



# Supplementary Materials: Kinetic and Microhydrodynamic Modeling of Fenofibrate Nanosuspension Production in a Wet Stirred Media Mill

Gulenay Guner, Dogacan Yilmaz and Ecevit Bilgili

**Table S1.** Average stirrer power per unit volume  $P_w$ , apparent shear viscosity  $\mu_L$  and density  $\rho_L$  of the milled drug suspensions as well as the calculated microhydrodynamic parameters for the wet milling experiments.

Run no.	$P_w$ (W/m <sup>3</sup> )	$\mu_L$ (mPa·s) <sup>a</sup>	$\rho_L$ (kg/m <sup>3</sup> )	$\theta \times 10^3$ (m <sup>2</sup> /s <sup>2</sup> )	$u_b$ (m/s)	$\nu$ (kHz)	$\sigma_b^{\max}$ (GPa)	$\alpha_b$ (μm)	$a$ (mHz)	$\Pi\sigma_y$ (J <sup>2</sup> /m <sup>6</sup> s)
1	$2.81 \times 10^5$	160	1030	1.28	0.06	2.15	$1.84 \times 10^{-2}$	3.82	15.9	$1.90 \times 10^{12}$
2	$8.65 \times 10^5$	119	1030	4.32	0.10	4.32	1.58	2.41	16.7	$2.73 \times 10^{16}$
3	$4.90 \times 10^5$	118	1030	0.74	0.04	5.60	$1.65 \times 10^{-2}$	3.42	61.7	$4.55 \times 10^{12}$
4	$9.48 \times 10^5$	57.4	1030	2.35	0.08	10.9	1.40	2.13	61.5	$6.05 \times 10^{16}$
5	$1.03 \times 10^6$	144	1020	5.15	0.11	4.31	$2.43 \times 10^{-2}$	5.04	55.5	$1.16 \times 10^{13}$
6	$1.49 \times 10^6$	67.4	1030	12.4	0.18	7.31	1.94	2.97	43.9	$1.07 \times 10^{17}$
7	$1.16 \times 10^6$	81.0	1030	2.50	0.08	10.3	$2.11 \times 10^{-2}$	4.37	185	$2.22 \times 10^{13}$
8	$2.49 \times 10^6$	32.5	1030	9.53	0.16	22.0	1.85	2.82	217	$3.73 \times 10^{17}$
9	$5.31 \times 10^5$	113	1030	1.77	0.07	4.44	$1.97 \times 10^{-2}$	4.07	51.2	$6.17 \times 10^{12}$
10	$1.45 \times 10^6$	57.6	1030	7.29	0.14	9.86	1.75	2.67	64.5	$1.15 \times 10^{17}$
11	$1.15 \times 10^5$	174	1030	0.78	0.04	1.15	$1.67 \times 10^{-2}$	3.46	5.50	$5.83 \times 10^{11}$
12	$5.31 \times 10^5$	123	1030	4.08	0.10	2.88	1.56	2.38	8.57	$1.48 \times 10^{16}$

<sup>a</sup>Taken at the shear rate  $\gamma$  of 1000 1/s.

**Table S2.** Statistics of the estimated MLRM coefficients, including the intercept, correlating the breakage rate constant  $k$  of the  $n$ th-order kinetic model to the microhydrodynamic parameters.

Fit	Parameter			Model			
	Symbol <sup>a</sup>	Coefficient <sup>b</sup>	p-Value	R <sup>2</sup>	Adj R <sup>2</sup>	SSR	p-Value
First-order MLRM, <i>BM</i> <sub>2</sub>	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$1.44 \times 10^{-1}$	$1.76 \times 10^{-1}$	0.828	0.799	0.182	$1.72 \times 10^{-3}$
	$a$ (mHz)	$4.65 \times 10^{-3}$	$1.72 \times 10^{-3}$				
First-order MLRM, <i>BM</i> <sub>3</sub>	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$6.15 \times 10^{-1}$	$3.65 \times 10^{-3}$	0.963	0.948	0.039	$2.61 \times 10^{-4}$
	$\alpha_b$ (μm)	$-1.44 \times 10^{-1}$	$7.80 \times 10^{-3}$				
	$a$ (mHz)	$4.85 \times 10^{-3}$	$1.08 \times 10^{-4}$				
First-order MLRM, <i>BM</i> <sub>4</sub>	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$5.49 \times 10^{-1}$	$1.96 \times 10^{-2}$	0.969	0.945	0.033	$1.82 \times 10^{-3}$
	$\alpha_b$ (μm)	$-1.23 \times 10^{-1}$	$4.76 \times 10^{-2}$				
	$a$ (mHz)	$4.43 \times 10^{-3}$	$2.79 \times 10^{-3}$				
First-order MLRM, <i>BM</i> <sub>5</sub>	$\Pi\sigma_y$ (×10 <sup>-16</sup> J <sup>2</sup> /m <sup>6</sup> s)	$3.66 \times 10^{-3}$	$4.46 \times 10^{-1}$	0.969	0.927	0.033	$1.36 \times 10^{-2}$
	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$5.43 \times 10^{-1}$	$1.53 \times 10^{-1}$				
	$\sigma_b^{\max}$ (GPa)	$1.37 \times 10^{-3}$	$9.82 \times 10^{-1}$				
	$\alpha_b$ (μm)	$-1.21 \times 10^{-1}$	$1.72 \times 10^{-1}$				
	$a$ (mHz)	$4.44 \times 10^{-3}$	$1.28 \times 10^{-2}$				
Second-order MLRM, <i>BM</i> <sub>4</sub>	$\Pi\sigma_y$ (×10 <sup>-16</sup> J <sup>2</sup> /m <sup>6</sup> s)	$3.55 \times 10^{-3}$	$6.24 \times 10^{-1}$	0.975	0.956	0.026	$1.16 \times 10^{-3}$
	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$5.50 \times 10^{-1}$	$1.00 \times 10^{-2}$				
	$\alpha_b$ (μm)	$-1.56 \times 10^{-1}$	$8.26 \times 10^{-3}$				
	$a$ (mHz)	$8.05 \times 10^{-3}$	$2.64 \times 10^{-2}$				
Second-order MLRM, <i>BM</i> <sub>5</sub>	$a^2$ (mHz <sup>2</sup> )	$-1.35 \times 10^{-5}$	$2.39 \times 10^{-1}$	0.995	0.989	0.005	$8.36 \times 10^{-4}$
	Intercept (μm <sup>(n-1)min<sup>-1</sup>)</sup>	$3.65 \times 10^{-1}$	$1.98 \times 10^{-2}$				
	$\alpha_b$ (μm)	$-1.16 \times 10^{-1}$	$9.76 \times 10^{-3}$				
	$a$ (mHz)	$9.23 \times 10^{-3}$	$4.92 \times 10^{-3}$				
$\Pi\sigma_y$ (×10 <sup>-16</sup> J <sup>2</sup> /m <sup>6</sup> s)		$7.85 \times 10^{-3}$	$3.85 \times 10^{-2}$				

	$a^2$ (mHz <sup>2</sup> )	-2.28x10 <sup>-2</sup>	2.70x10 <sup>-2</sup>					
MLRM with interaction terms, BM <sub>4</sub>	<b>Intercept</b> ( $\mu\text{m}^{(n-1)}\text{min}^{-1}$ )	7.11x10 <sup>-2</sup>	1.37x10 <sup>-1</sup>					
	$a$ (mHz)	1.63x10 <sup>-2</sup>	1.68x10 <sup>-3</sup>					
	$\alpha_b a$ ( $\mu\text{m}\cdot\text{mHz}$ )	-2.81x10 <sup>-3</sup>	3.91x10 <sup>-3</sup>	0.987	0.978	0.013		2.3x10 <sup>-4</sup>
	$a\Pi\sigma_y$ ( $\times 10^{-16}$ mHz J <sup>2</sup> /m <sup>6</sup> s <sup>2</sup> )	-7.35x10 <sup>-5</sup>	2.98x10 <sup>-2</sup>					
MLRM with interaction terms, BM <sub>5</sub>	<b>Intercept</b> ( $\mu\text{m}^{(n-1)}\text{min}^{-1}$ )	4.26x10 <sup>-2</sup>	6.40x10 <sup>-2</sup>					
	$a$ (mHz)	1.25x10 <sup>-2</sup>	1.32x10 <sup>-3</sup>					
	$\sigma_b^{\max} a$ (GPa.mHz)	2.18x10 <sup>-3</sup>	1.33x10 <sup>-2</sup>	0.999	0.997	0.001		1.06x10 <sup>-4</sup>
	$\alpha_b a$ ( $\mu\text{m}\cdot\text{mHz}$ )	-1.91x10 <sup>-3</sup>	4.16x10 <sup>-3</sup>					
	$a\Pi\sigma_y$ ( $\times 10^{-16}$ mHz J <sup>2</sup> /m <sup>6</sup> s <sup>2</sup> )	-1.45x10 <sup>-4</sup>	2.70x10 <sup>-3</sup>					

<sup>a</sup>Statistically insignificant ( $p$ -value > 0.01) parameters are **bolded**.  $\Pi\sigma_y$  is treated as a single parameter as  $\sigma_y$  is a constant.

<sup>b</sup>The coefficients have the units that make the MLRM equation dimensionally homogeneous.

## S1. Sample MATLAB code for the microhydrodynamic calculations

### Main.m

```

global Pw      % Power applied to the stirrer per unit volume, W/(m^3)
global Db      % Milling bead diameter, m
global c       % solids volumetric concentration
global g0      % radial distribution function
global k       % restitution coefficient for bead-bead collisions
global Rdiss0 % dissipation coefficient taking into account squeezing the liquid film
global ub      % average particle oscillation velocity, m/s
global v       % frequency of the single bead oscillation, 1/s
global Em      % non-dimensional particle-particle gap thickness at which the lubrication force stops continuous
increase and becomes a constant
global visliq   % dynamic viscosity of the equivalent liquid to be measured from viscometer, kg/ms
global dliq     % density of the equivalent liquid, kg/(m^3)
globaldbeads   % density of the media beads, kg/(m^3)
global K        % empirical correlation coefficient for correction for large Reynolds numbers
global Eht      % granular energy balance for a well-mixed slurry in the mill
global Rb      %m radius of bead
global etab    %Poisson ratio of the bead
global Yb      %Young modulus of the bead
global Rp      %radius of the particle
global eps     %volume fraction of the drug in the suspension
global Ystar    %reduced elastic modulus of the beads
global Yp      %Young modulus of the particle
global etap    %Poisson ratio of the particle
global gamma
global clim    %maximum bead concentration

```

```
y0=[1e-6]; % case with 1 unknown, 1 equation, the initial guess was gotten from Eskin's paper at 3200rpm
```

```
% Solver based on medium scale Gauss-Newton optimization with quadcubic line search
```

```
% Do NOT change the solver parameters below:
```

```
options=optimset('Diagnostics','on','Display','iter','Largescale','off','TolX',[1e-6],'TolFun',[1e-10],...
'MaxIter',[2e4],'MaxFunEvals',[2e4],'TolCon',[1e-10],'DiffMaxChange',[1e-8],'DiffMinChange',[1e-10]);
[y,fval,exitflag,output]=fsolve(@Equationset,y0,options);
```

```
% y(1) is equal to the granular temperature theta
```

```
ub=sqrt((8/pi)*y(1)); %m/s
```

```
V=((24*c*g0)/Db)*sqrt(y(1)/pi); %Hz
```

```
v=V/1000 ; %KHz
```

```

Fbn=1.96*(Yb/(1-etab^2))^(2/5)*(dbeads^(3/5))*(Rb^2)*(y(1)^(3/5));
Alphab=(0.75*(1-etab^2)/Yb*Rb*Fbn)^(1/3); %m
alphab=Alphab*10^6; %micrometer
sigmabmax=3*Fbn/(2*pi*(Alphab)^2)/10^9; %GPa
p=0.97*c/(1-c)*((dbeads*(1-etab^2)/Yb)^(2/5))*(y(1)^(2/5))*Rp/Rb;
A=p*V; %Hz
a=A*1000; %mHz
pisigmaA=2.23*(c^2)*2*g0/((pi^(5/2))*eps);
pisigmaB=(Yb/(1-etab^2))^(18/15);
pisigmaC=((Ystar/Yp)^gamma);
pisigmaD=(dbeads^(4/5))/Rb^2*(y(1)^(13/10));
pisigma=2.23*(c^2)*2*g0/((pi^(5/2))*eps)*((Yb/(1-
etab^2))^(18/15))*((Ystar/Yp)^gamma)*(dbeads^(4/5))*Rp/Rb^2*(y(1)^(13/10)); %(J2/m6.s)
granulartemperature=y; %m2/s2

% END OF MAIN PROGRAM %
g0
granulartemperature %m2/s2
ub %m/s
v %KHz
sigmabmax %GPa
alphab %(micrometer)
a %mHz
pisigma %J2/m6.s)
format shortg
Result=[g0; y(1); ub; v; sigmabmax; alphab; a; pisigma]

```

### Equationset.m

```

global Pw      % Power applied to the stirrer per unit volume, W/(m^3)
global Db      % Milling bead diameter, m
global c       % solids volumetric concentration
global g0      % radial distribution function
global k       % restitution coefficient for bead-bead collisions
global Rdiss0 % dissipation coefficient taking into account squeezing the liquid film
global ub      % average particle oscillation velocity, m/s
global v       % frequency of the single bead oscillation, 1/s
global Em      % non-dimensional particle-particle gap thickness at which the lubrication force stops continuous
increase and becomes a constant
global visliq  % dynamic viscosity of the equivalent liquid to be measured from viscometer, kg/ms
global dliq    % density of the equivalent liquid, kg/(m^3)
global dbeads  % density of the media beads, kg/(m^3)
global K       % empirical correlation coefficient for correction for large Reynolds numbers
global Eht     % granular energy balance for a well-mixed slurry in the mill
global Rb      %m redius pf bead
global etab   %Poisson ratio of the bead
global Yb     %Young modulus of the bead
global Rp     %radius of the particle 0min
global eps    %volume fraction of the drug in the suspension
global Ystar   %reduced elastic modulus of the beads
global Yp     %Young modulus of the particle
global etap   %Poisson ratio of the particle

```

```

global gamma
global clim %maximum bead concentration
Pw=822916.6667; % please get from data % Power applied to the stirrer per unit volume, W/(m^3)
Eht=0; % please get from data % granular energy balance for a well-mixed slurry in the mill
%other parameters
c= 0.55;% please get from data % solids volumetric concentration i.e (50 ml bead powder *void fraction)/total volume of chamber
k= 0.76; % particle-particle restitution coef. ref. Tatsumi see coefficient of restitution paper 0.76 for YSZ, 0.9 for CPS
Em=0.003; % non-dimesnional particle-particle gap thickness
visliq=0.048390987;%kg/(m·s) Please measure for each sample
dliq= 1026; %kg/(m^3) Please measure for each sample
dbeads=6000;%kg/(m^3)% measured
Db= 0.000405; %m please include the diameter of the bead with different sizes.
Rb= Db/2; %m radius of the bead
etab=0.2; %poisson ratio of the bead (0.2 for YSZ 0.33 for CPS)
Yb=200*10^9; %Pa Young modulus of the bead (200 GPa for YSZ, 1.5 GPa for CPS)
Rp=13.723*10^-6; %0 min (m)radius of the particle
eps=0.07444882; %volume fraction of the drug in the suspension
Ystar=((1-etab^2)/Yb+(1-etab^2)/Yp)^(-1); %reduced elastic modulus of the beads
Yp=8.93*10^9; %Pa Young modulus of the particle
etap=0.3; %Poisson ratio of the particle
gamma=1/3;
clim=0.63;
% calculate the empirical correlation coefficient
K=(0.096+0.142*c^0.212)/((1-c)^4.454);

%Calculate the radial distribution function
g0=(1-(c/clim)^(1/3))^(-1)

%Dissipation Coefficient
Rdiss=1+3*((0.5*c)^0.5)+(135/64)*c*log(c)+11.26*c*(1-5.1*c+16.57*(c^2)-21.77*(c^3))-log(Em)*g0*c;
Re=Db*dliq*(y(1)^0.5)/visliq;

Rdiss=Rdiss0+Re*K;
nb=6*c/(pi*(Db^3));
epsvis= 9*pi*visliq*Db*nb*y(1)*Rdiss;
epscoll=(12/(Db*sqrt(pi)))*(1-(k^2))*(c^2)*dbeads*g0*(y(1)^1.5);
func1=Pw-epsvis-epscoll-Eht;

```

## S2. R code for the subset selection algorithm

```

for (i in c(1:4)) {
  print(paste("running variable", i))
  bestAdjR=0
  bestRSS=Inf
  regnames=combn(colnames(data,!names(data) %in% c('k'))),i)
  for (j in c(1:length(regnames[1,]))) {
    model=paste0("k~",paste("0",paste(regnames[,j],collapse="+"),sep = "+"))
    #model=paste0("k~",paste(regnames[,j],collapse="+"))
    fit=lm(as.formula(model),data = data)
    adjR=summary(fit)$adj.r.squared
    RSS=anova(fit)[["Residuals", "Sum Sq"]]
  }
}

```

```
R2=summary(fit)$r.squared
Pvalue=summary(fit)$coefficients[,4]
Pmodel=lmp(fit)
if (adjR>=bestAdjR) {
    bestAdjR=adjR
    bestRSS=RSS
    bestModel=model
    bestR2=R2
    bestcoef=coef(fit)
    bestPvalue=Pvalue
    bestfit=fit
    bestPmodel=Pmodel
}
print("best model")
print("best coef")
print(formatC(bestcoef, format="e", digits = 2))
print("best Pvalue")
print(formatC(bestPvalue, format="e", digits = 2))
print("Best R2")
print(bestR2)
print("adj r")
print(bestAdjR)
print("bestRSS")
print(bestRSS)
print("bestPmodel")
print(formatC(bestPmodel, format="e", digits = 2))
}
```