

*Supporting Information*

## **Effects of Surface Functionalization of Lignin on Synthesis and Properties of Rigid Bio-based Polyurethanes Foams**

**Xuefeng Zhang\*, Dragica Jeremic, Yunsang Kim, Jason Street, Rubin Shmulsky\***

Department of Sustainable Bioproducts, Mississippi State University, Mississippi State, MS 39762, USA

**Contents:**

**10 Pages, including 10 tables and 4 figures.**

1. Inventory data for life cycle assessment (LCA) .....	S2-S4
2. Characterization of lignin and polyol .....	S5-S8
3. LCA units and model output .....	S9

**Inventory data for life cycle assessment (LCA)**

**Table S1.** Flows of traditional polyurethane creation.

Flow input	Category	Amount	Unit
disposal, polyurethane, 0.2% water, to municipal incineration - CH	waste management/municipal incineration	0.02	kg
methylene diphenyl diisocyanate, at plant - RER	plastics/monomers	0.5	kg
pentane, at plant - RER	chemicals/organics	0.054	kg
polyols, at plant - RER	plastics/monomers	0.5	kg
Flow Output	Category	Amount	Unit
Pentane	Emission to air/high population density	0.003	kg
polyurethane, rigid foam, at plant - RER	plastics/polymers	1	kg

**Table S2.** Flows of functionalized lignin-based polyurethane creation.

Flow input	Category	Amount	Unit
disposal, polyurethane, 0.2% water, to municipal incineration - CH	waste management/municipal incineration	0.02	kg
kraft lignin (Bernier)	Agriculture, forestry	0.15	kg
methylene diphenyl diisocyanate, at plant - RER	plastics/monomers	0.5	kg
pentane, at plant - RER	chemicals/organics	0.054	kg
polyols, at plant - RER	plastics/monomers	0.35	kg
Flow Output	Category	Amount	Unit
Pentane	Emission to air/high population density	0.003	kg
polyurethane, rigid foam, at plant - RER	plastics/polymers	1	kg

**Table S3.** Flows of liquefaction polyurethane creation.

Flow input	Category	Amount	Unit
disposal, polyurethane, 0.2% water, to municipal incineration - CH	waste management/municipal incineration	0.02	kg
kraft lignin (Bernier)	Agriculture, forestry	0.15	kg
methylene diphenyl diisocyanate, at plant - RER	plastics/monomers	0.5	kg
pentane, at plant - RER	chemicals/organics	0.054	kg
sulphuric acid, at plant	ecoinvent 2.2	0.015	kg
glycerine, from epichlorohydrin, at plant - RER	chemicals/organics	0.07	kg
ethylene oxide, at plant –RER	chemicals/organics	0.27933	kg
ethylene glycol, at plant - RER	chemicals/organics	0.00098	kg
Flow Output	Category	Amount	Unit
Pentane	Emission to air/high population density	0.003	kg
polyurethane, rigid foam, at plant - RER	plastics/polymers	1	kg

Polyethylene glycol was modeled using the following chemical reaction of ethylene glycol and ethylene oxide with a chain length of 400 (n=400)



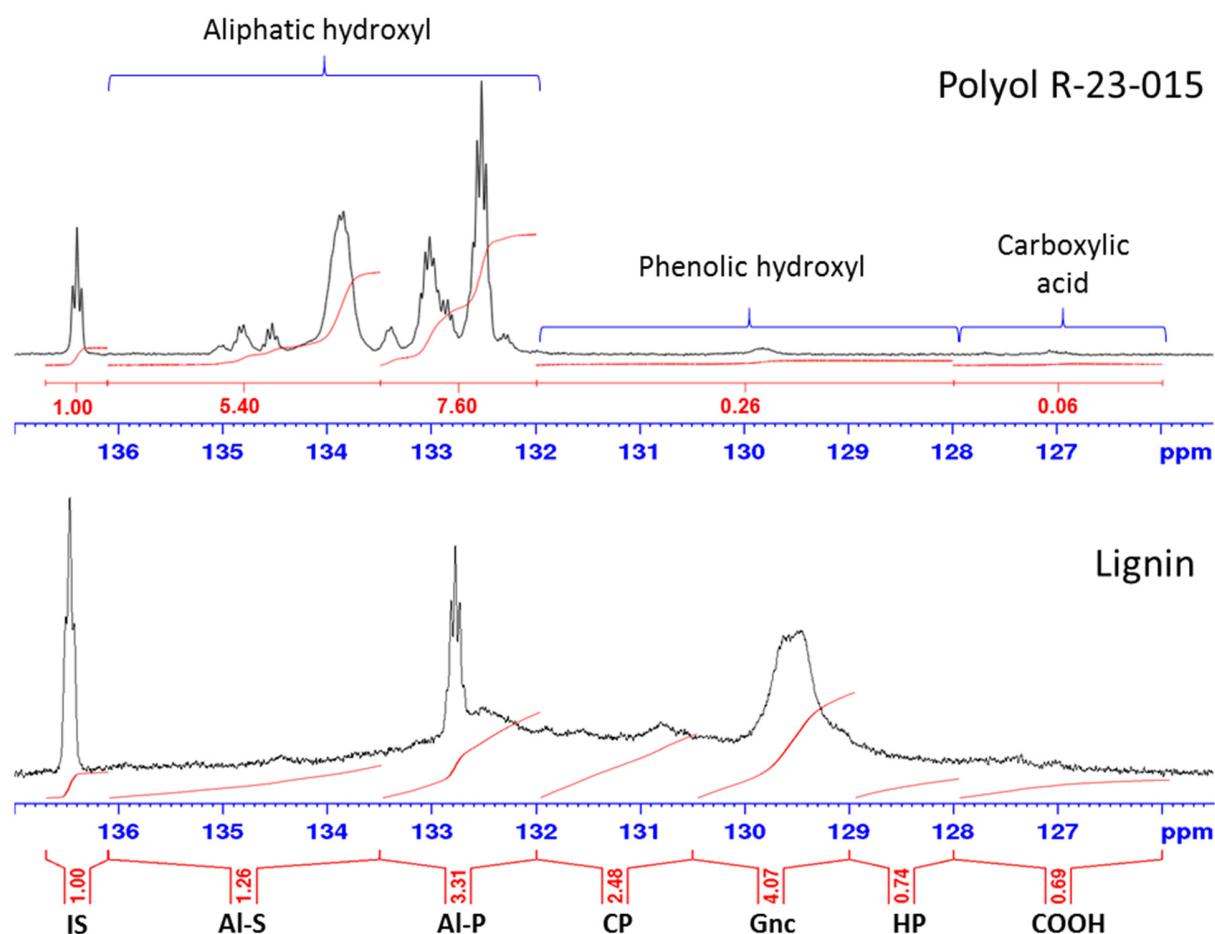
**Table S4.** Flows of oxypropylation polyurethane creation.

<b>Flow input</b>	<b>Category</b>	<b>Amount</b>	<b>Unit</b>
disposal, polyurethane, 0.2% water, to municipal incineration - CH	waste management/municipal incineration	0.02	kg
kraft lignin (Bernier)	Agriculture, forestry	0.15	kg
methylene diphenyl diisocyanate, at plant - RER	plastics/monomers	0.5	kg
pentane, at plant - RER	chemicals/organics	0.054	kg
potassium hydroxide, at regional storage - RER	chemicals/inorganics	0.015	kg
propylene oxide, liquid, at plant - RER	chemicals/organics	0.35	kg
<b>Flow Output</b>	<b>Category</b>	<b>Amount</b>	<b>Unit</b>
Pentane	Emission to air/high population density	0.003	kg
polyurethane, rigid foam, at plant - RER	plastics/polymers	1	kg

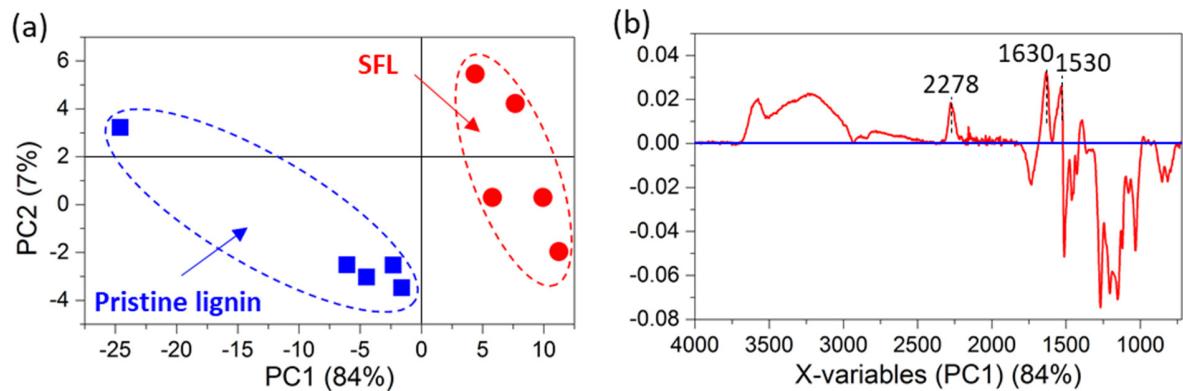
**Table S5.** Flows of kraft lignin creation (Bernier) [S1].

<b>Flow input</b>	<b>Category</b>	<b>Amount</b>	<b>Unit</b>
carbon dioxide, at plant/RER U	ecoinvent2.2	0.3	kg
electricity, medium voltage, at grid - US	ecoinvent2.2	0.01	kWh
natural gas, burned in boiler modulating >100kW	ecoinvent2.2	31.5	MJ
lime, hydrated, packed, at plant	ecoinvent2.2	0.23	kg
sodium hydroxide, 50% in H <sub>2</sub> O, production mix, at plant	ecoinvent2.2	1.07	kg
sulphuric acid, liquid, at plant	ecoinvent2.2	0.23	kg
transport, lorry 16-32t, EURO4	ecoinvent2.2	0.934	t×km
Water, process, unspecified natural origin	water/unspecified	0.00485	m <sup>3</sup>
<b>Flow Output</b>	<b>Category</b>	<b>Amount</b>	<b>Unit</b>
kraft lignin (Bernier)	Agriculture, forestry	1	kg

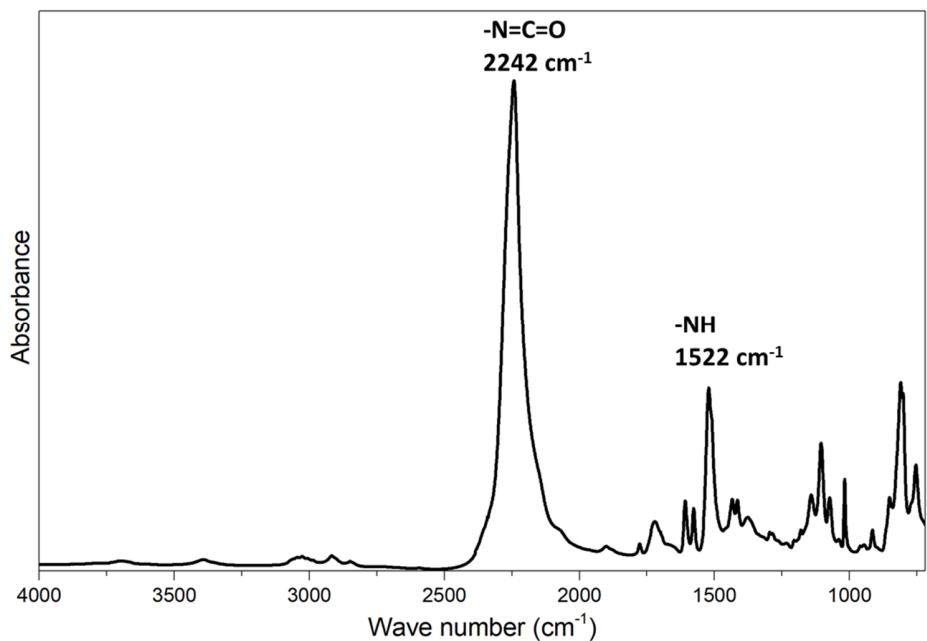
### Characterization results



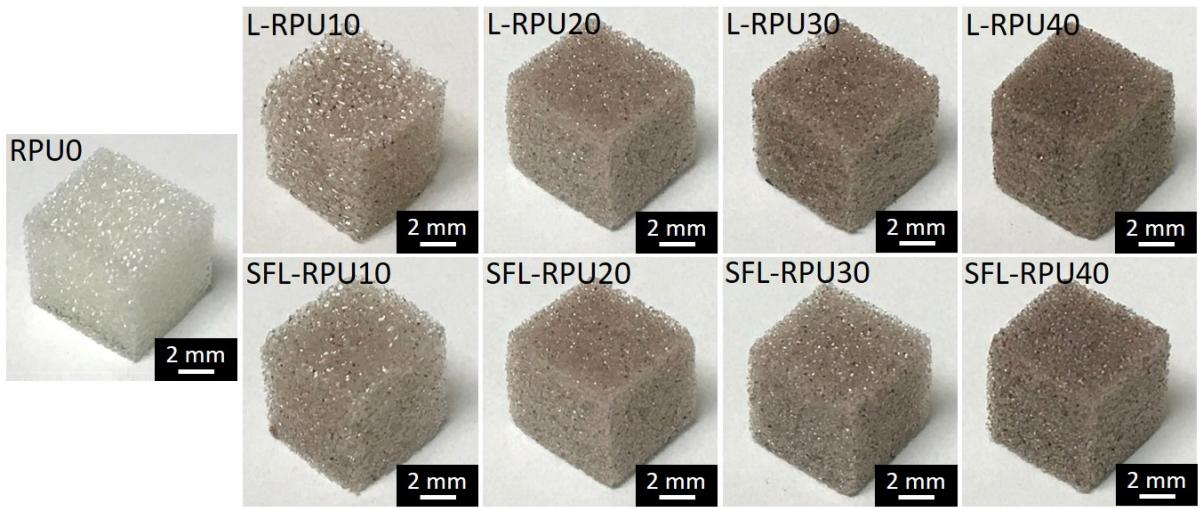
**Figure S1.**  $^{31}\text{P}$ -NMR spectra of the polyol R-23-015 and lignin. IS, internal standard (136.7-136.1 ppm); Al-S, secondary aliphatic OH (136.1-133.5 ppm); Al-P, primary aliphatic OH (133.5-132.0 ppm); CP, condensed phenolic OH (132-130.5 ppm); Gnc, non-condensed guaiacyl (130.5-129 ppm); HP, hydroxyphenyl OH (129-128 ppm); COOH, carboxylic acid (128-126 ppm).



**Figure S2.** (a) score plot of PCA model (PC1 vs. PC2) and (b) loading plot of PC1 of PCA model.



**Figure S3.** FTIR spectrum of pMDI (A-23-015).



**Figure S4.** Photographs of RPU foams made with different amounts (0-40%) of lignin: L-RPU (top row) and SFL-RPU (bottom row).

**Table S6.** Compressive properties of RPU foams containing 0-40% lignin.

Samples	Compressive strength ( $\sigma$ , kPa)	Compressive modulus ( $E$ , kPa)	Specific compressive strength [ $\sigma_p$ , kPa/(kg/m <sup>3</sup> )]	Specific compressive modulus [ $E_p$ , kPa/(kg/m <sup>3</sup> )]
<b>RPU0</b>	166.3±7.7	189.5±26.0	4.8±0.4	5.5±0.8
<b>L-RPU10</b>	146.2±16.5	174.3±21.1	4.3±0.5	5.1±0.7
<b>L-RPU20</b>	174.4±32.8	193.0±31.7	4.8±0.7	5.3±0.7
<b>L-RPU30</b>	160.9±19.2	188.1±29.5	3.9±0.3	4.5±0.6
<b>L-RPU40</b>	135.9±33.5	153.9±35.6	2.5±0.5	2.9±0.6
<b>SFL-RPU10</b>	174.6±14.3	193.2±18.2	4.9±0.4	5.4±0.5
<b>SFL-RPU20</b>	196.1±19.7	225.5±14.8	5.1±0.4	5.9±0.4
<b>SFL-RPU30</b>	205.1±26.5	228.9±27.9	4.9±0.6	5.5±0.6
<b>SFL-RPU40</b>	157.8±51.8	176.1±57.8	3.7±1.1	4.2±1.3

**Table S7.** The intensity ratio of N=C=O band to C=O band ( $I_{NCO}/I_{CO}$ ) of RPU foams containing 0-40% lignin.

Samples	$I_{NCO}/I_{CO}$
<b>RPU0</b>	0.17±0.04
<b>L-RPU10</b>	0.27±0.04
<b>L-RPU20</b>	0.30±0.05
<b>L-RPU30</b>	0.36±0.04
<b>L-RPU40</b>	0.41±0.05
<b>SFL-RPU10</b>	0.21±0.02
<b>SFL-RPU20</b>	0.25±0.03
<b>SFL-RPU30</b>	0.29±0.03
<b>SFL-RPU40</b>	0.32±0.06

**Table S8.** TGA results ( $T_{5\%}$ , DTG-max temperatures, and char yield at 750°C) of RPU foams.

Sample	$T_{5\%}$ (°C)	DTG-max (°C)	Char yield at 750°C (wt%)
<b>RPU0</b>	240.3	0.757	20.3
<b>L-RPU10</b>	245.9	0.698	22.7
<b>L-RPU20</b>	252.6	0.609	25.2
<b>L-RPU30</b>	251.8	0.578	26.2
<b>L-RPU40</b>	258.9	0.514	28.4
<b>SFL-RPU10</b>	245.2	0.720	22.1
<b>SFL-RPU20</b>	246.4	0.661	23.1
<b>SFL-RPU30</b>	247.6	0.585	25.2
<b>SFL-RPU40</b>	253.9	0.517	29.1

## **LCA units and model output**

**Table S9.** LCIA Categories and Units

<b>Impact category</b>	<b>Unit</b>
environmental impact - acidification	moles of H+-Eq
environmental impact - ecotoxicity	kg 2,4-D-Eq
environmental impact - eutrophication	kg N
environmental impact - global warming	kg CO <sup>2</sup> -Eq
environmental impact - ozone depletion	kg CFC-11-Eq
environmental impact - photochemical oxidation	kg NO <sub>x</sub> -Eq
human health - carcinogenics	kg benzene-Eq
human health - non-carcinogenics	kg toluene-Eq
human health - respiratory effects, average	kg PM2.5-Eq

**Table S10.** Desired model output stipulations.

<b>Name</b>	<b>Product system</b>	<b>Flow</b>	<b>Amount</b>	<b>Unit</b>
Liquefaction	Liquefaction Method, at plant	polyurethane, rigid foam, at plant - RER	1	kg
Oxypropylation	Oxypropylation Method, at plant	polyurethane, rigid foam, at plant - RER	1	kg
Surface Functionalization	Surface Functionalization Method, at plant	polyurethane, rigid foam, at plant - RER	1	kg
Traditional	polyurethane, rigid foam, at plant (modified)	polyurethane, rigid foam, at plant - RER	1	kg

## **REFERENCE**

[S1] Bernier, Etienne, Chantal Lavigne, and Pierre Yves Robidoux. "Life cycle assessment of kraft lignin for polymer applications." The International Journal of Life Cycle Assessment 18, no. 2 (2013): 520-528.