

Supplementary materials

Ag- and Cu-Promoted Mesoporous Ta-SiO₂ Catalysts Prepared by Non-Hydrolytic Sol-Gel for the Conversion of Ethanol to Butadiene

Denis D. Dochain ¹, Ales Styskalik ^{1,2,3} and Damien P. Debecker ^{1,*}

¹ Institut of Condensed Matter and Nanosciences – Université catholique de Louvain (UCLouvain), Place Louis Pasteur, 1, 1348 Louvain-la-Neuve, Belgium; d.dochain@student.uclouvain.be (D.D.D.); ales.styskalik@ceitec.muni.cz (A.S.)

² Department of Chemistry, Masaryk University, Kotlarska 2, CZ-61137 Brno, Czech Republic

³ CEITEC MU, Masaryk University, Kamenice 5, CZ-62500 Brno, Czech Republic

* Correspondance: damien.debecker@uclouvain.be

Table S1. Textural properties (N₂-physisorption) for catalysts used in catalytic study.

Sample	S _{BET} (m ² g ⁻¹)	V _p (cm ³ g ⁻¹) ^a	V _μ (cm ³ g ⁻¹) ^b	D _p (nm) ^c
4TaSi_{NHSG}-5Ag	490	0.43	0.08	3.5
2TaSi_{NHSG}-2Ag	670	0.58	0.11	3.5
2TaSi_{NHSG}-5Ag	580	0.55	0.08	3.8
2Ta^{IMPSi}-5Ag	n.m	n.m	n.m	n.m
2TaSi5Ag_{NHSG}	710	0.89	0.08	5.0
2TaSi5Cu_{NHSG}	640	0.60	0.07	3.8

^a Pore volume at P/P₀=0.98; ^b Micropore volume at P/P₀=0.98; ^c Calculated as 4V_p/S_{BET}.

Table S2. Synthesis of Si-Ta binary oxides – amounts of precursors and surfactant.

Sample	Si(OAc) ₄ mass (g)	Ta(NMe ₂) ₅ mass (g)	F127 mass (g)
4Ta _{NHSG}	7.0927	0.1796	3.6331
2Ta _{NHSG} ^a	10.6386	0.1346	5.4475
Si _{NHSG}	7.0930	0.0035	3.6308

^a Quantity x1.5, amount of solvent was adjusted accordingly.

Table S3. Impregnation of silver – amounts of catalyst and Ag salt used.

Sample	Impregnated mass (g)	AgNO ₃ mass (g)
4Ta _{NHSG} -2Ag	1.0002	0.0321
4Ta _{NHSG} -5Ag	1.0026	0.0841
2Ta _{NHSG} -2Ag	1.0017	0.0325
2Ta _{NHSG} -5Ag	1.0009	0.0845

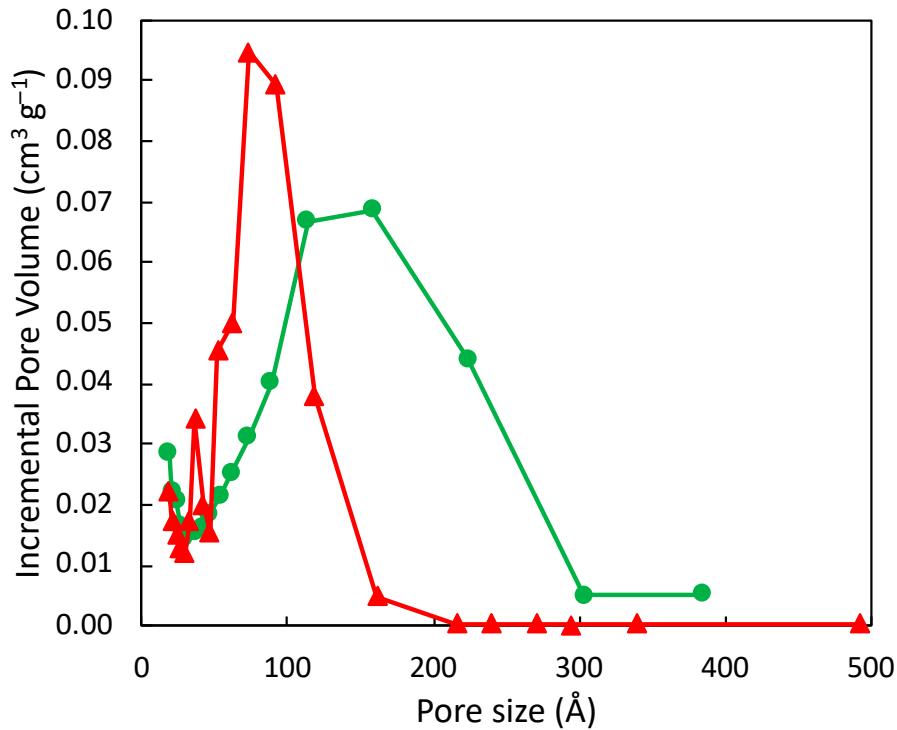


Figure S1. Pore size distribution in 4TaSinhSG-2Ag by the BJH model (from the adsorption curve in green ●; from the desorption curve in red ▲).

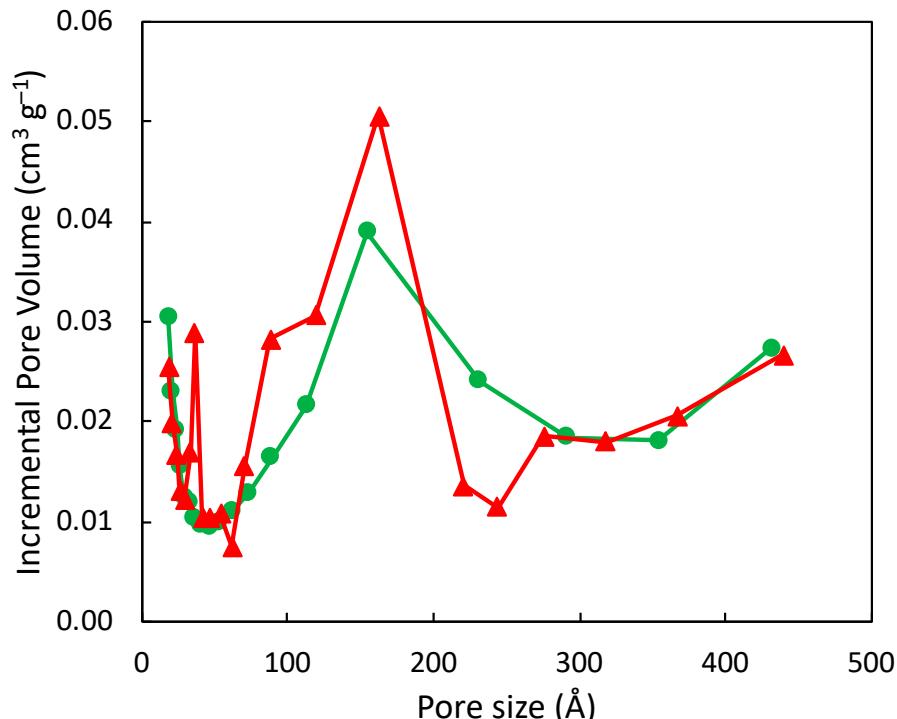


Figure S2. Pore size distribution in 4TaIMPSi-2Ag by the BJH model (from the adsorption curve in green ●; from the desorption curve in red ▲).

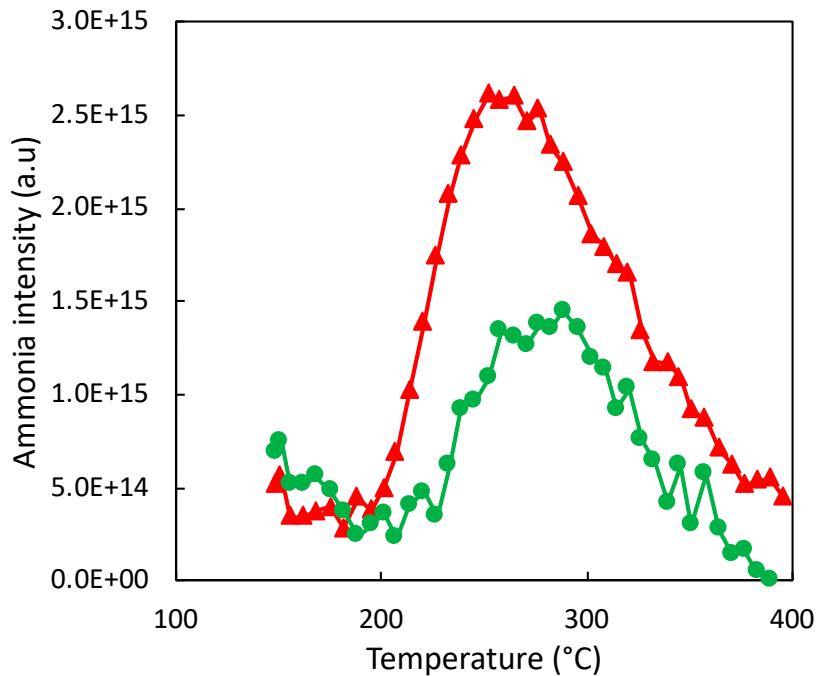


Figure S3. Ammonia desorption profiles of 4TaSiNHSG-2Ag (red ▲) and 4TaIMPSi-2Ag (green ●).

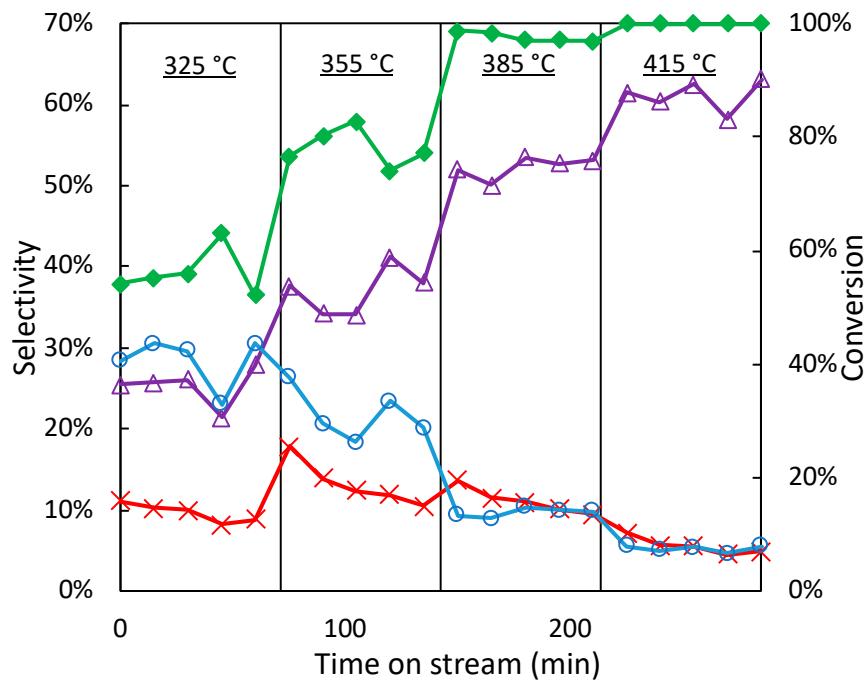


Figure S4. Evolution of ethanol conversion (green ◊), butadiene selectivity (red ×), acetaldehyde selectivity (blue ○) and ethylene selectivity (purple Δ) over time for all tested temperatures for 4TaSiNHSG-2Ag. Note: the spent catalyst has a brownish color, indicative of coke formation. At 385 °C and 415°C, the carbon balance is incomplete (at lower temperature, it accounts for >95%).

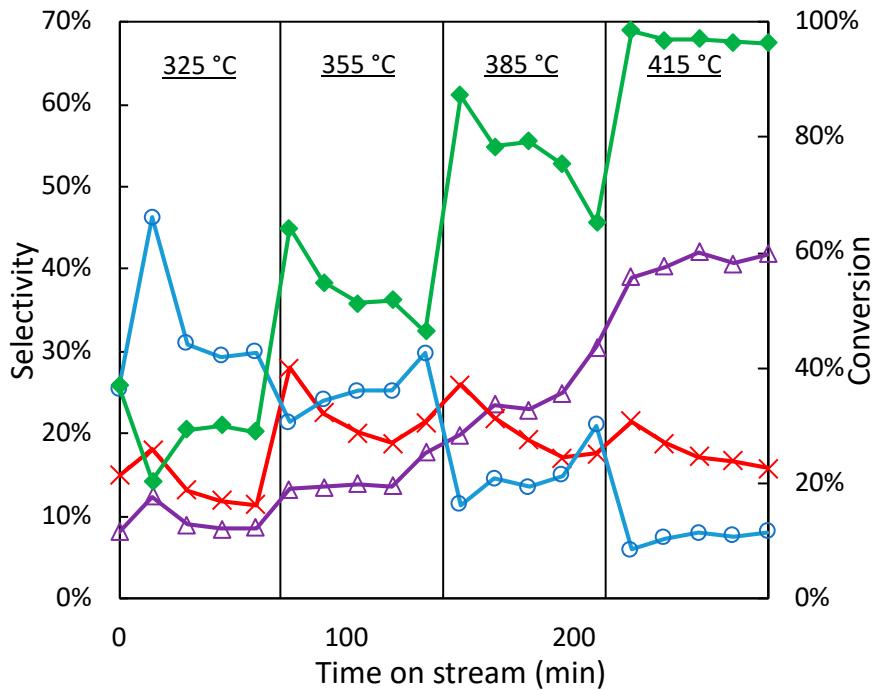


Figure S5. Evolution of ethanol conversion (green ◊), butadiene selectivity (red ×), acetaldehyde selectivity (blue ○) and ethylene selectivity (purple Δ) over time for all tested temperatures for 4Ta_{1.5}Si 2Ag.

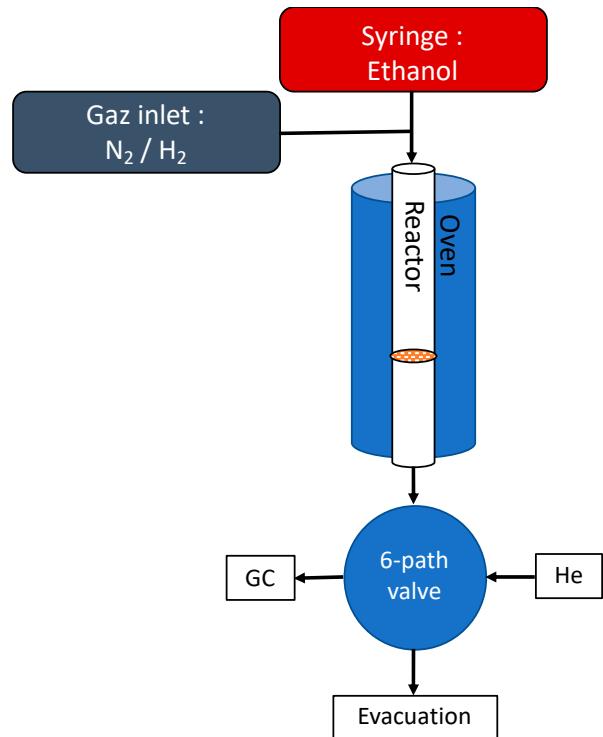


Figure S6. Schematic view of the catalytic setup.