

## Article

# Electroreduction of CO<sub>2</sub> into Ethanol over an Active Catalyst: Copper Supported on Titania

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**Abstract:** A simple, inexpensive, and novel method was used to prepare electrocatalysts from Cu supported on titanium dioxide (Cu/TiO<sub>2</sub>). XRD, SEM, and TEM characterizations confirmed different loadings of Cu nanoparticles (NPs) on TiO<sub>2</sub>. Cyclic voltammetry tests indicated that Cu/TiO<sub>2</sub> exhibited lower overpotential for CO<sub>2</sub> reduction than that of Cu NPs. Moreover, 40 wt % Cu/TiO<sub>2</sub> exhibited the highest faradaic efficiency for ethanol (FE<sub>ethanol</sub>) of 27.4%, which is approximately 10-fold higher than that for Cu NPs (FE<sub>ethanol</sub> = 2.7%). The 40 wt % Cu/TiO<sub>2</sub> electrocatalyst exhibits a stable current density of 8.66 mA/cm<sup>2</sup> over a 25 h stability test. The high efficiency towards CO<sub>2</sub> electroreduction to ethanol may be attributed to the synergistic effect of Cu and TiO<sub>2</sub> NPs. This work highlights the importance of compositional effect of NPs on their catalytic activities and provides a strategy for designing efficient catalysts for CO<sub>2</sub> electroreduction in the future.

**Keywords:** CO<sub>2</sub> reduction; Cu nanoparticles; titanium dioxide; faradaic efficiency; ethanol

## 1. Introduction

Large-scale consumption of fossil fuel has increased CO<sub>2</sub> concentration in the atmosphere. High atmospheric CO<sub>2</sub> concentrations are associated with greenhouse effect and climate change, which have gained increased research attention [1,2]. Once captured, CO<sub>2</sub> is a potentially useful feedstock if it can be converted into formate/formic acid, carbon monoxide, or more highly reduced hydrocarbon products. Electroreduction is a potential efficient method for CO<sub>2</sub> utilization and recycling, which can be performed at moderate temperature and atmospheric pressure and exhibits high product selectivity compared with other reduction methods, such as chemical, photochemical, and thermochemical methods. Besides, electrical energy could be provided by other green and sustainable energy sources, including wind, solar, and wave [3].

Hori et al. [4] performed pioneering works on electrochemical CO<sub>2</sub> reduction using transition metal electrocatalysts. In addition to metal and metallic oxide, alloys and other semiconductors have been studied as catalysts. Thus far, few studies have investigated the use of metal supported on metal oxides to form different composites, which have been reported to possess improved faradaic efficiencies (FEs) for CO<sub>2</sub> reduction compared to both parent metal and metal oxide. Besides, support materials have been designed to support and stabilize small nanoparticles (NPs) with high current density (J) and FE. For instance, Yu and his team [5] report that copper nanoparticle interspersed MoS<sub>2</sub> nanoflowers facilitate CO<sub>2</sub> electroreduction to hydrocarbon, such as CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub> with high FE at low overpotentials. Sun et al. [6] demonstrated a new strategy of controlling synergistic effect between Cu and SnO<sub>2</sub> in the core/shell Cu/SnO<sub>2</sub> structure to achieve selective electrochemical reduction of CO<sub>2</sub> to CO with FE reaching 93% at −0.7 V vs. reversible hydrogen electrode (RHE) in 0.5 M KHCO<sub>3</sub>.

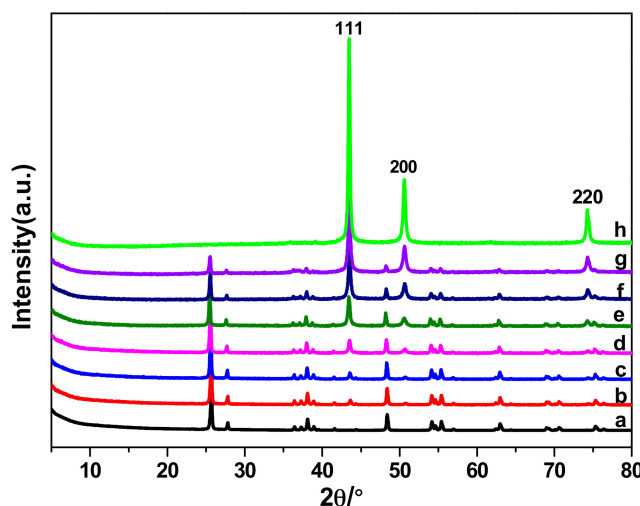
Compared with the noble metals, such as Pd [7] and Au [8], Cu has been considered an ideal electrode material for CO<sub>2</sub> reduction because of its low cost and good catalytic effect. According to a previous report [9,10], it is the only metal electrocatalyst possessing the ability to form a substantial amount of hydrocarbons, which are regarded as ideal products due to their high energy density. Strasser et al. [11] used Cu NPs with different thicknesses as catalysts in electroreduction of CO<sub>2</sub> into CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub>; the investigated activity-selectivity-size relations provide novel insights into the CO<sub>2</sub> electroreduction reaction on nanoscale surfaces. Kuhl et al. [12] reported new insights into the electrochemical reduction of CO<sub>2</sub> on a metallic copper surface and observed a total of 16 different CO<sub>2</sub> reduction products, such as methanol, ethanol, formate, and methane.

Normally, titanium on its own has no significant catalytic activity towards CO<sub>2</sub> electroreduction. However, TiO<sub>2</sub> has shown some activity in both photocatalysis and electrocatalysis for CO<sub>2</sub> reduction [13–15]. When thin TiO<sub>2</sub> films or mixtures of TiO<sub>2</sub> and other metal and metal oxides are used as an electrocatalyst to catalyze CO<sub>2</sub> electroreduction, they show more excellent performance than TiO<sub>2</sub> NPs. For example, in the preparation of a CO<sub>2</sub> catalytic electrode, Monnier et al. [15] prepared TiO<sub>2</sub>, TiO<sub>2</sub>-Ru (or RuO<sub>2</sub>), and TiO<sub>2</sub>-Pt thin film electrodes by thermal deposition on titanium rods. Bandi [16] deposited metallic oxide mixtures (including RuO<sub>2</sub>, TiO<sub>2</sub>, MoO<sub>2</sub>, Co<sub>3</sub>O<sub>4</sub>, and Rh<sub>2</sub>O<sub>3</sub>) on titanium foil. Cueto and Hirata [17] prepared a TiO<sub>2</sub>-indium-tin oxide thin-film glass electrode via a fixed-potential bulk electrolysis process, in which 1-butyl-3-methylimidazolium tetrafluoroborate (BMImBF<sub>4</sub>, an ionic liquid) was used as both solvent and supporting electrolyte. In addition, TiO<sub>2</sub> acts as a redox electron carrier that facilitates various reduction reactions, which include CO<sub>2</sub> conversion [18,19]. The TiO<sub>2</sub> surface assists in CO<sub>2</sub> adsorption to stabilize the intermediate of CO<sub>2</sub> electroreduction and reduces the overpotential [20,21]. In fuel cells, Pt-supported titanium dioxide exhibits improved electrocatalytic properties, such as increased Pt catalyst activity, stability, and durability [22]. To the best of our knowledge, however, no comprehensive research reports the synergistic effect of Cu and TiO<sub>2</sub> on the stability of the composite electrocatalysts for CO<sub>2</sub> reduction. Inspired by the initial results of Cu-based materials, we successfully synthesized TiO<sub>2</sub> as catalyst support for Cu in electroreduction of CO<sub>2</sub>. Structural characterizations and electrochemical experiments were performed to compare different Cu loadings supported on TiO<sub>2</sub>. Cu nanocatalysts supported on TiO<sub>2</sub> show high catalytic activity for CO<sub>2</sub> electroreduction to ethanol.

## 2. Results and Discussion

### 2.1. Performance Comparison of Different Cu-Supported TiO<sub>2</sub> Catalysts

Cu/TiO<sub>2</sub> catalysts were characterized through powder X-ray diffraction (XRD) analysis. Figure 1 (curves b–h) shows diffraction peaks at 43.3°, 50.4° and 74.1°, which are attributed to Cu (111), (200) and (220) reflections, respectively. The rest of peaks can be ascribed to the TiO<sub>2</sub>, which were observed in Figure 1 (curves a–g), indicating that Cu and TiO<sub>2</sub> formed a composite electrocatalyst. Moreover, the peaks of Cu became evident in the XRD patterns with increasing Cu proportion. The presence of Cu and TiO<sub>2</sub> was confirmed by energy dispersive X-ray (EDX) analysis (Figure S1, Supplementary Materials (SM)); the results showed signals corresponding to copper, titanium, and oxygen. The values for actual Cu loading of the synthesized catalysts are determined through inductive coupled plasma (ICP) emission spectrometer (Table 1). The actual loading values are consistent with the predicted values.



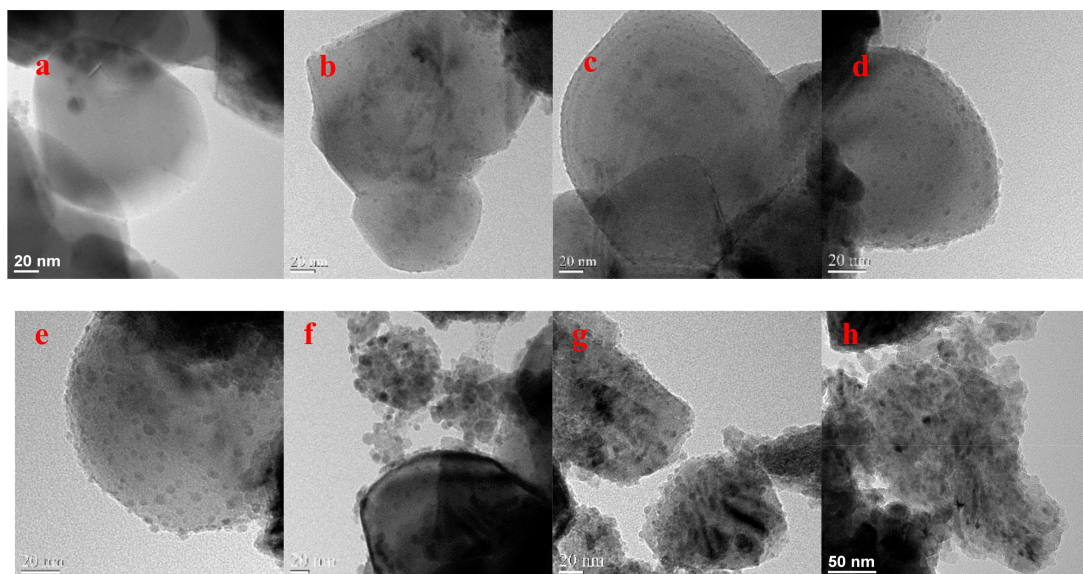
**Figure 1.** XRD patterns of X wt % Cu/TiO<sub>2</sub>: (a) pure TiO<sub>2</sub>; (b) 5 wt % Cu/TiO<sub>2</sub>; (c) 10 wt % Cu/TiO<sub>2</sub>; (d) 20 wt % Cu/TiO<sub>2</sub>; (e) 40 wt % Cu/TiO<sub>2</sub>; (f) 60 wt % Cu/TiO<sub>2</sub>; (g) 80 wt % Cu/TiO<sub>2</sub> and (h) pure Cu NPs.

**Table 1.** Cu composition of the synthesized catalysts <sup>a</sup>.

Catalyst	Cu loading (wt %)	
	Intended	Actual <sup>a</sup>
5 wt % Cu/TiO <sub>2</sub>	5	4.68
10 wt % Cu/TiO <sub>2</sub>	10	8.52
20 wt % Cu/TiO <sub>2</sub>	20	18.39
40 wt % Cu/TiO <sub>2</sub>	40	37.12
60 wt % Cu/TiO <sub>2</sub>	60	53.06
80 wt % Cu/TiO <sub>2</sub>	80	73.02

<sup>a</sup> Obtained by ICP.

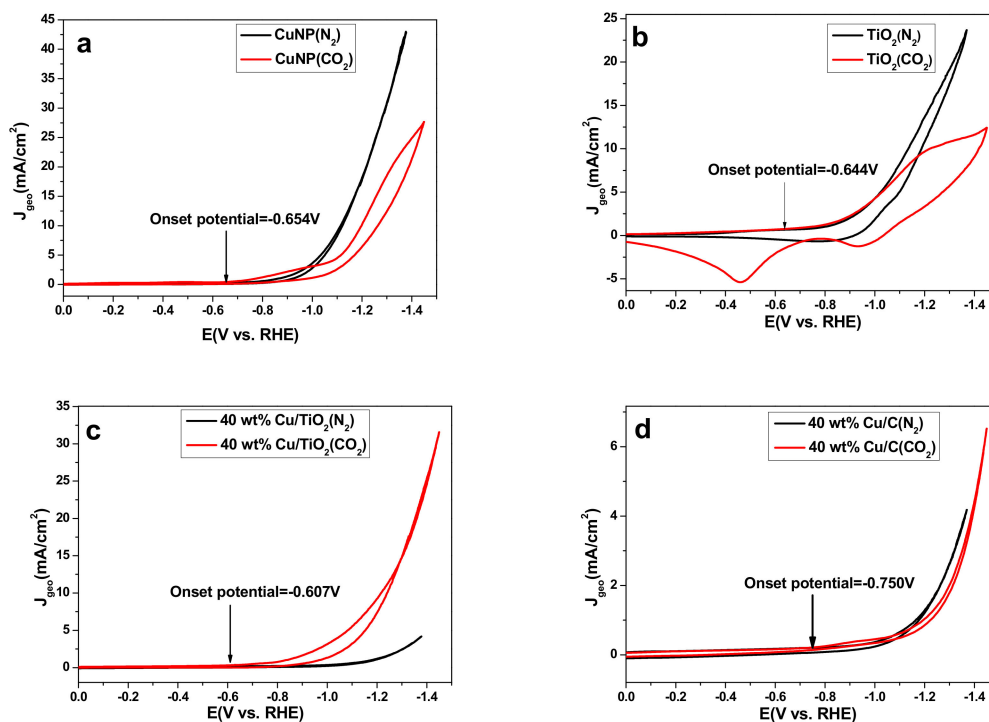
Scanning electron microscopy (SEM) and transmission electron microscopy (TEM) images were collected to observe morphological differences among Cu/TiO<sub>2</sub> catalysts (Figure 2 and Figure S2 in SM). The results indicated how Cu NPs are progressively loaded on the TiO<sub>2</sub> surface. The Cu/TiO<sub>2</sub> catalysts possess a three-dimensional (3D) irregular nanoblock structure, with an average size of about 300 nm, and are covered with tiny NPs. Cu NPs gradually spread all over the TiO<sub>2</sub> surface, forming a massive and compact layer, with increasing Cu loadings. For few Cu loadings, TiO<sub>2</sub> was clearly covered by the sporadic Cu particles. Unexpectedly, the TEM images of 60 wt % and 80 wt % Cu/TiO<sub>2</sub> showed that Cu NPs are more prone to agglomerate than 40 wt % Cu/TiO<sub>2</sub>, which stem from the increased loading of Cu, leading to the decline of active sites for CO<sub>2</sub> reduction. Predictably, the current density and FE on 60 wt % and 80 wt % Cu/TiO<sub>2</sub> are lower than those observed on 40 wt % Cu/TiO<sub>2</sub>; this finding will be comprehensively described in the catalyst test section. Interestingly, without TiO<sub>2</sub> as support material, Cu NPs exhibited a large diameter, which varied between 20 and 100 nm. Thus, TiO<sub>2</sub> helps to create and stabilize small and well-dispersed Cu NPs, which allows more active sites-Cu NPs for CO<sub>2</sub> reduction.



**Figure 2.** TEM images of the synthesized catalysts: (a) pure  $\text{TiO}_2$ , (b) 5 wt %  $\text{Cu}/\text{TiO}_2$ , (c) 10 wt %  $\text{Cu}/\text{TiO}_2$ , (d) 20 wt %  $\text{Cu}/\text{TiO}_2$ , (e) 40 wt %  $\text{Cu}/\text{TiO}_2$ , (f) 60 wt %  $\text{Cu}/\text{TiO}_2$ , (g) 80 wt %  $\text{Cu}/\text{TiO}_2$ , (h) pure Cu NPs with high magnification. Dark spheres or dots are Cu particles; the grey larger structures are the support materials.

## 2.2. Catalyst Activity in a Standard Three-Electrode Cell

Figure 3 shows the cyclic voltammograms (CVs) obtained with pure Cu NPs,  $\text{TiO}_2$ , 40 wt %  $\text{Cu}/\text{TiO}_2$  and 40 wt %  $\text{Cu}/\text{C}$ , which was successfully synthesized, characterized by XRD, SEM, and TEM (Figures S3–S5, SM), coated on glass carbon electrode ( $d = 2 \text{ mm}$ ). When the electrolyte was bubbled with  $\text{CO}_2$ , reduction peaks associated with  $\text{CO}_2$  reduction were observed. Comparison of Figure 3a,c,d, 40 wt %  $\text{Cu}/\text{TiO}_2$  ( $-0.607 \text{ V}$  vs. RHE) showed a 47 mV lower onset potential for  $\text{CO}_2$  reduction than that on Cu NPs ( $-0.654 \text{ V}$  vs. RHE) and a 143 mV lower onset potential than 40 wt %  $\text{Cu}/\text{C}$  ( $-0.750 \text{ V}$  vs. RHE), respectively. The improvement of 40 wt %  $\text{Cu}/\text{TiO}_2$  may be because of the adsorption and stabilization of  $\text{CO}_2$  on the  $\text{TiO}_2$  surface [23]. In order to better explain the phenomenon,  $\text{TiO}_2$  alone as catalyst exhibited low onset potential of  $-0.644 \text{ V}$  vs. RHE for  $\text{CO}_2$  electroreduction (Figure 3b). The large overpotential of  $\text{CO}_2$  reduction could be due to the barrier of the initial electron in forming a  $\text{CO}_2^-$  intermediate, which exhibits poor stability on most metal surfaces [4]. The CV of the 40 wt %  $\text{Cu}/\text{TiO}_2$  catalyst was seen to have an earlier onset potential, which is in agreement with the better performance on the 40 wt %  $\text{Cu}/\text{TiO}_2$  catalyst surface than that on the Cu NPs and 40 wt %  $\text{Cu}/\text{C}$  catalysts surface. In addition, for the pure Cu NPs electrode, as shown in Figure 3a, much higher reduction current density  $J_{\text{geo}}$  (based on geometric area of  $0.0314 \text{ cm}^2$ ) was observed for  $\text{N}_2$  saturated solution than that for  $\text{CO}_2$  saturated solution. It strongly indicates  $\text{CO}_2$  reduction reaction was inhibited on the surface of Cu NPs in the entire potential range. The  $J_{\text{geo}}$  of 40 wt %  $\text{Cu}/\text{C}$  presents a slight increase under  $\text{CO}_2$  atmosphere compared with  $\text{N}_2$  atmosphere. However, in sharp contrast, for 40 wt %  $\text{Cu}/\text{TiO}_2$  sample, rapid increment of the  $J_{\text{geo}}$  was observed under both conditions, in comparison with the  $J_{\text{geo}}$  curve (black line) in  $\text{N}_2$  atmospheres, the  $\text{CO}_2$ -saturated solution showed larger  $J_{\text{geo}}$  in the entire potential range, which indicates 40 wt %  $\text{Cu}/\text{TiO}_2$  sample exhibited obvious catalytic activity towards  $\text{CO}_2$  reduction (Figure 3c). Besides, the maximum  $J_{\text{geo}}$  in  $\text{CO}_2$  saturated solution of Cu NPs and 40 wt %  $\text{Cu}/\text{C}$  are  $27.94 \text{ mA}/\text{cm}^2$  and  $6.7 \text{ mA}/\text{cm}^2$  at  $-1.45 \text{ V}$  vs. RHE, respectively, which are lower than the  $J_{\text{geo}}$  of 40 wt %  $\text{Cu}/\text{TiO}_2$  ( $31.79 \text{ mA}/\text{cm}^2$ ) at  $-1.45 \text{ V}$  vs. RHE. This once again proves that 40 wt %  $\text{Cu}/\text{TiO}_2$  shows remarkable performance of  $\text{CO}_2$  electroreduction, which was reconfirmed by the electrolytic data in the following text.



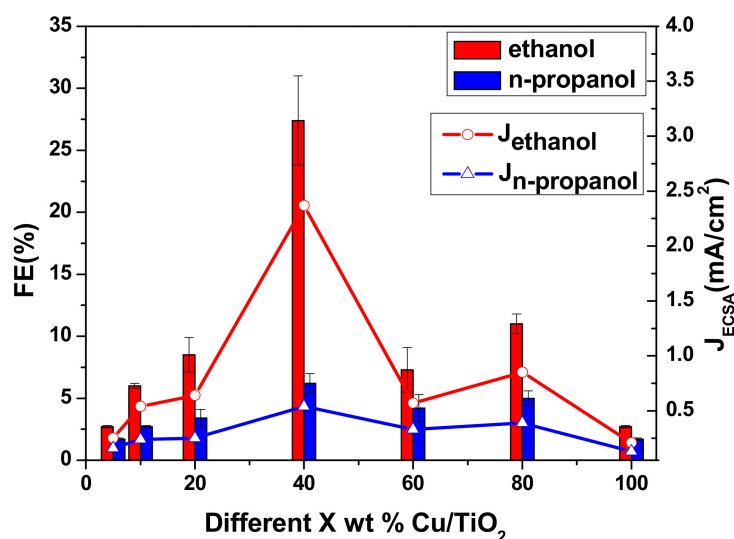
**Figure 3.** CVs of (a) pure Cu NPs, (b)  $\text{TiO}_2$ , (c) 40 wt % Cu/ $\text{TiO}_2$  and (d) 40 wt % Cu/C catalyst after bubbling  $\text{N}_2$  (black) or  $\text{CO}_2$  (red). All experiments were carried out in 0.2 M KI solution and at a scan rate of 100 mV/s.

### 2.3. The Electrocatalytic Activity of Various Cu/ $\text{TiO}_2$

Electrolysis was performed in 0.2 M KI solution saturated with  $\text{CO}_2$  at a constant cathodic potential of  $-1.45$  V vs. RHE to evaluate the catalytic activity of Cu/ $\text{TiO}_2$ . The products were detected through GC analysis (Figure S6, SM). The results demonstrated that ethanol (with little propanol and trace methanol) is the main product, and we are only interested in liquid products. Figure 4 reveals a dramatic difference in the amount of Cu content in the overall  $\text{CO}_2$  electrocatalytic reduction activity of Cu/ $\text{TiO}_2$ . In the case of bare  $\text{TiO}_2$  catalyst, neither ethanol nor n-propanol were detected after electroreduction of  $\text{CO}_2$ . Comparatively, after loading of the Cu NPs, 40 wt % Cu/ $\text{TiO}_2$  exhibited the optimal performance in terms of total FE (33.6%) among all the prepared samples. The total FE decreased to about 10–16% for loadings of 20, 60, and 80 wt % and to below 10% for loading of 10 wt %; the efficiency significantly decreased for loadings of 5 wt % and pure Cu NPs. For the sake of explaining the phenomenon, the TEM images of various Cu/ $\text{TiO}_2$  were again compared and analyzed, and electrochemistry surface area (ECSA) test of various Cu/ $\text{TiO}_2$  were carried out. As the TEM images in Figure 2 and histograms in Figure S7 (SM) show, the TEM images of 60 wt % and higher content of Cu samples suggest that Cu particles are more prone to agglomerate than 40 wt % sample, resulting in smaller surface area for these samples, and then the active surface of samples for  $\text{CO}_2$  electroreduction decrease, which was consistent with the results of ECSA test for various Cu/ $\text{TiO}_2$  (Figure S8 and Table S1, SM). Moreover, as seen from Figure 4 and Table S1 (SM), along with the mass ratio of Cu NPs in the Cu/ $\text{TiO}_2$  samples increasing, the catalytic activity and ECSA revealed synchronous change. 40 wt % Cu/ $\text{TiO}_2$  possesses a largest ECSA of  $3.32 \text{ cm}^2$  in all various Cu/ $\text{TiO}_2$  catalysts. Besides, 60 wt % Cu/ $\text{TiO}_2$  displays lower catalytic activity than 80 wt %, due to the decrease of active surface, as confirmed by ECSA. It could be clearly seen that the catalytic activity of various Cu/ $\text{TiO}_2$  had a close connection to the corresponding ECSA. In fuel cell applications, Ag supported on titanium dioxide exhibited the same properties [23]. For comparison, potentiostatic electrolysis was conducted by applying a potential of  $-1.45$  V vs. RHE on 40 wt % Cu/C in 0.2 M KI solution saturated



with CO<sub>2</sub>, which only results in 8.4% FE for ethanol. As shown in Table S1 (SM), both ECSA and current density  $J_{\text{ECSA}}$  (based on ECSA) of 40 wt % Cu/C were smaller than those of 40 wt % Cu/TiO<sub>2</sub>, which indicates that high performance for CO<sub>2</sub> electroreduction on Cu/TiO<sub>2</sub> may be ascribed to the synergistic effect between Cu and TiO<sub>2</sub>. Furthermore, although 5 wt % Cu/TiO<sub>2</sub> and Cu NPs have a similar ECSA (Table S1, SM), the  $J_{\text{ECSA}}$  of 5 wt % Cu/TiO<sub>2</sub> was slightly larger than the one of Cu NPs. It was reconfirmed that the prepared composites with excellent activity for CO<sub>2</sub> conversion are obtained by the synergetic effect of Cu NPs and TiO<sub>2</sub>.



**Figure 4.** FEs and partial  $J_{\text{ECSA}}$  on different Cu/TiO<sub>2</sub> catalyst at the constant potential (−1.45 V vs. RHE) in a CO<sub>2</sub>-saturated 0.2 M KI aqueous solution.

#### 2.4. Electrocatalytic Characterization

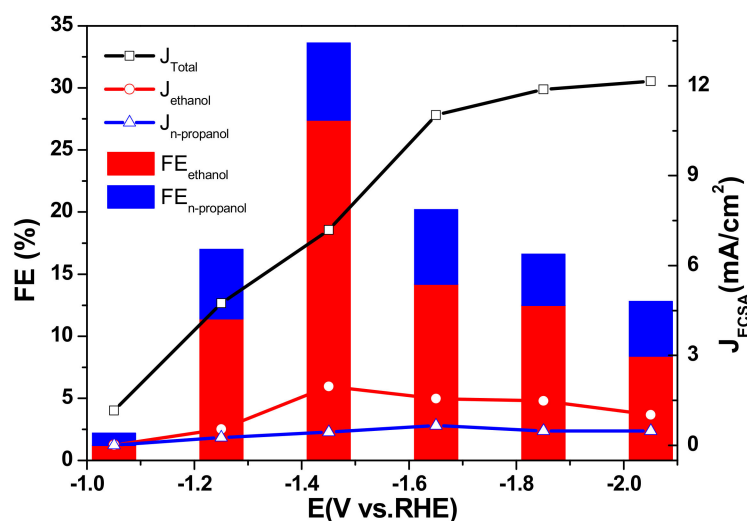
We also explored the performance of the catalyst amounts. The amounts of the catalyst loading—such as 0.5, 1, 2, 3, 4, and 5 mg·cm<sup>−2</sup>—for 40 wt % Cu/TiO<sub>2</sub> were painted on a carbon paper to form a cathode. As shown in Table 2, the catalyst amount of 1 mg·cm<sup>−2</sup> exhibited the optimal performance among all other amounts. Despite the increasing catalyst amount from 0.5 to 5 mg·cm<sup>−2</sup>, the activity did not increase. The accessible surface area is not proportional to the corresponding catalyst loading. This finding is important because the resulting activity is correlated with the actual active surface area. Thus, to evaluate this finding, we performed SEM for analyzing the catalytic layer thickness and morphology of the as-prepared electrodes. The SEM images (Figure S9, SM) indicate how the Cu/TiO<sub>2</sub> NPs are progressively deposited on the carbon paper with increasing catalyst loading. Interestingly, for high loadings (3, 4, and 5 mg·cm<sup>−2</sup>), the Cu/TiO<sub>2</sub> NPs completely cover the porous structure of the carbon paper, forming a massive and compact layer, which results in Cu/TiO<sub>2</sub> NPs hardly contacting the catholyte and CO<sub>2</sub>. For low loadings (0.5 mg·cm<sup>−2</sup>), the carbon fibers were uncovered by the Cu/TiO<sub>2</sub> NPs, and these fibers were deposited and formed clusters. Despite the clusters being relatively well accessible for the reactants, the amount of the electrocatalytic material is very low, thus the activities are also low. An intermediate situation was observed for medium loadings (1 and 2 mg·cm<sup>−2</sup>). In these electrodes, the carbon fibers were well covered with the Cu/TiO<sub>2</sub> NPs, and a massive and compact layer was not formed. The limit for the massive and compact layer formation is approximately 1 mg·cm<sup>−2</sup> metal loading. These observations are in accordance with the results shown in Table 2.

**Table 2.** FEs for ethanol and n-propanol with different amounts of 40 wt % Cu/TiO<sub>2</sub> deposited over carbon paper at −1.45 V vs. RHE <sup>a</sup>

Cu/TiO <sub>2</sub> Amount (mg/cm <sup>2</sup> )	FE <sub>ethanol</sub> (%) <sup>b</sup>	FE <sub>n-propanol</sub> (%) <sup>b</sup>
5	2.1	1.2
4	4.6	1.8
3	7.2	3.2
2	19.0	6.0
1	27.4	6.2
0.5	6.3	2.5

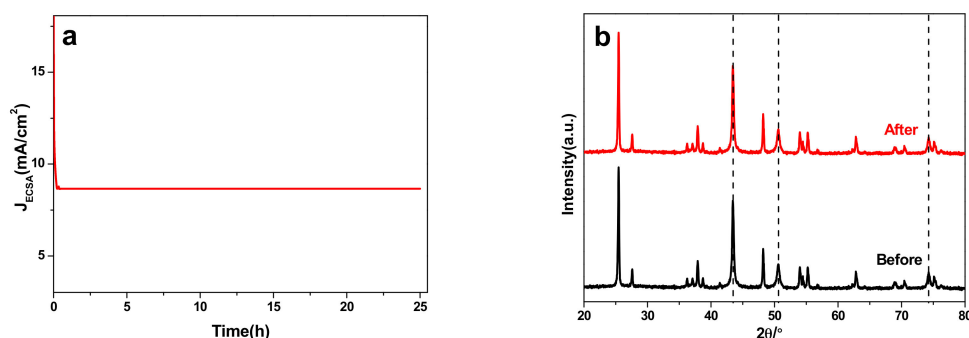
<sup>a</sup> Electrolysis condition: electrolyte = 0.2 M KI, E = −1.45 V vs. RHE. <sup>b</sup> Obtained by GC.

In order to evaluate the optimal potential, CO<sub>2</sub> reduction measurements on 40 wt % Cu/TiO<sub>2</sub> exhibiting its superior electrochemical characteristics was firstly carried out at the potential range from −1.05 to −2.05 V vs. RHE. Figure 5 shows the remarkable influence of cathodic potential on FE. As cathodic potential shifts from −2.05 V to −1.05 V vs. RHE, the total FE increased first, reached a maximum of 33.6% at −1.45 V vs. RHE, and decreased to 2.2% at −1.05 V vs. RHE. Similar results were found for the FE of ethanol, whereas it is almost insensitive to n-propanol. Presumably, the pathways for ethanol and propanol production are different, resulting in different FE tendencies. The total J<sub>ECSA</sub> increased with decreasing potential. However, partial J<sub>ECSA</sub> for ethanol is very different from the total J<sub>ECSA</sub> and achieves the maximum at −1.45 V vs. RHE (Figure 5). This fact may be mainly caused by the competitive hydrogen evolution reaction, which becomes important for negative potentials that decrease the objective FEs.

**Figure 5.** J<sub>ECSA</sub> and FE of CO<sub>2</sub> reduction products on 40 wt % Cu/TiO<sub>2</sub> catalyst at various potentials in the range of −1.05 V to −2.05 V vs. RHE in 0.2 M KI solutions.

To evaluate the stability of 40 wt % Cu/TiO<sub>2</sub> electrocatalysts, potentiostatic electrolysis measurements were carried out in continuous CO<sub>2</sub> electrochemical reduction at the optimal potential over a long time test. Figure 6a displays the J<sub>ECSA</sub> vs. time curve at the corresponding potentials for 25 h. It can be clearly seen that the J<sub>ECSA</sub> is sharply decreased at the beginning of about 25 min, and then keeps steady at a constant value (8.66 mA/cm<sup>2</sup>), indicating its excellent stability as well. Figure 6b shows the comparison of XRD curves for 40 wt % Cu/TiO<sub>2</sub> before and after 25 h reaction, of which the significant characteristic diffraction peaks for Cu NPs were represented by the dash lines. Similarly, there was not any obvious variation in the XRD curves for 40 wt % Cu/TiO<sub>2</sub>, which offers powerful proof of the excellent stability of 40 wt % Cu/TiO<sub>2</sub>. Furthermore, the comparison of SEM images

of 40 wt % Cu/TiO<sub>2</sub> before and after 25 h reaction is presented in Figure S10 (SM). The negligible difference presented in the Figure S10 (SM) demonstrates the superior stability of 40 wt % Cu/TiO<sub>2</sub> samples in a prolonged electrochemical process.



**Figure 6.** (a) The stability test of 40 wt % Cu/TiO<sub>2</sub> sample at the optimal potential  $-1.45$  V vs. RHE. (b) XRD curves of 40 wt % Cu/TiO<sub>2</sub> before and after 25 h CO<sub>2</sub> electrochemical reduction.

### 3. Materials and Methods

#### 3.1. Materials

Cu(NO<sub>3</sub>)<sub>2</sub>·3H<sub>2</sub>O, sodium citrate and hydrazine hydrate (AR grade), TiO<sub>2</sub> (CP grade) were purchased from Sinopharm Chemical Reagent Co. (SCR, Shanghai, China) with 99% purity. Conductive carbon black (C, VXC72R) was purchased from Shanghai Hesun Electrical Co. (Shanghai, China) Nafion® 117 solution (5%) and Nafion® 117 membrane was obtained from Dupont (Wilmington, DE, USA).

#### 3.2. Material Characterization and Product Measurement

Potentiostatic electrolysis and cyclic voltammetry were performed using a CHI 660 C electrochemical station (Shanghai Chenhua Instrument Co. Ltd., Shanghai, China). Crystal-phase XRD patterns of Cu/TiO<sub>2</sub> catalysts were recorded using an Ultima IV X-ray powder diffractometer (Kurary, Tokyo, Japan) equipped with Cu K $\alpha$  radiation ( $k = 1.5406$  Å). The SEM image of the samples was obtained using a Hitachi S-4800 field-emission scanning electron microscope (Tokyo, Japan). The average particle size and different morphologies of the samples were analyzed using a high-resolution Hitachi JEM-2100F transmission electron microscope (Tokyo, Japan). The values for actual Cu loading of the synthesized catalysts were determined on an inductively coupled plasma atomic emission spectroscopy (IRIS Intrepid II XPS, Waltham, MA, USA). Liquid-phase products were analyzed by gas chromatography instrument equipped with a flame ionization detector (SHIMADZU, GC-2014C, Tokyo, Japan). Analysis of the product (Figure S3, SM) and calculation of FE (Equation (S1), SM) are detailed in SM.

#### 3.3. Material Synthesis

Citrate-protecting method was used to obtain different Cu/TiO<sub>2</sub> catalysts. For synthesis of 40 wt % Cu/TiO<sub>2</sub>, Cu(NO<sub>3</sub>)<sub>2</sub>·3H<sub>2</sub>O (0.761 g) was dissolved in the distilled water (60 mL). TiO<sub>2</sub> (0.300 g) was added to the solution and stirred for 40 min. Sodium citrate (1.471 M, 20 mL) dropwise was then added to the solution and stirred. Cu<sup>2+</sup> was reduced by dropwise addition of hydrazine hydrate (50%, 5 mL) with vigorous stirring at room temperature. After gently stirring the solution overnight, the mixture was centrifuged, washed with distilled water, and dried in a vacuum oven at 80 °C for 4 h. Samples with Cu loadings of 5, 10, 20, 60, and 80 wt % were obtained by changing the amount of TiO<sub>2</sub>, while pure Cu NPs was prepared without addition of TiO<sub>2</sub>. Moreover, the prepared of 40 wt % Cu/C was used the same method, just replacing TiO<sub>2</sub> to C.



### 3.4. Electrode Preparation and Electrochemical Test

In electrochemical measurements, X wt % Cu/TiO<sub>2</sub> NPs were painted on a porous carbon paper (Toray, TGP-H60, Tokyo, Japan) to form the working electrodes. Potentiostatic electrolysis was carried out in a gas diffusion electrode cell, which contains a piece of Nafion<sup>®</sup> 117 cation exchange membrane (H<sup>+</sup> form) as a separator, platinum plate electrode as a counter electrode, and saturated calomel electrode (SCE) as a reference electrode. KI aqueous solution (0.2 M) was used as electrolyte and saturated with CO<sub>2</sub> by bubbling for 20 min before the electrolytic experiment. CO<sub>2</sub> was bubbled continuously during the experiment. The electrochemical behavior of the electrodes was tested in a three-electrode electrochemical cell, with a specific volume of catalytic ink coated on the glass carbon electrode (diameter = 2 mm) as the working electrode. A platinum plate electrode was employed as a counter electrode, and SCE was used as reference electrode. All these tests were performed at ambient temperature and pressure. All potentials were converted into the reversible hydrogen electrode (RHE) by the conversion

$$E(\text{RHE}) = E(\text{SCE}) + 0.059 \times \text{pH} + 0.241. \quad (1)$$

## 4. Conclusions

The electroreduction of CO<sub>2</sub> to ethanol under ambient conditions was investigated on Cu/TiO<sub>2</sub> electrodes in a CO<sub>2</sub>-saturated KI aqueous solution. By using TiO<sub>2</sub> as support, small and well-dispersed Cu NPs are loaded on the TiO<sub>2</sub> surface simply, which is beneficial for CO<sub>2</sub> electroreduction. Among various Cu/TiO<sub>2</sub> catalysts, 40 wt % (the optimal mass ratio) shows the highest electrocatalytic activity with the total FE, which is approximately eight-fold higher than the unsupported Cu NPs. The 40 wt % Cu/TiO<sub>2</sub> electrode shows the highest current density compared with other Cu/TiO<sub>2</sub> electrodes under similar experimental conditions. The prepared 40 wt % Cu/TiO<sub>2</sub> with excellent activity for CO<sub>2</sub> conversion is obtained by the high surface area effect and synergistic effect of Cu NPs and TiO<sub>2</sub>. In addition, the 40 wt % Cu/TiO<sub>2</sub> possessed outstanding stability during a 25 h electrochemical process. It is anticipated that the Cu/TiO<sub>2</sub> composite electrocatalyst may provide new insights for transition metal and metal oxide particles applied in CO<sub>2</sub> conversion to useful chemicals.

**Supplementary Materials:** The following are available online at [www.mdpi.com/2073-4344/7/7/220/s1](http://www.mdpi.com/2073-4344/7/7/220/s1). Figure S1. The EDX spectrums of Cu/TiO<sub>2</sub>: (a) 5 wt % Cu/TiO<sub>2</sub>, (b) 10 wt % Cu/TiO<sub>2</sub>, (c) 20 wt % Cu/TiO<sub>2</sub>, (d) 40 wt % Cu/TiO<sub>2</sub>, (e) 60 wt % Cu/TiO<sub>2</sub>, and (f) 80 wt % Cu/TiO<sub>2</sub>. Figure S2. SEM images of (a) pure TiO<sub>2</sub>, (b) 5 wt % Cu/TiO<sub>2</sub>, (c) 10 wt % Cu/TiO<sub>2</sub>, (d) 20 wt % Cu/TiO<sub>2</sub>, (e) 40 wt % Cu/TiO<sub>2</sub>, (f) 60 wt % Cu/TiO<sub>2</sub>, (g) 80 wt % Cu/TiO<sub>2</sub>, and (h) pure Cu NPs. Figure S3. XRD pattern of pure C (black line) and 40 wt % Cu/C (red line). Figure S4. SEM images of pure C (a) and 40 wt % Cu/C (b). Figure S5. TEM images of 40 wt % Cu/C. Figure S6. Gas chromatogram of product solution after a certain time bulk electrolysis of 0.2 M KI solution saturated with CO<sub>2</sub> at a constant cathodic potential. Figure S7. TEM histograms of the Cu particle size distribution from: (a) 5 wt % Cu/TiO<sub>2</sub>, (b) 10 wt % Cu/TiO<sub>2</sub>, (c) 20 wt % Cu/TiO<sub>2</sub>, (d) 40 wt % Cu/TiO<sub>2</sub>, (e) 60 wt % Cu/TiO<sub>2</sub>, and (f) 80 wt % Cu/TiO<sub>2</sub>. Figure S8. CVs in the capacitance current range (from 0.35 to 0.10 V vs. SCE) with (a) 5 wt % Cu/TiO<sub>2</sub>; (b) 10 wt % Cu/TiO<sub>2</sub>; (c) 20 wt % Cu/TiO<sub>2</sub>; (d) 40 wt % Cu/TiO<sub>2</sub>; (e) 60 wt % Cu/TiO<sub>2</sub>; (f) 80 wt % Cu/TiO<sub>2</sub>; (g) pure Cu NPs, and (h) 40 wt % Cu/C in N<sub>2</sub>-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> solution. Figure S9. SEM images of the 40 wt % Cu/TiO<sub>2</sub> electrodes containing: (a) 0.5, (b) 1, (c) 2, (d) 3, (e) 4, and (f) 5 mg/cm<sup>2</sup>. Figure S10. SEM images of 40 wt % Cu/TiO<sub>2</sub> (a) before and (b) after 25 h CO<sub>2</sub> electrochemical reduction. Table S1. The analysis of ECSA and J<sub>ECSA</sub> for ethanol and n-propanol on various Cu/TiO<sub>2</sub> and 40 wt % Cu/C catalysts.

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**Conflicts of Interest:** The authors declare no conflict of interest.

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