Magnesium Effect in K/Co-Mg-Mn-Al Mixed Oxide Catalyst for Direct NO Decomposition

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Figure S1. Dependence of (a) the lattice parameter *a* on Mg/Co molar ratio; (b) the coherent domain size L_c on Mg/Co molar ratio; (c) the coherent domain size L_c on specific surface area for spinel B.



Figure S2. Intensity ratio I (220)/(440) for (a) 0K/Mg*i*, (b) 2K/Mg*i*, (c) 4K/Mg*i*.



Figure S3. Consumed amount of H₂ during TPR-H₂ for: (**a**) the 0K/Mg*i* and 2K/Mg*i* catalysts; (**b**) the *a*K/Mg1 and *a*K/Mg2.2 catalysts.



Figure S4. TPR-H₂ of K/Co-Mg-Mn-Al mixed oxide catalysts: (**a**) the 0K/Mg*i* catalysts; (**b**) the 2K/Mg*i* catalysts; (**c**) the *a*K/Mg1 catalysts; (**d**) the *a*K/Mg2.2 catalysts.



Figure S5. Time on stream dependence of NO conversion. Conditions: 4K/Mg1 catalyst, 1000 ppm NO balanced by N₂ or 1000 ppm NO + 2 mol. % O₂ balanced by N₂, GHSV = 6 L g⁻¹ h⁻¹.



Figure S6. Dependence of NO conversion on potassium desorption activation energies.



Figure S7. Catalytic measurement procedure - stability verification. Conditions: 2K/Mg1 catalyst, 1000 ppm NO balanced by N_2 GHSV = 6 L g⁻¹ h⁻¹.