

Microbial Recycling of Bioplastics via Mixed-Culture Fermentation of Hydrolyzed Polyhydroxyalkanoates into Carboxylates

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Table S1. Typical material properties of PHBV [1].

| Item | Data | Test Standard |
|----------------------------------|-----------|--|
| Specific gravity | 1.25 | ISO 1183-3:1999 |
| Melt flow index | 12-25 | ISO 1133:1997, g/10 min, 190 °C, 2.16 kg |
| Yield stress (MPa) | 31-36 | ISO 527-1:1993 |
| Tensile strength (MPa) | 39 | ISO 527-1:1993 |
| Elongation at break (%) | 3.8 | ISO 527-1:1993 |
| Young's modulus (MPa) | 160–2100 | ISO 527-1:1993 |
| Flexural modulus (MPa) | 2200–2900 | ISO 178:1993 |
| Vicat softening temperature (°C) | 166 | ISO 306:1994 |
| Izod impact (J/m) | 55–60 | ISO 180:2000 |
| Heat deflection temperature (°C) | 157–165 | ISO 75-2:2003 |
| DSC melting point (°C) | 175–180 | ISO 11357-3:1999 |

Table S2. Compositions of stock solutions used to prepare medium for mixed culture fermentation of PHBV.

| Compound | Concentration (g/L) | Dilution Factor |
|---|---------------------|-----------------|
| Stock solution I-Minerals | | |
| NH ₄ H ₂ PO ₄ | 180 | 50× |
| MgCl ₂ ·6H ₂ O | 16.5 | |
| MgSO ₄ ·7H ₂ O | 10 | |
| Stock solution II-Minerals | | |
| CaCl ₂ ·2H ₂ O | 10 | 50× |
| KCl | 7.5 | |
| Trace metals | | |
| FeCl ₂ ·4H ₂ O | 30.0 | 2000× |
| MnCl ₂ ·4H ₂ O | 0.6 | |
| H ₃ BO ₃ | 6.0 | |
| CoCl ₂ ·6H ₂ O | 4.0 | |
| CuCl ₂ ·H ₂ O | 0.2 | |
| NiCl ₂ ·6H ₂ O | 0.4 | |
| ZnSO ₄ ·7H ₂ O | 2.0 | |
| Na ₂ MoO ₄ ·2H ₂ O | 0.6 | |
| Na ₂ SeO ₃ | 0.2 | |
| EDTA | 12.4 | |
| Vitamins | | |
| Biotin | 0.106 | 1000× |
| Folic acid | 0.005 | |
| Pyridoxal-HCl | 0.0025 | |
| Lipoic acid | 0.015 | |
| Riboflavin | 0.0125 | |
| Thiamine-HCl | 0.266 | |
| Ca-D-pantothenate | 0.413 | |
| Cyanocobalamin | 0.0125 | |
| P-aminobenzoic acid | 0.0125 | |
| Nicotinic acid | 0.0125 | |
| Supplements | | |
| Yeast extract | 0.1 | |
| HCl | 1 M | |
| KOH | 4 M | |

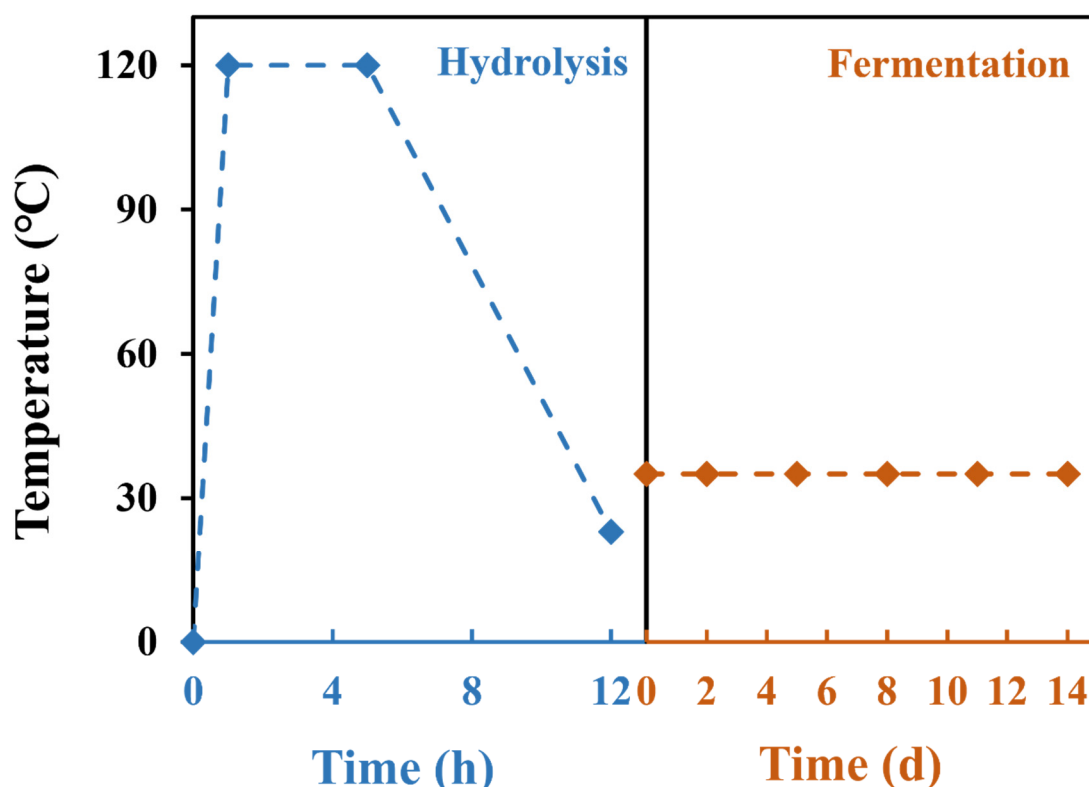


Figure S1. Temperature changes in thermal hydrolysis and fermentation process.

Table S3. Total Chemical Oxygen Demand (TCOD).

| Material | Test | COD (g/kg) | Average COD (g/kg) |
|--------------|------|------------|--------------------|
| PHBV (2% HV) | A | 1570 | 1588 |
| | B | 1605 | |

a. To determine the chemical oxygen demand z. B. according to DIN 38409/German standard procedure H41. b. Digestion in the aluminum heating block with precise temperature control. c. Heat samples to 148 °C in less than 10 min.

Calculations S1. Estimated COD recovery for a potential PHA to PHA recycling process

The PHA to PHA recovery percentage was calculated according:

$$PHA_{recovery} = (Yield_{PHA\ hydrolysis} - Yield_{biomass}) * Yield_{PHA\ from\ VFA} * 100\% \quad [\%] \quad (S1)$$

where by the following targets or experimental findings were used:

Yield_{crotonate+3-HB from PHA} = 1 [g crotonate+3HB-COD/g PHA-COD];

Yield_{PHA from VFA}: 0.61-0.68 [g PHA-COD/g VFA-COD] could be produced in a synthetic or nutrient-poor stream [2];

Yield_{biomass}: a typical 0.05 biomass yield for microbial growth [3] [g biomass-COD/g VFA-COD];

So the overall recovery percentage of PHA was estimated to be 58% (= (1-0.05)*0.61*100%) to 65% (= (1-0.05)*0.68*100%).

Calculations S2. The overall yields of VFAs from PHA hydrolysis

$$Yield_{VFA} = \frac{C_{VFA}}{C_{original\ PHA}} * (COD_{hydrolysates} / COD_{start\ of\ fermentation}) \quad [g\ VFA / g\ PHA] \quad (S2)$$

COD_{hydrolysates}: 16.3 [g COD/L];

COD_{start of fermentation}: 4 [g COD/L];

So the Yield acetate was $0.07 = (1.71/100) * (16.3/4)$ [g acetate/g PHA], and Yield butyrate was $0.049 = (1.20/100) * (16.3/4)$ [g butyrate/g PHA].

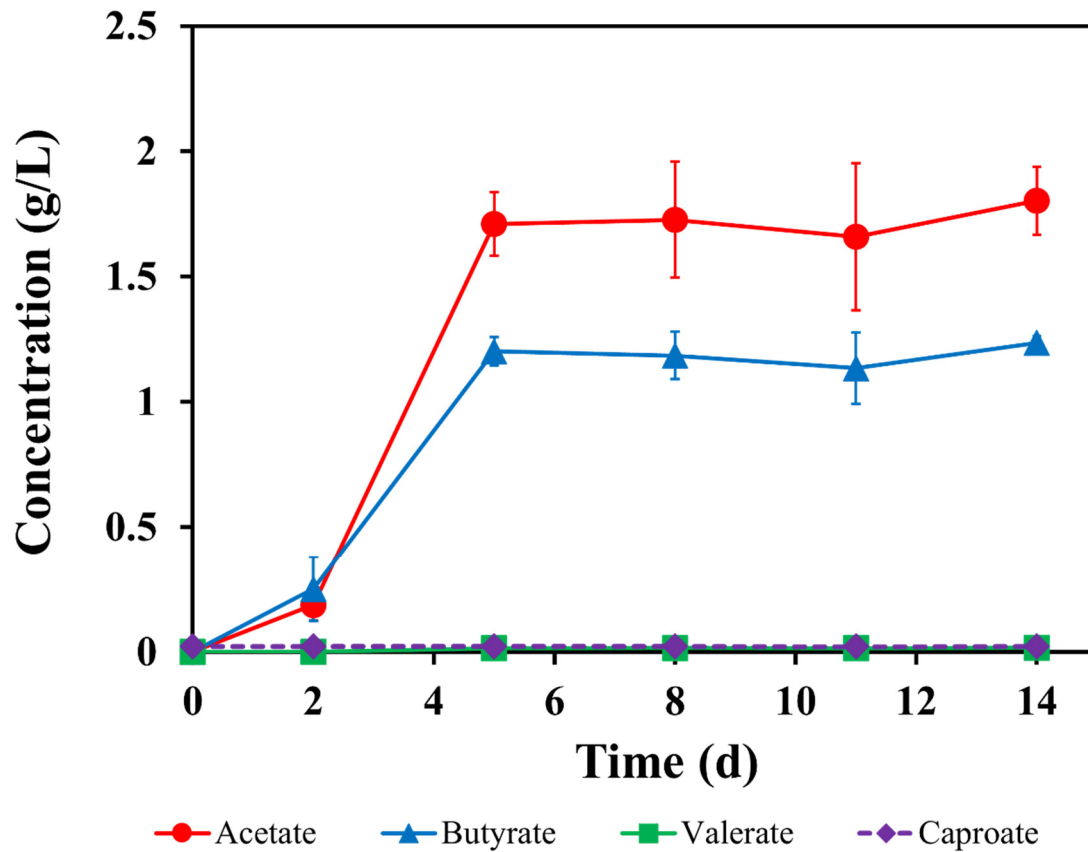


Figure S2. Volatile fatty acids distribution during mixed culture fermentation of PHA. The visible error bars represent the standard deviation of the triplicate experiments.

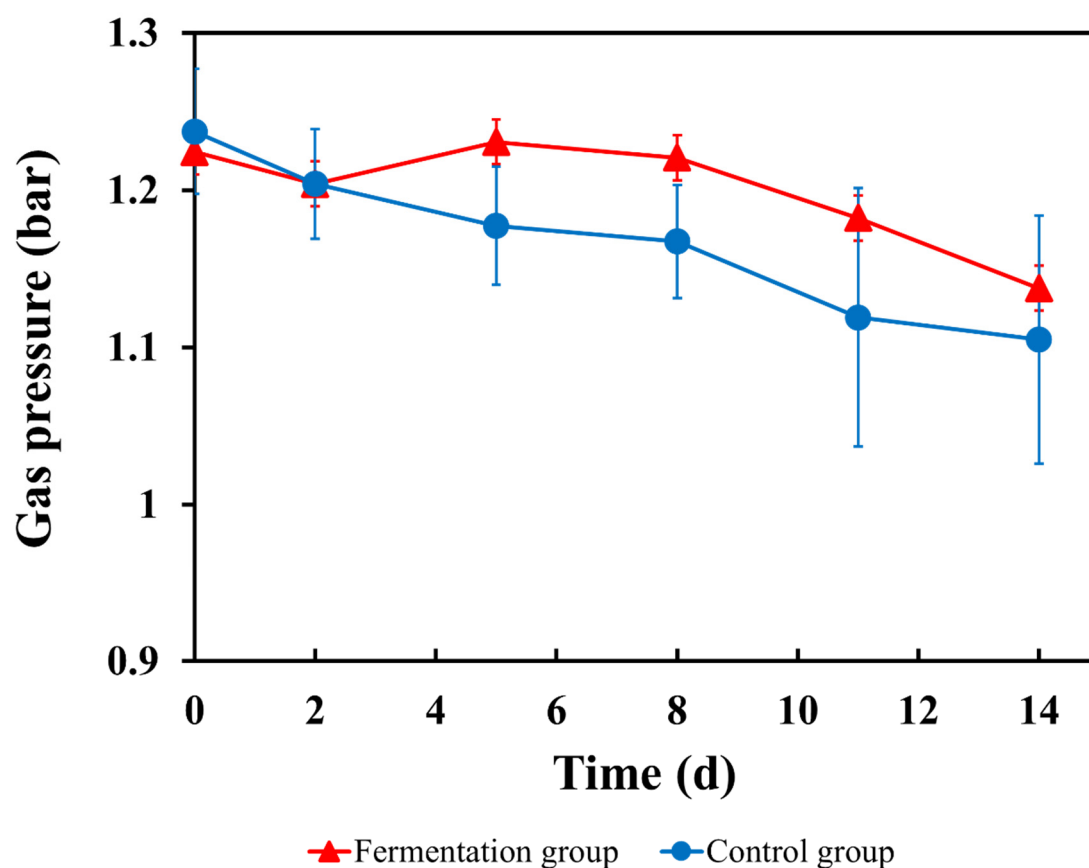


Figure S3. Gas pressure measured during mixed culture fermentation of PHA. The visible error bars represent the standard deviation of the triplicate experiments.



Figure S4. Carboxylates measurement in a gas chromatograph (GC) of selected samples. **Note:** A is the standard curve in high-concentration solution; B is the curve of the start experiment of the control group; C is the curve of the end experiment of the control group; D is the curve of the start experiment of the fermentation group; E is the curve of the end experiment of fermentation group.

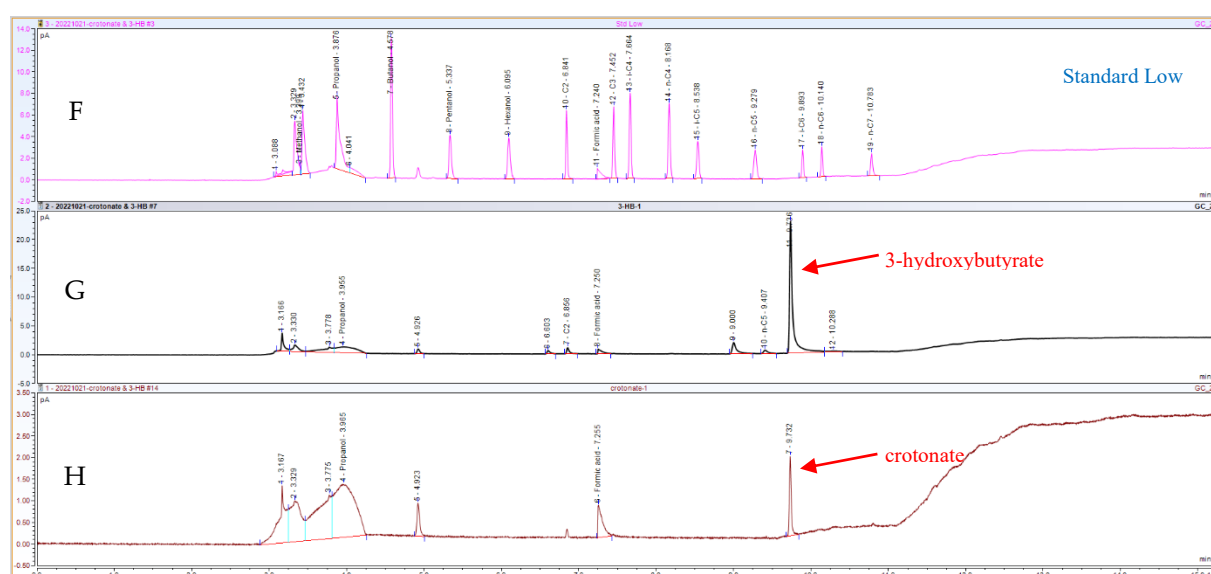


Figure S5. Crotonate and 3-hydroxybutyrate (3-HB) measurement in a gas chromatograph (GC). **Note:** F is the standard curve in low-concentration solution; G is the curve of 500 mg/L 3-hydroxybutyrate; H is the curve of 10 mg/L crotonate. G and H are selected from duplicate samples.

Compared with the retention time of the peaks of quantitatively measured crotonate and 3-hydroxybutyrate in groups G and H, here the peaks showed with red rows in groups B–D indicating that there were some crotonate and/or 3-hydroxybutyrate produced from PHBV hydrolysis, and in group E, no peak at the same time as showed in B to D, this can qualitatively identify the present crotonate and/or 3-hydroxybutyrate and the conversion of them into acetate and butyrate (both peaks of these two carboxylates increased apparently).

Table S4. Compositions of gas in headspace measured at the end of fermentation.

| Group | O ₂ (%) | N ₂ (%) | CO ₂ (%) | H ₂ (%) | CH ₄ (%) |
|----------------|--------------------|--------------------|---------------------|--------------------|---------------------|
| Fermentation 1 | 0.22 | 84.7 | 13.7 | 0.010 | 0 |
| Fermentation 2 | 0.21 | 86.3 | 12.7 | 0.588 | 0 |
| Fermentation 3 | 0.23 | 85.7 | 13.0 | n.a. | 0 |
| Control 1 | 0.17 | 96.9 | 10.1 | n.a. | 0 |
| Control 2 | 0.17 | 90.4 | 8.96 | n.a. | 0 |
| Control 3 | 0.21 | 90.5 | 8.66 | n.a. | 0 |

Note: n.a. means ‘not available’.

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