony f. Microgravity λ_E and λ_S varies	Growth depends on product yield (Figure 9)
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3.3.1a-b	Intermediate Diffusion a. Flat cylindrical on floor b. Spherical on floor	2000 cells, 44 E : 1 S	1g Gravity	Not steady state (Figure 8b)
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