



Efficient Removal of Cu(II), Zn(II), and Cd(II) from Aqueous Solutions by a Mineral-Rich Biochar Derived from a Spent Mushroom (*Agaricus bisporus*) Substrate

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Supplementary Materials and Method

Mathematical Models for Adsorption Kinetics and Isotherm

The adsorption capacity of spent Agaricus bisporus substrate biochar was calculated according to Equation (1):

$$Q_e = (C_0 - C_e) \cdot \frac{V}{m} \tag{1}$$

where Qe (mg·g⁻¹) is the adsorption capacity of biochar at equilibrium; V (L) is the solution volume; C0 (mg·L⁻¹) is the initial heavy metal (Cd(II) or Cu(II) or Zn(II)) concentration; C_e is the Cd(II) or Cu(II) or Cu(II) or Cn(II) concentration after time adsorption, and m (g) is the weight of biochar samples.

The kinetics of Cd(II) or Cu(II) or Zn(II) sorption were fitted to the pseudo-first order (PF-order model, Equation (2)), pseudo-second order (PS-order model, Equation (3))

$$Q_t = Q_e(1 - e^{-k_1 t})$$
 (2)

$$Q_{t} = \frac{k_{2}Q_{e}^{2}t}{1+k_{2}Q_{e}t}$$
(3)

where Qt (mg·g⁻¹) is the sorbed amount at time t; k1 (h⁻¹) and k2 (g·mg⁻¹·h⁻¹) are the apparent first-order and second-order sorption rate constants, respectively.

The Freundlich isotherm model (Equation (4)) and Langmuir isotherm model (Equation (5)) was used to simulate Cd or Cu or Zn sorption to biochars,

$$Q_e = k_F C_e^{\ n} \tag{4}$$

$$Q_e = \frac{Q_{max}k_LC_e}{1+k_LC_e}$$
(5)

Qmax (mg·g⁻¹) is the maximum adsorption capacity; KL (L·mg⁻¹) is the Langmuir constant related to the adsorption affinity; Kf (mg·g⁻¹) is the Freundlich constant related to the adsorption capacity; n is the adsorption strength.

Biochar	Fe	Mn	Al	Zn (mg·g ⁻¹)	Cu	Cd	Pb
SAS350	3.233	0.167	14.60	0.165	0.042	N.D	0.014
SAS450	3.173	0.165	15.91	0.146	0.039	N.D	0.009
SAS550	2.997	0.159	16.13	0.145	0.037	N.D	0.007
SAS650	3.270	0.163	16.49	0.140	0.036	N.D	0.004
SAS750	3.434	0.163	17.32	0.135	0.034	N.D	0.003

Table S1. The concentrations of metals in biochars derived from spent Agaricus Bisporus substrate.

SAS350-SAS750 were the biochars derived from spent Agaricus bisporus substrate (SAS) at 350–750 °C. N.D.: Not detected (below the detection limit).

Table S2. Pseudo-first (PF) order and pseudo-second (PS) order model parameters for the Cu(II) or Zn(II) or Cd(II) sorption onto SAS-derived biochars produced at 350, 550, and 750 °C.

D's deserve		PF Order Model			PS Order Model			
	Biochars	Qe(mg·g ⁻¹)	k ₁ (1 h⁻¹)	R ²	Qe (<i>mg</i> · <i>g</i> ^{−1})	k₂ (g mg ⁻¹ h ⁻¹)	R ²	
	SAS350	28.6 ± 0.98	0.691 ± 0.098	0.963	30.4 ± 0.84	0.033 ± 0.005	0.980	
Cu	SAS550	16.0 ± 0.38	1.61 ± 0.164	0.974	16.9 ± 0.11	0.141 ± 0.006	0.998	
	SAS750	65.2 ± 2.54	0.547 ± 0.080	0.956	70.3 ± 1.82	0.010 ± 0.001	0.985	
Zn	SAS350	21.2 ± 0.81	0.987 ± 0.149	0.951	22.7 ± 0.46	0.059 ± 0.006	0.988	
	SAS550	10.9 ± 0.53	1.55 ± 0.355	0.911	11.7 ± 0.34	0.171 ± 0.030	0.973	
	SAS750	52.4 ± 1.20	0.208 ± 0.017	0.990	59.2 ± 0.70	0.004 ± 0.001	0.998	
Cđ	SAS350	29.6 ± 0.81	0.308 ± 0.036	0.972	32.7 ± 0.60	0.013 ± 0.001	0.992	
	SAS550	12.9 ± 0.49	0.765 ± 0.147	0.913	13.47 ± 0.35	0.080 ± 0.013	0.971	
	SAS750	62.3 ± 1.89	0.524 ± 0.074	0.956	66.72 ± 1.23	0.012 ± 0.001	0.988	

Table S3. Langmuir and Freundlich isotherm parameters for Cu(II) or Zn(II) or Cd(II) sorption onto SAS-derived biochars produced at 350, 550, and 750 °C.

		La	ngmuir Model		Freundlich Model			
	Biochars	Qe(mg·g ⁻¹)	<i>K</i> ^L (mg L ⁻¹)	R^2	<i>K</i> _F (mg ^{1−n} g ^{−1} L ^{−n})	n	R^2	
	SAS350	28.9 ± 2.11	0.150 ± 0.058	0.927	8.27 ± 0.46	3.623 ± 0.181	0.995	
Cu	SAS550	11.6 ± 0.92	2.089 ± 1.39	0.860	6.37 ± 0.37	6.509 ± 0.618	0.986	
	SAS750	68.1 ± 4.85	0.640 ± 0.339	0.890	37.3 ± 1.73	7.001 ± 0.601	0.987	
Zn	SAS350	25.6 ± 1.82	0.138 ± 0.045	0.954	6.64 ± 0.27	3.276 ± 0.114	0.998	
	SAS550	16.9 ± 1.79	0.034 ± 0.010	0.970	1.82 ± 0.14	2.293 ± 0.100	0.996	
	SAS750	55.2±4.90	0.389 ± 0.274	0.838	29.6 ± 0.65	7.180 ± 0.288	0.998	
Cd	SAS350	47.2 ± 3.12	0.035 ± 0.008	0.963	7.66 ± 0.58	3.044 ± 0.152	0.993	
	SAS550	17.2 ± 1.36	0.072 ± 0.031	0.896	6.02 ± 0.46	5.289 ± 0.459	0.985	
	SAS750	64.8 ± 2.82	2.59 ± 0.97	0.930	37.20 ± 2.07	7.501 ± 0.750	0.977	

Table S4. Comparison of SASC adsorption capacity of Cd(II), Cu(II) and Zn(II) with other biochar.

	_	Experiment Conditions				_	
Metal	Feedstock	Pyrolysis Temperature	Initial pH	Co (mg·L ⁻¹⁾	Sorbent Dosage (g·L ⁻¹)	Q _{max} (<i>mg</i> ·g ⁻¹)	Reference
	Spent Agaricus bisporus substrate	750	5	0–250	1	68.1	Current study
	Jarrah	700	5.5	0–193	1.25	4.39	1
Cu	Corn straw	800				25.6	2
	Algae-dairy-manure	600	6	5-300	2	14.83	3
	Cattle manure	500	2	2-50	5	44.50	4
	Cauliflower leaves	600	-	50-200	2.5	53.96	5

	corn straw	600	5	6–318	5	12.52	6
	Spent Agaricus	750	5	0–250	1	55.2	Current study
	bisporus substrate						
7.5	Rice straw	550	5	0-65	1.25	39.69	7
ZII	Chicken manure	550	5	0–65	1.25	11.24	7
	Sewage sludge	550	5	0–65	1.25	4.25	7
	Jarrah	700	5	0-327	5	2.31	1
	Spent Agaricus	750	5	0–250	1	61.8	Current study
	bisporus substrate					04.0	
Cd	Bamboo	700	5	2-300	1	76.18	8
	Pine needle	600	6	2.5-360	2	53.8	9
	Municipal sewage sludge	550	7	10–50	5	41.67	10



Figure S1. The SEM images (3000×) and corresponding EDS spectra of spent *Agaricus bisporus* derived biochars at 350–750 °C. SAS300–SAS700 were the biochars at 350–750 °C.



Figure S2. The SEM images (3000×) and corresponding EDS spectra of spent *Agaricus bisporus* derived biochars after adsorption of Cd(II), Cu(II) and Zn(II) at 750 °C.



Figure S3. The amount of Ca^{2+} (**a**), K^+ (**b**) and Mg^{2+} (**c**) released from SABCs into solution after Zn(II) adsorption at different initial pH values. (pH of 5, 24 h, initial concentration of 100 mg·L⁻¹ and adsorbent dosage of 1 g·L⁻¹).



Figure 4. The contribution percentage of different mechanisms to Cu(II) (**a**), Zn(II) (**b**) and Cd(II) (**c**) sorption on SASCs. (pH of 5, 24 h, initial concentration of 100 mg·L⁻¹ and adsorbent dosage of 1 g·L⁻¹).

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