

Supporting Information

Raw biogas as feedstock for the OCM process

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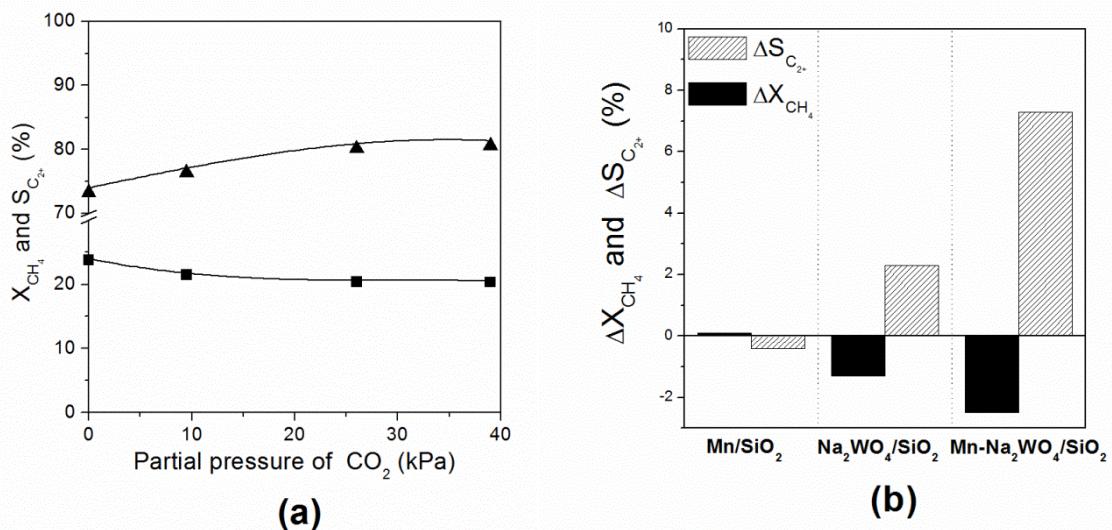


Figure S1. (a) Variation of (■) methane conversion and (▲) selectivity to C_{2+} with partial pressure of CO_2 over Mn-Na₂WO₄/SiO₂ catalyst. (b) Calculated differences between methane conversion (ΔX_{CH_4}) and selectivity to C_{2+} ($\Delta S_{C_{2+}}$) for OCM reaction carried out in presence and in absence of CO_2 over Mn/SiO₂, Na₂WO₄/SiO₂, and Mn-Na₂WO₄/SiO₂ catalysts. Reaction conditions: T = 1073 K; GHSV = 23400 cm³·g⁻¹cat·h⁻¹; m_{cat} = 400 mg; molar ratio of CH₄ : O₂ : He : CO₂ = 3.8 : 1 : X : (4.8 - X), where: X = 4.8, 3.9, 2.3, 1.1; total flow rate 156 cm³·min⁻¹.

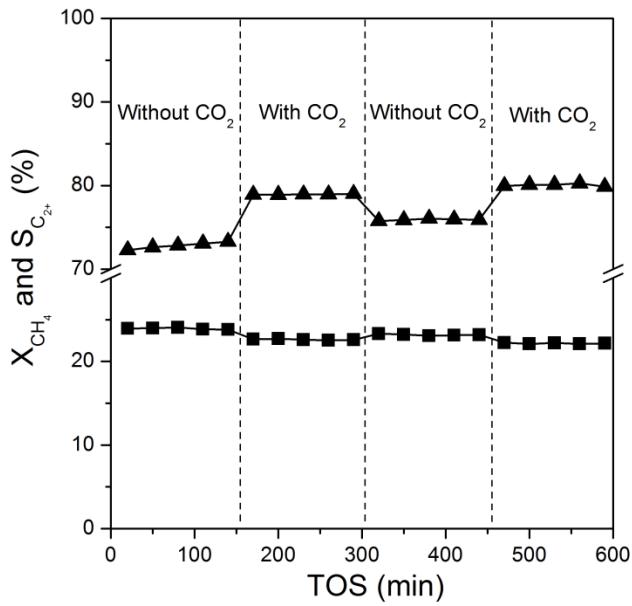


Figure S2. Variation of (■) conversion of CH_4 and (▲) selectivity to C_{2^+} with time-on-stream during repeatable switching on CO_2 during OCM process over the Mn-Na₂WO₄/SiO₂ catalyst. Reaction conditions: $T = 1073$ K; GHSV = $23400 \text{ cm}^3 \cdot \text{g}^{-1}_{\text{cat}} \cdot \text{h}^{-1}$; $m_{\text{cat}} = 400$ mg; molar ratio of $\text{CH}_4 : \text{O}_2 : \text{He} : \text{CO}_2 = 3.8 : 1 : 4.8 : 0$ (without CO_2) and $\text{CH}_4 : \text{O}_2 : \text{He} : \text{CO}_2 = 3.7 : 1 : 1.1 : 3.7$ (with CO_2); total flow rate $156 \text{ cm}^3 \cdot \text{min}^{-1}$.

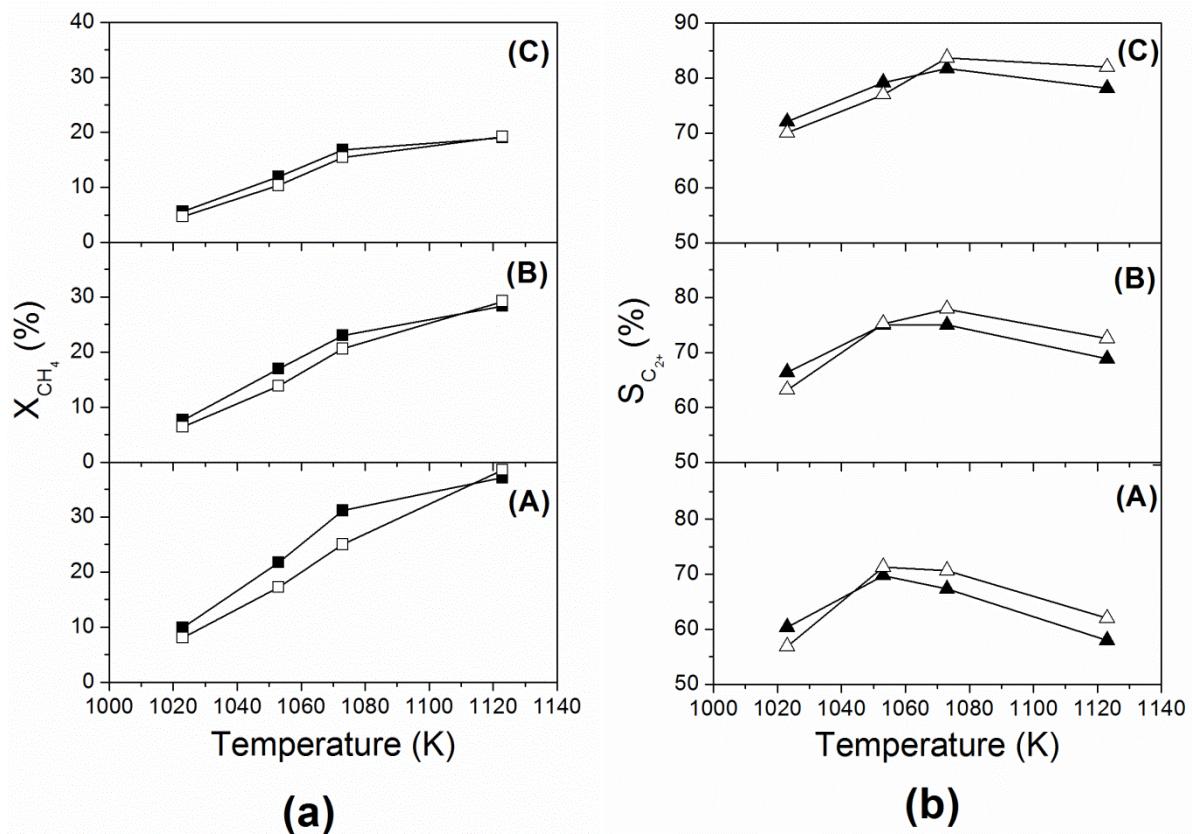


Figure S3. (a) Variation of methane conversion and (b) selectivity to C_{2^+} with temperature in the OCM process carried out with (open symbols) and without (solid symbols) CO_2 over Mn-Na₂WO₄/SiO₂ catalyst. Reaction conditions: GHSV = $23400 \text{ cm}^3 \cdot \text{g}^{-1}_{\text{cat}} \cdot \text{h}^{-1}$; $m_{\text{cat}} = 400$ mg; molar ratio of $\text{CH}_4 : \text{O}_2 : \text{He} : \text{CO}_2$ (A) $3.8 : 1.5 : 0.6 : 3.7$, (B) $3.8 : 1 : 1.1 : 3.7$, and (C) $3.8 : 0.6 : 1.5 : 3.7$; total flow rate $156 \text{ cm}^3 \cdot \text{min}^{-1}$.