

# **Supporting Information**

## **Chlorobenzene Oxidation over Phosphotungstic Acid Coated Cerium Oxide: Synergistic Effect of Phosphotungstic and Cerium Oxide and Inhibition Mechanism of Sulfur Dioxide**

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Content including: Eleven pages, two table, and six figures.

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## **Comparison of the performance of HPW/CeO<sub>2</sub> for CB oxidation with other reported catalysts**

The performance of HPW/CeO<sub>2</sub> for CB oxidation is compared with those of other reported catalysts (Table S2). HPW/CeO<sub>2</sub> exhibited excellent activity for CB oxidation, and its CB conversion at 300 °C was approximately 70%, which were higher than those of RuVWTi [1], Mo/VWTi [2], AlVMoTi [3], and Ru/ST [4]. Although the CB conversion of HPW/CeO<sub>2</sub> was slightly lower than those of PMnCe [5], Cu<sub>20</sub>CeAl [6], FeVO<sub>4</sub>-Fe<sub>2</sub>O<sub>3</sub> [7], and MnO<sub>x</sub>-CeO<sub>2</sub> [8], it exhibited higher HCl selectivity at 300 °C with approximately 100%. Therefore, HPW/CeO<sub>2</sub> might be a promising catalyst for Cl-VOCs oxidation.

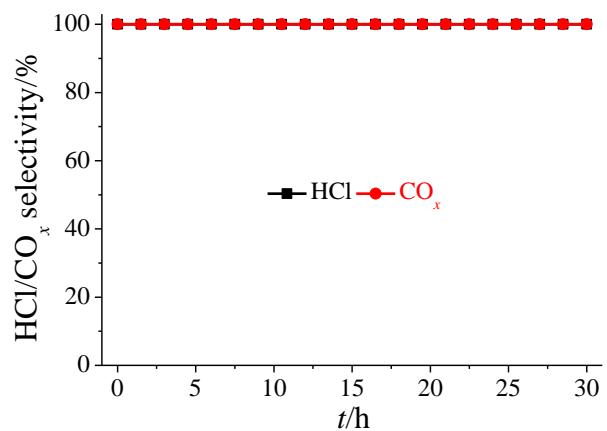
**Table S1** Percentages of Ce and W species on/in HPW/CeO<sub>2</sub>

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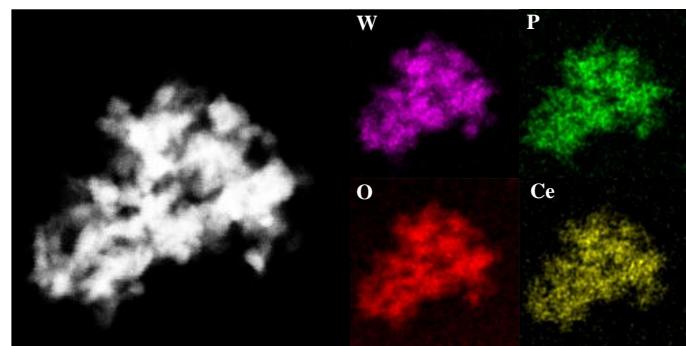
	Ce	W	Ce/W
XPS analysis	21	3.8	5.5
XRF analysis	31	2.0	15.5

**Table S2** Comparison of the performance of HPW/CeO<sub>2</sub> for CB oxidation with other reported catalysts

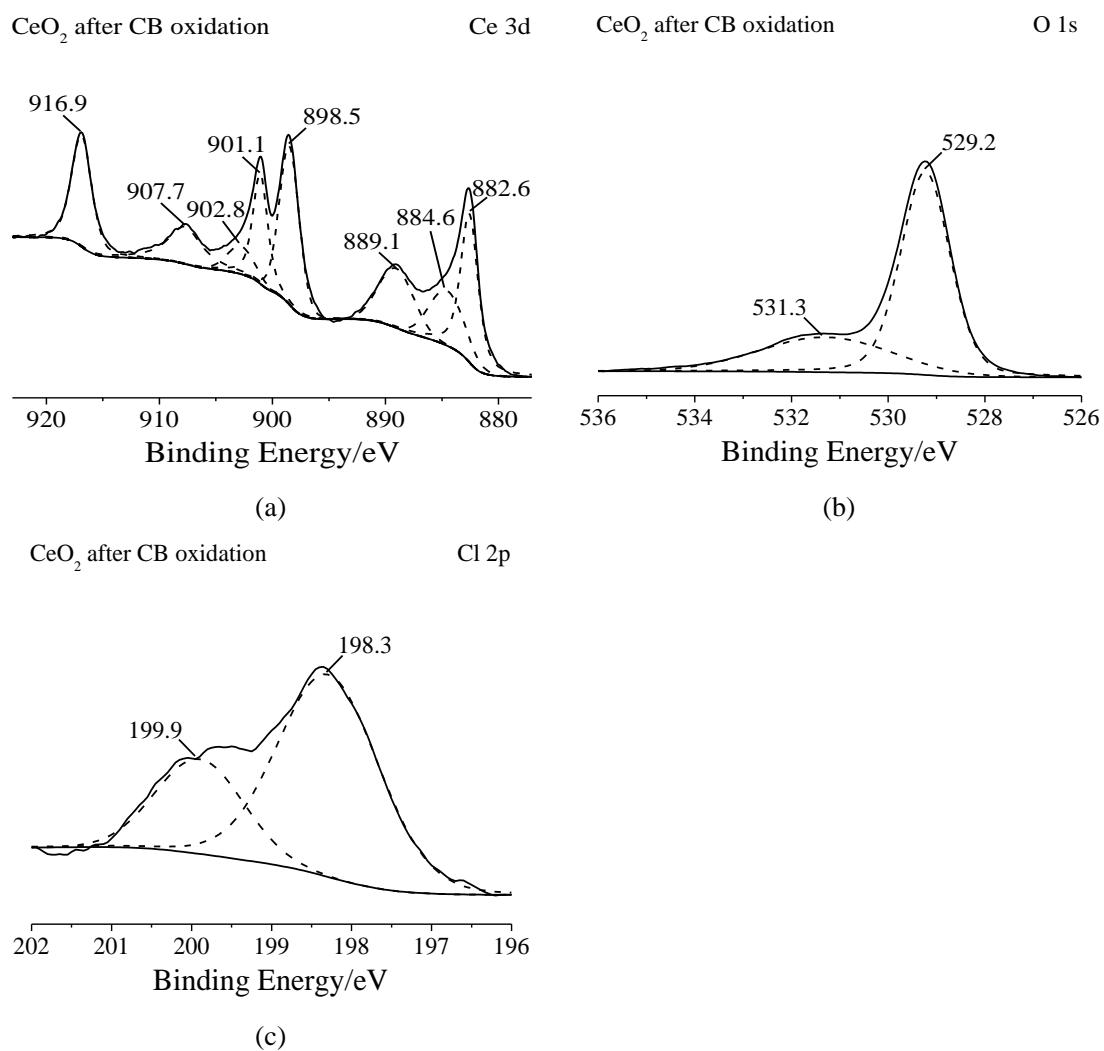
Catalyst	Reaction condition	CB conversion at 300 °C	HCl selectivity at 300 °C
PMnCe [5]	100 ppm CB, 60000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~80%	~90%
Cu <sub>20</sub> CeAl [6]	100 ppm CB, 40000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~85%	~85%
RuVWTi [1]	100 ppm CB, 40000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~68%	~0%
Mo/VTi [2]	100 ppm CB, 30000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~45%	~68%
AlVMoTi [3]	100 ppm CB, 120000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~25%	~70%
FeVO <sub>4</sub> -Fe <sub>2</sub> O <sub>3</sub> [7]	50 ppm CB, 60000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~75%	~75%
Ru/ST [4]	150 ppm CB, 60000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~55%	-
MnO <sub>x</sub> -CeO <sub>2</sub> [8]	150 ppm CB, 60000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~87%	~75%
HPW/CeO <sub>2</sub>	100 ppm CB, 60000 cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup>	~70%	~100%



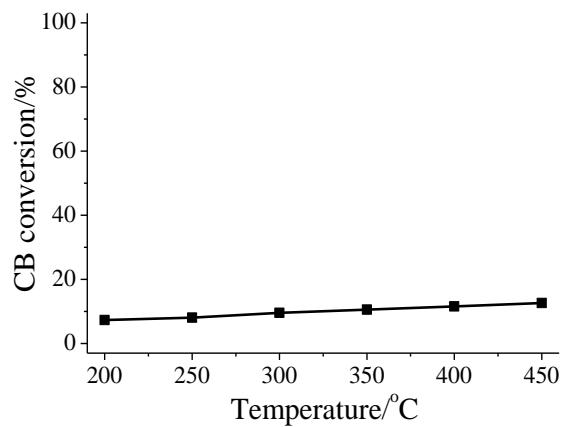
**Figure S1.** Selectivities of HCl and CO<sub>x</sub> during CB oxidation over HPW/CeO<sub>2</sub> at 300 °C for 30 h.



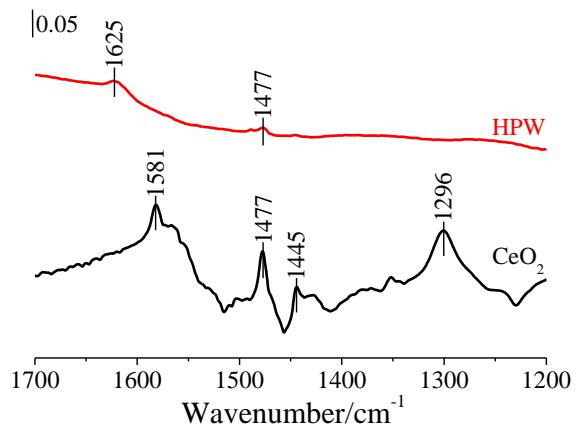
**Figure S2.** STEM image and corresponding EDS mapping of HPW/CeO<sub>2</sub>.



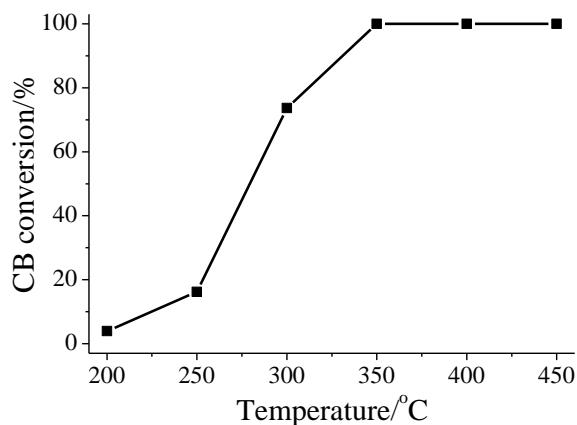
**Figure S3.** XPS spectra of  $\text{CeO}_2$  after CB oxidation in the spectral regions of Ce 3d, O 1s, and Cl 2p.



**Figure S4.** CB conversion efficiency of HPW. Operating conditions: [CB] = 100 ppm, [O<sub>2</sub>] = 5%, catalyst mass = 200 mg, total flow rate = 200 mL min<sup>-1</sup>, and WHSV = 60,000 cm<sup>3</sup> g<sup>-1</sup> h<sup>-1</sup>.



**Figure S5** .*In situ* DRIFTS spectra of passing CB over  $\text{CeO}_2$  and HPW at 100 °C for 30 min.



**Figure S6.** CB conversion efficiency of HPW/CeO<sub>2</sub> under normal flue gas condition at a low WHSV. Operating conditions: [CB] = 100 ppm, [O<sub>2</sub>] = 5%, [SO<sub>2</sub>] = 100 ppm, [H<sub>2</sub>O] = 5%, catalyst mass = 8800 mg, total flow rate = 200 mL min<sup>-1</sup>, WHSV = 15,000 cm<sup>3</sup> h<sup>-1</sup> g<sup>-1</sup>.

## References

1. Song, Z. J.; Peng, Y.; Zhao, X. G.; Liu, H.; Gao, C.; Si, W. Z.; Li, J. H., Roles of Ru on the V<sub>2</sub>O<sub>5</sub>-WO<sub>3</sub>/TiO<sub>2</sub> catalyst for the simultaneous purification of NO<sub>x</sub> and chlorobenzene: A dechlorination promoter and a redox inductor. *ACS Catal.* **2022**, *12*, 11505-11517.
2. Huang, X.; Liu, Z.; Wang, D.; Peng, Y.; Li, J. H., The effect of additives and intermediates on vanadia-based catalyst for multi-pollutant control. *Catal. Sci. Technol.* **2020**, *10*, 323-326.
3. Yu, S. X.; Niu, X. W.; Song, Z. J.; Huang, X.; Peng, Y.; Li, J. H., Improvement of Al<sub>2</sub>O<sub>3</sub> on the multi-pollutant control performance of NO<sub>x</sub> and chlorobenzene in vanadia-based catalysts. *Chemosphere* **2022**, *289*, 133156.
4. Hua, Z. S.; Song, H.; Zhou, C.; Xin, Q.; Zhou, F. Y.; Fan, W. T.; Liu, S. J.; Zhang, X.; Zheng, C. H.; Yang, Y.; Gao, X., A promising catalyst for catalytic oxidation of chlorobenzene and slipped ammonia in SCR exhaust gas: Investigating the simultaneous removal mechanism. *Chem. Eng. J.* **2023**, *473*, 145106.
5. Zhu, X.; Yuan, X.; Song, Z. J.; Peng, Y.; Li, J. H., A dual-balance strategy via phosphate modification on MnO<sub>2</sub>-CeO<sub>2</sub> for NO<sub>x</sub> and chlorobenzene synergistic catalytic control. *Appl. Catal. B: Environ. Energ.* **2024**, *342*, 123364.
6. Yan, X.; Zhao, L. K.; Huang, Y.; Zhang, J. F.; Jiang, S., Three-dimensional porous CuO-modified CeO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> catalysts with chlorine resistance for simultaneous catalytic oxidation of chlorobenzene and mercury: Cu-Ce interaction and structure. *J. Hazard. Mater.* **2023**, *455*, 131585.
7. Yin, R. Q.; Chen, J. J.; Mi, J. X.; Liu, H. Y.; Yan, T.; Shan, L.; Lang, J. Y.; Li, J. H., Breaking the activity-selectivity trade-off for simultaneous catalytic elimination of nitric oxide and chlorobenzene via FeVO<sub>4</sub>-Fe<sub>2</sub>O<sub>3</sub> interfacial charge transfer. *ACS Catal.* **2022**, *12*, 3797-3806.
8. Song, Z. J.; Yu, S. X.; Liu, H.; Wang, Y.; Gao, C. Y.; Wang, Z. S.; Qin, Y. M.; Peng, Y.; Li, J. H., Carbon/chlorinate deposition on MnO<sub>x</sub>-CeO<sub>2</sub> catalyst in chlorobenzene combustion: The effect of SCR flue gas. *Chem. Eng. J.* **2022**, *433*, 133552.